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ORBIT TRANSFER ROCKET ENGINE TECHNOLOGY PROGRAM

ENHANCED HEAT TRANSFER COMBUSTOR TECHNOLOGY - SUBTASKS I & II TASK C.1

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16. Abstract			***************************************	
increasing the heat extraction This effort is being conducted advanced, expander-cycle, oxapplications. Increased heat this higher chamber pressure, is detailed the heat-transfer surface area enhance cooling and maintain the	in conjunction with o ygen/hydrogen engine extraction, needed to rived from combustion . Life improvement i	ther tasks to planned fo raise availabl chamber hot-g s obtained th	develop technolo r upper-stage e turbine drive as wall ribs th	gies for an propulsion energy for
Laboratory test programs were hot-gas rib and coolant channe Detailed velocity profile maps obtained for the candidate des layer behavior and heat transferesults were substantiated by scaled to hot-fire conditions coolant channel configurations	l geometries selected, previously unavailal igns using a cold floor characteristics wer hot-air calorimeter tand the results use	through an and ole for rib and ole for rib and old old old old old old old old old ol	alytical screening channel geome imeter facility rom the velocity	ng process. tries, were . Boundary maps. Rib
The next program phase will i The program will culminate i combustor.	nclude hot-fire calor n design, fabrication	imeter testing n, and test o	of the selecte of a full scal	ed designs. e enhanced
This report describes the an experiments and analytical sca designs for further testing.	alytical screening of ling conducted to eva	rib and challing rib	annel candidates cepts and selec	, and the t the best
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FORWARD

This report documents the results of the first two subtasks of a program conducted for the NASA Lewis Research Center by Rocketdyne, a division of Rockwell International. Mr. H. G. Price was the NASA-LeRC Task Manager. At Rocketdyne, Mr. A. T. Zachary was the Program Manager and Mr. R. D. Baily the Project Engineer.

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1.0 INTRODUCTION

The thrust chamber combustor of a high-performance, expander-cycle engine, such as the engine proposed for the advanced OTV propulsion system, serves a dual function. First, it performs the normal function of a combustion chamber of containing the high pressure combustion process and accelerating the combusted gases to sonic velocity for expansion in the exhaust nozzle, thereby producing thrust. The second, unique, function is to provide a majority of the energy required to power the propellant turbopumps used to produce the high chamber pressure. These functions must be accomplished while achieving the overall engine goals for service life, maintainability, packaging, and weight.

In general, a higher chamber pressure leads to higher engine performance due to improved expansion properties of the combustion gases. In an oxygen-hydrogen expander cycle engine, the turbopump turbines are powered by hydrogen (fuel) heated by regenerative cooling of the thrust chamber components. Approximately 75% of the heat input to the hydrogen is derived from the combustor assembly. The remainder is supplied by the regenerative section of the nozzle assembly or by a supplemental heat exchanger such as a turbine gas regenerator.

Significant benefits, in terms of overall system optimization, are derived from obtaining increases in heat load through enhancement of the combustor heat extraction capability. That is, improving the performance of the combustor in its role as a heat exchange device reduces the reliance of the engine on auxiliary components for obtaining the desired system heat load. Since the combustor must already be present to serve as a combustion chamber, the overall complexity of the system is minimized by eliminating or reducing the requirements and size of the other heat exchange components. Further benefits such as reduced engine weight and envelope result from this.

However, a higher combustor heat load must not prevent achievement of other system goals such as overall system performance and service life. For instance, all other things remaining the same, increasing the heat load from

the combustor will cause an increase in the hot gas wall material temperature that will reduce the combustor service life. This is an undesirable trend due to the need for a long and maintenance free life in a space based mode of operation. As a result, technology advances that increase the heat extraction efficiency of the combustor must also exhibit the ability to maintain or improve its service life capabilities and maintainability requirements. Enhancements in the coolant channel configuration is one technology area projected to provide such benefits by significantly reducing the hot gas wall material temperature.

Combustor performance has a central role in determining the overall performance of the advanced expander cycle engine. Therefore, developing the technologies for enhancing combustor heat extraction and service life performance is crucial to meeting the goals of the propulsion system technology program.

OBJECTIVE AND APPROACH

The primary objective of this task is to perform a program of analysis, design, fabrication, and testing of an advanced combustion chamber design to increase enthalpy extraction from the combustor of an advanced OTV propulsion system. This program will demonstrate a hot-fire proven combustor assembly that features advanced heat transfer and life characteristics that meet the needs of the advanced OTV expander cycle engine. Specific goals are to optimize engine performance through increased heat extraction efficiency of the combustor while meeting the system requirements for life, maintainability, envelope, weight, and cost. In support of this, an early program objective was to establish a design database, through investigation, test and assessment of the proposed technologies, that will anchor the subsequent analysis.

A series of design, analysis, and laboratory test tasks were performed to evaluate means of enhancing the combustor heat load and service life. These tasks address the main issues that must be resolved in evaluating enhanced combustor concepts. These unresolved issues are:

- 1. Fluid boundary layer behavior and resulting heat transfer capability;
- Service life capability of alternate hot-gas wall/coolant channel configurations;
- 3. Fabricability of these alternate geometries;
- 4. Test verification of the analysis techniques to be used for future design efforts.

The program will culminate in test of an optimized combustor assembly whose-design is based on the results of preliminary technology tasks. Four technical subtasks have been identified to accomplish the program objectives. These tasks and a brief description of each are presented in Table 1-1. Efforts for this task will be supported by hot-fire evaluation of a smooth wall tapered combustor.

TABLE 1-1 ENHANCED HEAT TRANSFER COMBUSTOR TECHNOLOGY SUBTASKS

I. HEAT LOAD MAXIMIZATION STUDIES (HOT-GAS WALL RIBS)

HOT-AIR PANEL CHAMBER TESTS
COLD FLOW BOUNDARY LAYER MAPPING TESTS

- II. INCREASED LIFE STUDIES (COOLANT CHANNEL ENHANCEMENTS)

 COLD FLOW BOUNDARY LAYER MAPPING TESTS
- III. CALORIMETER INSERT HOT-FIRE TESTS

 HIGH Q TEST OF BEST CONFIGURATIONS
- IV. FULL SCALE RIBIFLEX COMBUSTOR

 INCORPORATE FINAL RIB AND CHANNEL CONFIGURATIONS

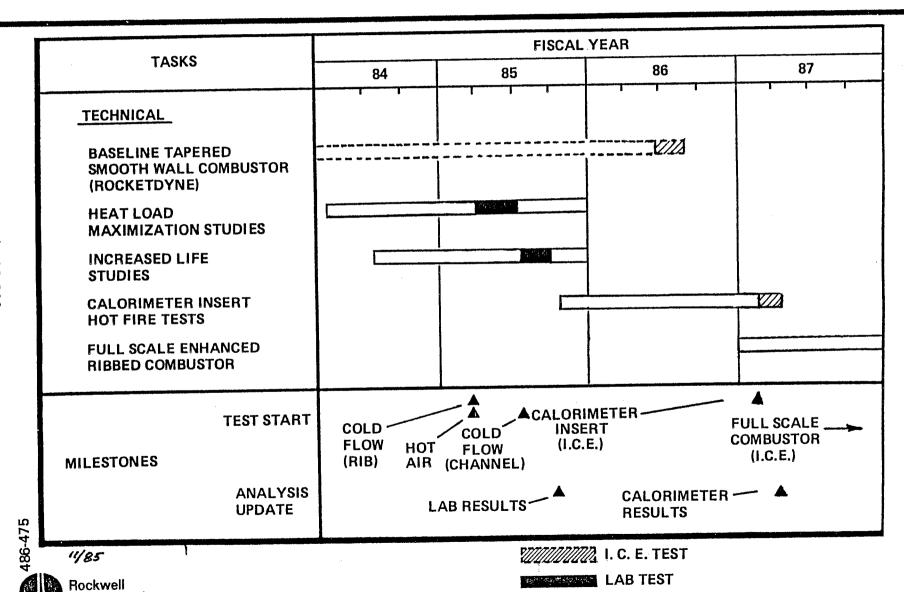
The smooth wall tapered combustor and the calorimeter insert hot-fire tests will be conducted using the Integrated Component Evaluation (ICE) test system. The ICE is a 15,000-pound thrust engine-type system that operates in an expander cycle mode and incorporates all of the major OTV engine components. This provides an accurate environment for testing advanced combustor technologies.

An approximately 50-month period will be required to complete the task. The overall task schedule is presented in Figure 1-1.

The objective of the two initial subtasks was to evaluate potential hot-gas wall rib (Heat Load Maximization) and coolant-channel (Increased Life) geometries and select configurations to be tested under hot-fire conditions. In particular, the heat transfer characteristics of the designs were determined and the results used to anchor analysis tools.

Laboratory test programs were formulated to evaluate flow field and heat transfer properties of the rib and channel designs. The tests were designed to determine whether boundary layer behavior close to the complex geometries prevents full realization of the potential heat transfer enhancement. Prior to the tests, analyses and a comparative selection process were completed to select the test configurations. A flow diagram for this initial phase is presented in Figure 1-2.

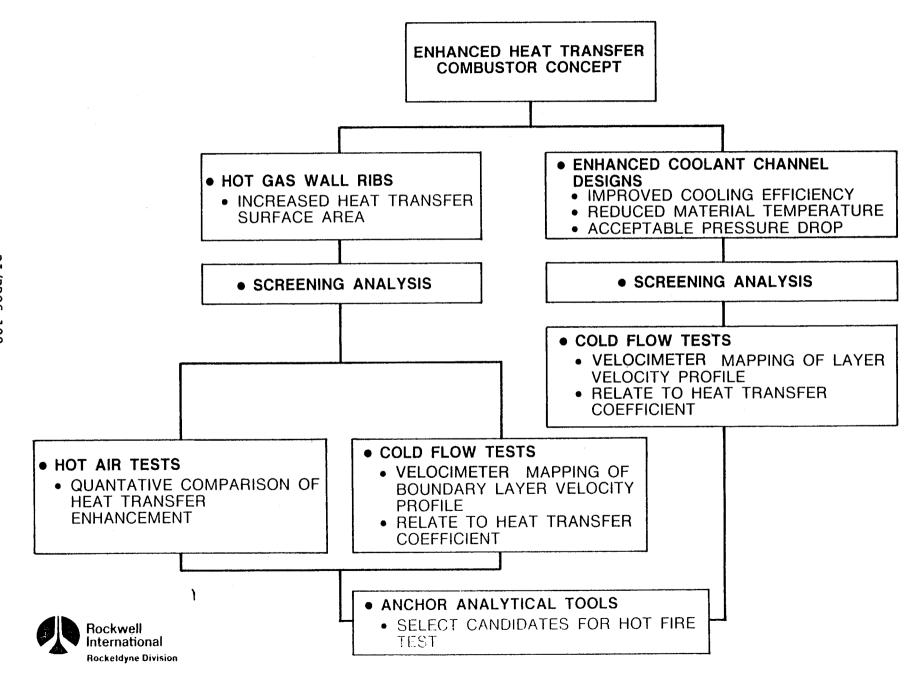
TASK C.1-ENHANCED HEAT TRANSFER COMBUSTOR TECHNOLOGY



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international
Rockeldyne Division

SCREENING PHASE TASK FLOW



REPORT ORGANIZATION

Two main sections follow this introduction, one each for the heat load maximization and increased life subtasks. These sections present summaries of the analyses and experimental efforts. Detail data from these tasks are contained in appendicies. A concluding section summarizes the efforts, discusses implications of the results, and introduces further planned efforts.

2.0 SUBTASK I - HEAT LOAD MAXIMIZATION STUDY

OBJECTIVE

The overall objective of this subtask was to assess the use of hot-gas wall ribs to increase the heat extraction capability of an expander cycle engine combustor. Supporting objectives were: screen appropriate rib configuration candidates; evaluate flow characteristics around the candidate ribs; compare the designs at hot-fire conditions; and select the best designs for hot-fire test evaluation.

APPROACH

The approach followed in this subtask is summarized in the left hand side of Figure 1-2. A matrix of candidate rib configurations was formulated based on preliminary studies conducted at Rocketdyne. The matrix featured ribs with varying heights, widths, pitches (spacing), and base geometries (sharp or curved). These candidates were screened by evaluation for heat transfer enhancement, wall temperature, risk of boundary layer build-up, and producibility. Heat transfer analysis was conducted with two dimensional computer models using a uniform heat transfer coefficient for all surfaces. Results of these analyses and the other evaluations were used to select laboratory test configurations.

Two laboratory test programs were identified for hot-gas wall rib flow evaluation. A hot-air program was conducted on exact scale calorimeter panels to obtain a quantitative comparison of heat transfer enhancement. Cold flow velocity mapping tests were conducted to obtain detailed rib flow field characteristics. Velocity profile results were related to boundary layer behavior and heat transfer properties and scaled to hot-fire conditions. The hot-air test results were also used to anchor this process.

The first objective in Subtask I was to screen candidate hot-gas wall rib geometries utilizing available boundary layer and heat transfer modeling techniques. The six best rib configurations were to be selected for the two lab tests planned; 1) the hot-air calorimeter panel tests, and 2) the cold-air flow boundary layer mapping tests. A matrix of 21 rib geometries was analyzed, covering a full range of rib geometry variations, including rib height, base width, rib pitch (spacing), and radiused contouring. These 21 rib types are depicted in Figure 2-1. The 21 rib geometries were evaluated in four categories: Heat transfer enhancement; boundary layer risk; producibility; and structural/life considerations. A scale of 0 to 10 was used for each rating category, with zero indicating an unacceptable risk or benefit, and ten being an optimum condition within that category. Criteria for determining ratings within each category are included in Appendix A.

Rating of each rib type with respect to heat transfer enhancement was based on comparisons against a conventional smooth walled combustor. This evaluation was conducted using two-dimensional finite difference Differential Equation Analyzer Program (DEAP) ribbed combustor models of the various rib geometries. These model results, contained in Appendix A, were in the form of two-dimensional "slices" of the hot-gas wall and combustor liner at discrete axial stations. Rib designs were rated in terms of a heat transfer "enhancement factor", relating rib potential compared to a smooth wall liner, and the steady state temperature profile. A graph depicting typical rib enhancement factors verses rib height is included as Figure 2-2. Rating of ribs in this category resulted, as expected, in the taller ribs being rated highest, due mainly to increased hot-gas surface area.

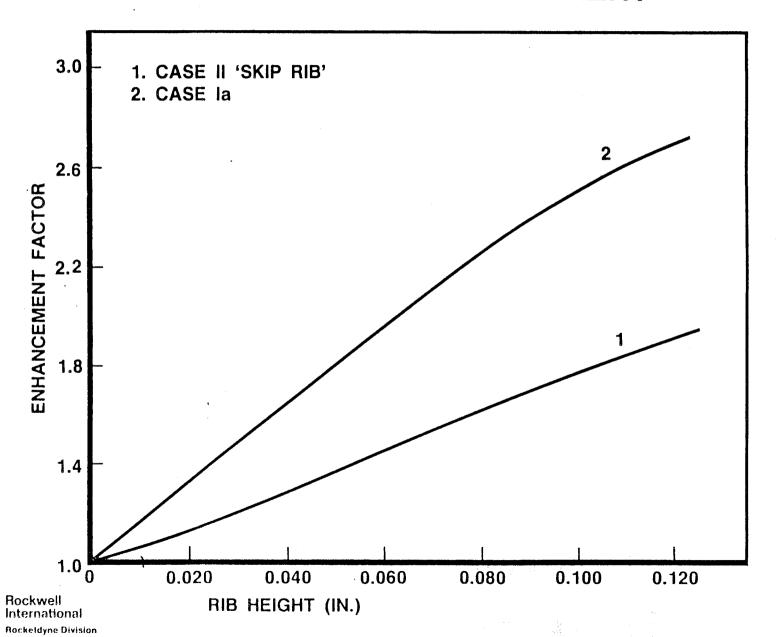
A comparison of heat transfer enhancement was made for orientation of the rib over the land area or over the coolant channel. No difference in enhancement was noted. Therefore, from a heat transfer standpoint the cases are equivalent and can be interchanged. Structural considerations will be used to select the best approach following Subtask 3 of the task.

FIGURE 2-1

RIB GEOMETRY SELECTION MATRIX

ТҮРЕ	HEIGHT	SHAPE	ТҮРЕ	HEIGHT	SHAPE
la. STANDARD RIB	0.040		III. HALF PITCH RIB	0.040	
RIB OVER LAND 0.040 BASE WIDTH 0.0785 PITCH	0.060		0.020 BASE WIDTH 0.0385 PITCH 0.010 TIP	0.0785	
0.020 TIP	0.080				
	0.120				
Ib. STANDARD RIB	0.040		IV. RADIUS 0.020	0.040	
RIB OVER LAND 0.060 BASE WIDTH 0.0785 PITCH	0.060		0.0785 PITCH 0.020 TIP	0.060	
0.020 TIP	0.080			0.080	
(RIB OVER CHANNEL FOR 0.060)	0.120			0.120	
II. SKIP RIB	0.060		V. RADIUS 0.060	0.060	
0.040 BASE WIDTH 0.1570 PITCH 0.020 TIP	0.080		0.1570 PITCH 0.020 TIP	0.080	
•	0.120			0.120	





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Boundary layer risk was evaluated based on a best estimate of boundary layer growth over combustor wall length, taking into account the insulating effect of a "filled" rib contour, and rib corner effects on boundary layer formation. Results, and subsequent ratings, reflect that the wider spacing of ribs is best, yielding the most effective boundary layer contour with minimized risk of heat flux degrading boundary layer build-up.

Producibility risk addressed the difficulty in machining complex liner geometries. Rib complexity is driven by aspect ratio, scale and multiple contours. As expected, the larger and simpler rib geometry types rated higher.

The structural and life considerations were based primarily on material property degradation with increased temperature. Comparison data was obtained from the DEAP steady state temperature profiles. These were relative temperature comparisons, since some rib tip temperatures went well beyond material limits (see Figure 2-3). Potential advances in material and cooling technology were considered in selecting cases to be tested. An .080 high rib was selected as a lab test configuration to acquire data for analysis of material survivability at its upper temperature limits. Evaluation of ribs in this category showed that the taller ribs rated lowest, due mainly to excessive material temperatures. Again, note that there is essentially no difference in the rib over land and rib over channel configurations.

A rib sensitivity study was conducted to evaluate how potential variations in hot-gas wall film coefficient (Hg) due to boundary layer effects would impact rib temperature and heat transfer enhancement. The results, depicted in Figure 2-4, show that Hg variations do affect heat transfer enhancement directly, but due to a parallel effect of lower material temperature, Figure 2-5, may allow the use of taller ribs. Additionally, a study was made to determine the effect on Hg of large temperature gradients from rib tip to — trough. Results showed only a 12% change in Hg for a 1000F temperature gradient, which fell well into the Hg range covered in the sensitivity studies described above.

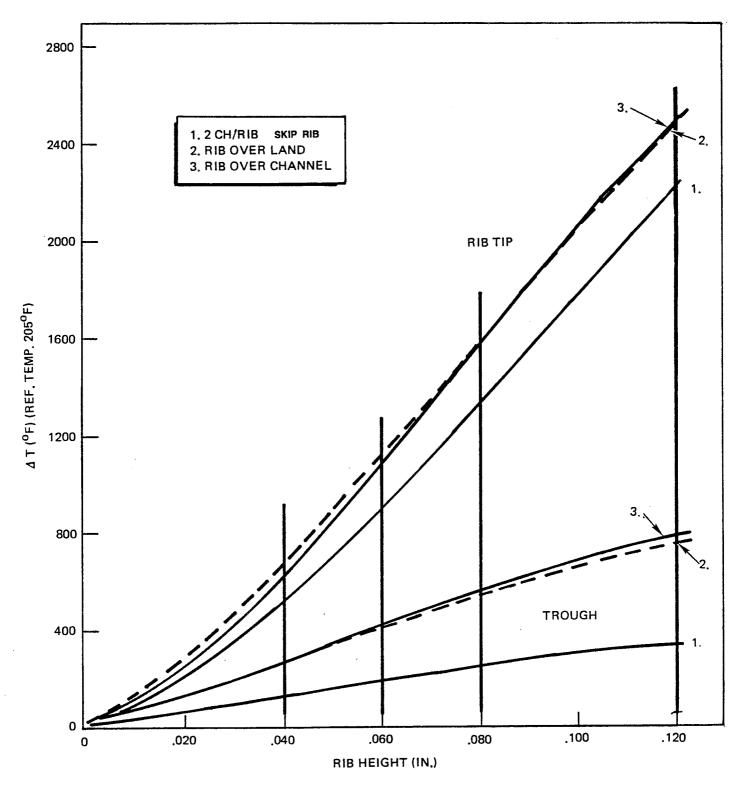


Figure 2-3. Structure/Life Considerations

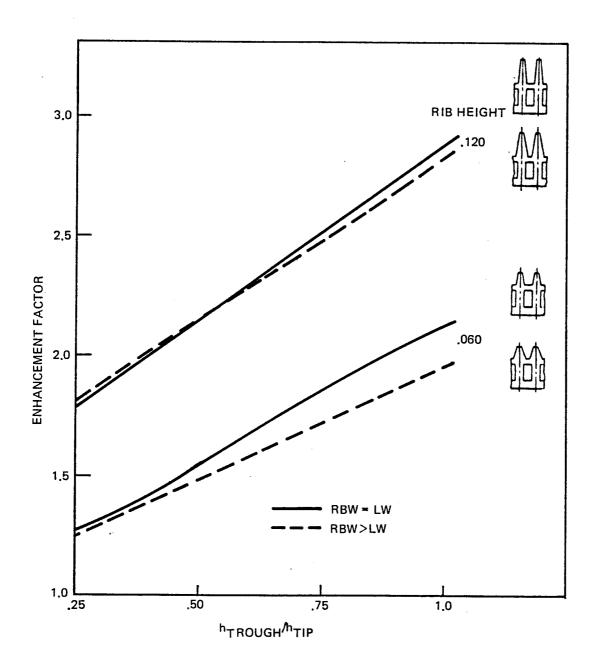


Figure 2-4. Enhancement Factor Sensitivity to Variations in Hot Gas Wall Film Coefficient (hg)

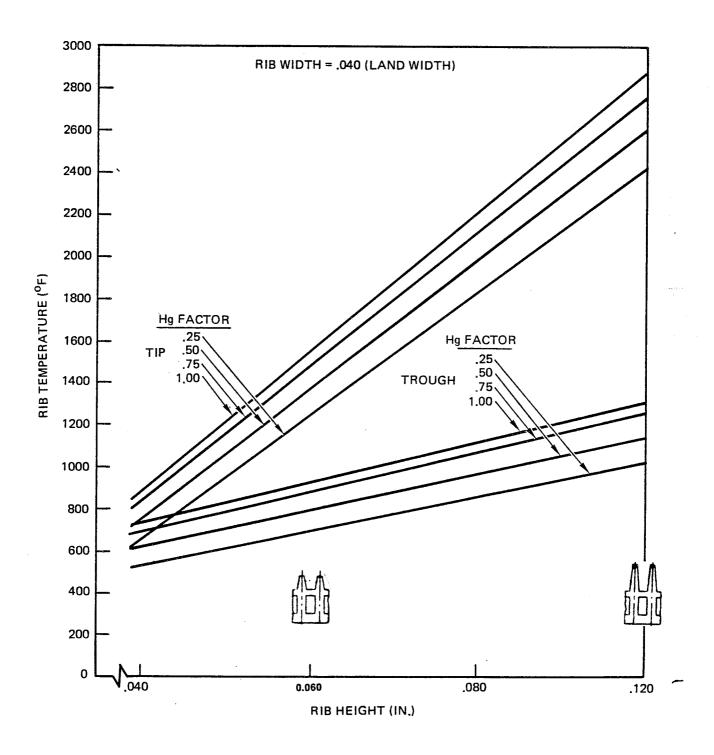


Figure 2-5. Rib Temperature Sensitivity to Variations in hg Factor

Final rib selection was based on total weighted scores for each rib type in the four categories, plus "other factors", such as duplication of data, and broadening of the data base. The concept scores and relative weighting of the selection criteria are shown in Table 2-1. Both boundary layer risk and heat transfer were weighted highest, due to their direct influence on rib effectiveness. Producibility was weighted low due to the relatively narrow range of influence it has, considering that all ribs analyzed are within the state-of-the-art for machining processes. Structure/life considerations, though important, will play a much larger role in structural analysis studies farther along in the program. The overall weighted rating score gives a priorized ranking of the candidates for the four quantified evaluation criteria.

The selected concepts are indicated in prioritized order on the right hand column of Table 2-1. Ribs of 0.040, 0.060, and 0.080 height were selected. Two base width values were selected for the 0.060 high rib to evaluate the impact of this parameter. A twice-nominal pitch configuration, the 'skip rib' case, was included based on its overall ranking and low boundary layer growth risk. Finally, a radius based design rated highly and was also selected for technical breadth.

Table 2-1. Hot Gas Side Rib Selection Matrix

RIB GEOMETRY		HEIGHT		AT SFER GHTED	BOUNDARY LAYER .30 WEIGHTED		PRODUCIBILITY		STRUCTURE/ LIFE .25 WEIGHTED		WT'D SUMS			SEL
<u></u> .				Q'TW		ML.D	RAT'G			WT'D	SUMS	RANK	OTHER FACTORS	RANK
RIB OVER LAND .040 .040 BASE WIDTH			6	1.8	6	1.8	10	1.5	9	2.25	7.35	1		1
.0785 PITCH .020 TIP	.080		7	2,1	5.5	1.86	10	1.5	4	1.0	6,26	3		2
	.080	W.	8.5	2.55	5	1.50	8	1.2	0	0	5.25	9	EXPAND DATA BASE FOR ADV MAT'L DEV	8
<u> </u>	.120		10	3.0	4	1.20	8	.9	٥	0	6.10	11 .		
IB. STANDARD RIB RIB OVER LAND .060 BASE WIDTH	.040		6	1.5	5	1,6	10	1.5	9	2,25	8.76	2	DUPLICATION: CHANGE IN BASE WIDTH TO BE	-
.0785 PITCH .020 TIP	.080		6	1.8	. 4.5	1.35	10	1.5	4	1.0	5.65	7	COMPARED AT ,060 HT	4 .
·	.080.	₩.	7,5 ·	2.25	4	1.2	9	1.35	0	0	4.80	13		
	.120	e di di	9	2.7	3	.9	7	1.06	٥	0	4,85	14		
II. SKIP RIB ,040 BASE WIDTH	,080		3	.9	8	2.4	8	1.2	5	1.25	8.75	8	TECHNICAL BREADTH	3
.1570 PITCH .020 TIP	.080		4.6	1.35	8	2.4	7	1.05	0	0	4.80	12		
	.120		6	1.8	9	2,7	6	.76	0	0	5,25	10		
III. HALF PITCH RIB		14AA1												
.020 BASE WIDTH .0365 PITCH .010 TIP	.040		-	-	0	C	5	.75	-	-	.75	20	HEAT TRANSFER AND LIFE NOT ANALYZED DUE TO EXTREME	
	.0786	<u> </u>	-		0	0	3	.45	-		.46	21	BOUNDARY LAYER RISK	<u> </u>
IV. RIB/CHANNEL SH RIB OVER CHANNEL .040 BASE WIDTH .0786 PITCH	.080	釬	7	2.1	6.5	1.65	10	1.5	4	1.0	6.25	4	DUPLICATION: HOT GAS WALL IDENTICAL TO IA J.080	-
V. RADIUS .020														
.0785 PITCH .020 TIP	.040		5,5	1.66	. 4	1.2	7	1.06	9	2.25	6.15	5	DUPLICATION: CHANGE IN THROUGH GEOMETRY TO BE COMPARED AT	-
	.060		6.6	1.95	4	1.2	7	1.05	5	1,25	5,45	8	.060 HEIGHT TECHNICAL BREADTH	5
	.080		6	2.4	3	.9	6	.9	0	0	4.25	15		
	.120	81019 11019	9	2.7	2	.8	4	.6	0	0	3.90	17	•	
VI. RADIUS .060 ,1570 PITCH .020 TIP	.080		2	.6	4	1.2	8	,0	5	1,25	3.05	18		
	.080		3.5	1.05	5	1.5	5	.75	0	٥	3.30	18		_
	.120		6	1.6	4	1.2	3	.46	٥	٥	3,16	19		

Two air test programs were formulated for hot-gas wall rib flow evaluation. A hot-air test program was planned for obtaining a quantitative comparison of heat transfer enhancement. Detailed boundary layer velocity profile mapping was planned in the second test series. Analyses were conducted to define test conditions that would provide the best simulation of hot-fire conditions possible for each laboratory test. Fixtures were designed for each test program.

<u>Analysis</u>

Proper simulation of the hot-fire combustor boundary layer was of prime importance in the planned hot-air and cold flow tests. There are vast differences between the actual combustor boundary layer and that which can be produced in an air flow simulation. The most important difference is the high heat flux into the cooled combustor wall; this cannot be recreated in a cold flow test. The resultant temperature gradient at the wall greatly reduces the momentum and displacement thicknesses of the boundary layer (while having little effect on the velocity thickness). Therefore, the boundary layer cannot be entirely recreated in an air flow test, but certain characteristics can be. The problem was then to choose the proper characteristic to be matched or scaled to the hot-fire conditions.

The scaling characteristic chosen for the air flow simulation is the boundary layer momentum thickness (θ) , since it is closely related to the heat transfer. The momentum thickness is defined as,

$$\Phi = \int \frac{\overline{\rho} \overline{u}}{\rho u} \left(1 - \frac{\overline{u}}{u} \right) dy \tag{1}$$

where, ρu = freestream density and velocity $\rho \overline{u}$ = turbulent (rms) density and velocity

The momentum thickness is calculated for hot-fire conditions by the Rocketdyne boundary layer computer program. The calculated value of the momentum thickness at the end of the cylindrical portion of the combustor (\sim 13 inches from the injector) is,

$$\theta = 0.029 \text{ inches} \tag{2}$$

for the combustor conditions: Pc = 1650 (psia), Tc = 6571 (R). The momentum boundary layer thickness as a function of axial position on the combustor cylindrical section is plotted in Figure 2-6.

In the air flow tests, it is desirable to scale this value at the downstream end of the ribbed plate test section. The theoretical growth rate of a turbulent boundary layer on an adiabatic flat plate is written,

$$\Theta = \frac{0.0142}{\sqrt{Rex}} \times \tag{3}$$

Where, x = distance from start of turbulent B.L. Rex = ux/ν Reynolds no. based on x

In order to account for any physical geometry differences between the air flow test section and the actual ribbed combustor wall, a scale factor S is introduced as a multiplier to the momentum thickness (eq. 1). In the case of the cold flow study, an enlargement of the rib dimensions is desired in order to make detailed measurements of the correspondingly larger boundary layer.

By multiplying equation (1) by S and equating with equation (2), the following expression for the required air flow velocity is derived,

$$U = \nu \left[\frac{L}{(0.1267) (S)^{1.17}} \right]^{6}$$
 (4)

where.

U = the freestream velocity (ft/s)

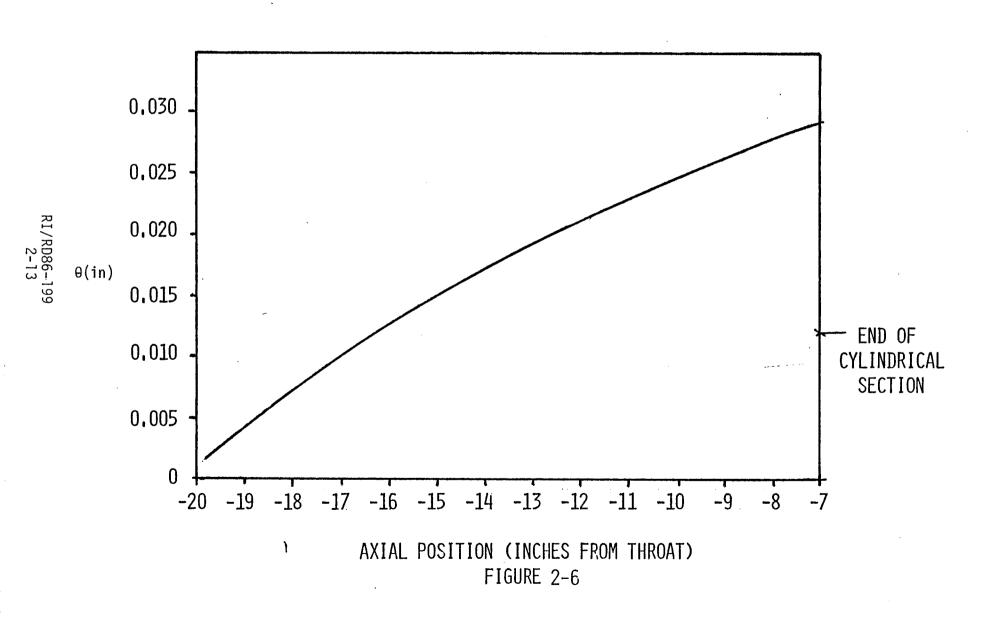
 ν = air kinematic viscosity (ft2/s)

L = length of the test section (ft)

S = geometric scale factor

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PREDICTED COMBUSTOR MOMENTUM BOUNDARY LAYER THICKNESS



As an example, for a 2 ft test section which has ribs of twice the actual size (S=2), and for air flow conditions of P = 14.7 psia, and T = 80° F (ν = 1.69E-4), equation (4) gives the required air velocity as,

$$U = 21 \text{ ft/s}$$

This corresponds to a plate Reynolds number of 2.4E5 which is in the turbulent regime. This will result in a match of the momentum thickness of the air boundary layer to the hot-fire momentum thickness as desired.

In order to summarize the effects of plate length and air flow conditions in the momentum thickness, a rearrangement of the growth equation (3) was performed to give,

$$\Theta/(x)^{6/7} = 0.0142/(U/\nu)^{1/7}$$
 (5)

Since the right hand side contains air flow properties only, a flow parameter was defined as,

$$\emptyset = (\nu/U) /c \tag{6}$$

where c = constant of proportionality

For a known dependence of air kinematic viscosity on temperature and pressure. the air flow parameter was related to the basic thermodynamic variables. For air temperature above 0°F and pressures not exceeding 400 psi, the absolute viscosity can be expressed as a function of temperature only,

$$u/u. = (T/T.)^{0.7}$$
 (7)

Where the subscripted values are taken as a reference condition. The air density is found from the Perfect Gas law as,

$$p/p. = (P/T) / (P./T.)$$
 (8)

Combining (7) and (8) gives the kinematic viscosity as,

$$\nu/\nu$$
. = $(T/T.)^{1.7} (P./P)$ (9)

RI/RD86-199 2-14 Assuming a reference of T. = 560 (R), P. = 14.7 (psia), and ν . = 17.9E-5 (ft2/s) gives the result,

$$\nu(\text{ft}^2/\text{s}) = C \frac{(T(R))^{-1.7}}{P(\text{psia})}$$
(10)

where, C = 5.6E-8 for alr

By combining this with (6), and choosing the proportionality constant c as equal to the constant C derived above, then the flow parameter is shown to be.

$$\phi = \frac{T^{1.7} (R)}{P (psia) u (ft/s)}$$
(11)

Then the momentum thickness growth equation (5) is written,

$$\theta / x^{6/7} = 0.0142 (c\phi)^{1/7}$$
or, $\theta / x^{6/7} = 0.00131\phi^{1/7}$ (12)

The air flow parameter is governed by the limitations of the test facility. It is evident from equation (12) that in order to develop a thick layer, a large ϕ is required. By inspection of equation (11), this implies that the air temperature should be as high as possible, and the pressure and velocity as low as possible.

The lower limit on the velocity is governed by the Reynolds number requirement for the maintenance of a fully turbulent boundary layer. If the velocity were allowed to drop too low, the layer may become laminar. As a rule of thumb, it was determined that the Reynolds number should be above Re = 1,000,000 over most of the test section. The Reynolds number at any location increases for smaller air flow parameter values. This suggested that the maximum allowable value be,

$$\phi_{\text{max}} = 100$$

Given a value of the flow parameter (0), the required test plate length was determined for a selected scale factor. This process is summarized in Figures 2-7 and 2-8. A graphical representation of equation 12 is presented in Figure 2-9.

For the hot-air tests, a one-to-one rib scale was used. Accordingly, a momentum boundary layer thickness matching the predicted 0.029-inch value at the end of the combustor cylindrical section was to be simulated. For test conditions of 900°F and 300 psi, a test panel length of 18 inches and a flow velocity of approximately 70 ft/sec produce an air-flow parameter of 10 giving the desired momentum boundary layer thickness.

For the ambient air-flow, boundary-layer mapping tests, an increased test panel scale was used to provide adequate space for flow mapping. For a rib scale of four-to-one, a 72-inch test panel length with a flow parameter of less than 50 results in a momentum boundary layer thickness four times the combustor value.

BOUNDARY LAYER RELATIONSHIP RELATES AIR FLOW TO HOT-FIRE CONDITIONS

ullet COMBUSTOR MOMENTUM BOUNDARY LAYER (heta) BASED ON FLAT PLATE ANALYSIS

•
$$\theta = \frac{0.0142}{(u/\nu)^{1/7}} \times \frac{6/7}{v}$$

 $v = \text{KINEMATIC VISCOSITY}$
 $v = \text{DISTANCE ALONG COMBUSTOR}$

- EVALUATED BY ROCKETDYNE'S 9R-247 COMPUTER PROGRAM
- \bullet AT END OF CYLINDRICAL SECTION θ = 0.029 INCH
- SIMILAR RELATIONSHIP USED FOR AIR FLOW TEST ANALYSIS

$$\theta = 0.0142 \ (\phi/C)^{1/7} \ x^{6/7}$$

$$\begin{cases} \phi = \text{AIR FLOW PARAMETER} \\ C = \text{AIR CONSTANT} = 1.287 \ x^{10} \\ X = \text{DISTANCE ALONG TEST PANEL} \\ \phi = C_1 \ (\nu/u) = T^{1.7}/P \ u \end{cases}$$

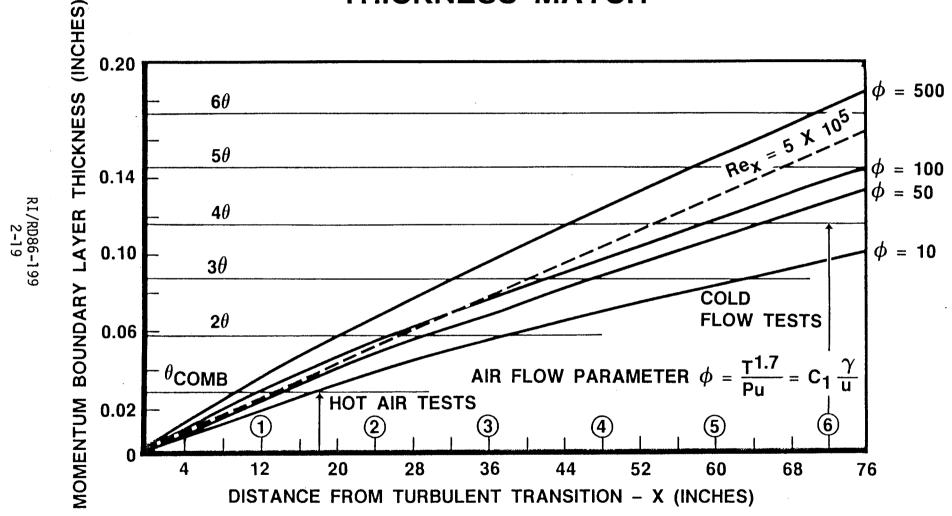
$$\begin{cases} T = \text{AIR TEMPERATURE} \\ P = \text{AIR PRESSURE} \end{cases}$$

1

TEST FIXTURE DIMENSIONS SET BY COMBUSTOR CONDITIONS

- ullet REQUIRED LENGTH A FUNCTION OF SCALE FACTOR(S), heta, AND ϕ
 - L = $(S\theta/0.0142)^{7/6}$ $(C_1/\phi)^{1/6}$
- \bullet FOR TURBULENT FLOW $\phi \leq 100$, AND WITH $\theta = 0.029$ INCH
 - $L = 0.9507 S^{7/6}$
- S = 4 PROVIDES ADEQUATE SPATIAL SCALE AND ACCEPTABLE LENGTH
 - L = 60 INCHES (5 FT)

FLOW PARAMETER VALUES FOR AIR TEST/ COMBUSTOR BOUNDARY LAYER MOMENTUM THICKNESS MATCH



Test Fixtures Design

Hot-Air Test Chamber. The calorimeter test chamber was designed with segmented test panels to allow different rib configurations to be tested in the same set-up. A two-piece clamshell housing confines the four separable 90 degree test panel segments. The housing has attach flanges at both ends for facility interface. Spacer rings are used at both ends to house instrumentation and flow devices. Panel water feed lines and axial thermocouples are fed through ports in the housing. A chamber assembly layout is shown in Figure 2-10.

The test panels are identical in design with the exception of the hot-gas wall configuration which is varied to match a candidate design. One panel had a smooth wall for reference heat transfer values. The panel consists of an OFHC copper liner brazed into a CRES structural shell. The liner back has coolant channels machined axially between the integral manifolds at both ends. The manifolds are fed by a single water supply (drain) tube at each end. Bosses are provided for thermocouples that are inserted in coolant channels at five axial locations on each panel. The panel edges have a relief and a seal to minimize heat transfer between adjacent panels at the interface.

The forward spacer ring houses a flow plate that straightens and trips the air flow just upstream of the chamber. It also contains a port for a thermocouple rake to measure inlet radial air temperature distribution. The aft spacer ring also contains a boss for a thermocouple rake for measuring exit radial air temperature distribution. A replaceable exit nozzle, which partially controls the air flow rate, is bolted to the end of the discharge spacer.

The chamber is a bolted assembly with o-ring seals used between the mating parts and the facility flanges. Detail drawings for the chamber components are contained in Appendix B.

<u>Cold Flow Test Fixture</u>. The cold flow test fixture was designed as a long box-like passage for flowing the air past the rib geometries. The fixture was configured to use a structural beam as a support and assembly means. It consists of two side members, a replaceable test panel, a cover plate which

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includes three velocimeter access windows, and an inlet plenum. A design objective was to use this fixture for the Subtask 2 test effort, so a configuration that would allow easy modification to the channel test mode was formulated. Detail drawings for the assembly are given in Appendix C and a cross section layout is shown in Figure 2-11.

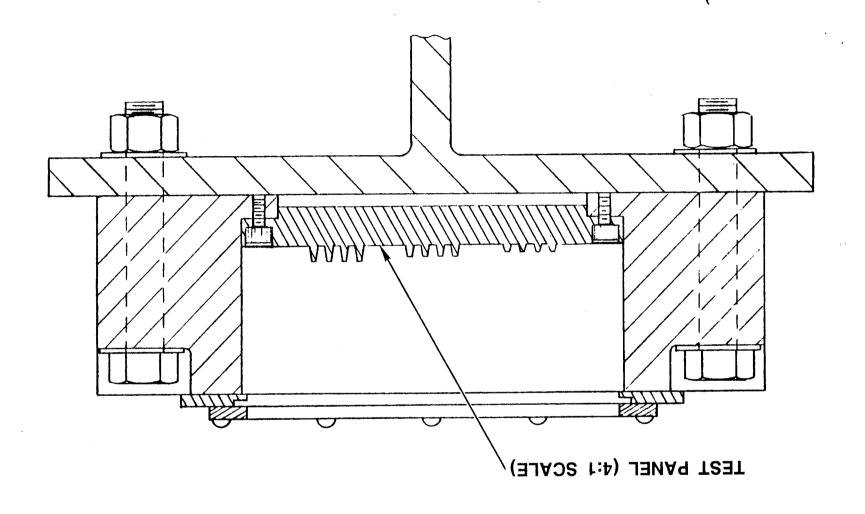
The side members are bolted directly to a structural beam with a matching bolt hole pattern. Spacing for the members is provided by the replaceable test panel which is bolted into lands on the side members. For the rib test configuration, the test panel is at the bottom of the fixture, away from the cover plate, to provide the proper undisturbed free stream boundary condition. The test panel and side members form the lower three sides of the flow box.

The test panels contained four-times scale ribs for each of the six selected configurations. Additionally, for one panel, half of the panel was left flat for reference flat plate measurements. Two to three rib types were included on a panel, but several ribs of each type were provided on each side of the measurement centerline to provide the proper boundary conditions. A black anodize surface treatment was selected to minimize plate reflectivity which could cloud velocimeter measurements and limit the ability to obtain measurements close to the surface.

The top closeout of the box is provided by the cover plate. It is a sheet metal panel that is bolted to the top of the side members. Three windows are included to provide access for the velocimeter laser beams. The windows are fused silica glass that are polished for flatness and have an antireflective surface coating. Extreme clarity, flatness, and antireflectivity are necessary to prevent distortion of the velocimeter laser beams that would reduce data accuracy. The windows are held in place with a cover plate and a thin cushioning film gasket.

An inlet plenum was designed to interface the test fixture with the facility. The plenum entrance adapted to facility ducting quick disconnect couplings. From the entrance, the air is turned 90 degrees and funneled to match the box dimensions. The air was exhausted to atmosphere, so no special fixture was designed for the exit.

COLD FLOW TEST FIXTURE - HOT-GAS RIB CONFIGURATION



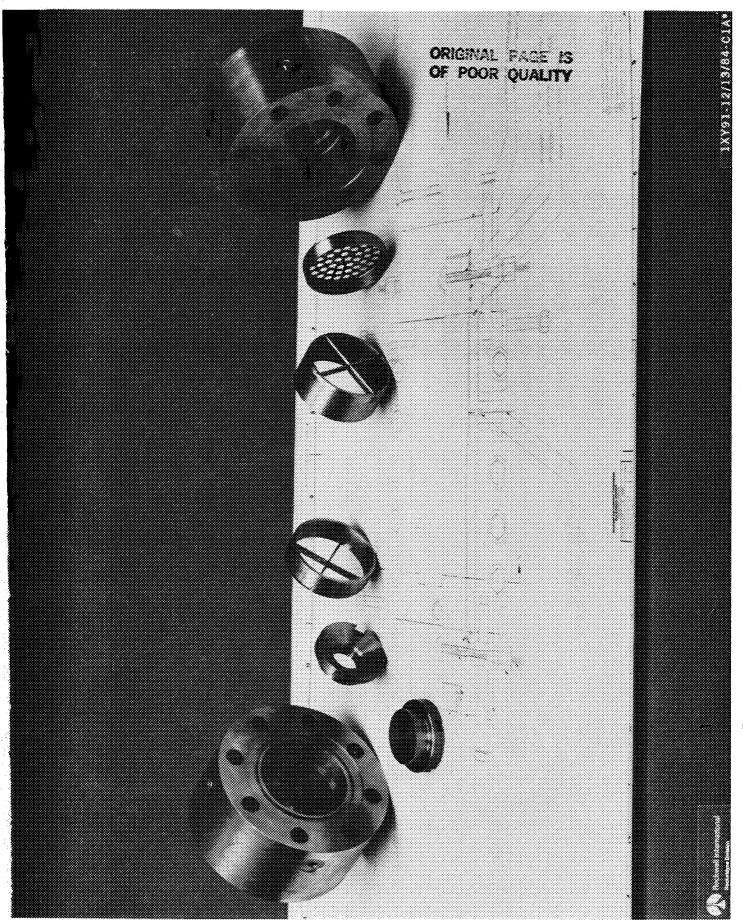
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Fabrication

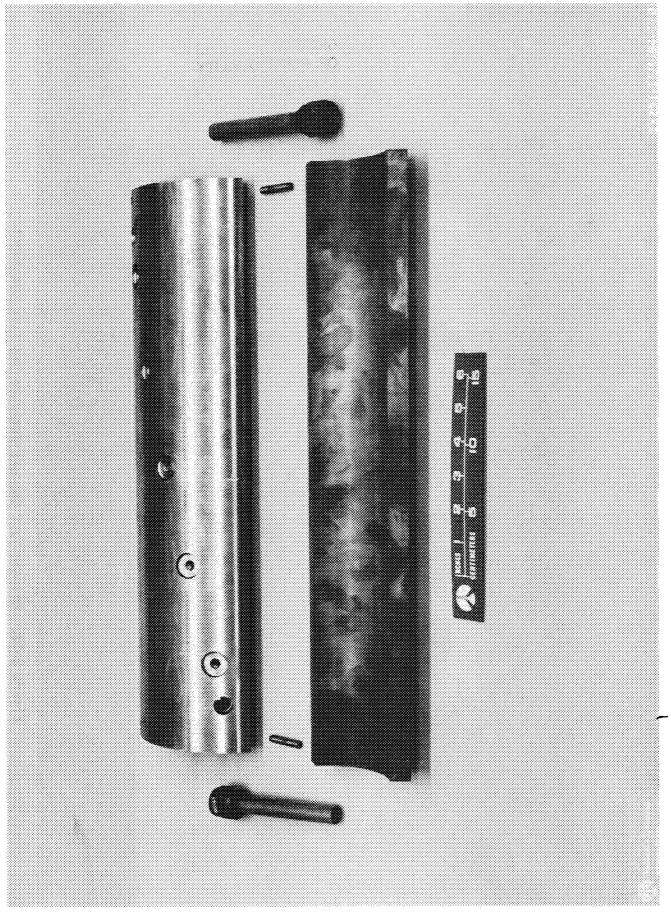
The components fabricated include the entrance and exit sections, the two shell halves, and seven calorimeter panels (six with rib configurations and one smooth wall reference). The inlet and exit components are machined parts made from CRES material. The individual components, shown in Figure 2-12, include thermocouple support crossmembers at each end, an entrance flow turbulator, and a replaceable exit flow nozzle.

The calorimeter panels are brazed assemblies consisting of a CRES strongback, an OFHC copper liner, and CRES feed tubes. The fabrication sequence was:

- machine the CRES strongback curvature and manifold sections, leaving extra stock on the ends for braze tooling;
- 2) machine coolant channels into the copper liner outside diameter (OD) leaving extra stock at the ends for braze tooling;
- 3) machine a curved inside diameter (ID) on the copper liner for interface with braze tooling, leaving extra stock for later machining of the hot-gas rib geometries;
- 4) check fit the components, Figure 2-13, and tack Nicoro braze alloy foil on the strong back in the channel areas;
- 5) assemble the liner to the strong back and insert positioning pins located in the extra stock area;
- 6) place the coated tooling bar, which matched the liner ID, on the liner and wrap the assembly with tungsten wire to apply a closing force during brazing, insert the feed tubes and braze alloy;
- 7) braze the assembly in an inert furnace, disassemble tooling when complete;



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- 8) leak test the panel for overall leakages and x-ray to observe channel bonding;
- 9) final machine the panel hot-gas rib configuration, the thermocouple access bosses, and the end and side interfaces.

All seven panels were completed without significant problem. Some channel clogging appears to have occurred in the middle channels (lowest point channels during brazing) on several panels which reduced water flow area. The effect was localized, so it was concluded that the overall panel results would not be affected.

The two-piece clamshell housing was also machined from CRES material. It provides sealed interfaces for the entrance and exit sections, passages for the panel feed tubes and thermocouples, and bolted closure flanges to allow disassembly for panel replacement. The housing and a set of completed tests panels are pictured in Figure 2-14.

The chamber was assembled simply by placing the panels in the shell halves and bolting the halves together to encase and compress the panels. This formed a seal at the panel interfaces. A top and overall view of the assembly, prior to bolting together, are shown in Figure 2-15.

<u>Testing</u>

A test plan, contained in Appendix B, was prepared to define the hot-air test approach and requirements. In summary, it was planned to test each of two chamber builds (three ribbed panels and the smooth wall reference panel in each build) at two temperatures and varying cooling flowrates to determine the heat transfer characteristics. Water flowrates, water temperatures at the inlet and outlet and at several axial locations on the panel, and inlet and exit air properties were to be measured to provide the data for this characterization.

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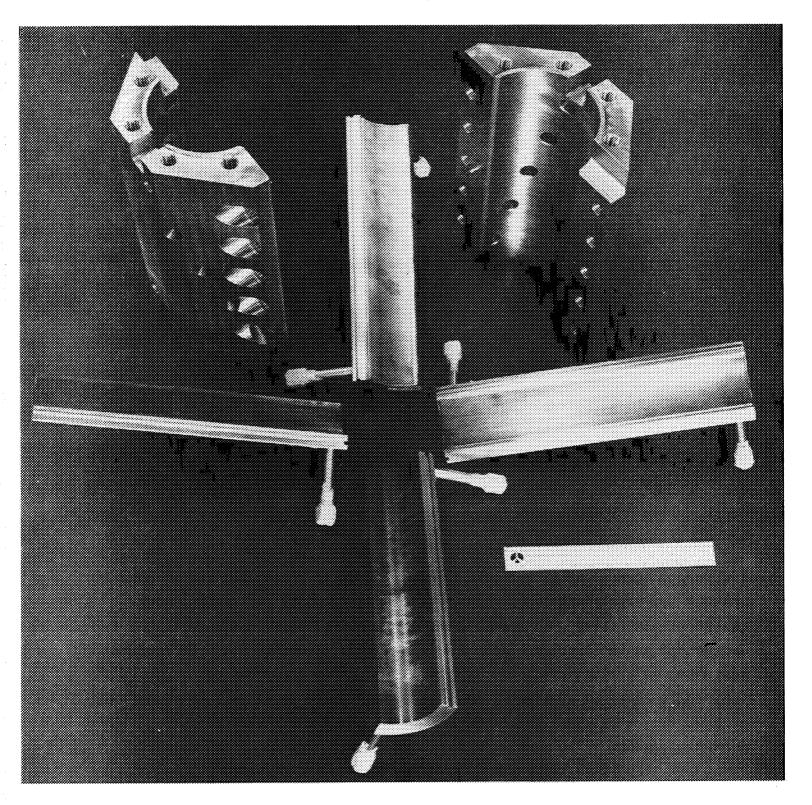
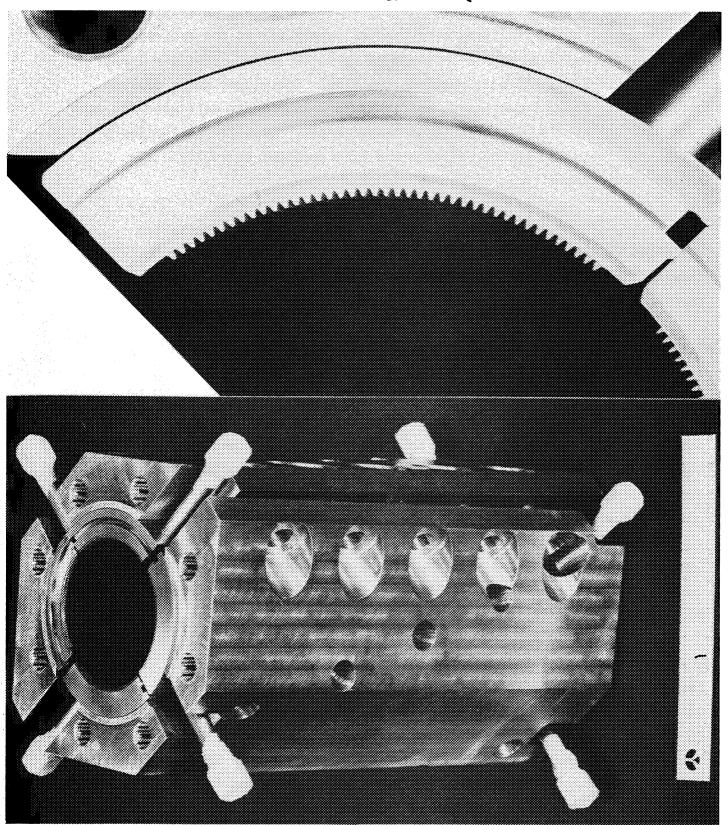


Figure 2-14. Hot-Air Test Chamber Components

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Installation. A test position was established at Rockwell's North American Aircraft Operations (NAAO) Thermodynamics Laboratory to conduct the tests. The facility is illustrated schematically in Figure 2-16. An existing compressor and heater facility were used to supply air at the desired 700 -900 F, 300 psia conditions with a flowrate of up to 10 lb/sec. Hot air inlet conditions were available to regulate the flow. Individual water cooling circuits with flow, temperature, and pressure measurements were used for each test panel to obtain bulk heat input measurements. Crossbar thermocouple rakes were installed in the entrance and exit sections to evaluate air temperature uniformity.

An overview of the test position with the chamber and instrumentation installed is shown in Figure 2-17. A closer view is given in Figure 2-18, showing the entrance, test chamber, exit section, water feed lines, and the thermocouple junctions.

Data collection was provided by a high-speed Astrodata acquisition system available at NAAO.

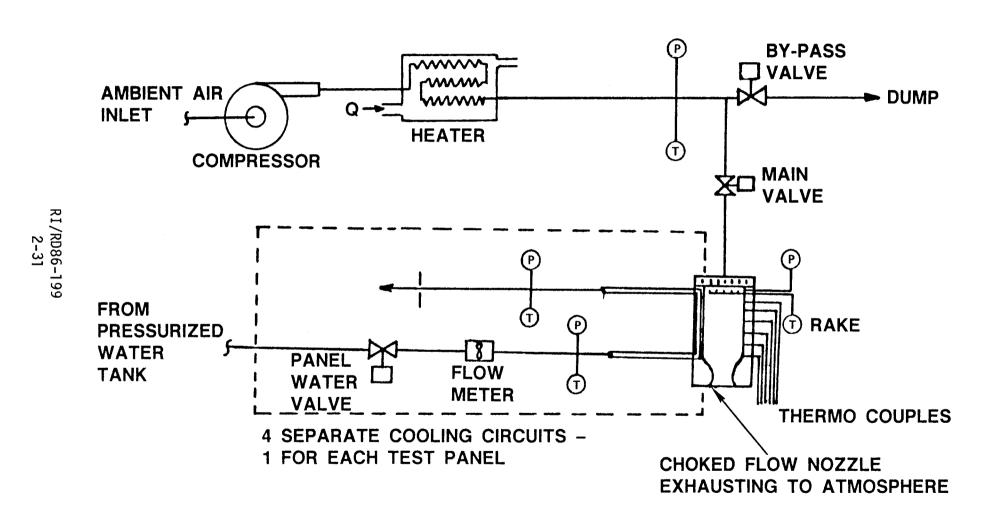
<u>Tests.</u> A large number of steady-state data slices were obtained for each chamber set-up. A summary of the test points and conditions is given in Figure 2-19. Varying hot-gas heating-to-water circuit cooling ratios were explored by running at extreme hot-air and water flowrates for the test temperatures of 700° and 900°F.

Summary tables for the tests conducted are contained in Appendix B. The tables list the pertinent conditions and the resulting water temperature rise as a function of axial position.

Representative axial thermocouple data are graphed in Figure 2-20. The curves show the higher temperature rise for the ribbed panel section compared to the smooth wall reference. A tendency for the ribbed panel to rise to near the final temperature rapidly and 'level off' towards the exit is notable. The smooth wall reference had a more linear temperature rise. This is evidence that the boundary layer build-up in the ribbed contour was limiting the heat transfer enhancement near the end of the panel section. Since the test panel length and conditions were selected to represent the boundary layer formation

FIGURE 2-16

HOT-AIR TEST SETUP SCHEMATIC



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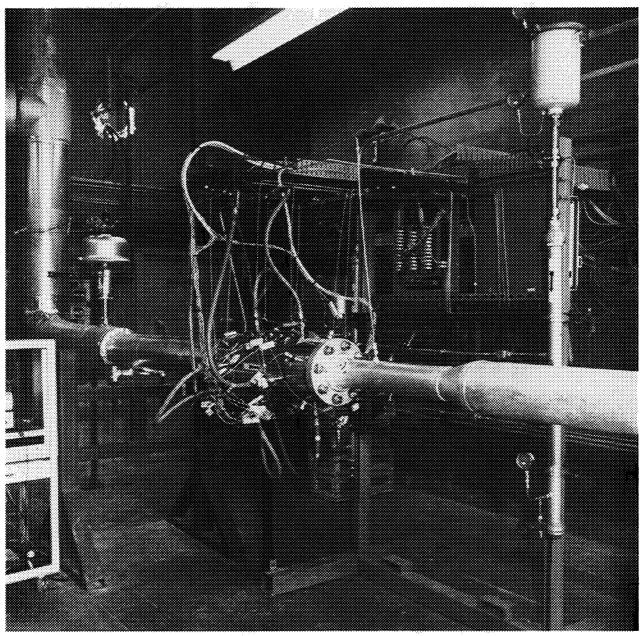


Figure 2-17. Hot-Air Test Installation

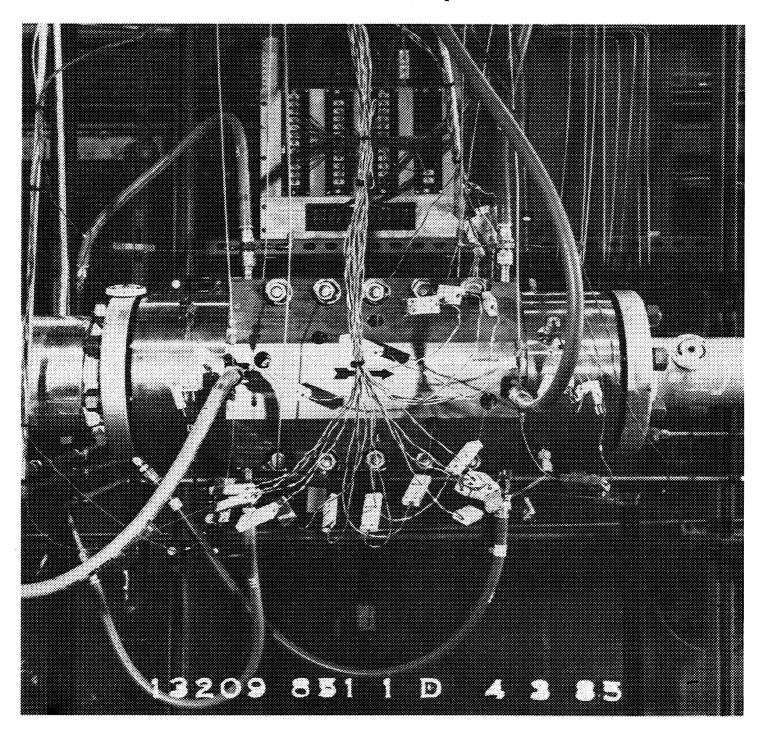


Figure 2-18. Hot-Air Chamber Test Setup

HOT AIR CALORIMETER PANEL TEST POINTS FIGURE 2-19

(lb/sec) AIR

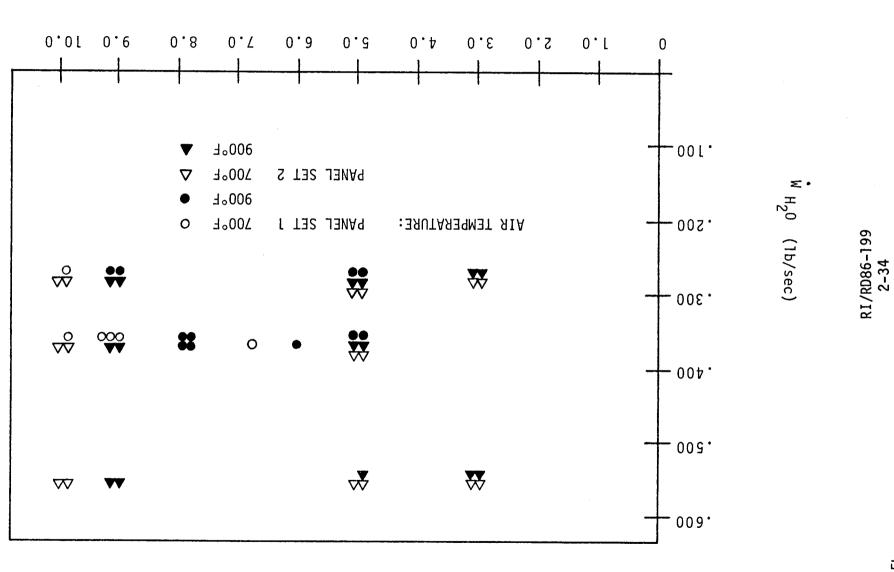
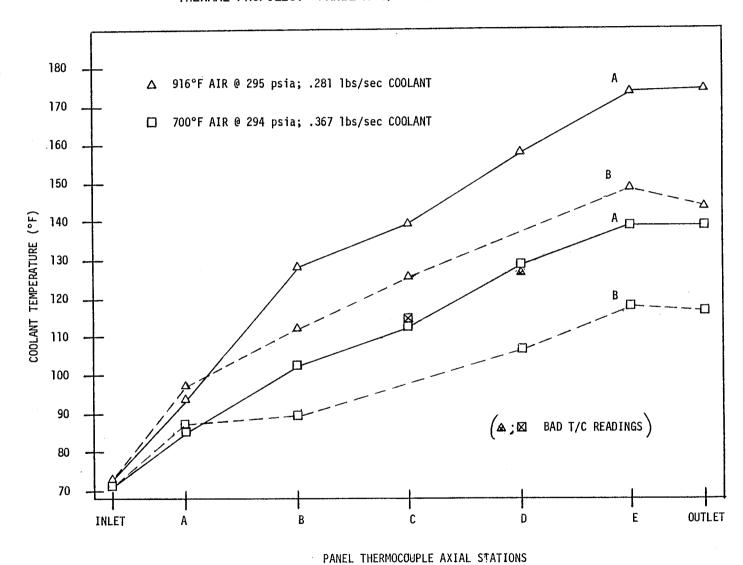


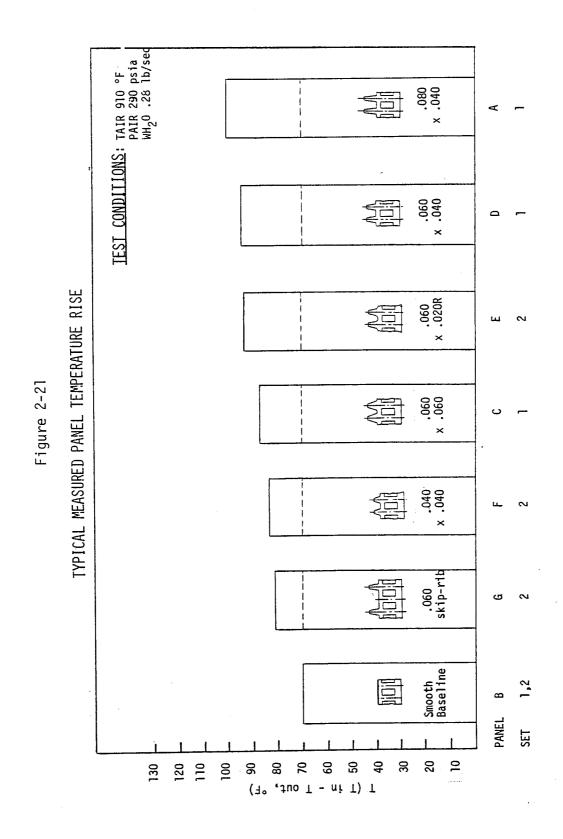
Figure 2-20
THERMAL PROFILES: PANEL A (.080 RIB) VS. PANEL B (BASELINE)



in the combustor at hot-fire conditions (see test program definition analysis), this information is representative of the axial enhancement profile for the combustor.

Representative bulk temperature rise results are presented in Figure 2-21. The taller ribs had a greater temperature rise, indicating a higher enhancement factor for the hot-air conditions. However, the difference between the taller and shorter ribs was not as large as expected based on the initial analysis at hot-fire conditions.

Results from the hot-air tests provided: 1) a direct measurement of the axial heat transfer enhancement development profile; and 2) a quantitative measure of the heat transfer enhancement at known conditions that could be used to anchor analytical methods for extrapolating results to hot-fire conditions.



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Fabrication

The ambient temperature and pressure conditions allowed the cold flow test fixture to be fabricated from aluminum stock. Bars and sheet stock in greater than six foot lengths were available in the sizes needed, so the large size of the fixture posed no difficulties. The components fabricated included the side members, a cover plate and windows, an inlet plenum, and three test panels.

The side members were simple rails with interfaces for the test panels and cover plate and a bolt hole pattern that matched the structural support beam. The members were machined with particular attention to the relative position of the various bolt hole patterns to ensure ease of assembly.

The cover is a 0.250 inch thick sheet that has three window openings. Fused silica windows were procured from a speciality glass supplier to meet the stringent needs for accurate velocimeter data acquisition. The windows were polished to one-quarter wavelength (coherent light) flatness and parallelism within 3 arc seconds. A broadband antireflective coating, encompassing the 514.5 nanometer laser wavelength, was applied to the outside surface to reduce reflection losses. Aluminum window 'blanks' were made to fill in for the windows not used during data collection at a particular axial station.

The test panels containing the four-times scale rib geometries were machined from plate stock. Parallelism was tightly controlled to ensure a uniform gap between the ribs. The panels were black anodized following machining to reduce reflectivity. A photograph of a test panel is presented in Figure 2-22. The panels were dimensionally inspected after completion to check acceptability and to provide exact dimensions for precise velocimeter focal volume positioning with respect to the ribs.

The inlet plenum was welded from sheet to form a funneled shape. A section of facility piping that had an existing coupling interface was welded into the plenum as the inlet piece. Prior to assembly to the test fixture, it was

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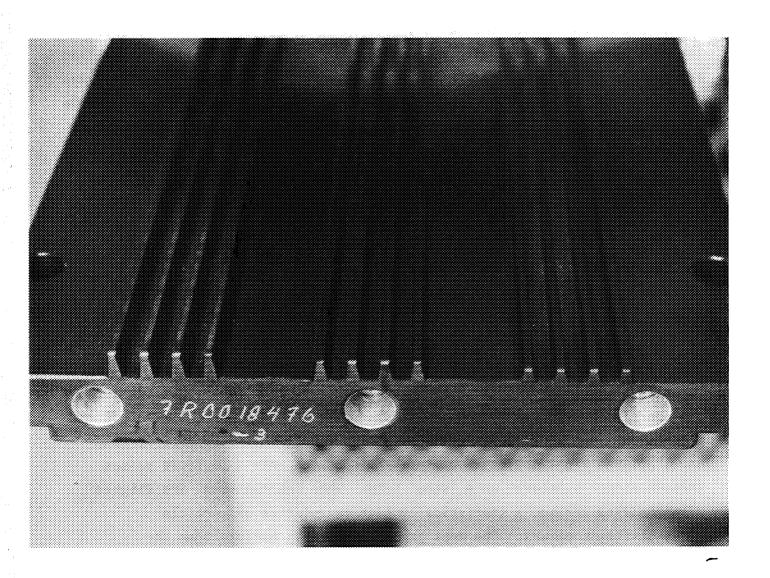


Figure 2-22. Rib Cold Flow Test Panel

decided to add a flow straighter tube bundle and flow trip screen to the straight section of the plenum that is just upstream of the fixture entrance. The bundle and screen were assembled and tacked into the plenum.

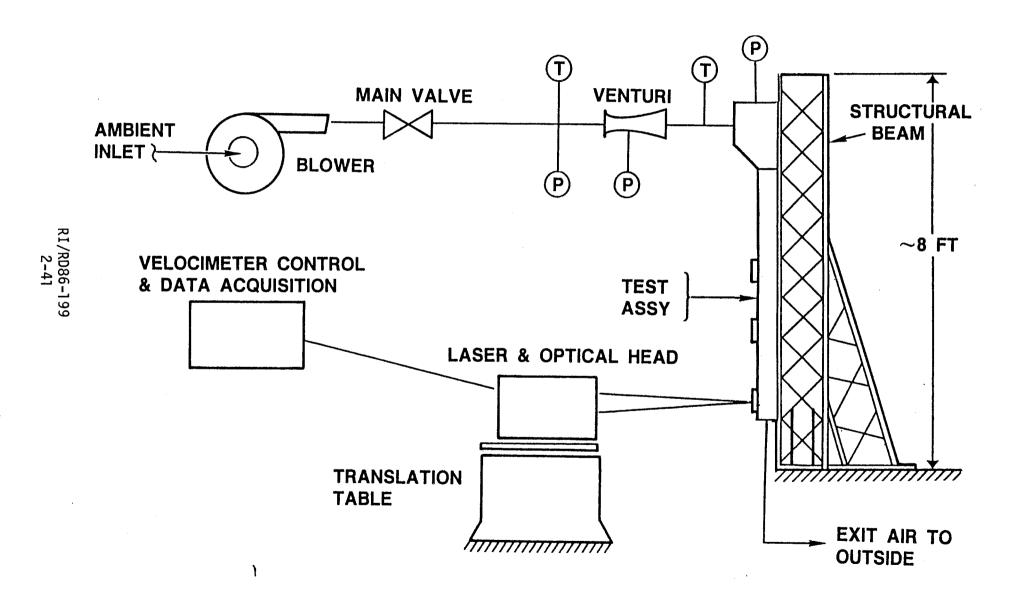
Testing

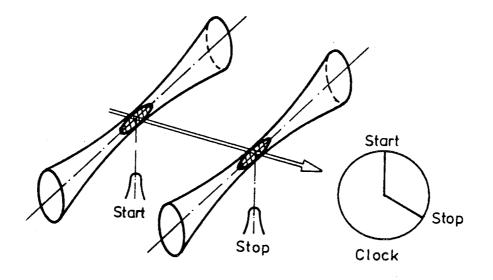
A test plan was developed to define and specify requirements for the cold flow tests (see Appendix C). The basic approach was to map the flow field around the ribs using the laser velocimeter at a single freestream flow velocity that met the conditions specified in the test planning analysis. Originally it was planned to do this at all three available axial positions, however, attainable data acquisition rates and the available test period and budget required that testing be limited to the end position.

<u>Installation</u>. The test position for the cold flow tests was established in Rocketdyne's Engineering Development Laboratory (EDL). The schematic for the facility is illustrated in Figure 2-23. The system used an existing low pressure air blower system with venturi measurement device to feed the test fixture. The primary measurement tool for the test set-up was the laser two-focus (L2F) velocimeter.

The velocimeter allows non-intrusive measurement of flow velocities and turbulence levels around the ribs shapes. The L2F type of velocimeter uses two sharply focused laser beams to form a 'gate' through which time-of-flight measurements can be made for small particles entrained in the flow stream. Backscattered light collected by the L2F indicates when a particle passes through either a 'start' or a 'stop' beam. When the two beams are aligned with the flow stream, a statistically high correlation of particle times-of-flight occurs. The most probable speed is derived from the statistically highest time-of-flight and the precisely known beam separation, Figure 2-24. The velocity vector is determined from the angulation of the line between the beams and a reference line. The turbulence level is determined from the breadth of the times-of-flight distribution around the most prominent value.

COLD-FLOW TEST SETUP SCHEMATIC





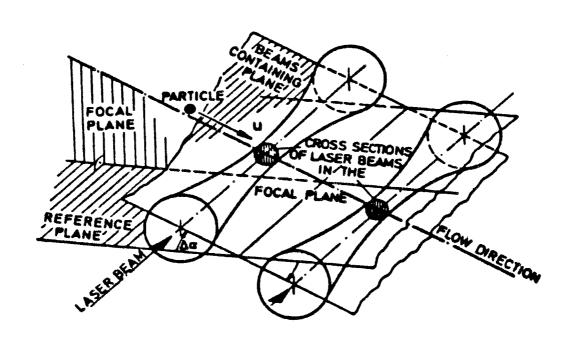


Figure 2-24. Velocimeter Time of Flight Measurement

The L2F system consists of the laser and optical head, a control processor, signal conditioning electronics, and a multichannel analyzer. Additionally, for this set-up, a remotely controlled translation system that provides precise optical head movement and positioning was used to allow a matrix of points to be collected efficiently.

The completed test set-up is shown in Figure 2-25. The fixture was positioned with the entrance at the top to eliminate the need for placing the translation table on a high platform. Fixture assembly was accomplished by: loosely bolting the side members to the structural beam, fitting the initial test panel in place and securing at the ends, check fitting the cover panel to verify alignment, final torquing the side member bolts with the panel in place, and final installation and sealing of the test panel and cover plate. The inlet plenum was secured to the beam and test fixture and the piping attached to the plenum with a coupling. Exposed interfaces were sealed with foil tape to prevent leakage.

The flow venturi and instrumentation, used to set the basic flow conditions, are visible in the left hand side of the figure. A 'bank' of insence sticks was positioned at the blower inlet to introduce small smoke particles into the flow to enhance the data collection rate.

The velocimeter optical head and translating table are shown in the test position in front of the last window. The microcomputers and processors for control of the velocimeter and translating table were in a remote clean room, Figure 2-26, and were connected to the velocimeter through data buses.

The exhaust air was collected in a large box at the fixture exit and was routed away from the test area through a flexible duct and discharged to the atmosphere.

Tests. Prior to conducting tests on each panel the velocimeter angular reference was established by alignment with the installed test panel. This was accomplished using a tool that referenced off the panels at the first and third windows (removed) and provided a 'line' for the velocimeter to use as a zero degree reference.

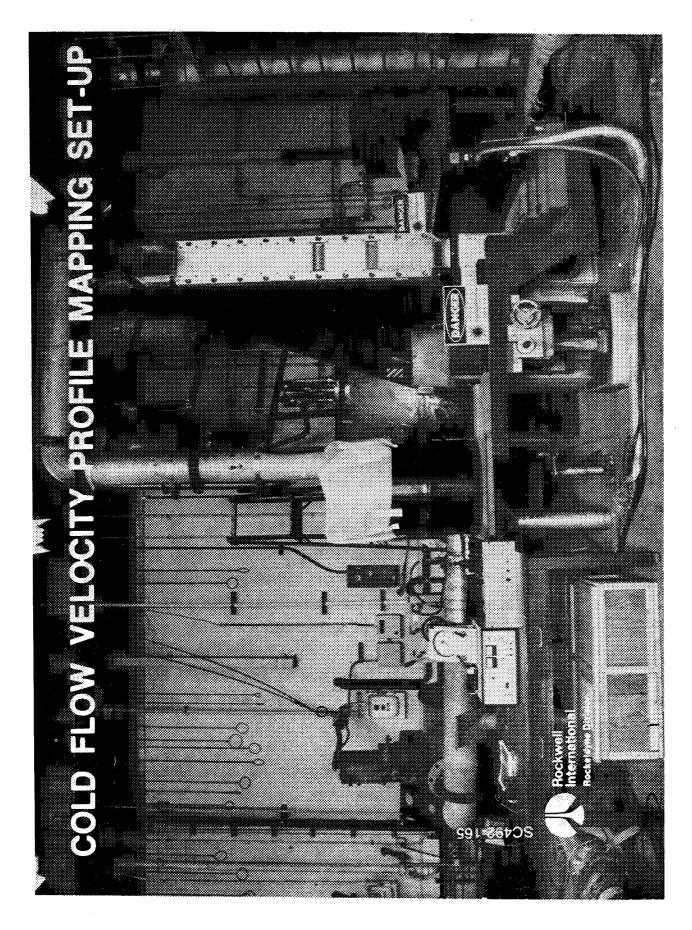


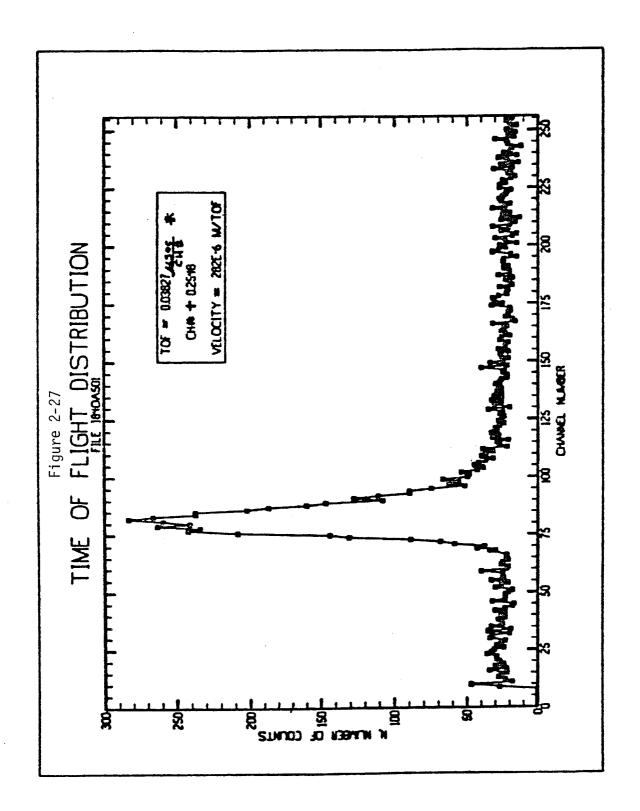
Figure 2-26. Velocimeter Data System

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The initial checkout for the system was conducted with the -7 panel which contained the flat plate region and the double pitch 'skip rib' configuration. A sweep of measurements in the free stream indicated an acceptably uniform velocity field. However, in attempting to obtain measurements close to the flat plate surface, it was determined that the number of particles in the flow near the surface was insufficient to achieve a reasonable data rate. This would have limited the ability to accurately assess boundary layer behavior.

As a result, it was decided that an improved flow seeding method (over the smoke) was needed. A fluid atomizer was selected as the best candidate method. A jet baffle atomizer that creates droplets of salt water at a density of 6 million droplets per cubic centimeter with a mean diameter of 2 microns was leased for the test set-up. The salt water droplets were introduced into the system in the air feed ducting. It was anticipated that the water droplets would evaporate, leaving minute particles of salt that would seed the flow.

Initial tests with the revised system resulted in significantly increased data rates and measurements within 0.012 to 0.020 inch from the surface were achieved. The typical data collection process for a velocity point was: 1) the velocimeter focal volume was positioned at a specific location with respect to the ribs by computer control of the translating table: 2) times-of- flight measurements were collected at a discrete angular alignment between the fixed and moving laser beams and a histogram of occurances (events) versus time-of-flight values (listed as channels) obtained, Figure 2-27; 4) after a threshold number of events at the predominant time-of-flight had been collected, the angle was incremented to a new position; 5) half-degree increments for a range of +/- 5 degrees off the panel centerline were completed. These steps defined the velocity at thepoint, the angular flow orientation (for this case the orientation was always nearly exactly along the centerline), and the turbulence level (derived from the width of the statistical event versus channel distribution) at the particular point.



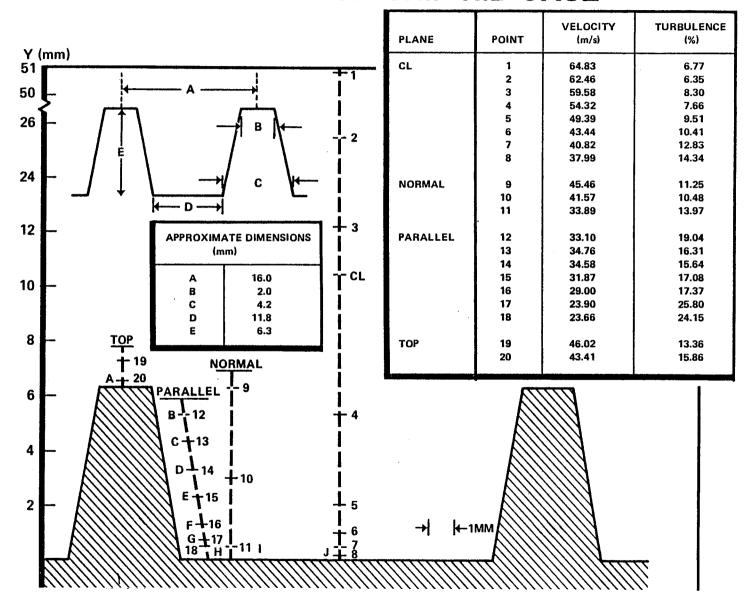
Velocity fields were mapped for the scaled up models of four rib geometries; the dual pitch 'skip' rib (0.060 high), the 0.040 tall rib, the 0.060 tall rib, and the 0.080 tall rib. In each case, the free stream velocity at the centerline of the measurement grid was measured to provide a reference velocity. A grid of points, as exemplified in Figure 2-28, was collected for each configuration to evaluate the velocity profile.

The velocity fields for each configuration are contained in Appendix C. Figure 2-29 is a graph of the normalized centerline velocity as a function of distance off the surface for the rib types. These curves illustrate the velocity degradation encountered with the taller ribs, indicating an increasing boundary layer thickness. This thickness is directly related to the heat transfer capability.

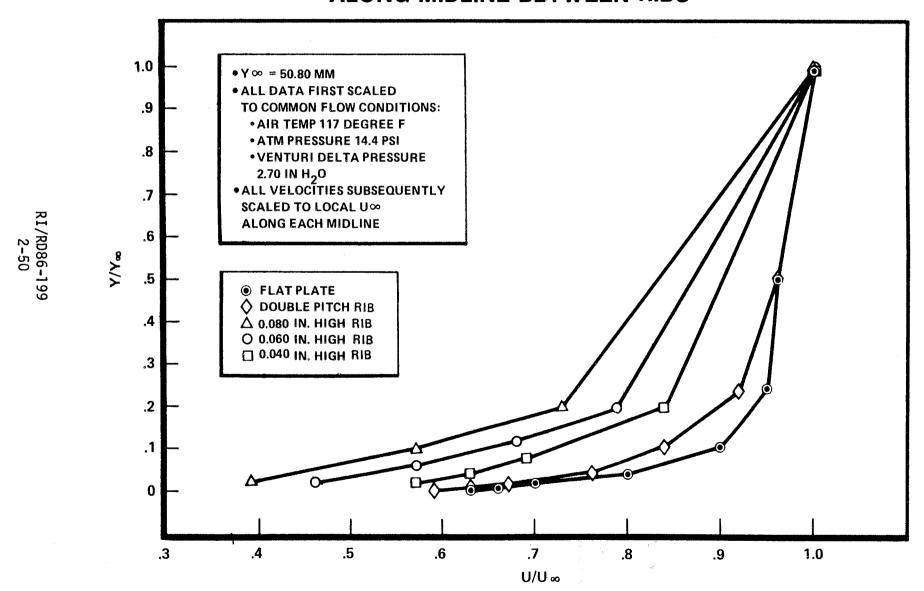
These tests provided quantified profiles of the velocity fields around the rib configurations for representative momentum boundary layer development conditions. This information was collected to provide a basis for adjusting hot-fire boundary layer predictions to obtain accurate hot-fire heat transfer calculations.

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AIR FLOW VELOCITY MAPPING RESULTS FOR SKIP RIB CASE



NONDIMENSIONALIZED SCALED VELOCITIES ALONG MIDLINE BETWEEN RIBS



SELECTION ANALYSIS

Scaling Procedure

The scaling procedure for the velocimeter data, which provides a comparison of heat transfer enhancement at hot-fire conditions, is summarized below. A flow diagram of the scaling process is presented in Figure 2-30 as an aid in following the summary. A numerical example of the rib scaling analysis is presented in Appendix D.

Velocity profile data were obtained as close as possible to the model wall to provide the best indication of the boundary layer behavior. A nondimensional heat transfer parameter, the Stanton number, was determined from the velocity profile. The Stanton number varies around the rib profile and directly reflects the influence of the boundary layer development on the heat transfer. The Stanton number is derived from a process in which the local skin friction is determined from a piecewise wall velocity evaluation.

The velocity profiles are fit to a universal profile in the logarithmic overlap region of the turbulent boundary layer, Figure 2-31. The universal velocity profile has a best fit equation for the logarithmic overlap region as,

 $U^{+=}$ 2.43 ln (y+) + 4.9 Log overlap region velocity profile

where,

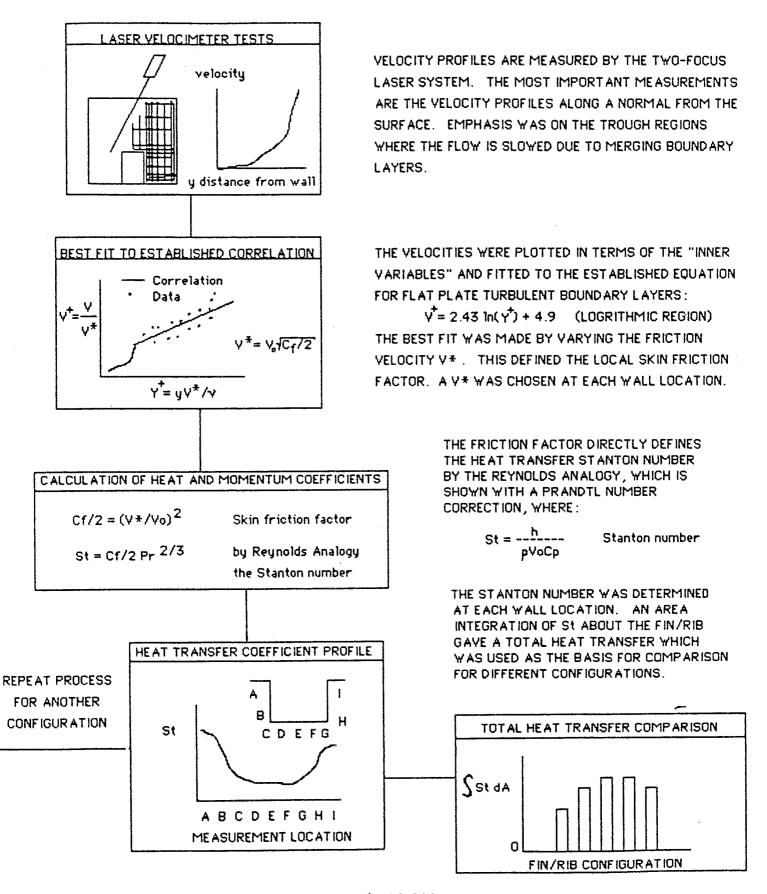
u⁺= U/V*

v+- vv*/v

Dimensionless velocity

Dimensionless distance above the plate or rib

Figure 2-30. FLOWCHART OF THE DATA REDUCTION PROCEDURE FOR THE COLD FLOW TESTS.



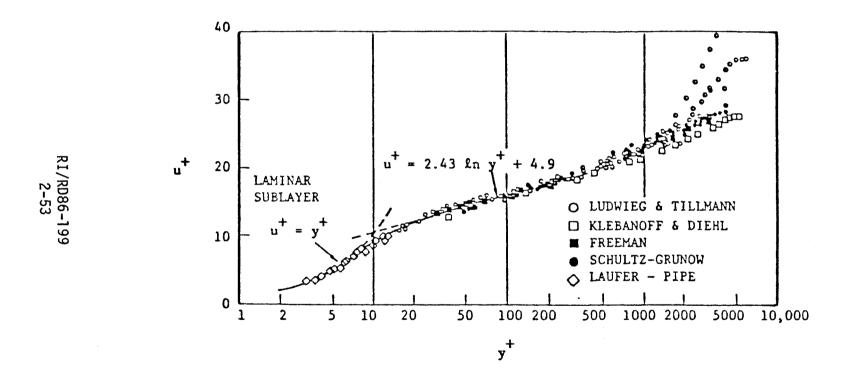


Figure 2-31. Turbulent Boundary Layer Universal Velocity Profile

U = local velocity [m/s]

y = distance from surface [m]

 $v^* = \sqrt{Tw/\rho}$ Uo = $\sqrt{Cf/2}$ "Friction velocity"

Uo = Freestream velocity

Tw = Wall shear stress

 ρ = fluid density

Cf = Skin friction coefficient

The basic premise for the data analysis method was that, at any location on a rib or fin, the boundary layer could be characterized by a flat plate boundary layer having the same near-wall region called the "logrithmic overlap region". Under these test conditions, the overlap region extends from about one-half millimeter to several millimeters from the wall.

As evidence of the applicability of the established correlation, it was compared to the measurements from the Cold Flow tests performed on a flat plate as shown in Figure 2-32. The agreement was very good except at large distances from the wall where the correlation is no longer valid. Therefore, it was shown that the cold flow velocimeter measurements could reproduce the results of past flat plate studies.

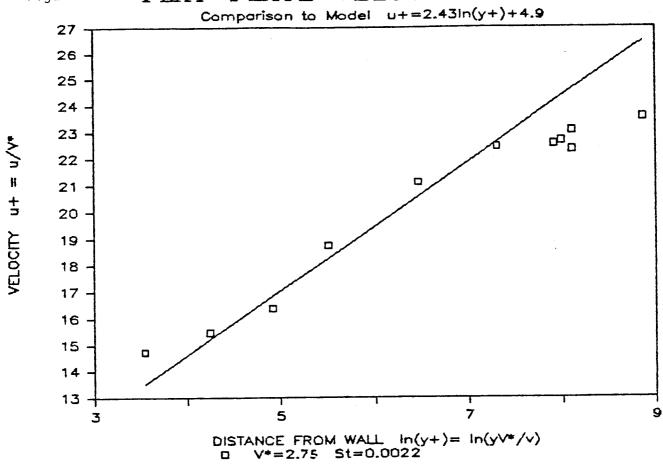
The data from the cold flow tests were fit to this universal profile by choosing an appropriate friction velocity V*. This defines the shear stress at the wall based upon the empirical results of past flat plat turbulent boundary layer studies. In effect, it is assumed that the boundary layer at each location around the rib is equivalent to a flat plate boundary layer of the same thickness.

The heat transfer Stanton number is derived from the wall shear stress or skin friction coefficient by the Reynold's analogy,

St =
$$Pr^{2/3}$$
 Cf/2 (1)
where, St = h/ρ (UoCp) Stanton number (2)
 $Pr = 0.69$ Prandtl number for air
 $h = local$ heat transfer coefficient

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Figure 2-32. FLAT PLATE VELOCITY PROFILE



The Stanton number can be thought of as a dimensionless heat transfer coefficient. Specifically, it is the ratio of the heat transferred to the total heat (enthalpy) content of the flowing gases. The Stanton number profile for the 'skip-rib' case that was derived from the previously presented velocity profile is shown on Figure 2-33.

The heat transfer coefficient (h) values for hot-air calorimeter or hot-fire conditions are determined by scaling the density, freestream velocity, and gas heat capacity denominator in equation (2) above to the appropriate conditions. For the hot-air calorimeter test series this provides an accurate scaling since the conditions are not radically different than the cold flow tests. This is reflected in the typically close results for the scaled calorimeter and the actual test results.

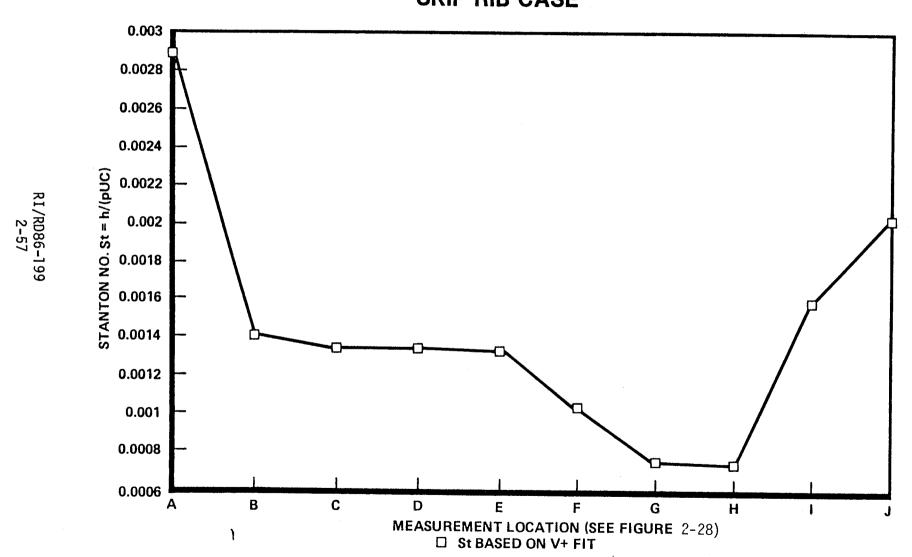
For hot-fire test conditions, a further scaling or compensation must be made for the extreme conditions produced by the combustion process. Conditions not present in the cold flow testing, such as an extremely high freestream velocity, compressibility due to high pressures, and other properties that vary with temperature are accounted for in the scaling. The scaling factors were determined from hot-fire conditions analysis using Rocketdyne's boundary layer analysis program. This scaling results in a more realistic or 'best' treatment of the cold flow data by accounting for these factors that cannot be simulated in the laboratory.

Results

Extrapolation of the cold flow test results to hot-fire conditions was performed in two ways. The difference lies in the scaling of the Stanton number. A conservative estimate of the cooling performance of a rib/fin configuration was afforded by direct usage of the cold flow test Stanton number profiles. A more realistic estimate was provided by the utilization of an appropriately scaled Stanton number profile. In both cases, the Stanton numbers were used to provide heat transfer coefficients to a DEAP thermal model of the combustor wall and channel.

FIGURE 2-33

RIB HEAT TRANSFER PROFILE SKIP RIB CASE



Scaling the Stanton number required the utilization of thrust chamber aerodynamic and thermal computer models. A boundary layer computer model was required to provide a realistic hot-fire heat transfer coefficient between the combustion gases and the combustor wall. A regenerative cooling computer model named REGEN was used to determine a realistic heat transfer coefficient between the channel wall and the coolant.

The boundary layer computer model predicts a different heat transfer coefficient than a typical flat plate correlation because of the extreme environment existing in a combustor or nozzle. The influence of many effects such as high velocity, fluid compressibility, high pressure, high temperature and thermal gradients, and non-uniform fluid properties are modeled in this program. A scaling factor Sg was applied to the Stanton number profile on the ribs as defined by,

The REGEN computer model has been used extensively by Rocketdyne in the thermal design of regeneratively cooled thrust chambers. REGEN was used to determine the heat transfer coefficient on the liquid side. This was expected to differ from a typical internal flow correlation because of the differences in thermal properties between fluids such as air and a supercritical cryogenic coolant. A scaling factor S_1 was applied to the channel Stanton number profile as defined by,

After these scaling factors were applied to the Stanton number profiles, the corresponding heat transfer coefficients were calculated based upon rocket engine conditions (by definition, h = St pUoCp). These values provided the

boundary conditions for DEAP thermal model of the combustor wall and channel. This model predicted the hot-fire wall temperatures and heat fluxes corresponding to the different rib and channel configurations.

The heat transfer enhancement predictions for hot-fire conditions are shown in Figure 2-34, which compares the heat transfer rates relative to a smooth wall. The percent of heat transfer enhancement is listed above each bar. The lower, conservative, estimate was based upon unscaled Stanton number profiles. The best estimate utilized the scaling factors S_g and S_l before inputting the Stanton number profiles into the DEAP model. These values provide a bracket on the enhancement that can be expected in an actual combustor.

A summary of the rib flow test results and analyses is shown in the bar chart in Figure 2-35. Each rib configuration has four bars associated with it corresponding to the results of: unscaled Cold Flow tests, Hot Calorimeter tests, a DEAP thermal model for calorimeter conditions, a DEAP model for hot-fire conditions.

A comparison of the first two bars of each configuration demonstrates that the Cold Flow tests and the Calorimeter tests yield comparable results. These tests predict the heat transfer enhancement within 5% of each other. This lends support to the cold flow test data analysis procedure used in the transformation of velocity profiles to heat transfer rates.

The third bar of each configuration represents the result of a ribbed wall and channel DEAP thermal model which was run for the calorimeter test conditions. In this model, the Stanton number profiles predicted in the cold flow tests were used to determine the heat transfer coefficient about the rib. This represents the heat transfer prediction based upon cold flow results for a location near the end of the cylindrical combustor. Since this is the region of minimum enhancement due to boundary layer growth, it was expected that this predicted value would be less than the corresponding calorimeter result.

The fourth bar represents the DEAP model best estimate for hot-fire conditions. A substantial lowering of the rib effectiveness was expected due



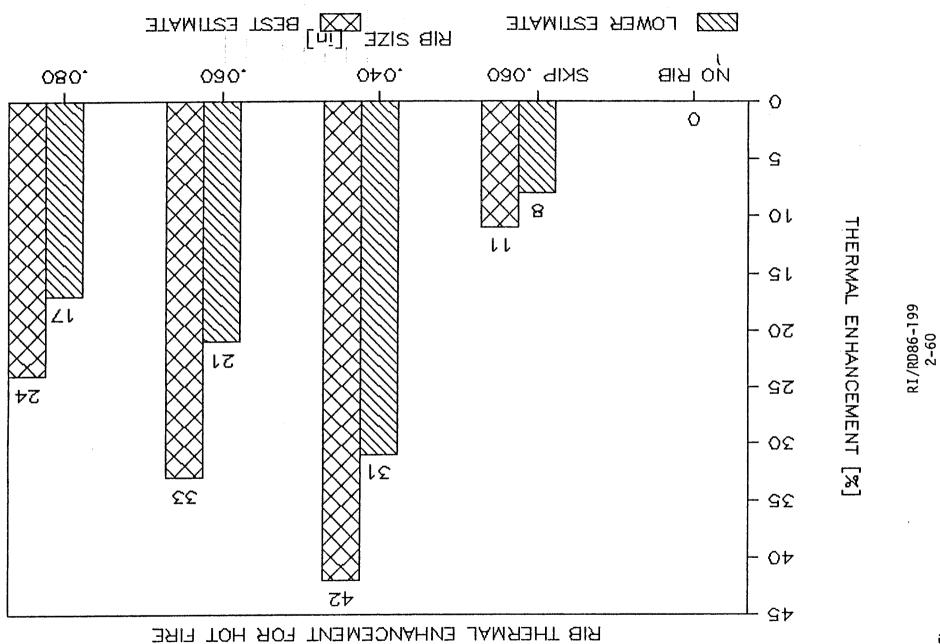
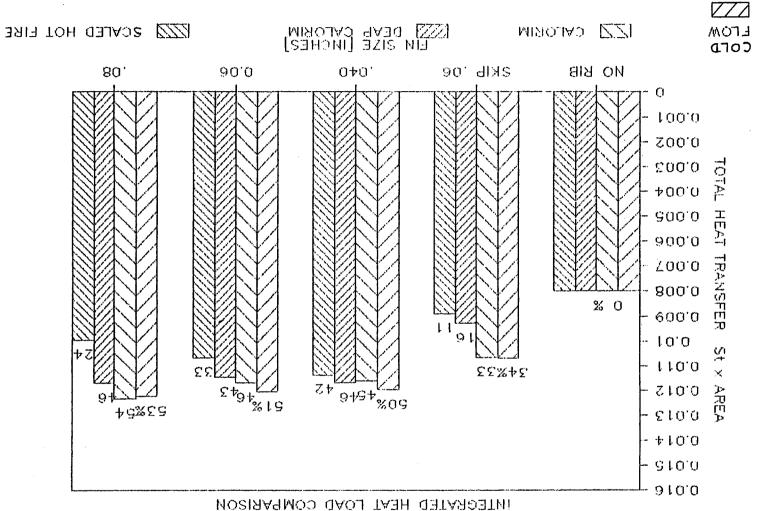


FIGURE 2-35

RIBBED COMBUSTOR HEAT TRANSFER RESULTS



RI/RD86-199 2-61 to the non-isothermal rib effect at high heat fluxes. Since the calorimeter tests were performed at relatively low heat fluxes, the ribs were isothermal. However, under hot-fire conditions the rib tip was predicted to be much hotter than the rib base, thus decreasing the effectiveness of the rib.

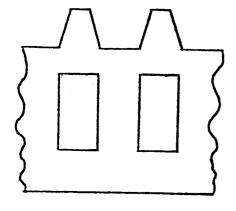
Selected Rib Configurations

Results of scaling analysis using the cold flow velocimeter data have indicated that a 0.040 high-0.040 base truncated triangular rib with a 0.020 tip width and a pitch of 0.0785 had the highest performance. Wall temperatures for this configuration are projected to be acceptable and fabricability was demonstrated during fabrication of the hot-air calorimeter test chamber. Accordingly, this design is the top recommended configuration.

The second recommended configuration is a 0.030 high-0.040 base truncated triangular rib with a 0.020 tip width and a 0.0785 pitch. This design was not directly tested in the air test programs, but is projected to be near the peak of the enhancement curve derived from test data. The design will also have a lower wall temperature than a taller option having the same enhancement so will have a longer life.

Taller rib configurations and those with greater pitches, such as the 'skip rib' design, are not favored due to lower enhancement at hot-fire conditions. The taller ribs are also predicted to have higher wall temperatures which reduce combustor life.

The selected configurations are depicted in Figure 2-36 with standard 0.040 \times 0.080 coolant channels included as a reference.



0.040 tall - 0.040 base rib with 0.020 tip width - 0.0785 pitch

0.030 tall - 0.040 base rib with 0.020 tip width - 0.0785 pitch

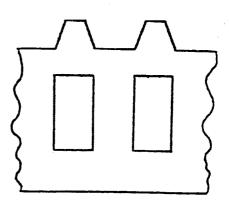


Figure 2-36. Selected Rib Configurations

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3.0 SUBTASK II - INCREASED LIFE STUDY

OBJECTIVE

The objective of this study was to evaluate alternate combustor coolant channel geometries that will enhance the combustor liner service life. Design objectives are to maintain an acceptable wall temperature with the increased heat extraction due to hot-gas wall ribs without excessive coolant circuit pressure drop or adverse structural efficiency. Supporting task objectives were to: screen appropriate channel candidate configurations; evaluate the flow characteristics in the channels; compare the designs at hot-fire conditions; and select the best designs for hot-fire test evaluations.

APPROACH

The approach followed for this subtask is summarized in the right hand side of Figure 1-2. A matrix of candidate channel configurations was developed based on previous design studies at Rocketdyne. The matrix featured channels with base fins, high aspect ratio rectangular channels, rounded corner channels, and channels with interrupted flow fins. The base fins were of varying width, aspect ratio, shape, and number (one or two).

These candidates were screened by relative rating for temperature reduction capability (life), pressure drop, boundary layer build-up risk, producibility, and heat transfer enhancement. Heat transfer analyses were conducted using a two-dimensional computer model using fully developed flow characteristics in the channels. Results of the thermal analyses and evaluations in the other categories were used to select eight configurations for laboratory testing.

A cold flow velocity profile mapping test series, using the same fixture as—in the hot-gas rib series, was conducted for the various channel configurations. The air flow velocity data were analytically scaled to hot-fire conditions to evaluate channel performance.

Three enhanced channel configurations were selected for hot-fire evaluation in the next program phase.

SCREENING ANALYSIS

A matrix of enhanced coolant channel concepts was formulated to provide a number of options for enhancing cooling efficiently. Five categories of channel enhancement methods were included:

- I. Standard rectangular shape varied aspect ratio
 - Variations on present channel design no change in fabrication methods.
- II. Finned base varied aspect ratio, number of fins, and the fin taper
 - Preliminary analysis shows promise in reducing hot-gas rib temperature.
- III. Varied corner radii for cases I and II
 - To evaluate effects of varied radii on boundary layer and ΔP .
- IV. Alternating channels, of Case I and II or I and III
 - Using alternate channel types may allow specific cooling of hot spots (ribs) without a great sacrifice in coolant ΔP .
- V. Interrupted fins intermittent fin or channel base posts
 - To investigate advantages of boundary layer break-up and evaluate effect on ΔP .

The channel geometries are depicted in Figure 3-1 along with the feature dimensions.

Heat transfer and other data for all geometries originally proposed were analyzed, and each geometry rated in five categories: Structure & Life Considerations; Coolant Pressure Drop; Boundary Layer Risk; Producibility and Heat Transfer. A scale of 0 to 10 was used for each rating category, with zero indicating an unacceptable risk or benefit and ten being an optimum condition within that category.

A category weighting system was employed to rate each category with respect to its importance in determining selection rank. Structural considerations and

FIGURE 3-1

PRELIMINARY MATRIX OF ENHANCED COOLANT CHANNEL CONFIGURATIONS

FIN GEOMETRY " INTERNAL OF INTERUPTION	CHANNEL HEIGHT ,080 CHANNEL WIDTH ,0740 CHANNEL PITCH ,0785	۸ <u>۳</u>	
COMBINATIONS OF "BEST" CHANNEL CASES:	CHWINEL HEIGHTS ,080 CHANNEL WIDTHS ,0740 CHANNEL PITCH ,0785 RIB PITCH ,1570 RIB OVER CHANNEL)	٨١	
CORNER RADII , 001 TO ,020 BOTH CHANNEL AND FIN WALLS INTERSECTIONS		III	
FIN HEIGHT .015 TO .024 FIN BASE WIDTH .010 TO 020 FIN TIP WIDTH .010 TO 015 FIN MUMBER/CHANNEL 1.5.3	сничиец нетент ,080 " мтотн ,040 сничиец рттсн ,0785	11	
СНАИИЕL ASPECT RATIO: 1,5 - 4 НЕІGHT ,08 ТО ,12 МІТПН ,020 ТО ,060 СНАИИЕL РІТСН ,0397 - ,100 RIB РІТСН (М/СНАИИЕLS) ,0785 - 100		I	
VARIABLES	CONSTANTS		СНАИИЕГ СЕОМЕТВУ

RI/RD86-199 3-3 coolant pressure drop were considered to be most important in determining selection ranking, together representing 60% of the weighted sums. Criteria for determining ratings within each category are included in Appendix E.

As mentioned previously, several cases were evaluated with the channel positioned under the hot-gas rib and under the land for comparison of heat transfer capability. No significant difference was noted, so from a heat transfer standpoint the location of the channel is not crucial. Further evaluation of structural considerations will be made following Subtask 3 of the task.

The final selection ranking, and the recommended channel candidates were based mainly on the weighted score rank. Another factor affecting selection was avoidance of duplication in flow analysis effort.

The dual-finned channel geometries were the highest ranked of the 27 configurations rated in this study. This is the result of the increased heat transfer provided by the two coolant side fins, resulting in a much lower maximum material temperature. The additional channel width aids in offsetting the increased pressure drop associated with the addition of fins to a channel. Both dual-fin geometries are recommended to study the effect of differing fin aspect ratio on coolant flow in the channel.

Single-finned channels were the most consistent in their beneficial enhancement effects, and four were selected for this flow study. The .015 x .015 finned channel showed the highest score in rating and is the lowest in fin aspect ratio. The .024 x .015 finned channel was selected for its higher aspect ratio, and to study flow effects of the higher, wider fin (as it differs from the .010 wide fins in the dual-fin channels). The two tapered fin geometries were also selected, and will allow comparison with the standard rectangular fin.

The increased corner radii selection was selected for testing in order to gain additional insight in coolant channel flow/boundary layer characteristics.

High aspect ratio rectangular channels were analyzed for widths between 0.020 and the 0.040 reference. The number of channels was increased in accordance with the width, but the land width was held at 0.040. Initial results indicated increased wall temperature and pressure drop for these configurations compared to the reference case $(0.040 \times 0.080 \text{ rectangle})$. Therefore, these configurations were not selected for test.

Subsequent review of computer outputs showed that a program override feature was mistakenly increasing the heat flux when the channel width was reduced. The cases were, therefore, invalid since they could not be directly compared to the other configurations. Later analysis indicated that high aspect ratio channels could provide a cooling benefit if both channels and land widths were reduced simultaneously.

The combination geometries (category IV) resulted in a very good compromise between rib temperature reduction and channel pressure drop. Such channel geometry combinations show promise, but were not selected for this test since cold flow study of the individual channels shown would be duplicated by selection in categories I & IIa.

Specific heat transfer models of interrupted-flow (category V) type configurations were not made due to the time and complexity involved in such a task. Other analysis of this type of channel geometry have concluded that any advantage gained in utilizing an "interrupted fin" geometry would be more than off-set by the cost and complexity of fabricating it. The concept of breaking up the boundary layer along the coolant channel fin may be worthy of additional study, but is outside the scope of this task.

The ratings and ranking of the channel geometries considered in the study are presented on Table 3-1. The coolant geometries recommended for testing were:

- 1. & 2. Dual fin geometries; fin aspect ratios 1.5 and 2.4.
- 3, 4, 6 & 7 Single fin geometries; fin aspect ratios 1.0 and 2.4, and taper fin.
- 5. Finned channel with large corner radii (flow study)
- 8. Baseline .040 x .080 standard channel.

	 	STRUCTURE/	COOLANT	YRAGNUOS	PRODUCIBILITY	HEAT	T		<u> </u>	
CATEGOR	CHANNEL CO.	LIFE .JS WEIGHTED	ΔP .25 WEIGHTED	LAYER .20 WEIGHTED	.10 WEIGHTED	TRANSFER	WEIGHTED SUMS	WEIGHTED RANK	SELECTION RATIONALE	SELECTION
CATEGORY	CHANNEL GEOMETRY	RAT'O WT'D	RAT'D WT'D	RAT'G WT'D	HAT'G WT'D	C'TW B'TAR	anma	HANK	BATIONALE	7445
I. ASPECT RATIO	AR									
	x.040 2.0	0 0	9 2.25	8 1.60	10 1.00	0 0	4.86	16	BASELINE CHANNEL,	8
.080 HEIGHT	x.030 2.67	2 .70	a .76	7 1.40	10 1.00	6 .60	4.46	22	FOR COMPARISONS	
	026 3.2	2 .70	0 0	6 1.20	g .80	8 .80	3.60	24		
	a.020 4.0	0 0	a 0	6 1.00	B .80	8 .80	2.00	28		
	N.040 3.0	0 0	10 2.50	8 1.60	10 1.00	0 0	6.10	14		
.120 HEIGHT	x.030 4.0	0 0	9 2.26	7 1.40	8 .80	4 .40	4.86	19		
	A.025 4.8	0 0	6 1.60	6 1.20	8 .80	6 .60	4.10	23		
·	x.020 6.0	0 0	0 0	5 1.00	8 .80	8 .80	2.60	27		
,	x.040 3.76	a 0	10 2.60	8 1.60	10 1.00	0 0	5.10	16		
150 HEIGHT	a.030 5.0	0 0	10 2.50	7 1.40	8 .80	4 .40	6.10	16		
	s.026 6.0	0 0.	8 2.00	6 1.20	B .BO	6 .60	4.60	21		*
	s.020 7.5	Q 0	3 .75	6 1.00	6 .60	8 .80	3.15	25		· · · · · · · · · · · · · · · · · · ·
IIA. SINGLE FIN	FIN GEOM. AR	7 2.45	7 1.76	4 .80	7 .70	4 .40	6.10	,	NARHOW FINS ALSO IN DUAL FIN GEOM'S	
STANUARO .080± .040 CHANNEL	M .024π.010 2.4	8 2.80	6 1.60	3 .60	6 .BQ	4 .40	8.00	g	ICAT. IIBI	
	.016x.016 1.0	8 2.90	7 1.76	3 .60	7 .70	4 .40	6.2b	.	BEST OF SINGLE FIN	3
	∭ .024×.016 1.8	8 2.80	6 1.26	2 .40 .	e .ec	4 .40	5.46	13	WIDE FIN STUDY	7
TAPERED FIN	.010 TIP	8 2.80	6 1.6Q	4 80	6 .50	4 .40	8.00	8	TAPERED FIN	4
-	.015 TIP	8 2.80	6 1.26	3 .60	6 .50	4 .40	6.50	12]	6
IIB. DUAL FIN 080x.060 CHANNEL	.016x.010 1.6	10 3.60	9 2.25	3 .80	4 .40	8 .60	7.36	1	BEST OVERALL	1
	.024a,010 2.4	10 3.60	9 2.26	2 .40	4 .40	8 .60	7,16	2		2
III. <u>CORNER RADII</u>	.080x.040 .020R	g G	9 2.25	8 1.60	8 .80	0 0	4.66	20		
	.015x.010 FIN .006010R	7 2.46	7 1.76	4 .8G	4 .40	4 .40	6.80	11	FLOW STUDY	6
IV. COMBINATION	FIN GEOM.									
STANDARD ,080 x .040 CHANNEL.	016x.010	7 2.46	8 2.00	4 .80	7 .70	4 .40	8.36	4	FLOW EFFECTS	_
• 2 CHANNELS/RIB. • FIN UNDER RIB	024H.010	8 2.80	7 1.76	08. C	8 .60	4 .40	6.15	a	CHAHACTEHIZED IN CATEGORY	
ONLY	M	a 2.80	8 2.00	ο ε	7 .70	4 .40	6,50	3	I, IIA & IIB SELECTIONS	
	M 015±.024	8 2.80	7 1.76	2 .40	6 60	4 .40	6.95	10	<i>J</i>	
IV. INTERRUPTED		8 2.80	4 1.00	4 .80	0 0	4 .40	5.00	17	PRODUCIBILITY	
"SAWTOOTH" IVARIATION OF SINGLE FINI				ļ						
	1	1		RT/RDS					L	

RI/RD86-199

AIR TEST PROGRAM DEFINITION

The cold flow velocity mapping test method was selected as the evaluation means for the coolant channel designs. An analysis was conducted to select the channel scale and flow conditions for testing. A design for modifying the existing fixture design was completed.

Analysis

The channel flow conditions required for accurate simulation were less stringent than those required by the external rib flow tests. Whereas for external flow tests a growing boundary layer must be correctly scaled, no such scaling problem arises in channel flows. The only requirement is that the channel flow be both hydrodynamically and thermally fully developed, and be fully turbulent as is the case for combustor channel flow.

The requirement for fully developed turbulence was satisfied by the Reynold's number capability of the Cold Flow test bed. A typical channel air flow velocity of 72 meters/sec corresponds to a Re = 50,000 which is far above the transition Re = 2500. This is based upon an eight times scale channel hydraulic diameter of Dh = 0.424 inches. Thus, the channel flow was assured to be fully turbulent. Although this is still an order of magnitude below the Reynold's number of an actual combustor channel, hydrodynamic similarity affords the extrapolation of the cold flow test results to these conditions.

The requirement of a hydrodynamically and thermally developed flow was based upon a conservative estimate of an entrance length of one hundred hydraulic diameters L=100Dh. This corresponds to a length of L=42.4 inches. Therefore, velocimeter measurements were taken at a distance of 72 inches downstream of the channel inlet. This insured that the internal flow in the channel was fully developed.

Test Fixture Design

The channel test panels were designed to fit into the existing test fixture with minimal changes. The main requirement for the test fixture was to

properly create the correct channel flow conditions by providing a fixed boundary at the channel 'outside' wall to simulate the channel closeout. This was accomplished by positioning the test panel flush against the cover plate, using the cover as the closeout with the channel shape in the test panel itself.

Spacers were designed to raise the test panel from the lower (rib) test position to the upper (channel) test position. Exact measurements of the fabricated side panels were made to precisely size the spacers to provide a minimum gap between the test panels and the cover.

Two test panels were designed with four of the selected channel configurations in each panel. The channels were eight times scale as specified by the test analysis. A black anodize surface treatment was selected to reduce reflectivity.

A cross section of the channel cold flow test fixture configuration is presented in Figure 3-2. The detail drawings for the spacers and panels are contained in Appendix F.

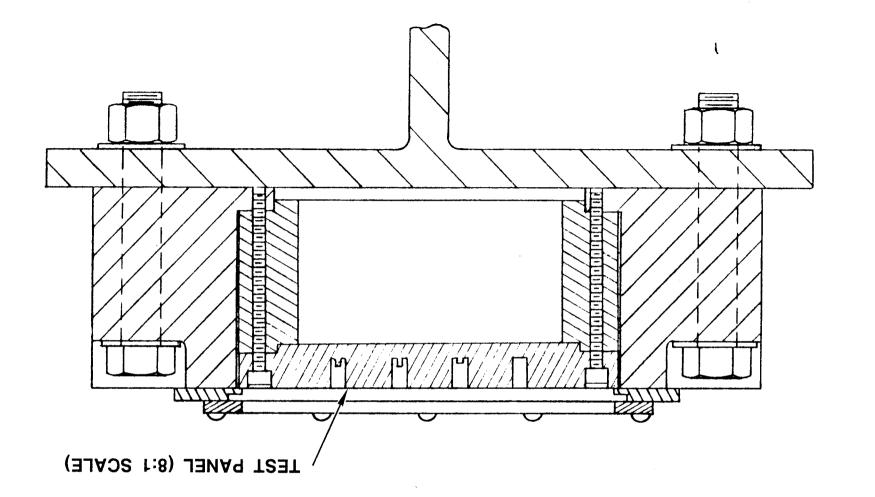
COLD FLOW TEST PROGRAM (CHANNELS)

Fabrication

The spacers and test panels were fabricated per the drawing requirements. The aluminum spacers were machined to match the test fixture bolt hole patterns.

The test panels were machined from aluminum plate. Special attention was given to maintaining smooth machine cuts in the channel shapes to prevent flow disturbances. The panels were black anodized after machining to provide a non-reflective surface. Photographs of the completed test panels are given in Figure 3-3. The channel configurations were dimensionally inspected at completion to ensure acceptability and to provide exact dimensions for use in formulating grid points for the velocity measurement matrix.

COLD FLOW TEST FIXTURE - COOLANT CHANNEL CONFIGURATION



RI/RD86-199 3-9



Testing

The same basic test approach as used for the rib flow evaluation was followed for the channel tests. A test matrix, Appendix F, similar to that used for the rib tests was initially planned, however, it was decided to observe the channel results only at the end window station as was done with the ribs.

Installation. The change-over to the channel test set-up was made without significant alteration to the overall test system. The channel panels were installed using the spacers without need to adjust the fixture side panels. An endplate was made for the fixture to cover the open area under the channel test panel and force the air to go only through the channel passages. The flow tubes and screens were removed from the plenum and the end section carefully sealed.

Just prior to installing the cover, a very thin coating of RTV elastomer was applied to the areas between the channels to provide a gap filler and a seal to preclude cross flow. The cover was installed and tightened down prior to RTV curing.

<u>Tests.</u> Initially, channel center velocities were measured to ensure that the required test conditions were met. Velocities of approximately 70 m/sec were obtained, resulting in a Reynolds number much greater than the 10,000 minimum. The seeding system was used for these tests and high data rates were obtained due to the particle concentration in the flow.

The data collection process was the same as for the rib tests. The reference channel and five enhanced channel geometries were mapped. Results are exemplified by the velocity field for the single tall fin configuration, Figure 3-4. As many as eighty data points were collected within the channels. Velocity maps for all of the tested channels are contained in Appendix F.

The results from these tests provide the first detailed flow velocity information in enhanced and rectangular coolant channels. The quantified velocity profiles were obtained to allow analytical assessments to be adjusted for heat transfer degradation due to velocity decreases in the corner and fin valley sections.

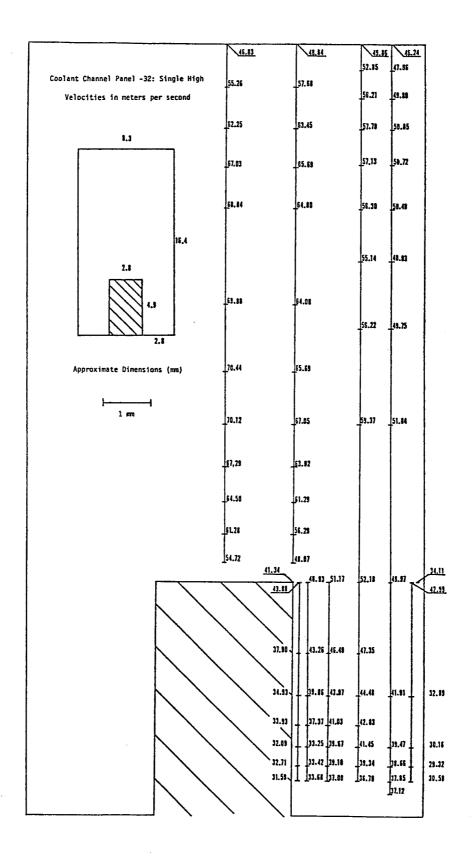


Figure 3-4. Velocity Profile for Single High Fin Configuration RI/RD86-199 3-12

Scaling Results (Channels)

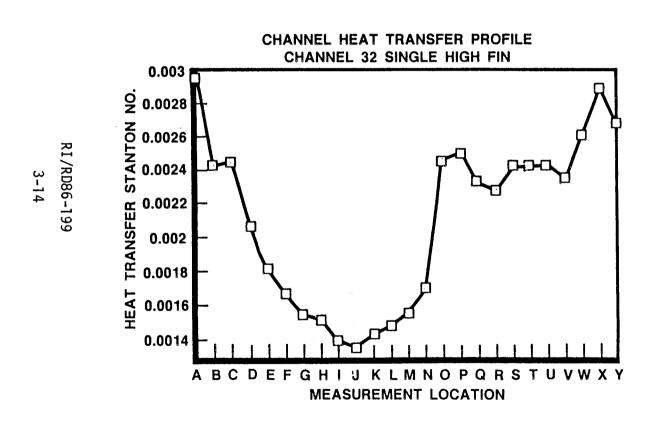
The scaling analysis for the coolant side conditions follows the same procedure as for the ribs. The coolant properties are scaled for hydrogen at the proper conditions at the end of the combustor cylindrical section. In the final scaling, corrections are made for the supercritical fluid properties, large bulk wall temperature gradients, and high heat flux effects. Again, these could not be simulated in the laboratory and a more realistic assessment of channel performance is obtained by this scaling. An example Stanton number profile for tall fin configuration is shown in Figure 3-5. The integrated cooling benefit (transfer coefficient x area) for the candidate channels is shown in Figure 3-6.

In addition to these configurations, high aspect ratio channels were considered in the analysis. No cold flow data were obtained for a rectangular channel other than the 2:1 aspect ratio reference channel. Analysis conducted compared a case where double the number of channels were evaluated. This configuration, with two 0.020 wide channels with 0.0204 land widths per channel, was evaluated at various channel heights (flow areas). A slight temperature increase occurred compared to the reference case, but the combustor pressure drop was lower. The pressure drop decreased further with increased channel height, but the wall temperature also increased. Reducing the channel height would be expected to increase velocities and decrease the wall temperature although the pressure drop would increase correspondingly.

Maintaining a wall temperature commensurate with long life at the higher heat fluxes is the primary goal for the enhanced channel designs. Accordingly, the temperature reduction compared to the reference channel is an appropriate means for comparing the configurations. (The heat flux enhancement is not affected appreciably by the channel design.) A graph of the temperature benefit for the tested enhanced geometries compared to the reference channel is presented in Figure 3-7. It can be noted in comparing figures 3-6 and 3-7 that only small differences in the cooling enhancement are sufficient to produce the temperature differences.

FIGURE 3-5.

TYPICAL COOLANT CHANNEL TEST RESULTS



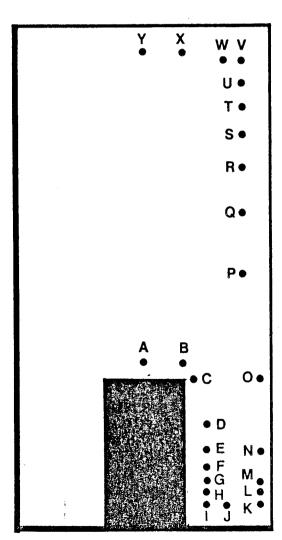
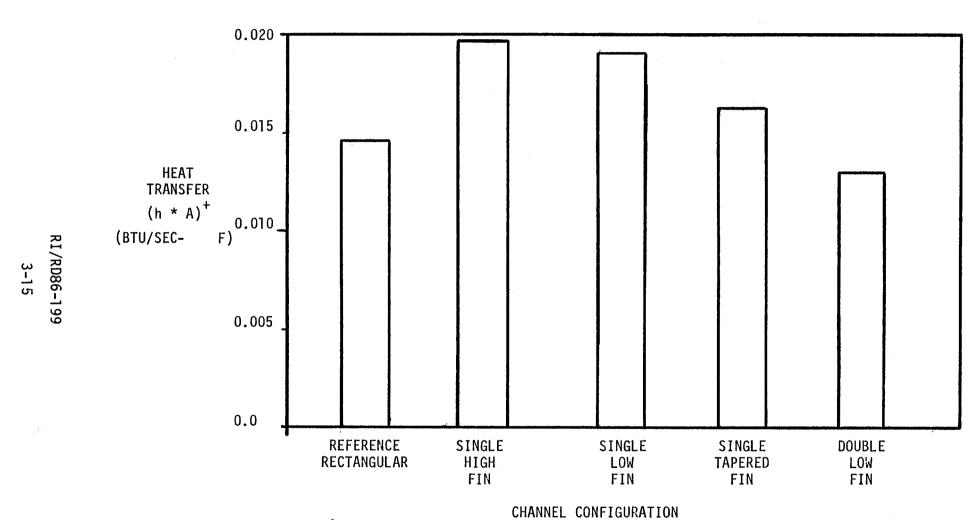


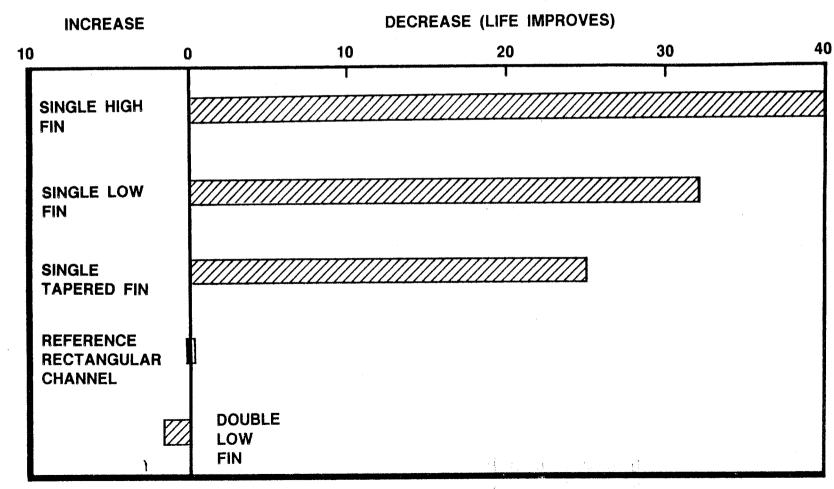
Figure 3-6. Cooling Enhancement For Candidate Channels



+ h * A =
$$N_{st} \left(\frac{\dot{M}C_p}{A_f}\right) * A$$

LINER TEMPERATURE CHANGE WITH ENHANCED CHANNELS

TEMPERATURE CHANGE, F



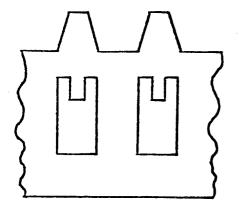
RI/RD86-199

Selected Enhanced Channel Configurations

The two recommended channel configurations tested in the cold flow velocity mapping program are the single fin designs with a high and low aspect ratio fin. The 'tall fin' is a 0.024 tall-0.015 wide rectangular fin placed in the center of a 0.040 wide-0.080 tall rectangular channel. The land width is slightly more than the 0.040 channel width. The second design is similar to the first except that the fin height is reduced to 0.015.

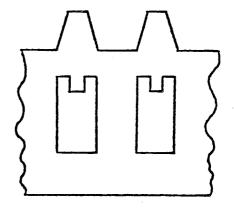
High aspect ratio channels (AR>2.0) were investigated by analysis, but were not flow tested. Evaluation of a configuration with double the number of channels in the ribbed section (a 0.020 wide-0.080 tall rectangular channel with a land of approximately 0.020) was made using unadjusted flow conditions. A lower pressure drop resulted, although the trough wall temperature was higher than the reference case. A lower wall temperature could be achieved by reducing the channel height although the pressure drop would increase accordingly. Without specific flow data to support a refined analysis, this design cannot be completely evaluated and compared to the other designs. Because of the potential benefits, it is recommended that this configuration be included in the channel test calorimeter to complete the evaluation. This would require the test sections in the calorimeter to be quarter sections rather than one-thirds arcs. This is not expected to impact the design or quality of the results significantly.

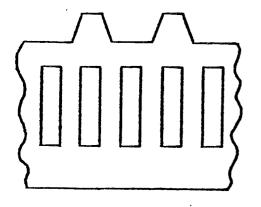
The configurations are depicted in Figure 3-8 with sample hot-gas wall ribs included as a reference to indicate channel orientation.



0.040 wide - 0.080 tall channel with 0.015 wide - 0.024 tall fin

0.040 wide - 0.080 tall channel with 0.015 wide - 0.015 tall fin





0.020 wide - 0.080 tall high aspect ratio channel

Figure 3-8. Selected Channel Configurations

RI/RD86-199

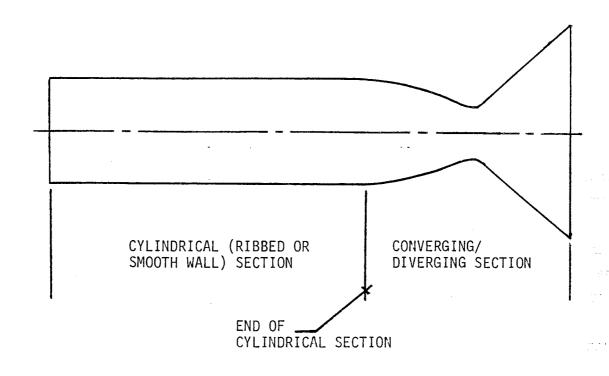
4.0 CONCLUSION

A structured selection analysis process has been completed to determine the best hot gas rib and enhanced coolant channel candidates for hot-fire evaluation. The process included analytical screening using available computer models with an assumption that ideal boundary layer behavior occured. Laboratory test programs were conducted to further screen the candidates and to evaluate the flow assumption. The test results provided a base for directly comparing the designs. Quantative flow field data, previously not available for the enhanced combustor geometries and conditions, were obtained in the laboratory tests to anchor flow behavior representation.

The results lead to the selection of the 0.040 high - 0.040 base rib and the single high fin channel configurations as the top candidates. Other configurations selected were a 0.030 high - 0.040 base rib, a single low fin channel and high aspect ratio (0.020 wide - 0.080 tall) rectangular channels. Reference designs are a smooth hot gas wall and a 0.040 wide - 0.080 tall rectangular coolant channel.

The laboratory test results were crucial in arriving at this selection. The flow mapping tests showed that the flow field did not match the 'ideal' case and that several designs that appeared 'better' in the analytical screening could be expected to perform poorly under actual conditions. The designs selected provided the best blend of thermal enhancement and temperature and pressure drop control.

The integrated enhancement for the ribbed combustor section with the top candidate 0.040 high rib is 60% above the comparative smooth wall design. Laboratory flow test results showed that the design suffered a minimal amount of heat transfer degradation compared to an 'ideal' case where the boundary—layer was uniform. Although the enhancement at the end of the combustor cylindrical section was somewhat lower than the optimum value, the integrated heat load enhancement (following an exponential build-up) for the ribbed section was only 6% less. Further, in terms of the overall combustor heat load, including the converging throat section and the diverging nozzle portion, the difference compared to optimal was only 4%. These results are summarized in Figure 4-1.



	ENHANCEMENT			
COMBUSTOR SECTION	I IDEAL BOUNDARY LAYER CONDITIONS	ACTUAL BASED ON TEST RESULTS		
END OF CYLINDRICAL SECTION	66%	42%		
OVERALL CYLINDRICAL SECTION	66%	60%		
OVERALL COMBUSTOR (WITH CONVERGING/DIVERGING SECTION)	45.7% 	41.6% 		

Figure 4-1. Heat Load Enhancement for Ribbed Combustor

RI/RD86-199 4-2 Incorporating the enhancements into an OTV engine combustor can have several significant impacts. An overall increased heat load of 41.6% provides additional energy to drive the propellant pump turbines, thereby increasing engine chamber pressure capability. A comparison of the attainable chamber pressure for the smooth wall cylindrical contour, 'best estimate' for the 0.040 rib, and 'ideal' case (uniform heat transfer coefficient) for the 0.040 rib are indicated in Figure 4-2. The smooth wall tapered combustor contour used in the Integrated Component Evaluator (ICE) is also included as a reference for an enhanced combustor.

Hot-fire tests are planned to perform a final screening and verification of the candidate enhancements. These tests will be conducted at the design conditions to obtain accurate heat flux and hot gas flow conditions.

The test program will be conducted using the Integrated Components Evaluator (ICE) expander cycle test system. The enhanced combustor designs will be tested using a replaceable water cooled calorimeter spool section that is incorporated in the ICE thrust chamber. The spool fits between the injector and existing smooth wall tapered combustor as shown in Figure 4-3.

Tests will be conducted on the two rib designs and the smooth wall reference with circumferentially cooled spools. The three candidate enhanced channels and the reference channel will be tested using a single axially cooled, smooth walled spool.

These tests will provide the quantitative comparison of the candidates at hot-fire conditions needed to selecte the final designs to be incorporated in the enhanced combustor design. Additionally, the hot-fire results will be used to further anchor analytical tools so that a more accurate analysis of the detail combustor design can be made.

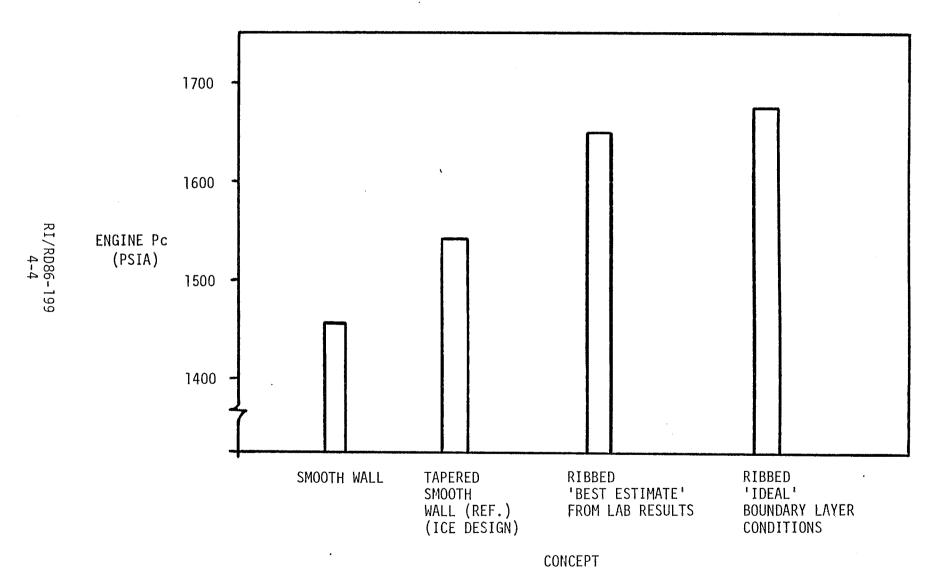
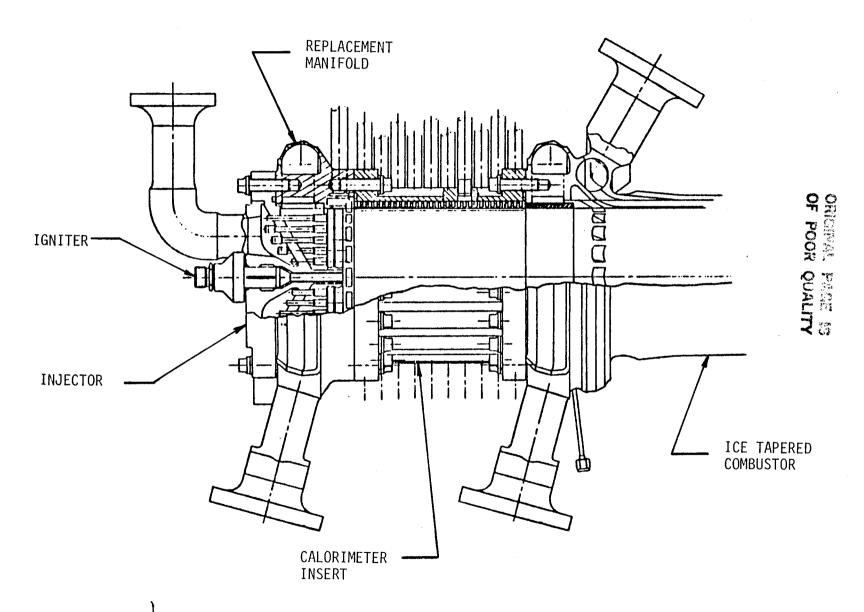


FIGURE 4-2. Attainable Chamber Pressure Comparison For Enhanced Combustor Concepts*

*Common S-O-A Turbomachinery Characteristics, 2000 Btu/Sec Regenerator in System

HOT FIRE VERIFICATION



RI/RD86-199 4-5

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APPENDIX A

RIB ANALYSIS COMPUTER OUTPUTS
RIB EVALUATION CRITERIA RATING SCALES

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LOC.
NUMBER
                 ADMITTANCES (Y)
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 11
      3.586E-03 3.588E-03 3.589E-03 1.569E-03 1.994E-03 9.129E+08 9.944E-04 2.946E-03 2.954E-03 3.258E-03
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LOC.
NUMBER
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                                                               0.
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                            'n
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259E+03-1,760E+02
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                                                                                                      LOC.
                                         LOCATIONS 181 THROUGH 2999 EQUAL
                                               5.646E-04 5.811E-04 5.939E-04 9.093E-04 6.349E-04 0.
                                      ' 0
5.794E-04 5.902E-04 8.959E-04 6.007E-04 4.196E-04 6.396E-04 4.608E-04 4.915E-04 5.194E-04 5.439E-04
                                                                                                      191
7.210E-05 7.210E-05 3.605E-05 3.991E-04 6.213E-04 4.546E-04 4.885E-04 5.177E-04 5.429E-04 5.429E-04
                                                                                                      191
2.438E-03 7.158E-04 6.949E-04 8.950E-05 1.790E-05 4.505E-05 7.220E-05 7.220E-05 7.225E-05
                                                                                                      161
1.150E-03 5.753E-03 5.762E-03 5.772E-03-2.804E-03-5.581E-03-5.694E-03-1.956E-03 4.027E-06 2.441E-03
9.705E-03 3.286E-03 3.296E-03 3.304E-03 3.311E-03 3.315E-03 3.316E-03 3.324E-03 3.324E-03 3.324E-03
                                                                                                      121
6.60ZE-03 6.615E-03 6.626E-03 6.633E-03 6.638E-03 6.640E-03 9.279E-04 9.091E-04 1.158E-02 9.683E-03
                                                                                                      111
6.633E-03 6.638E-03 6.640E-03 9.196E-04 8.768E-04 1.352E-02 7.857E-03 6.566E-03 6.566E-03 6.565E-03
                                                                                                      101
9.658E-04 1.132E-03 1.438E-02 4.023E-03 4.040E-03 6.665E-03 6.586E-03 6.60ZE-03 6.615E-03 6.625E-03
3.304E-03 3.310E-03 3.315E-03 3.319E-03 3.321E-03 3.323E-03 1.151E-03 1.084E-03 8.502E-04 8.056E-04
                                                                                                      18
5.754E-03 1.301E-03 1.612E-03 1.933E-03 2.265E-03 1.243E-02 9.664E-03 9.685E-03 3.295E-03
6,450E-04 7,201E-04 1,389E-03 6,842E-04 6,508E-04 8,064E-04 9,670E-04 1,133E-03 5,728E-03 5,742E-03
3.586E-03 1.538E-03 2.007E-03 8.827E-04 9.910E-04 1.999E-03 2.003E-03 7.026E-04 1.352E-03
9.901E-04 2.934E-03 2.941E-03 3.244E-03 3.551E-03 3.561E-03 3.569E-03 3.566E-03 3.580E-03 3.583E-03
3.549E-03 3.559E-03 3.567E-03 3.574E-03 3.578E-03 3.582E-03 3.584E-03 1.511E-03 1.973E-03 9.405E-04
3,580E-03 3,583E-03 3,686E-03 1,626E-03 1,962E-03 9,129E+08 9,879E-04 2,928E-03 2,938E-03 3,243E-03
1.224E-02 1.067E-02 6.816E-03 2.926E-03 2.936E-03 3.241E-03 3.560E-03 3.561E-03 3.569E-03 3.565E-03
9,187E-03 1,465E-02 1,226E-02 1,058E-02 6,616E-03 1,991E-03 1,997E-03 1,001E-03 9,183E-03 1,465E-02
                                                                         ADMITTANCES (Y)
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HUMBER LOC.

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ORIGINAL PAGE IS
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LOC.
 NUMBER
                 ADMITTANCES (Y)
      1.328E-02 2.125E-02 1.789E-02 1.559E-02 8.898E-03 1.981E-03 1.987E-03 9.965E-04 1.328E-02 2.125E-02
      1.788E-02 1.558E-02 8.899E-03 2.909E-03 2.923E-03 3.229E-03 3.539E-03 3.552E-03 3.561E-03 3.569E-03
      3.575E-03 3.579E-03 3.581E-03 1.493E-03 1.938E-03 9.129E+08 9.830E-04 2.914E-03 2.926E-03 3.232E-03
      3.539E-03 3.550E-03 3.560E-03 3.567E-03 3.573E-03 3.577E-03 3.580E-03 1.472E-03 1.945E-03 9.356E-04
      9.863E-04 2.923E-03 2.931E-03 3.233E-03 3.541E-03 3.553E-03 3.562E-03 3.569E-03 3.575E-03 3.579E-03
      3.582E-03 1.503E-03 1.975E-03 9.711E-04 9.876E-04 1.992E-03 1.996E-03 1.000E-03 6.926E-04 1.339E-03
      6.434E-04 7.086E-04 1.368E-03 6.748E-04 4.188E-04 5.217E-04 6.307E-04 7.463E-04 5.695E-03 5.711E-03
      5.726E-03 8.374E-04 1.043E-03 1.261E-03 1.493E-03 1.236E-02 9.606E-03 9.643E-03 3.269E-03 3.285E-03
      3.296E-03 3.304E-03 3.310E-03 3.315E-03 3.318E-03 3.320E-03 1.134E-03 1.078E-03 4.185E-04 5.211E-04 6.299E-04 7.459E-04 1.430E-02 4.003E-03 4.023E-03 6.544E-03 6.567E-03 6.586E-03 8.602E-03 6.615E-03
      6.624E-03 6.630E-03 6.633E-03 9.017E-04 8.707E-04 1.347E-02 7.804E-03 7.829E-03 6.545E-03 6.568E-03
      6.587E-03 6.603E-03 6.615E-03 6.624E-03 6.630E-03 6.634E-03 9.088E-04 8.973E-04 1.154E-02 9.650E-03
111
      9.673E-03 3.275E-03 3.288E-03 3.297E-03 3.305E-03 3.311E-03 3.315E-03 3.318E-03 3.321E-03 1.154E-03
121
      1.133E-03 5.734E-03 5.743E-03 5.753E-03-2.788E-03-6.544E-03-5.666E-03-1.949E-03 4.013E-05 2.440E-03
131
      2.438E-03 7.062E-04 6.850E-04 8.950E-06 1.790E-05 6.285E-05 1.078E-04 1.078E-04 1.078E-04 8.995E-05
      7.210E-05 7.210E-05 3.605E-05 3.740E-04 5.852E-04 4.311E-04 4.657E-04 4.961E-04 5.228E-04-5.454E-04
151
      5.634E-04 5.768E-04 8.812E-04 5.973E-04 4.009E-04 6.096E-04 4.396E-04 4.701E-04 4.985E-04 5.242E-04
161
      5.465E-04 5.649E-04 5.799E-04 8.922E-04 6.276E-04 0.
171
                                                                    ٥.
                                LOCATIONS 181 THROUGH 2999 EQUAL 0
LOC.
                TEMPERATURES (T) Z channels /RIB
NUMBER
      2.397E+03 2.400E+03 2.412E+03 0.
      2.188E+03 2.194E+03 2.209E+03 0.
                                                          0.
      1.811E+03 1.818E+03 1.838E+03 0.
                                                          ٥.
      1.310E+03 1.318E+03 1.342E+03 0.
                                               ٥.
      7.253E+02 7.221E+02 7.205E+02 5.988E+02 5.509E+02 5.354E+02 0.
                                                                               0.
      6.536E+02 6.490E+02 6.607E+02 5.631E+02 5.125E+02 4.969E+02 0.
                                                                               0.
      5.837E+02 5.505E+02 5.263E+02 4.840E+02 4.543E+02 4.630E+02 0.
                                                                          0. 00 00
      5,255E+02 4,529E+02 4,058E+02 4,005E+02 3.875E+02 4,089E+02 0,
 71
 81
      ٥.
                3.012E+02 3.111E+02 3.046E+02 2.749E+02 0.
                                                                    ٥.
 91
                2.018E+02 2.255E+02 2.214E+02 1.905E+02 0.
101
                1.299E+02 1.551E+02 1.529E+02 1.248E+02 0.
                                                                   · O.
111
                7.626E+01 9.982E+01 9.856E+01 7.368E+01 0.
                                                                    0,
121
                3.656E+01 6.797E+01 6.705E+01 3.473E+01 0.
                                                                              O. 1. 14
                                                                    ٥.
                8.123E+00 2.824E+01 2.715E+01 5.836E+00 0.
131
               -1.140E+01 9.996E+00 8.182E+00-1.574E+01 0.
     -3.889E+01-2.609E+01 4.285E+00 1.161E+00-3.580E+01-7.524E+01 0.
     -1.008E+01 1.214E+01 1.768E+01 5.981E+00-1.215E+01-2.883E+01 0.
      8.638E+00 7.000E+01 7.000E+01 2.543E+01 4.612E-01-1.429E+01 0.
                                LOCATIONS 181 THROUGH 999 EQUAL O.
LOC.
                CAPACITANCES (C)
NUMBER
                                LOCATIONS
LOC.
NUMBER
                GEN. RATES
                                LOCATIONS
                                             1 THROUGH
                                                        999 EQUAL
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LOC.
NUMBER
                ADMITTANCES (Y)
      4.699E-03 7.472E-03 6.210E-03 5.319E-03 4.269E-03 1.984E-03 1.988E-03 9.955E-04 4.697E-03 7.468E-03
      6.206E-03 5.316E-03 4.268E-03 2.914E-03 2.921E-03 3.221E-03 3.523E-03 3.530E-03 3.536E-03 3.541E-03
      3.544E-03 3.547E-03 3.550E-03 1.154E-03 1.672E-03 9.129E+08 9.836E-04 2.914E-03 2.921E-03 3.221E-03
      3.522E-03 3.529E-03 3.535E-03 3.540E-03 3.543E-03 3.546E-03 3.549E-03 1.133E-03 1.645E-03 8.828E-04
      9.844E-04 2.916E-03 2.922E-03 3.221E-03 3.523E-03 3.530E-03 3.536E-03 3.541E-03 3.544E-03 3.547E-03
      3.549E-03 1.144E-03 1.620E-03 8.390E-04 9.847E-04 1.986E-03 1.989E-03 9.959E-04 5.469E-04 1.144E-03
      6.016E-04 6.333E-04 1.097E-03 5.584E-04 1.329E-03 1.640E-03 1.953E-03 2.269E-03 5.711E-03 5.719E-03
      5.728E-03 2.658E-03 3.279E-03 3.905E-03 4.537E-03 1.239E-02 9.613E-03 9.634E-03 3.259E-03 3.268E-03
 71
      3.274E-03 3.279E-03 3.282E-03 3.285E-03 3.288E-03 3.291E-03 9.278E-04 1.003E-03 1.328E-03 1.638E-03
      1.951E-03 2.267E-03 1.432E-02 4.004E-03 4.015E-03 6.519E-03 6.532E-03 8.544E-03 6.554E-03 6.562E-03
      6.568E-03 6.573E-03 6.577E-03 7.359E-04 8.081E-04 1.345E-02 7.788E-03 7.805E-03 6.518E-03 6.532E-03
      6.544E-03 8.554E-03 6.562E-03 8.568E-03 6.573E-03 8.576E-03 7.266E-04 7.724E-04 1.161E-02 9.620E-03
      9.637E-03 3.260E-03 3.268E-03 3.274E-03 3.279E-03 3.282E-03 3.285E-03 3.288E-03 3.290E-03 9.021E-04
      9.330E-04 5.716E-03 5.723E-03 5.731E-03-2.795E-03-6.559E-03-5.669E-03-1.944E-03 4.001E-05 2.424E-03
      2.425E-03 5.462E-04 5.518E-04 8.500E-06 1.700E-05 2.607E-05 3.513E-05 3.513E-05 3.513E-05 5.181E-05
      6.848E-05 6.848E-05 3.424E-05 4.862E-04 7.417E-04 5.194E-04 5.383E-04 5.537E-04 5.666E-04 5.776E-04
      5.871E-04 5.962E-04 9.113E-04 6.310E-04 4.902E-04 7.445E-04 5.198E-04 5.384E-04 5.537E-04 5.665E-04
161
      5.772E-04 5.862E-04 5.942E-04 9.040E-04 6.151E-04 0. 0.
                               LOCATIONS 181 THROUGH 2999 EQUAL O.
LOC.
                TEMPERATURES (T) Z chaunels/P, 1
NUMBER
      9,369E+02 9,423E+02 9,580E+02 0,
      0.839E+02 0.902E+02 9.092E+02 0.
      8.119E+02 8.192E+02 8.417E+02 0.
                                                                                                ٥.
      7.284E+02 7.353E+02 7.589E+02 0.
      6.402E+02 6.437E+02 6.576E+02 6.312E+02 6.196E+02 6.161E+02 0.
      6.026E+02 6.066E+02 6.273E+02 6.014E+02 5.853E+02 5.819E+02 0.
      5.636E+02 5.534E+02 5.528E+02 5.464E+02 5.401E+02 5.466E+02 0.
      5.281E+02 4.983E+02 4.827E+02 4.914E+02 4.916E+02 5.135E+02 0.
                4.162E+02 4.274E+02 4.299E+02 4.149E+02 0.
                                                                 ٥.
 91
                3.611E+02 3.770E+02 3.778E+02 3.610E+02 0.
                3.201E+02 3.349E+02 3.352E+02 3.203E+02 0.
101
111
                2.881E+02 3.007E+02 3.010E+02 2.885E+02 0.
                                                                            ٥.
121
                2.625E+02 2.732E+02 2.736E+02 2.634E+02 0.
                                                                  ٥.
                2.414E+02 2.512E+02 2.521E+02 2.433E+02 0.
131
141
                2.221E+02 2.341E+02 2.359E+02 2.263E+02 0.
151
      1.552E+02 1.990E+02 2.224E+02 2.258E+02 2.088E+02 1.845E+02 0.
      1.409E+02 1.405E+02 1.500E+02 1.665E+02 1.747E+02 1.748E+02 0.
161
      1.268E+02 7.000E+01 7.000E+01 1.288E+02 1.559E+02 1.653E+02 0,
                               LOCATIONS 181 THROUGH 999 EQUAL 0.
LOC.
NUMBER
                CAPACITANCES (C)
                               LOCATIONS
LOC.
NUMBER
               GEN, RATES
```

LOCATIONS I THROUGH 999 EQUAL 0

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JAUD3 606 HDUORHT I
                                                                        LOCATIONS
                                                                                      GEN. I RATES
                                                1 THROUGH 999 EQUAL
                                                                        LOCATIONS
                                                                                CAPACITANCES (C)
                                                                                                          NUMBER
                                                                                                            LOC.
                                                ГОСУТІОИЗ 181 ТНВОИСН ВВВ ЕФПУГ
                                            1.610E+02 7.000E+01 7.000E+01 1.579E+02 2.006E+02 2.167E+02 0.
                                            1.031E+02 1.776E+02 1.897E+02 2.162E+02 2.301E+02 2.331E+02 0.
                                                                                                            171
   OUALITY
                                            2,076E+02 2,701E+02 2,987E+02.3,030E+02 2,851E+02 2,561E+02 0,
                                                                                                            191
                                  .0
                                                      3.001E+02 3.138E+02 3.165E+02 3.064E+02 0.
                                                      3.241E+02 3.34BE+02 3.361E+02 3.26BE+02 0.
                                                                                                            141
                                                      3,494E+02 3,610E+02 3,615E+02 3,504E+02 0.
                                                                                                            131
                                                                                                            121
                                                      3.794E+02 3.931E+02 3.932E+02 3.794E+02 0.
                                                      4,166E+02 4.327E+02 4.324E+02 4.156E+02 0.
                                                                                                            111
ORIGINAL
   POOR
                                            .0
                                                                                                            101
                                                      4.642E+02 4.811E+02 4.806E+02 4.613E+02 0.
                                                                                                            16
                                                      5,287E+02 5,391E+02 5,390E+02 5,207E+02 0.
                                            6.653E+02 6.260E+02 6.029E+02 6.03EE+02 6.03EE+02 6.234E+02 0.
                                                                                                            18
                                            7.070E+02 6.914E+02 6.842E+02 6.682E+02 6.553E+02 6.588E+02 0.
              .0
                                          7.542E+02 7.558E+02 7.724E+02 7.278E+02 7.026E+02 6.955E+02 0. ..
       2506+02
                                            8.010E+02 8.021E+02 8.096E+02 7.581E+02 7.368E+02 0.8
              . 0
                                                                                                            16
                                                      .0
                                                                .0
                                                                         9.738E+02 9.808E+02 1.004E+03 0,
                        . 0
                                            . 0
                                                     .0
                                                                                                            1 E
                                                                . 0
                                                                         1.133E+03 1.140E+03 1.161E+03 0.
                                            . 0
                                                                         1.262E+03 1.268E+03 1.286E+03 0.
                                            ٠,0
                                                                                                            11
                                                                         1.348E+03 1.353E+03 1.367E+03 0.
                                                           TEMPERATURES (T) Z OLANAPIS/R.'S
                                                                                                         NUMBER
                                                                                                           roc'
                                               LOCATIONS 181 THROUGH 2999 EQUAL
                                                     .0 P0-3621.8 P0-36E0.9 P0-3EE.04 B.039E-04 B.159E-04 O.
      5.869E-04 5.960E-04 9.140E-04 6.400E-04 4.904E-04 7.432E-04 5.181E-04 5.362E-04 5.514E-04 5.644E-04
      6.848E-05 6.848E-05 3.424E-05 4.803E-04 7.347E-04 5.158E-04 5.352E-04 5.511E-04 5.644E-04 5.758E-04
                                                                                                            191
      2.421E-03 5.000E-04 5.137E-04 8.500E-06 1.700E-05 3.438E-05 5.176E-05 5.176E-05 6.012E-05
      8.745E-04 6.690E-03 5.698E-03 5.706E-03-2.778E-03-6.520E-03-5.638E-03-1.935E-03 3.983E-05 2.419E-03
      9.595E-03 3.246E-03 3.255E-03 3.267E-03 3.271E-03 3.274E-03 3.277E-03 3.280E-03 8.252E-04
      6.519E-03 6.530E-03 6.539E-03 6.546E-03 6.552E-03 6.556E-03 6.666E-04 7,356E-04 1,146E-02 9.576E-03
      6,546E-03 6,552E-03 6,557E-03 6,811E-04 7,893E-04 1,338E-02 7,751E-03 7,769E-03 6,489E-03 6,505E-03
      1,286E-03 1,499E-03 1,424E-02 3,996E-03 8,490E-03 6,505E-03 6,519E-03 6,530E-03 6,530E-03
                                                                                                            101
      3.261E-03 3,267E-03 3,271E-03 3,276E-03 3,281E-03 8,646E-04 9,815E-04 1,077E-03
                                                                                                            16
      5.696E-03 1.744E-03 2.156E-03 2.574E-03 3.000E-03 1.232E-02 9.569E-03 9.563E-03 3.264E-03
                                                                                                            18
      5,897E-04 4,820E-04 1,018E-03 5,250E-04 8,724E-04 1,078E-03 1,287E-03 1,500E-03 5,676E-03 5,686E-03
      3.538E-03 1,026E-03 1,514E-03 8,013E-04 9,802E-04 1,977E-03 1,980E-03 9,916E-04 5,039E-04 1,089E-03
      9.796E-04 2.902E-03 2.908E-03 3.206E-03 3.508E-03 3.516E-03 3.528E-03 3.528E-03 3.53E-03
      3.507E-03 3.515E-03 3.522E-03.3.527E-03 3.531E-03 3.536E-03 3.538E-03 1.015E-03 1.555E-03 8.680E-04
                                                                                                           l b
      3.532E-03 3.536E-03 3.539E-03 1.041E-03 1.594E-03 9.129E+08 9.762E-04 2.898E-03 2.907E-03 3.206E-03
      9,191E-03 7,897E-03 5,390E-03 2,897E-03 2,905E-03 3,205E-03 3,508E-03 3,516E-03 3,523E-03 3,528E-03
      6.934E-03 1,104E-02 9,196E-03 7,902E-03 6,399E-03 1,977E-03 9,904E-04 6,931E-03 1,103E-02
                                                                              ADMITTANCES (Y)
                                                                                                        NUMBER
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LOC.
NUMBER
                ADMITTANCES (Y)
      9.004E-03 1.448E-02 1.210E-02 1.043E-02 6.522E-03 1.963E-03 1.968E-03 9.860E-04 9.080E-03 1.448E-02
      1.209E-02 1.043E-02 6.521E-03 2.883E-03 2.892E-03 3.192E-03 3.495E-03 3.504E-03 3.512E-03 3.517E-03
 11
      3.522E-03 3.526E-03 3.530E-03 9.449E-04 1.530E-03 9.129E+08 9.737E-04 2.885E-03 2.895E-03 3.194E-03
      3,494E-03 3.503E-03 3.510E-03 3.516E-03 3.521E-03 3.525E-03 3.528E-03 8.147E-04 1.482E-03 8.562E-04
      9.757E-04 2.891E-03 2.897E-03 3.194E-03 3.496E-03 3.505E-03 3.512E-03 3.517E-03 3.522E-03 3.526E-03
      3.529E-03 9.254E-04 1.427E-03 7.711E-04 9.764E-04 1.969E-03 1.973E-03 9.880E-04 4.677E-04 1.044E-03
      5.798E-04 4.386E-04 9.532E-04 4.979E-04 6.433E-04 7.967E-04 9.546E-04 1.117E-03 5.646E-03 5.658E-03
      6.670E-03 1.286E-03 1.593E-03 1.909E-03 2.234E-03 1.225E-02 9.513E-03 9.541E-03 3.231E-03 3.243E-03
      3,251E-03 3,257E-03 3,262E-03 3,265E-03 3,269E-03 3,273E-03 8,118E-04 9,639E-04 6,428E-04 7,959E-04
      9.535E-04 1.116E-03 1.417E-02 3.964E-03 3.979E-03 6.465E-03 6.482E-03 6.497E-03 6.509E-03 6.520E-03
      6.528E-03 6.535E-03 6.540E-03 6.352E-04 7.741E-04 1.332E-02 7.719E-03 7.738E-03 6.465E-03 6.482E-03
      6,497E-03 6.510E-03 6.520E-03 6.528E-03 6.534E-03 6.539E-03 6.166E-04 7.061E-04 1.141E-02 9.539E-03
      9.559E-03 3.234E-03 3.244E-03 3.251E-03 3.257E-03 3.261E-03 3.265E-03 3.268E-03 3.271E-03 7.610E-04
      8.270E-04 5.669E-03 5.677E-03 5.685E-03-2.764E-03-6.487E-03-5.612E-03-1.927E-03 3.967E-05 2.416E-03
      2.418E-03 4.624E-04 4.825E-04 8.600E-06 1.700E-05 4.279E-05 6.857E-05 6.857E-05 6.857E-05
      6.848E-05 6.848E-05 3.424E-05 4.782E-04 7.327E-04 5.152E-04 5.352E-04 5.513E-04 5.649E-04 5.767E-04
      5.872E-04 5.980E-04 9.189E-04 6.491E-04 4.925E-04 7.451E-04 5.188E-04 5.368E-04 5.520E-04 5.650E-04
      5.763E-04 5.860E-04 5.948E-04 9.069E-04 6.188E-04 0.
                                                               0.
                                                                             0.
                               LOCATIONS 181 THROUGH 2999 EQUAL 0.
LOC.
                TEMPERATURES (T) Z channels /R,'L
NUMBER
                                                      o.
o.
      1.780E+03 1.784E+03 1.797E+03 0.
                                                              0. 0.
0. 0.
0. 0.
     1.659E+03 1.665E+03 1.681E+03 0.
     1.463E+03 1.470E+03 1.490E+03 0.
      1.214E+03 1.221E+03 1.244E+03 0.
      9.360E+02 9.354E+02 9.386E+02 8.662E+02 8.353E+02 0.252E+02 0.
      8.816E+02 8.813E+02 8.953E+02 8.343E+02 8.010E+02 7.908E+02 0.
      8.274E+02 8.074E+02 7.950E+02 7.706E+02 7.520E+02 7.529E+02 0.
     7.803E+02 7.332E+02 7.039E+02 7.049E+02 6.972E+02 7.154E+02 0.
81
               6.229E+02 6.328E+02 6.306E+02 6.093E+02 0.
                5,506E+02 5.684E+02 5.868E+02 5.452E+02 0.
91
            4.974E+02 5.146E+02 5.139E+02 4.954E+02 0.
4.650E+02 4.707E+02 4.706E+02 4.667E+02 0.
4.224E+02 4.348E+02 4.354E+02 4.335E+02 0.
101
                                                                             ٥.
111
                                                                             0.
               4,224E+02 4,348E+02 4,354E+02 4,235E+02 0,
121
                                                                             ٥.
               3.937E+02 4.053E+02 4.069E+02 3.971E+02 0.
131
            3.660E+02 3.813E+02 3.847E+02 3.741E+02 0.
141
      2.517E+02 3.306E+02 3.636E+02 3.700E+02 3.496E+02 3.163E+02 0.
151
     2.183E+02 2.076E+02 2.217E+02 2.546E+02 2.755E+02 2.811E+02 0.
     1.896E+02 7.000E+01 7.000E+01 1.810E+02 2.367E+02 2.585E+02 0.
                              LOCATIONS 181 THROUGH 999 EQUAL O.
LOC.
NUMBER
               CAPACITANCES (C)
                              LOCATIONS
                                            1 THROUGH 999 EQUAL
LOC.
NUMBER
               GEN. RATES
```

 αn

LOCATIONS 1 THROUGH 999 EQUAL 0.

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OF POOR OUAL TO
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LOC.
NUMBER
                ADMITTANCES
      1.314E-02 2.102E-02 1.767E-02 1.537E-02 8.753E-03 1.948E-03 1.954E-03 9.798E-04 1.314E-02 2.101E-02
      1.766E-02 1.536E-02 8.754E-03 2.861E-03 2.873E-03 3.173E-03 3.476E-03 3.487E-03 3.496E-03 3.502E-03
      3.507E-03 3.512E-03 3.516E-03 8.014E-04 1.442E-03 9.129E+08 9.668E-04 2.866E-03 2.876E-03 3.175E-03
      3.475E-03 3.485E-03 3.494E-03 3.501E-03 3.506E-03 3.511E-03 3.515E-03 7.645E-04 1.381E-03 8.403E-04
      9.698E-04 2.873E-03 2.880E-03 3.177E-03 3.478E-03 3.487E-03 3.495E-03 3.502E-03 3.507E-03 3.511E-03
      3.515E-03 7.761E-04 1.306E-03 7.297E-04 9.709E-04 1.958E-03 1.962E-03 9.827E-04 4.141E-04 9.791E-04
      5.651E-04 3.744E-04 B.610E-04 4.601E-04 4.143E-04 5.155E-04 6.222E-04 7.350E-04 5.602E-03 5.617E-03
      5.631E-03 8.285E-04 1.031E-03 1.244E-03 1.470E-03 1.216E-02 9.446E-03 9.479E-03 3.212E-03 3.226E-03
      3.235E-03 3.242E-03 3.248E-03 3.252E-03 3.256E-03 3.261E-03 7.345E-04 9.394E-04 4.140E-04 5.150E-04
      6.216E-04 7.346E-04 1.406E-02 3.936E-03 3.954E-03 6.428E-03 6.448E-03 6.465E-03 6.479E-03 6.491E-03
      6.501E-03 6.509E-03 6.515E-03 5.683E-04 7.532E-04 1.324E-02 7.671E-03 7.693E-03 6.429E-03 6.449E-03
      6.466E-03 6.480E-03 6.491E-03 6.500E-03 6.508E-03 6.513E-03 5.437E-04 6.652E-04 1.135E-02 9.485E-03
      9.506E-03 3.217E-03 3.228E-03 3.236E-03 3.242E-03 3.247E-03 3.252E-03 3.255E-03 3.259E-03 6.675E-04
      7.603E-04 5.637E-03 5.645E-03 5.654E-03-2.743E-03-6.437E-03-5.572E-03-1.916E-03 3.945E-05 2.410E-03
131
      2.414E-03 4.078E-04 4.383E-04 8.500E-06 1.700E-05 5.969E-05 1.024E-04 1.024E-04 1.024E-04 8.543E-05
      6.848E-05 6.848E-05 3.424E-05 4.783E-04 7.344E-04 5.176E-04 5.383E-04 5.550E-04 5.690E-04 5.811E-04
      5.921E-04 6.036E-04 9.296E-04 6.646E-04 4.979E-04 7.517E-04 5.20E-04 5.406E-04 5.560E-04 5.692E-04
161
171
      5.807E-04 5.907E-04 5.999E-04 9.165E-04 6.259E-04 0.
                               LOCATIONS 181 THROUGH 2999 EQUAL O.
LOC.
                TEMPERATURES (T) Z = Lannels/R.L
NUMBER
      2.640E+03 2.644E+03 2.654E+03 0.
      2,453E+03 2,458E+03 2,471E+03 0.
 11
                                                       0.
                                                                  0.
      2.114E+03 2.119E+03 2.137E+03 0.
      1.663E+03 1.670E+03 1.691E+03 0.
                                              0.
      1.136E+03 1.134E+03 1.133E+03 1.025E+03 9.812E+02 9.663E+02 0.
      1.070E+03 1.068E+03 1.079E+03 9.928E+02 9.469E+02 9.317E+02 0.
      1.006E+03 9.795E+02 9.598E+02 9.227E+02 8.951E+02 8.919E+02 0.
      9.502E+02 8.919E+02 8.635E+02 8.492E+02 8.357E+02 8.510E+02 0.
 81
                7.619E+02 7.713E+02 7.659E+02 7.400E+02 0.
 91
                6.778E+02 6.972E+02 6.940E+02 6.689E+02 0.
101
                6.165E+02 6.366E+02 6.341E+02 6.129E+02 0.
                5.688E+02 5.852E+02 5.848E+02 5.680E+02 0.
111
121
                5.301E+02 5.439E+02 5.446E+02 5.314E+02 0.
                                                                           0.
131
                4.968E+02 5.098E+02 5.118E+02 5.010E+02 0.
                                                                          0,
141
                4.640E+02 4.817E+02 4.861E+02 4.743E+02 0.
                                                                           ٥.
      3.156E+02 4.208E+02 4.607E+02 4.690E+02 4.455E+02 4.050E+02 0.
      2.696E+02 2.497E+02 2.660E+02 3.098E+02 3.396E+02 3.495E+02 0.
                                                                          0.
      2.317E+02 7.000E+01 7.000E+01 2.121E+02 2.866E+02 3.173E+02 0.
                               LOCATIONS 181 THROUGH 999 EQUAL O.
LOC.
NUMBER
                CAPACITANCES (C)
                               LOCATIONS
LOC.
NUMBER
               GEN. RATES
```

1 THROUGH 999 EQUAL

LOCATIONS

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0
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LOC.
NUMBER
                 ADMITTANCES (Y)
       4,761E-03 6.317E-03 4.734E-03 3.790E-03 2.899E-03 2.008E-03 2.012E-03 1.008E-03 4.758E-03 6.313E-03
       4.730E-03 3.787E-03 2.898E-03 2.948E-03 2.956E-03 3.260E-03 3.567E-03 3.574E-03 3.580E-03 3.584E-03
  11
       3.587E-03 3.589E-03 3.590E-03 1.577E-03 2.000E-03 9.129E+08 1.193E-03 2.950E-03 2.957E-03 3.261E-03
  21
       3.586E-03 3.573E-03 3.570E-03 3.583E-03 3.586E-03 3.588E-03 3.588E-03 1.588E-03 2.018E-03 9.480E-04
  31
       1.194E-03 2.963E-03 2.959E-03 3.261E-03 3.567E-03 3.574E-03 3.580E-03 3.584E-03 3.587E-03 3.589E-03
  41
       3.591E-03 1.590E-03 2.055E-03 1.000E-03 1.195E-03 2.011E-03 2.014E-03 1.008E-03 7.178E-04 1.373E-03
  51
       6.496E-04 7.376E-04 1.422E-03 6.985E-04 1.496E-03 2.109E-03 2.726E-03 3.347E-03 5.777E-03 5.787E-03
       5,796E-03 2,991E-03 4,217E-03 5,451E-03 6,692E-03 1,109E-02 9,728E-03 9,750E-03 3,299E-03 3,309E-03
 7 1
      3,315E-03 3.319E-03 3.323E-03 3.325E-03 3.326E-03 3.327E-03 1.178E-03 1.094E-03 1.494E-03 2.106E-03
 8 1
      2.722E-03 3.343E-03 1.016E-02 4.053E-03 4.065E-03 6.599E-03 6.613E-03 6.625E-03 6.635E-03 6.642E-03
 91
      6.646E-03 6.649E-03 6.650E-03 9.467E-04 8.862E-04 8.795E-03 7.886E-03 7.903E-03 6.599E-03 :6.613E-03
 101
      6.625E-03 6.635E-03 6.642E-03 6.647E-03 6.650E-03 6.651E-03 9.571E-04 9.272E-04 9.724E-03 9.740E-03
111
      9.758E-03 3.301E-03 3.309E-03 3.315E-03 3.320E-03 3.323E-03 3.325E-03 3.327E-03 3.328E-03 1.207E-03
121
      1.175E-03 5.788E-03 5.795E-03 5.803E-03-1.384E-03-2.305E-03-9.224E-04 9.235E-04-9.240E-04 2.442E-03
131
      2.440E-03 7.304E-04 7.099E-04 8.950E-06 1.780E-05 2.805E-05 4.020E-05 4.020E-05 4.020E-05 5.018E-05
141
      6.017E-05 6.017E-05 3.008E-05 4.490E-04 6.937E-04 5.014E-04 5.326E-04 5.586E-04 5.799E-04 5.963E-04
151
      6.075E-04 6.132E-04 9.206E-04 6.065E-04 4.605E-04 7.032E-04 5.041E-04 5.338E-04 5.593E-04 5.805E-04
161
      5.973E-04 6.096E-04 6.181E-04 9.382E-04 6.469E-04 0.
171
                                                                    ٥.
                                                                              ٥.
                                LOCATIONS 181 THROUGH 2999 EQUAL O.
LOC.
NUMBER
                TEMPERATURES (T)
      6.087E+02 6.137E+02 6.335E+02 0.
      5.505E+02 5.596E+02 5.870E+02 0.
 11
                                                         0.
                                                                              0.
 21
      4.834E+02 4.939E+02 6.280E+02 0.
                                                         ο,
 31
      4.131E+02 4.228E+02 4.569E+02 0.
      3.451E+02 3.506E+02 3.680E+02 3.202E+02 3.039E+02 2.937E+02 0.
 41
      3.029E+02 3.040E+02 3.203E+02 2.810E+02 2.663E+02 2.606E+02 0.
                                                                                        6.259E+03-1.820E+02
                                                                                        0.
      2.603E+02 2.462E+02 2.410E+02 2.280E+02 2.204E+02 2.265E+02 0.
 81
 71
      2.228E+02 1.871E+02 1.676E+02 1.730E+02 1.713E+02 1.921E+02 0.
 8 1
                9.867E+01 1.101E+02 1.107E+02 9.329E+01 0.
                                                                   0.
 91
      0.
                4.084E+01 5.858E+01 5.836E+01 3.857E+01 0.
                                                                   0.
101
      ٥.
               -8.700E-01 1.693E+01 1.661E+01-1.879E+00 0.
                                                                   0.
111
               -3.104E+01-1.489E+01-1.528E+01-3.186E+01 0.
      ٥.
                                                                   0.
                                                                              0.
121
               -5.224E+01-3.777E+01-3.839E+01-5.349E+01 0.
                                                                   0.
                                                                              0.
131
               -6.578E+01-5.248E+01-5.387E+01-6.830E+01 0.
      O.
                                                                   ٥.
141
               -7.245E+01-5.935E+01-8.170E+01-7.804E+01 0.
                                                                   0.
     -8.458E+01-7.308E+01-6.789E+01-6.219E+01-8.611E+01-1.084E+02 0.
     -3.292E+01-1.600E+01-1.524E+01-3.283E+01-5.173E+01-8.550E+01 0.
     -1.120E+01 7.000E+01 7.000E+01 1.097E+00-3.275E+01-4.930E+01 0.
                               LOCATIONS 181 THROUGH 999 EQUAL
LOC.
NUMBER
                CAPACITANCES (C)
                               LOCATIONS
LOC.
NUMBER
                GEN. RATES
                             (Q)
```

HOUGHHT I

(0)

LOCATIONS

GEN, BATES

CAPACITANCES (C)

9,302E+02 8,361E+02 8,630E+02 0; TEMPERATURES (T)

ADMITTANCES (Y)

NUMBER roc.

иливев LOC.

HUMBER roc'

NUMBER roc.

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LOCATIONS 181 THROUGH 999 EQUAL 0;
                                                 -6.618E+00 7.000E+01 7.000E+01 7.380E+00-2.420E+01-4.027E+01 0.
                                      'n
                                                -2.697E+01-8.056E+00-6.775E+00-2.287E+01-4.157E+01-5,610E+01 0.
                                      , U
                                                -5.788E+01-6.104E+01-4.208E+01-4.609E+01-7.326E+01-9.972E+01 0.
                                                                                                                     191
                                      . 0
                                                           -6.688E+01-4.168E+01-4.391E+01-6.217E+01 0.
                                                                                                                     111
                                      ٠,
                                                           -4.694E+01-3.188E+01-3.307E+01-4.943E+01 0.
                                                                                                                     121
'Ω
                                                           -2.968E+01-1.329E+01-1.404E+01-3.105E+01 0.
                                                                                                                     121
                                                . 0
                                                           -3.572E+00 1,451E+01 1,381E+01-6,024E+00 0,
                                                                                                                     111
                                                'n
                                                           3,277E+01 5,248E+01 6,148E+01 3,033E+01 0,
                                                                                                                     101
                          . 0
                                                0'
                                     ' n
                                                           B,243E+01 1,017E+02 1,001E+02 7,715E+01 0,
                                                                                                                     16
                          10.
                                     '0
                                                           1'218E+01 1'824E+01 1'803E+01 1'383E+01 0'
                           .0
                                      'n
                                                3.066E+02 2.586E+02 2.300E+02 2.310E+02 2.256E+02 2.456E+02 0.
                0 '
                           . 0
                                      .0
                                                3.506E+02 3.290E+02 3.159E+02 2.927E+02 2.791E+02 2.816E+02 0.
                                                                                                                     19
                .0
                           ٠,
                                      ' 0
                                                4.022E+02 3.992E+02 4.094E+02 3.610E+02 3.280E+02 3.185E+02 0.
                                                                                                                     19
        259E+03-1,790E+02
                                     .0
                                                4.549E+O2 4.674E+O2 4.666E+O2 3,813E+O2 3,659E+O2 3,521E+O2 0,
                                                                                                                     11
                . 0
                           . 0
                                                          .0
                                                .0
                                                                     ٠0
                                                                                6.874E+02 5.970E+02 6.311E+02 0.
                                                                                                                     16
                , U
                           . U
                                                                     • 0
                                                                                7,202E+02 7,306E+02 7,629E+02 0,
                                                                                                                     12
                                                          0
                . 0
                           '0
                                                .0
                                                                     ٠٥
                                                                                8,309E+02 8,482E+02 8,729E+02 0,
                                                                                                                     11
                           . 0
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LOCATIONS 181 THROUGH 2999 EQUAL

.0

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.0
                                                2'833E-04 2'812E-04 8'080E-04 8'583E-04 8'451E-04 0'
5.955E-04 6.036E-04 9.106E-04 6.044E-04 4.436E-04 6.759E-04 4.853E-04 5.154E-04 5.419E-04 5.647E-04
                                                                                                      191
6.017E-05 6.017E-05 3.008E-05 4.237E-04 6.506E-04 4.797E-04 5.126E-04 5.404E-04 5.637E-04 5.822E-04
                                                                                                       191
2.439E-03 7.241E-04 7.035E-04 8.950E-06 1.790E-05 3.731E-05 5.672E-05 5.672E-05 5.672E-05 5.045E-05
                                                                                                      161
1.164E-03 6.775E-03 6.783E-03 5.791E-03-1,378E-03-2,296E-03-9,194E-04 9,212E-04-9,219E-04
                                                                                                      131
9.737E-03 3.294E-03 3.304E-03 3.311E-03 3.316E-03 3.320E-03 3.329E-03 3.326E-03 3.326E-03 3.326E-03 1.193E-03
                                                                                                       151
6.616E-03 6.627E-03 6.635E-03 6.641E-03 6.645E-03 6.646E-04 9.195E-04 9.701E-03 9.717E-03
                                                                                                       111
6.641E-03 6.644E-03 6.646E-03 9.353E-04 8.822E-04 6.771E-03 7.865E-03 7.884E-03 6.585E-03 6.502E-03
                                                                                                       101
1.800E-03 2.217E-03 1.013E-02 4.040E-03 4.054E-03 8.585E-03 8.601E-03 6.615E-03 8.626E-03 6.635E-03
                                                                                                       16
3.310E-03 3.316E-03 3.320E-03 3.322E-03 3.324E-03 3.325E-03 1.166E-03 1.090E-03 9.042E-04 1.390E-03
                                                                                                       18
5,778E-03 1,970E-03 2,782E-03 3,605E-03 4,437E-03 1,105E-02 9,695E-03 9,721E-03 3,291E-03 3,303E-03
                                                                                                      1 4
6.480E-04 7.301E-04 1.408E-03 6.924E-04 9.853E-04 1.392E-03 1.803E-03 2.219E-03 5.754E-03 6.766E-03
                                                                                                      19
3.508E-03 1.568E-03 2.034E-03 9.929E-04 1.192E-03 2.006E-03 2.010E-03 1.006E-03 7.113E-04 1.364E-03
                                                                                                      15
1.191E-03 2.845E-03 2.951E-03 3.254E-03 3.560E-03 3.569E-03 3.575E-03 3.580E-03 3.584E-03 3.587E-03
                                                                                                      16
3.559E-03 3.567E-03 3.574E-03 3.579E-03 3.583E-03 3.586E-03 3.567E-03 1.544E-03 1.999E-03 9.448E-04
                                                                                                      1 €
3'204E-03 3'200E-03 3'200E-03 1'222E-03 1'004E-03 8'150E+08 1'100E-03 5'041E-03 5'040E-03 3'524E-03
                                                                                                      12
7.029E-03 5.641E-03 3.673E-03 2.938E-03 2.947E-03 3.262E-03 3.558E-03 3.568E-03 3.580E-03
                                                                                                      11
7.051E-03 9.369E-03 7.035E-63 5.646E-03 3.674E-03 2.000E-03 2.005E-03 1.005E-03 7.048E-03 9.363E-03
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LOC.
NUMBER
                ADMITTANCES (Y)
      9.266E-03 1.233E-02 9.283E-03 7.473E-03 4.444E-03 1.993E-03 1.998E-03 1.002E-03 9.262E-03 1.232E-02
      9.275E-03 7.467E-03 4.443E-03 2.928E-03 2.939E-03 3.244E-03 3.552E-03 3.563E-03 3.571E-03 3.576E-03
 11
      3.581E-03 3.584E-03 3.586E-03 1.535E-03 1.968E-03 9.129E+08 1.185E-03 2.932E-03 2.942E-03 3.246E-03
      3.552E-03 3.562E-03 3.569E-03 3.575E-03 3.580E-03 3.583E-03 3.585E-03 1.520E-03 1.980E-03 9.417E-04
      1.180E-03 2.938E-03 2.945E-03 3.247E-03 3.554E-03 3.564E-03 3.571E-03 3.577E-03 3.581E-03 3.584E-03
 41
      3.586E-03 1.546E-03 2.014E-03 9.855E-04 1.189E-03 2.002E-03 2.005E-03 1.004E-03 7.049E-04 1.356E-03
      6.464E-04 7.228E-04 1.394E-03 6.864E-04 7.289E-04 1.032E-03 1.340E-03 1.655E-03 5.732E-03 5.745E-03
      5,750E-03 1.457E-03 2.063E-03 2.600E-03 3.309E-03 1.101E-02 9.663E-03 9,693E-03 3.284E-03 3.297E-03
 71
      3.305E-03 3.312E-03 3.316E-03 3.320E-03 3.322E-03 3.323E-03 1.156E-03 1.086E-03 7.281E-04 1.030E-03
      1.338E-03 1.653E-03 1.009E-02 4.027E-03 4.044E-03 6.571E-03 6.590E-03 6.606E-03 6.618E-03 6.628E-03
      6.635E-03 6.639E-03 6.641E-03 9.240E-04 0.783E-04 8.748E-03 7.846E-03 7.868E-03 6.572E-03 8.590E-03
101
      6.606E-03 6.619E-03 6.628E-03 6.635E-03 6.640E-03 6.642E-03 9.327E-04 9.119E-04 9.679E-03 9.696E-03
111
      9.716E-03 3.288E-03 3.298E-03 3.306E-03 3.312E-03 3.317E-03 3.320E-03 3.322E-03 3.324E-03 1.180E-03
121
      1.154E-03 5.762E-03 5.770E-03 5.779E-03-1.373E-03-2.288E-03-9.165E-04 9.189E-04-9.188E-04-2.441E-03
131
      2.439E-03 7.180E-04 6.972E-04 8.950E-06 1.790E-05 4.590E-05 7.390E-05 7.390E-05 7.390E-05 6.703E-05
      6.017E-05 6.017E-05 3.008E-05 4.037E-04.6.303E-04 4.616E-04 4.956E-04 5.247E-04 5.495E-04 5.696E-04
      5.847E-04 5.940E-04 9.012E-04 6.025E-04 4.291E-04 6.529E-04 4.692E-04 4.995E-04 5.268E-04 5.507E-04
      5.708E-04 5.866E-04 5.987E-04 9.153E-04 8.376E-04 0.
                                LOCATIONS 181 THROUGH 2999 EQUAL
LOC.
NUMBER
                TEMPERATURES (T)
      1,292E+03 1,207E+03 1,313E+03 0.
 11
      1.185E+03 1.173E+03 1.195E+03 0.
                                               0.
                                                                                                  0.
      9.829E+02 9.930E+02 1.024E+03 0.
 21
                                               0.
                                                                                                  O
      7.729E+02 7.829E+02 8.171E+02 0.
 41
      5.57NE+02 5.570E+02 5.610E+02 4.595E+02 4.265E+02 4.083E+02 0.
 5 i
      4.957E+02 4.891E+02 4.845E+02 4.100E+02 3.872E+02 3.742E+02 0.
                                                                                                  ٥.
      4.360E+02 4.076E+02 3.873E+02 3.548E+02 3.355E+02 3.356E+02 0.
                                                                             0.
      3.862E+02 3.260E+02 2.896E+02 2.867E+02 2.780E+02 2.971E+02 0.
 71
 81
                2.031E+02 2.126E+02 2.001E+02 1.837E+02 0.
                                                                   u,
                                                                             ٥.
 91
                1.228E+02 1.434E+02 1.404E+02 1.146E+02 0.
                                                                   0.
101
                6.542E+01 8.692E+01 8.528E+01 6.165E+01 0.
111
                2.320E+01 4.309E+01 4.209E+01 2.117E+01 0.
      0.
               -7.409E+00 1.058E+01 9.724E+00-9.094E+00 0.
121
      ٥.
                                                                             0.
131
               -2.846E+01-1.173E+01-1.291E+01-3.093E+01 D.
                                                                             ٥,
141
               -4.158E+01-2.435E+01-2.645E+01-4.657E+01 0.
                                                                             0.
151
     -5.132E+01-4.923E+01-2.654E+01-3.026E+01-6.060E+01-9.123E+01 0.
                                                                             0.
     -2.115E+01-1.180E+00 1.510E+00-1.310E+01-3.159E+01-4.679E+01 0.
     -2.052E+00 7.000E+01 7.000E+01 1.352E+01-1.581E+01-3.142E+01 0.
                               LOCATIONS 181 THROUGH 999 EQUAL
LOC.
NUMBER
                CAPACITANCES (C)
                               LOCATIONS
                                            1 THROUGH
                                                       999 EQUAL
LOC.
NUMBER
                GEN. RATES
```

N

LOCATIONS

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LOC.
NUMBER
                ADMITTANCES (Y)
      1.346E-02 1.798E-02 1.362E-02 1.104E-02 5.972E-03 1.981E-03 1.988E-03 9.988E-04 1.346E-02 1.797E-02
      1.360E-02 1.103E-02 5.973E-03 2.911E-03 2.924E-03 3.230E-03 3.541E-03 3.553E-03 3.563E-03 3.570E-03
      3.575E-03 3.579E-03 3.582E-03 1.499E-03 1.942E-03 9.129E+08 1.178E-03 2.917E-03 2.929E-03 3.234E-03
 21
      3.541E-03 3.552E-03 3.561E-03 3.568E-03 3.574E-03 3.578E-03 3.580E-03 1.479E-03 1.949E-03 9.364E-04
 31
      1.183E-03 2.926E-03 2.933E-03 3.235E-03 3.543E-03 3.554E-03 3.563E-03 3.570E-03 3.576E-03 3.579E-03
 41
      3.502E-03 1.509E-03 1.900E-03 9.730E-04 1.105E-03 1.994E-03 1.990E-03 1.001E-03 6.942E-04 1.341E-03
 51
      6.437E-04 7.104E-04 1.372E-03 6.763E-04 4.715E-04 6.705E-04 8.770E-04 1.091E-03 5.695E-03 5.712E-03
      5.727E-03 9.428E-04 1.341E-03 1.753E-03 2.182E-03 1.094E-02 9.609E-03 9.646E-03 3.271E-03 3.287E-03
 71
      3.297E-03 3.305E-03 3.311E-03 3.315E-03 3.318E-03 3.320E-03 1.137E-03 1.079E-03 4.711E-04 6.696E-04
      8.756E-04 1.091E-03 1.003E-02 4.006E-03 4.026E-03 6.547E-03 6.570E-03 6.589E-03 6.805E-03 6.817E-03
 91
101
      6.625E-03 6.631E-03 6.634E-03 9.047E-04 8.716E-04 8.709E-03 7.812E-03 7.835E-03 6.549E-03 6.571E-03
      6.590E-03 6.605E-03 6.617E-03 6.626E-03 6.632E-03 8.635E-03 9.119E-04 8.992E-04 9.640E-03 9.658E-03
111
      9.681E-03 3.277E-03 3.289E-03 3.299E-03 3.306E-03 3.311E-03 3.316E-03 3.319E-03 3.321E-03.1.157E-03
121
131
      1.136E-03 5.741E-03 5.749E-03 5.759E-03-1.364E-03-2.274E-03-9.116E-04 9.150E-04-9.163E-04 2.440E-03
      2.438E-03 7.078E-04 6.865E-04 8.950E-06 1.790E-05 6.342E-05 1.089E-04 1.089E-04 1.089E-04 8.456E-05
141
      6.017E-05 6.017E-05 3.008E-05 3.750E-04 5.888E-04 4.345E-04 4.694E-04 4.999E-04 5.266E-04 5.489E-04
151
      5.866E-04 5.796E-04 8.845E-04 5.984E-04 4.068E-04 6.175E-04 4.445E-04 4.747E-04 5.028E-04 5.282E-04
161
      5.502E-04 5.682E-04 5.828E-04 8.959E-04 6.293E-04 0.
                               LOCATIONS 181 THROUGH 2999 EQUAL O.
LOC.
NUMBER
                TEMPERATURES (T)
      2,068E+03 2,071E+03 2,083E+03 0.
      1,063E+03 1,869E+03 1,889E+03 0.
                                                                             0.
 21
      1.540E+03 1.550E+03 1.578E+03 0.
                                                        ٥.
                                                                             0.
                                                                                                  ٥.
     .1,149E+03 1,159E+03 1,193E+03 0,
                                                                             0.
      7.297E+02 7.266E+02 7.226E+02 5.761E+02 5.277E+02 5.048E+02 0.
      6.526E+02 6.406E+02 6.397E+02 5.327E+02 4.888E+02 4.699E+02 0.
                                                                                                  0.
 61
      5.798E+02 5.407E+02 5.092E+02 4.609E+02 4.322E+02 4.206E+02 0.
                                                                                                  0.
      5.208E+02 4.426E+02 3.915E+02 3.820E+02 3.679E+02 3.860E+02 0
 71
                2.907E+02 2.985E+02 2.900E+02 2.601E+02 0.
 B 1
                                                                   đ.
 91
      0.
                1.922E+02 2.147E+02 2.097E+02 1.790E+02 Q.
101
      0.
                1.217E+02 1.461E+02 1.434E+02 1.157E+02 0.
111
                6.933E+01 9.224E+01 9.076E+01 6.633E+01 0.
121
                3.077E+01 5.165E+01 5.061E+01 2.873E+01 0.
131
                3.313E+00 2.293E+01 2.176E+01 8.994E-01 0.
                                                                                       0.
               -1.534E+01 5.449E+00 3.571E+00-1.981E+01 0.
141
     -4.046E+01-2.908E+01 2.149E-01-3.003E+00-3.900E+01-7.715E+01 0.
                                                                                       ٥.
     -1.144E+01 1.044E+01 1.558E+01 3.505E+00-1,465E+01~3.109E+01 0.
      5.576E+00 7.000E+01 7.000E+01 2.390E+01-1.623E+00-1.647E+01 0.
                               LOCATIONS 181 THROUGH 999 EQUAL
LOC.
NUMBER
                CAPACITANCES (C)
                                                                                            RBW >LW
                               LOCATIONS
LOC.
NUMBER
                GEN, RATES
```

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14
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LOC.
NUMBER
                 ADMITTANCES (Y)
       4.712E-03 6.252E-03 4.684E-03 3.749E-03 2.867E-03 1.985E-03 1.989E-03 9.961E-04 4.710E-03 6.248E-03
      4.680E-03 3.746E-03 2.866E-03 2.916E-03 2.923E-03 3.223E-03 3.525E-03 3.532E-03 3.537E-03 3.542E-03
      3.545E-03 3.548E-03 3.550E-03 1.169E-03 1.676E-03 9.129E+00 1.180E-03 2.917E-03 2.924E-03 3.224E-03
      3.524E-03 3.531E-03 3.536E-03 8.541E-03 3.544E-03 3.547E-03 3.549E-03 1.140E-03 1.650E-03 8.835E-04
      1.181E-03 2.920E-03 2.925E-03 3.223E-03 3.525E-03 3.532E-03 3.537E-03 3.542E-03 3.545E-03 3.548E-03
      3.550E-03 1.150E-03 1.625E-03 8.406E-04 1.181E-03 1.988E-03 1.991E-03 9.969E-04 5.484E-04 1.146E-03
      6.019E-04 5.351E-04 1.100E-03 5.597E-04 1.480E-03 2.007E-03 2.697E-03 3.311E-03 5.714E-03 5.722E-03
      5.731E-03 2.960E-03 4.173E-03 5.393E-03 6.619E-03 1.097E-02 9.619E-03 9.640E-03 3.261E-03 3.269E-03
      3.275E-03 3.280E-03 3.283E-03 3.286E-03 3.289E-03 3.291E-03 9.304E-04 1.004E-03 1.479E-03 2.084E-03
      2.693E-03 3.307E-03 1.005E-02 4.007E-03 4.018E-03 6.523E-03 6.536E-03 6.547E-03 6.556E-03 6.564E-03
      6.570E-03 6.574E-03 6.578E-03 7.389E-04 8.090E-04 8.697E-03 7.797E-03 7.812E-03 6.522E-03 6.536E-03
      6.547E-03 6.556E-03 6.564E-03 6.570E-03 6.574E-03 6.577E-03 7.298E-04 7.742E-04 9.816E-03 9.630E-03
      9.647E-03 3.262E-03 3.270E-03 3.275E-03 3.280E-03 3.283E-03 3.286E-03 3.288E-03 3.290E-03 9.054E-04
      9.355E-04 5.723E-03 5.730E-03 5.737E-03-1.368E-03-2.280E-03-9.122E-04 9.133E-04-9.137E-04 2.424E-03
      2.425E-03 5.465E-04 5.533E-04 8.500E-06 1.700E-05 2.759E-05 3.817E-05 3.817E-05 3.817E-05 4.766E-05
      5.714E-05 5.714E-05 2.857E-05 4.899E-04 7.482E-04 5.238E-04 5.423E-04 5.573E-04 5.698E-04 5.803E-04
151
      5.894E-04 5.981E-04 9.137E-04 6.317E-04 4.975E-04 7.544E-04 5.253E-04 5.429E-04 5.575E-04 5.697E-04
161
      5.800E-04 5.886E-04 5.962E-04 9.064E-04 6.160E-04 0.
                                LOCATIONS 181 THROUGH 2999 EQUAL D.
LOC.
NUMBER
                TEMPERATURES (T)
      8.671E+02 8.735E+02 8.916E+02 0.
                                                          0.
                                                                    ٥.
      8.157E+02 8.240E+02 8.491E+02 0.
                                                          Ο.
                                                                     0.
      7.542E+02 7.630E+02 7.950E+02 0.
                                                0.
                                                                                                    0.
      6.898E+02 6.986E+02 7.299E+02 0.
                                                0.
                                                                    0.
      6.274E+02 6.326E+02 6.486E+02 6.050E+02 5.901E+02 5.807E+02 0.
                                                                                         6.259E+03 1.720E+02
      5.887E+02 5.900E+02 6.050E+02 5.691E+02 5.558E+02 5.504E+02 0.
                                                                               0.
      5.495E+02 5.371E+02 6.324E+02 b.200E+02 5.103E+02 4.876E+02 0. 5.147E+02 4.832E+02 4.653E+02 4.704E+02 4.691E+02 4.876E+02 0. 5.147E+02 4.832E+02 4.33E+02 3.885E+02 0.
      5.495E+02 5.371E+02 6.324E+02 5.206E+02 5.139E+02 5.182E+02 0.
                                                                               0.
 71
                                                                               0. .
                                                                               ٥.
 91
                3,501E+02 3.647E+02 3.848E+02 3.485E+02 0.
                                                                    0.
101
                3.110E+02 3.24BE+02 3.247E+02 3.105E+02 0.
                                                                    ٥.
111
                2.806E+02 2.924E+02 2.925E+02 2.807E+02 0.
                                                                    ٥.
121
                2.564E+02 2.684E+02 2.668E+02 2.571E+02 0.
                                                                    0.
131
                2.364E+02 2.456E+02 2.464E+02 2.381E+02 0.
      ٥.
141
                 2.181E+02 2.293E+02 2.310E+02 2.221E+02 0.
151
      1.539E+02 1.960E+02 2.181E+02 2.213E+02 2.055E+02 1.828E+02 0.
161
      1.397E+02 1.389E+02 1.480E+02 1.641E+02 1.723E+02 1.726E+02 0.
      1.258E+02 7.000E+01 7.000E+01 1.274E+02 1.640E+02 1.633E+02 0.
                                LOCATIONS 181 THROUGH 999 EQUAL O.
LOC.
NUMBER
                CAPACITANCES (C)
                                LOCATIONS
LOC.
NUMBER
                GEN. RATES
```

LOCATIONS

t THROUGH 999 EQUAL O. CARRELL AND THERE

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LOC.
NUMBER
                ADMITTANCES (Y)
      6.970E-03 9.259E-03 6.950E-03 5.575E-03 3.626E-03 1.974E-03 1.978E-03 9.910E-04 6.967E-03 9.253E-03
      8.944E-03 5.571E-03 3.626E-03 2.899E-03 2.908E-03 3.208E-03 3.510E-03 3.518E-03 3.524E-03 3.529E-03
      3.533E-03 3.537E-03 3.540E-03 1.047E-03 1.597E-03 9.129E+00 1.173E-03 2.902E-03 2.910E-03 3.209E-03
      3.509E-03 3.517E-03 3.523E-03 3.528E-03 3.532E-03 3.536E-03 3.538E-03 1.023E-03 1.560E-03 8.687E-04
      1.175E-03 2.906E-03 2.912E-03 3.209E-03 3.511E-03 3.510E-03 3.524E-03 3.529E-03 3.535E-03 3.536E-03
      3.539E-03 1.032E-03 1.519E-03 8.030E-04 1.176E-03 1.979E-03 1.982E-03 9.926E-04 5.055E-04 1.091E-03
      5.901E-04 4.838E-04 1.021E-03 5.264E-04 9.738E-04 1.375E-03 1.781E-03 2.191E-03 5.679E-03 5.690E-03
      5.700E-03 1.947E-03 2.749E-03 3.560E-03 4.380E-03 1.090E-02 9.566E-03 9.590E-03 3.246E-03 3.256E-03
      3.263E-03 3.260E-03 3.272E-03 3.275E-03 3.278E-03 3.282E-03 8.875E-04 9.824E-04 9.728E-04 1.373E-03
      1.778E-03 2.188E-03 9.994E-03 3.908E-03 3.999E-03 6.494E-03 6.509E-03 6.522E-03 6.532E-03 6.541E-03
 91
      6.548E-03 6.554E-03 6.558E-03 6.844E-04 7.903E-04 8.655E-03 7.760E-03 7.777E-03 6.494E-03 6.509E-03
      6.522E-03 6.532E-03 6.541E-03 6.540E-03 6.553E-03 6.557E-03 6.702E-04 7.375E-04 9.572E-03 9.587E-03
      9.604E-03 3.249E-03 3.257E-03 3.263E-03 3.268E-03 3.272E-03 3.275E-03 3.278E-03 3.280E-03 8.288E-04
      8.772E-04 5.698E-03 5.705E-03 5.712E-03-1.360E-03-2.266E-03-9.073E-04 9.089E-04-9.096E-04 2.419E-03
      2.422E-03 5.014E-04 5.152E-04 8.500E-06 1.700E-05 3.544E-05 5.387E-05 5.387E-05 5.387E-05 5.551E-05
      5.714E-05 5.714E-05 2.857E-05 4.839E-04 7.412E-04 5.200E-04 5.392E-04 5.546E-04 5.674E-04 5.784E-04
      5.882E-04 5.000E-04 9.164E-04 6.407E-04 4.972E-04 7.524E-04 5.232E-04 5.406E-04 5.551E-04 5.675E-04
161
      5.781E-04 5.871E-04 5.953E-04 9.063E-04 6.168E-04 0.
                               LOCATIONS 181 THROUGH 2999 EQUAL
LOC.
               TEMPERATURES (T)
NUMBER
      1.219E+03 1.224E+03 1.240E+03 0.
      1.137E+03 1.144E+03 1.167E+03 0.
 11
                                                                  ٥.
      1.028E+03 1.037E+03 1.067E+03 0.
                                              0.
   . 9.073E+02 9.161E+02 9.471E+02 0.
                                              ٥.
      7.866E+02 7.893E+02 7.979E+02 7.298E+02 7.068E+02 6.941E+02 0.
 41
      7.384E+02 7.363E+02 7.460E+02 6.933E+02 6.724E+02 6.635E+02 0.
      6.910E+02 6.727E+02 6.613E+02 6.406E+02 6.282E+02 6.299E+02 0.
      6.500E+02 6.088E+02 5.836E+02 5.848E+02 5.799E+02 5.969E+02 0.
 71
 81
               5.141E+02 5.227E+02 5.211E+02 5.032E+02 0.
91
                4.521E+02 4.676E+02 4.663E+02 4.478E+02 0.
                                                                  0.
                                                                ο.
                4.065E+02 4.215E+02 4.200E+02 4.050E+02 0,
                3.712E+02 3.840E+02 3.839E+02 3.709E+02 0.
                                                                  0.
121
               3.427E+02 3.535E+02 3.539E+02 3.435E+02 0.
                                                                  0.
131
                3.186E+02 3.286E+02 3.298E+02 3.211E+02 0.
                                                                  0.
141
                2,058E+02 3.084E+02 3,111E+02 3.018E+02 U.
      2.085E+02 2.668E+02 2.938E+02 2.988E+02 2.815E+02 2.543E+02 0.
151
      1.819E+02 1.759E+02 1.876E+02 2.126E+02 2.275E+02 2.308E+02 0.
161
      1.800E+02 7.000E+01 7.000E+01 1.565E+02 1.986E+02 2.145E+02 0.
171
                               LOCATIONS 181 THROUGH 999 EQUAL
LOC.
NUMBER
               CAPACITANCES (C)
                                          1 THROUGH 999 EQUAL
LOC.
NUMBER
                GEN. RATES
```

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LOC.
                ADMITTANCES
NUMBER
      9,154E-03 1,218E-02 9,182E-03 7,370E-03 4,379E-03 1,984E-03 1,989E-03 9,888E-04
      9.155E-03 7.364E-03 4.379E-03 2.865E-03 2.895E-03 3.194E-03 3.497E-03 3.506E-03 3.513E-03 3.518E-03
      3,523E-03 3,527E-03 3,530E-03 9,507E-04 1,534E-03 9,129E+08 1,168E-03 2,889E-03 2,887E-03 3,196E-03 3,496E-03 3,505E-03 3,512E-03 3,518E-03 3,522E-03 3,526E-03 3,529E-03 9,217E-04 1,488E-03 8,568E-04
 21
 31
      1,170E-03 2,894E-03 2,900E-03 3,197E-03 3,498E-03 3,506E-03 3,513E-03 3,519E-03 3,523E-03 3,527E-03
 41
      3.530E-03 9.315E-04 1.432E-03 7.726E-04 1.171E-03 1.972E-03 1.975E-03 9.889E-04 4.691E-04 1.046E-03
      5.801E-04 4.403E-04 9.561E-04 4.992E-04 7.199E-04 1.019E-03 1.322E-03 1.631E-03 5.649E-03 5.661E-03
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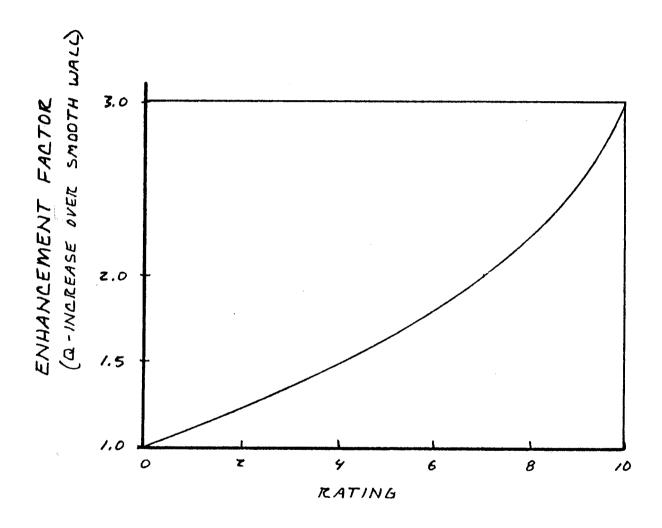
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1 THROUGH 999 EQUAL

RIB EVALUATION CRITERIA RATING SCALES



HEAT TRANSFER RATING

BOUNDARY LAYER RATING: Based on Estimated Boundary Layer Growth Over Ribbed Combustor Wall Length

RATING	DESCRIPTION
10	Optimum boundry layer growth on rib contour. No Q losses.
8	Well defined boundry layer to end of panel. Some Q losses.
6	Boundry layer blends to fill contour by end of panel.
4	Boundry layer blends to fill contour prior to end of panel. Significant Q Loss.
2	Contour filled prior to 50% length.
0	Contour fills quickly - negligible Q enhancement from ribbed wall contour.

Boundry Layer Rating

PRODUCIBILITY RISK RATING: Based on Scale, Aspect Ratio and Contour Complexity

RATING	EXAMPLE	DESCRIPTION
10		Simple in shape; moderate feature size (Approx040)
8		Basic Shape; higher aspect ratio (i.e. deeper cut)
6		Very high aspect ratio or contour complexity
5		Smaller feature sizes and/or complex contours
4-1		Combinations of small scale, high aspect ratio and complex contours
0		Size and complexity requirements make fabrication prohibitively difficult and expensive

PRODUCIBILITY RATING

STRUCTURAL/LIFE CONSIDERATIONS: Based Primarily on Material Property Degradation With Temperature (NARloy -Z)

RATING	DESCRIPTION
10	No life limit in application
9	Life well exceeds design requirements
8	Life meets design requirements
6	Occasional material roughening at rib tips (1400°F)
4	Material roughening on ribs over large areas
. 2	Material may survive in optimal conditions
0	Material will not survive in application

Structural/Life Rating

1774/d

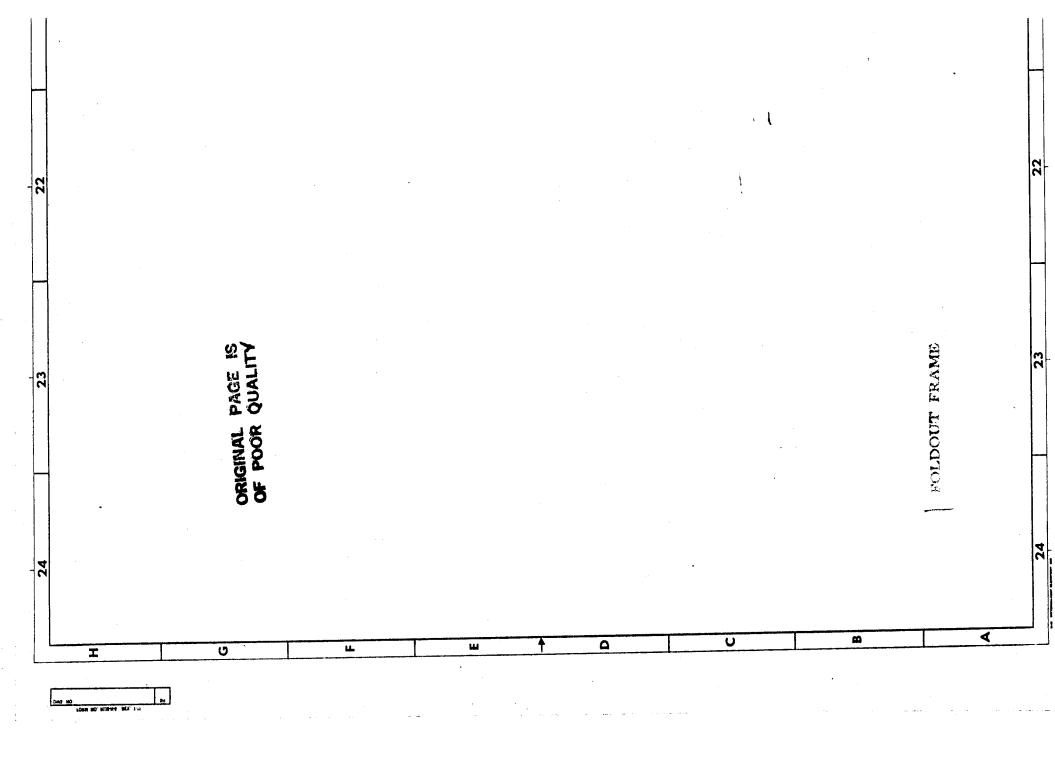
APPENDIX B HOT AIR TESTS

HOT AIR TEST FIXTURE DRAWINGS

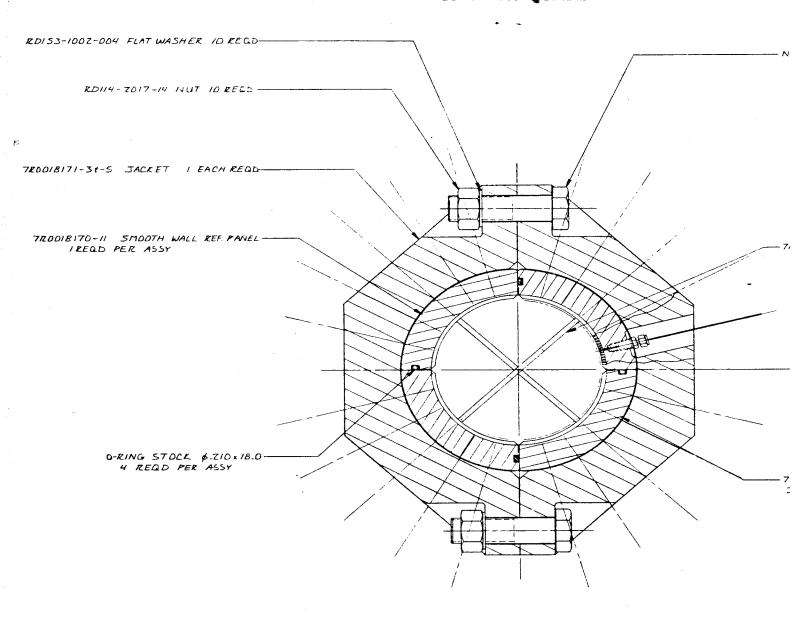
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HOT AIR TEST ASSEMBLY	7R0018169
TEST PANELS	780018170
JACKET	7R0018171
ENTRANCE SECTION	7R0018172
EXIT SECTION	7R0018168
REPLACEABLE NOZZLE	7R0018 1 83
RETAINER RING	7R0018 1 84
SUPPORT BAR (INSTRUMENTATION)	7R0018 1 85
TURBULATOR	7R0018 1 91

TEST PLAN
TEST DATA

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SECTION A-A 46

Z FOLDOUT FRAME

21 † 20 19 18

16 15 14 13

TEST FAC

NAS 1081-3-

18485-3,-5 T/C SUPPORT BARS (REF)

TROOIB483-5 REPLACABLE .

DIBITO - XX TEST PANELS (1) EQD PER ASSY (-XX TBD)

> NAS 1351-4-10 CA MS35338-139 LOCK W

72.0018485-34-5 T/C SUPPORT

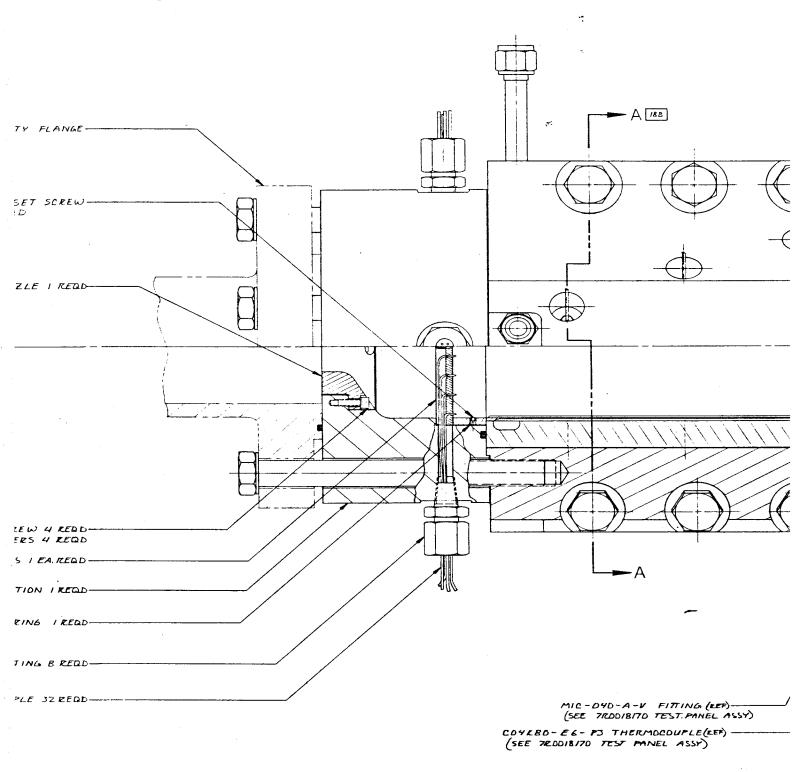
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TROOIB484-3 RETAIN

MHC-040-A4-V

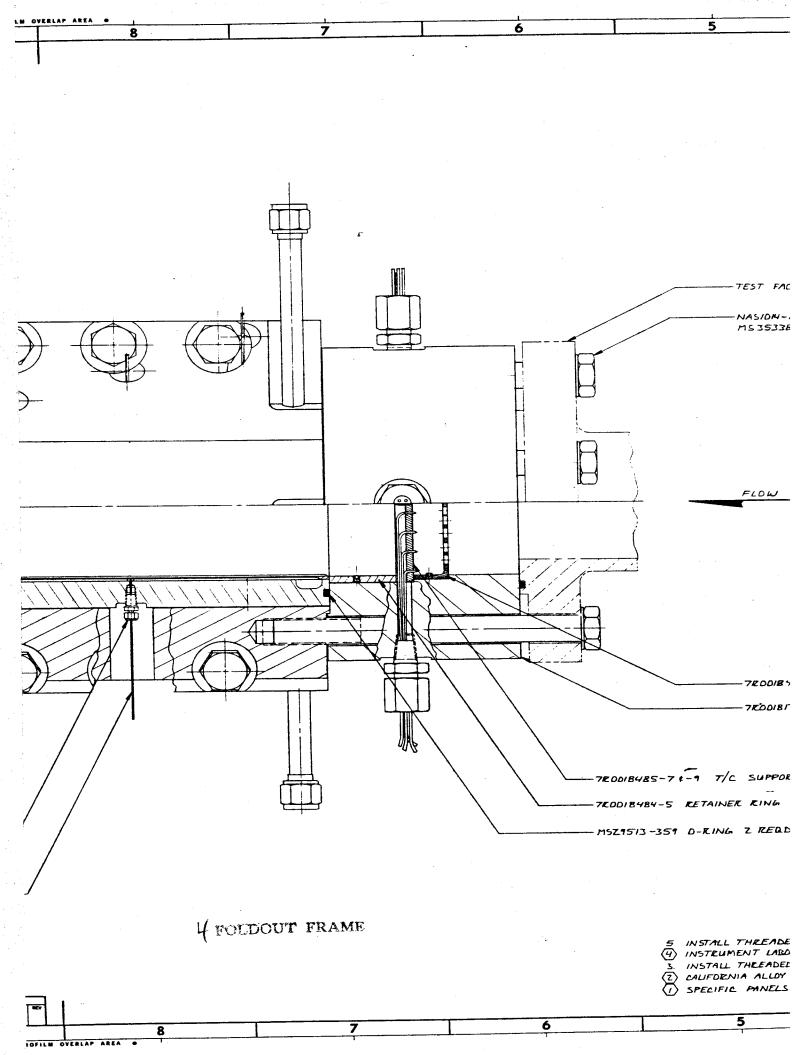
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3 FOLDOUT FRAME

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Y FLANGE

BOLT (140K EXTRA LONG) 16 REQ.D 7 LOCK WASHERS 16 READ

5 FOLDOUT FRAME

NFORMATION

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G

(PER PANEL) THEKMOCDUPLE ASSY 5 COHKBO-EL-PJ CONAX FITTING 131 8 MHC-040-A4-V (PER MINEL) (4) 10B MIC-040-A-V D 6.210 + 18.0 PER ZID VITON CORD STOCK 4 (TO FACILITY 50 O-KING z TED 6.13 MB324B/1-359 D-KING /3 C M535338-139 WASHER , LOCK CAPSCREW 4.250-2 /3C 4 NAS/357-4-10 SF M335338 -147 WASHER, LOCK 16 216 WASHETL, FLAT KD153-100Z-0014 10 NUT \$.875-14 206 10 KD114-2017-14 140L ; EXTEA LONG .5F BOLT \$.875-14 NAS/0/4-1/8 16 176 NAS/DIY-30 BOLT \$.875-14 10 13 F .250 LBN6 SETSCREW 6.190-32 NAS/DBI-3-4 12 5 C TURBULATOR 7/200/849/ -3 68 SUPPORT BAR

THERMOCOUPLE ASSY

TURBULATOR RING I REOLD

ENTRANCE SELTION I REOD

I EA. REQ.D ARS

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7K DD18168 -3 ENTRANCE SECTION 7E DD/8172 -3 SACKET HALF г 720018171-5 720018171-3 JACKET HALF TEST PANELS 720018170 - XX MATERIAL SPECS , NOTES NOMENALATURE READ PART NUMBER FSCM G DEFEVER HOT AIR PANEL ASSEMBLY

RETAINER RING

RETAINER KING

REPLACABLE NOTELE

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LD4 LBO - EIZ-PJ

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7/200/8485-7

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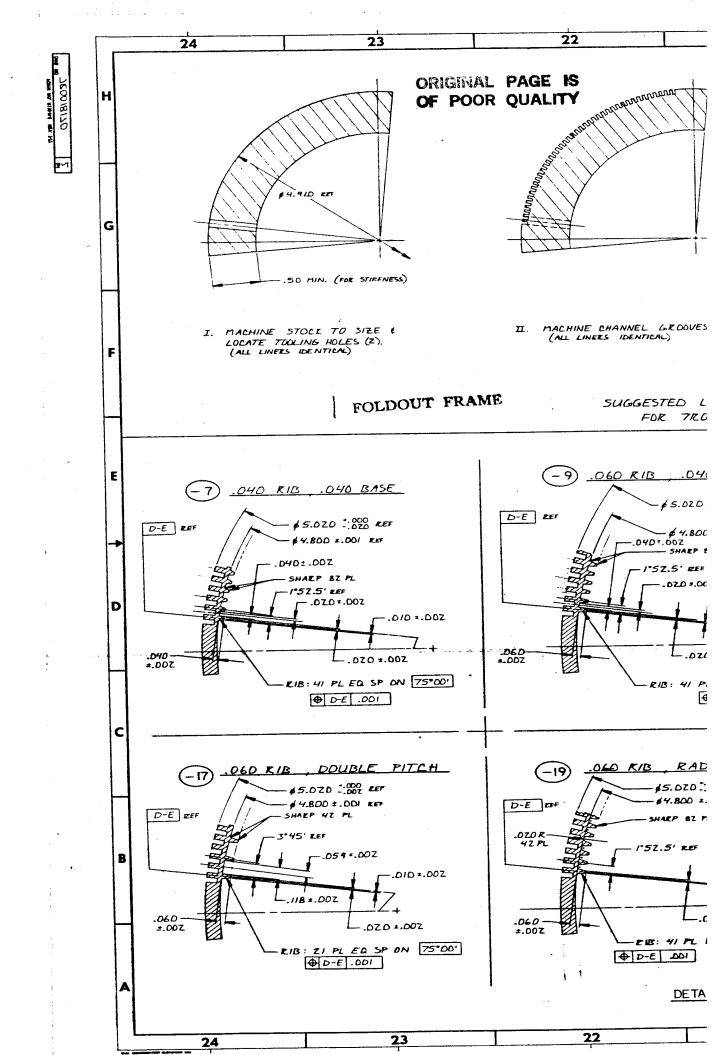
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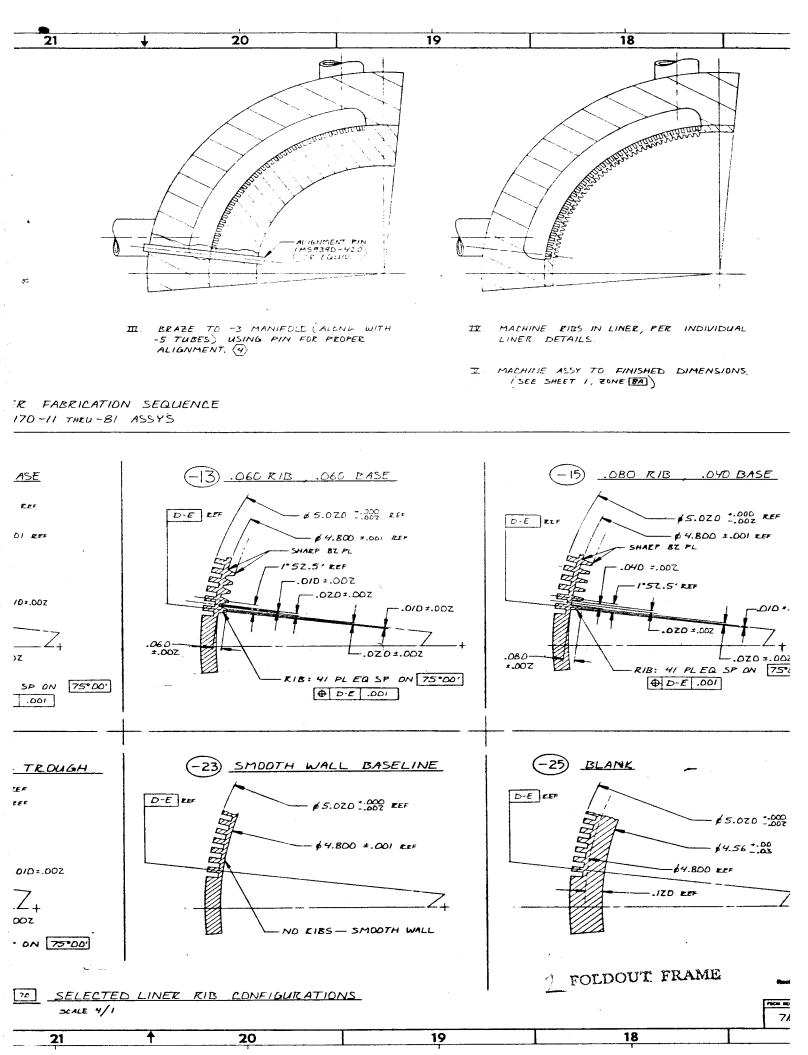
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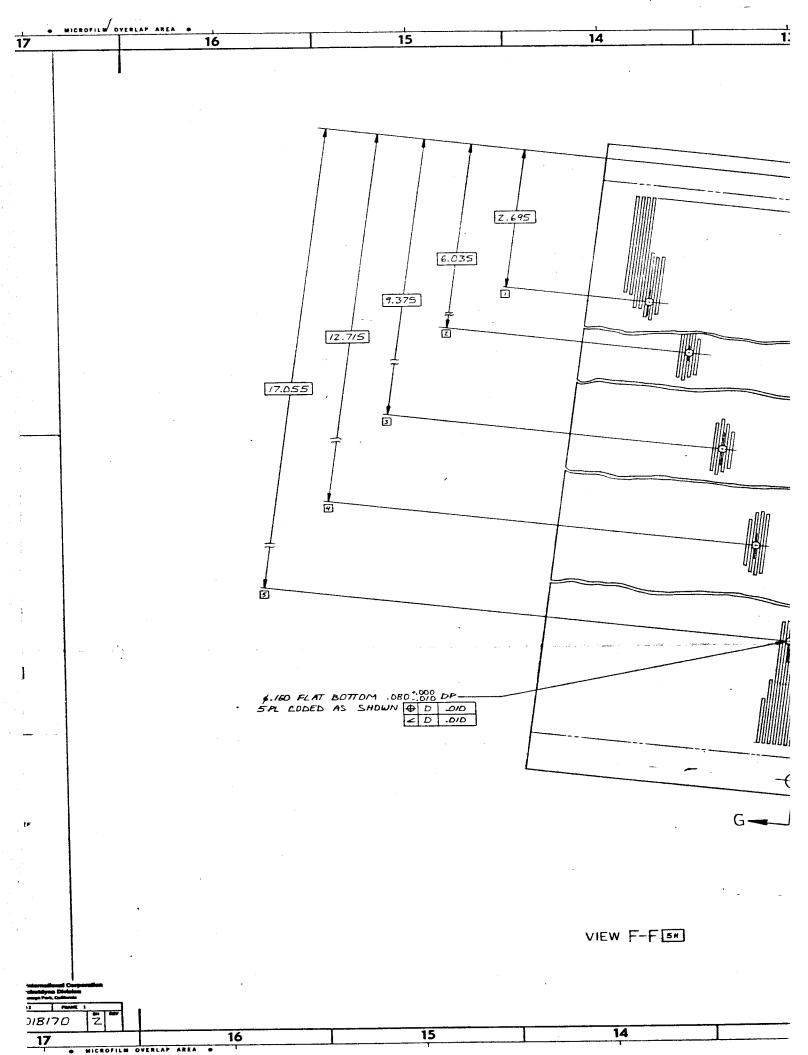
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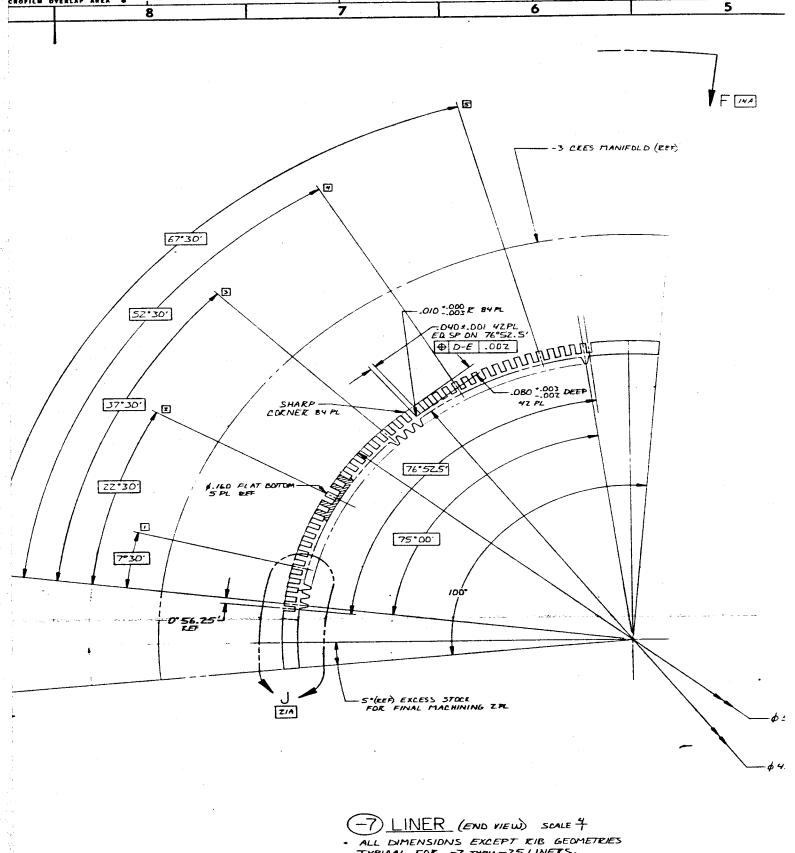
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- ALL DIMENSIONS EXCEPT RIB GEOMETRIES TYPICAL FOR -7 THEW 25 LINEES.
- INCLUDES EXCESS STOCK FOR TOOLING AND FINISH MACHINING.
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4 FOLDOUT FRAME

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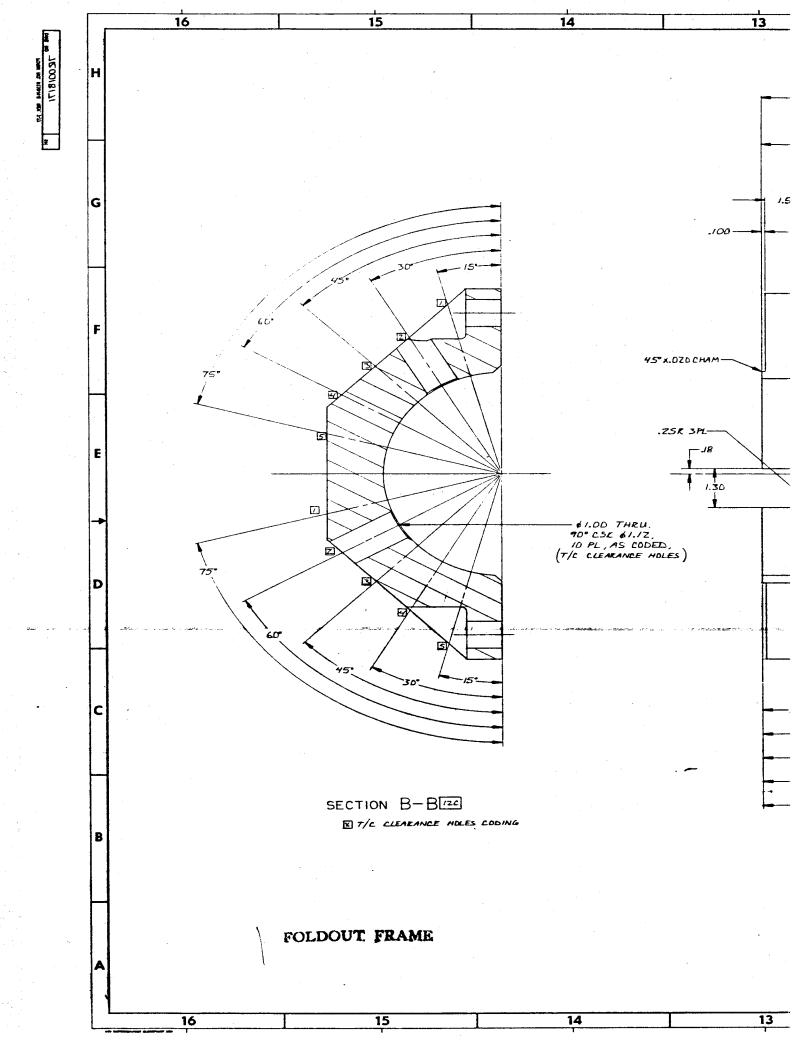
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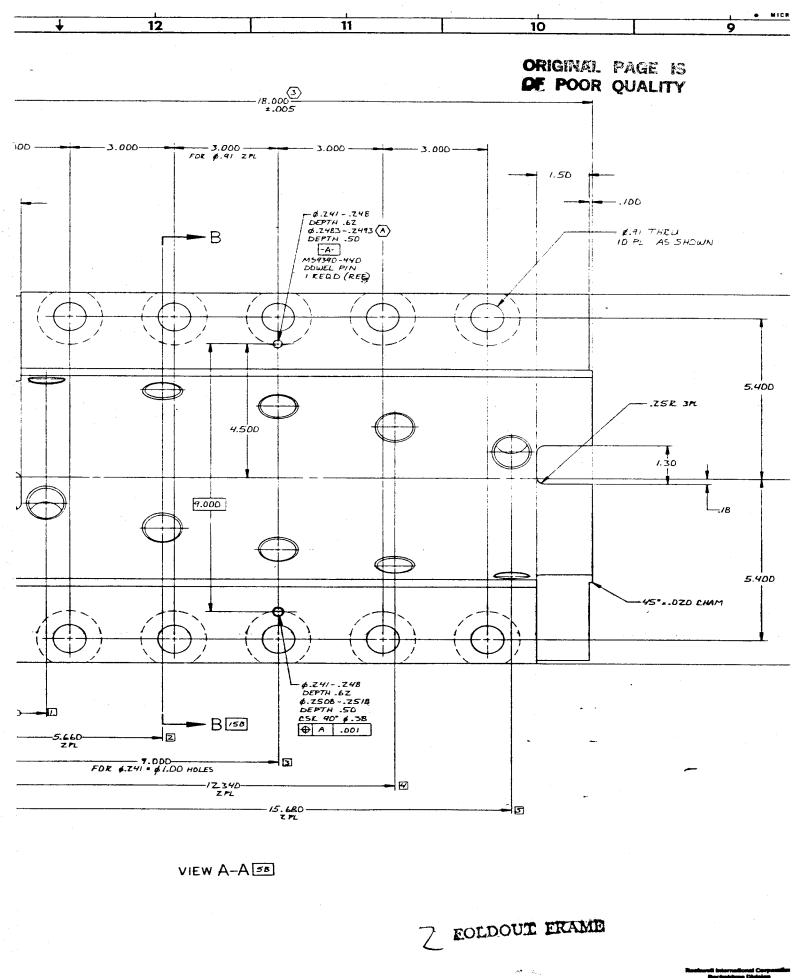
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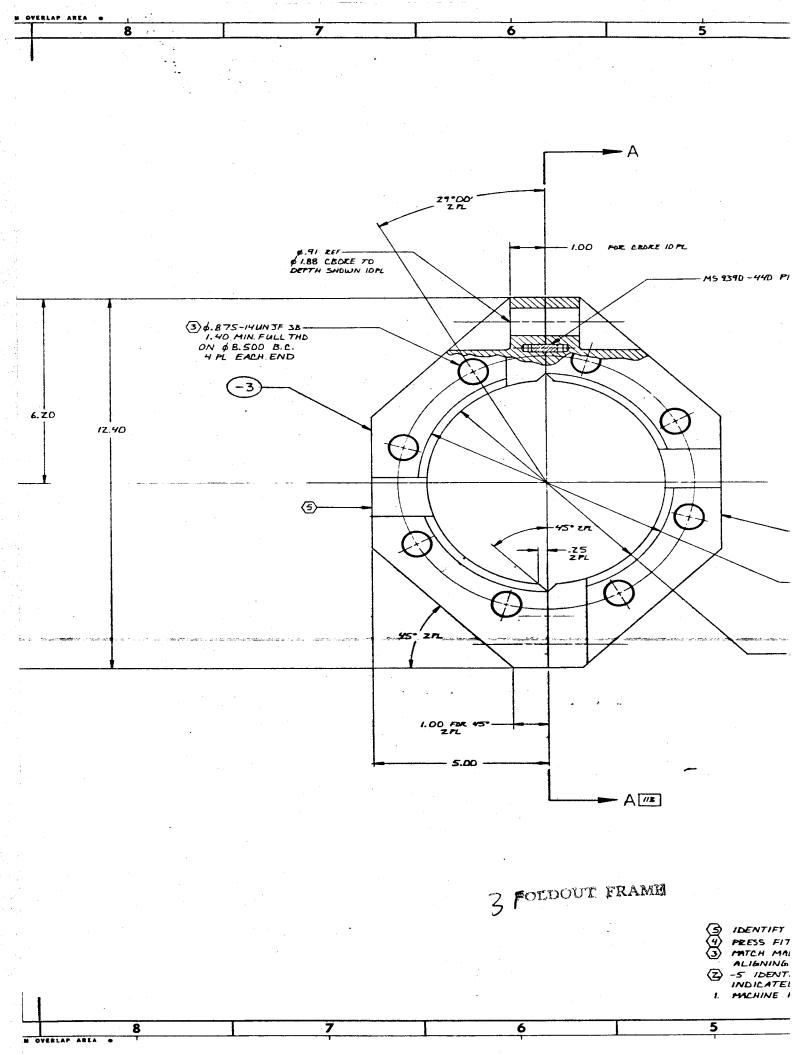
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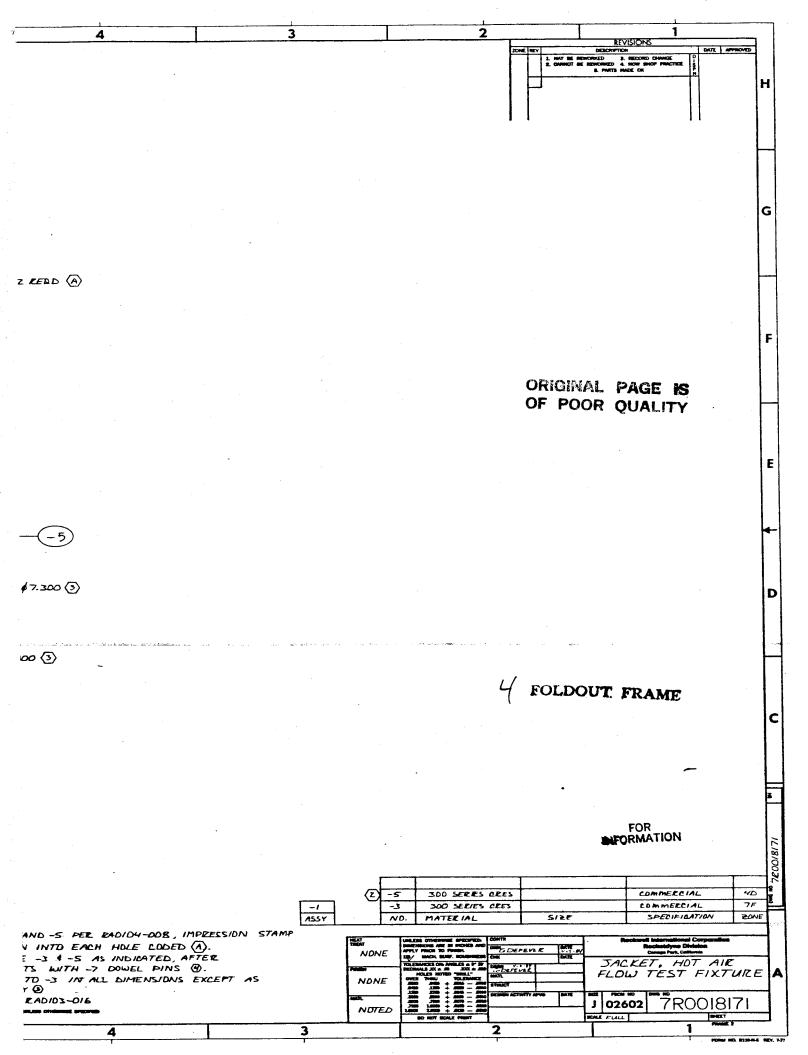
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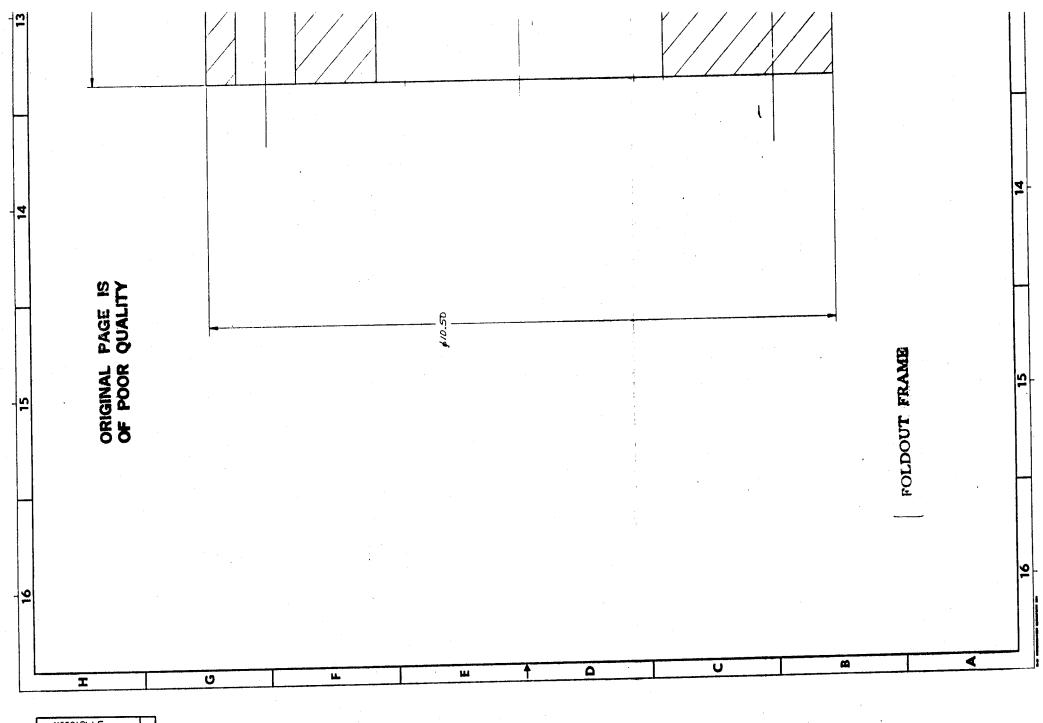




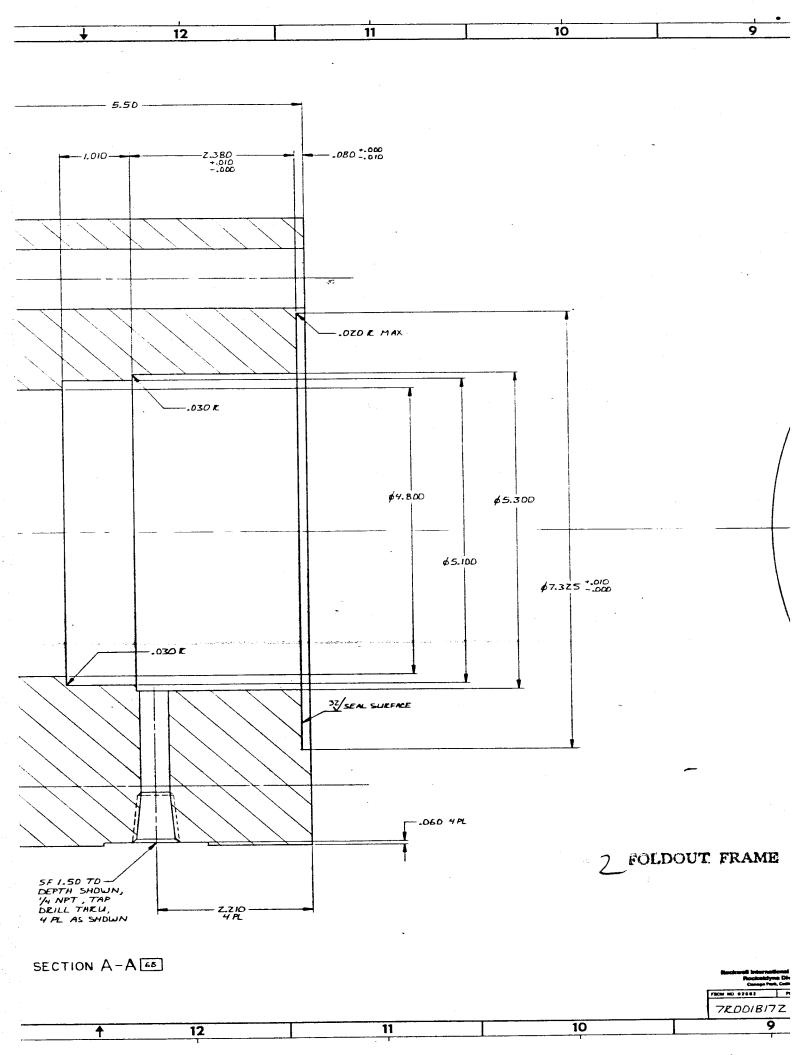
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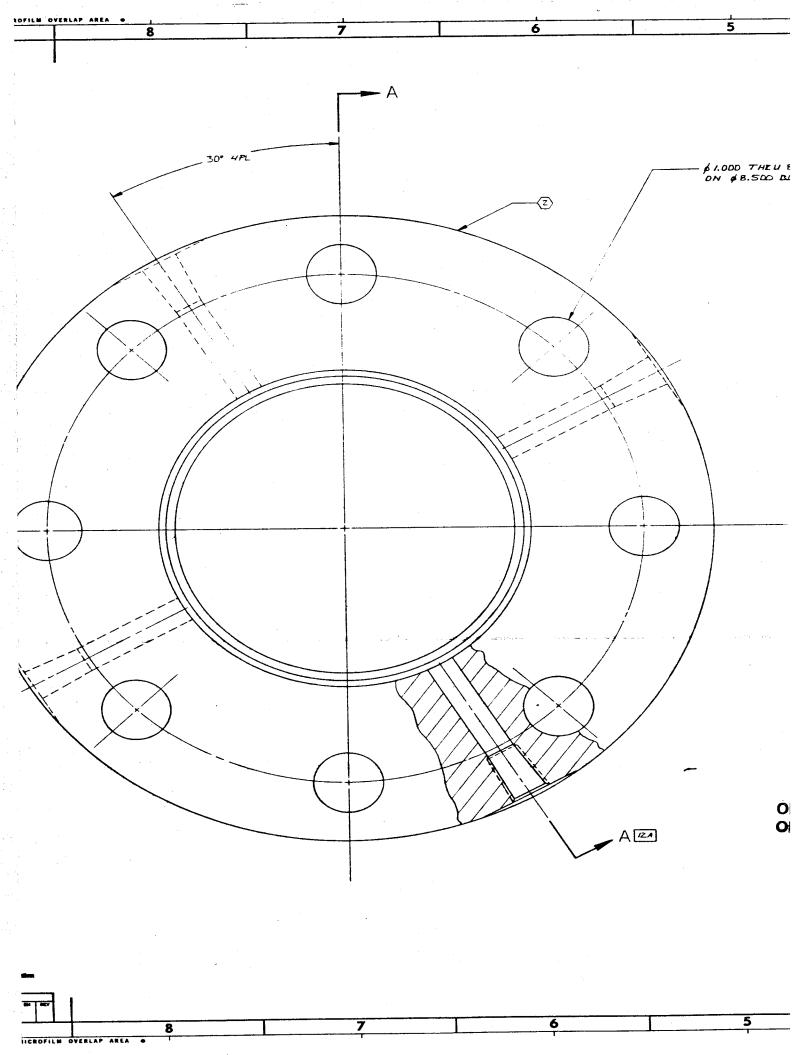


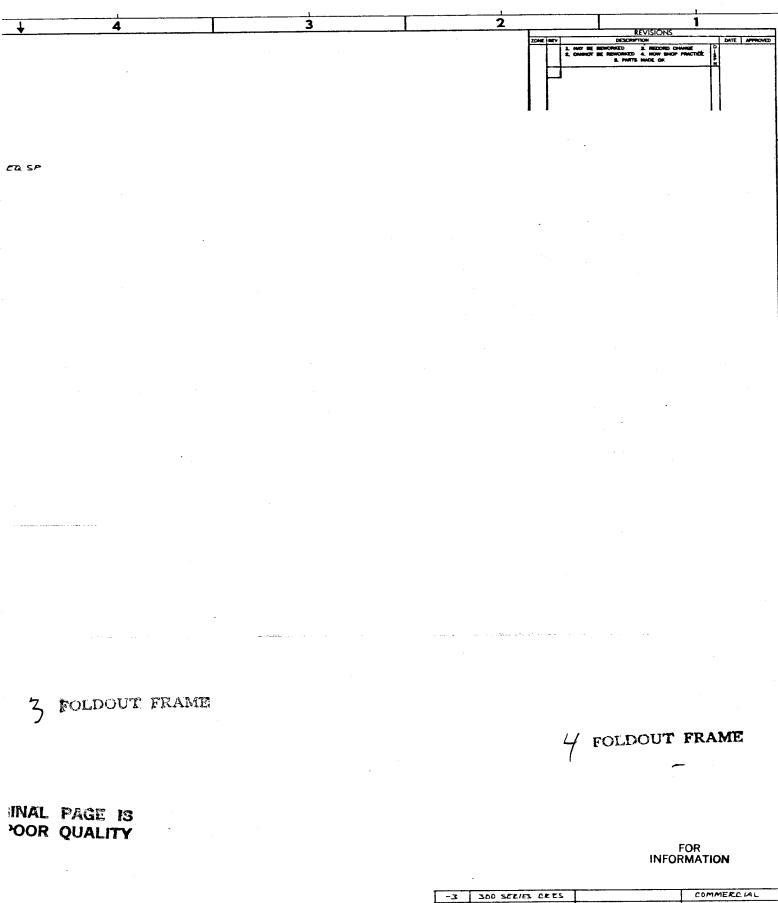




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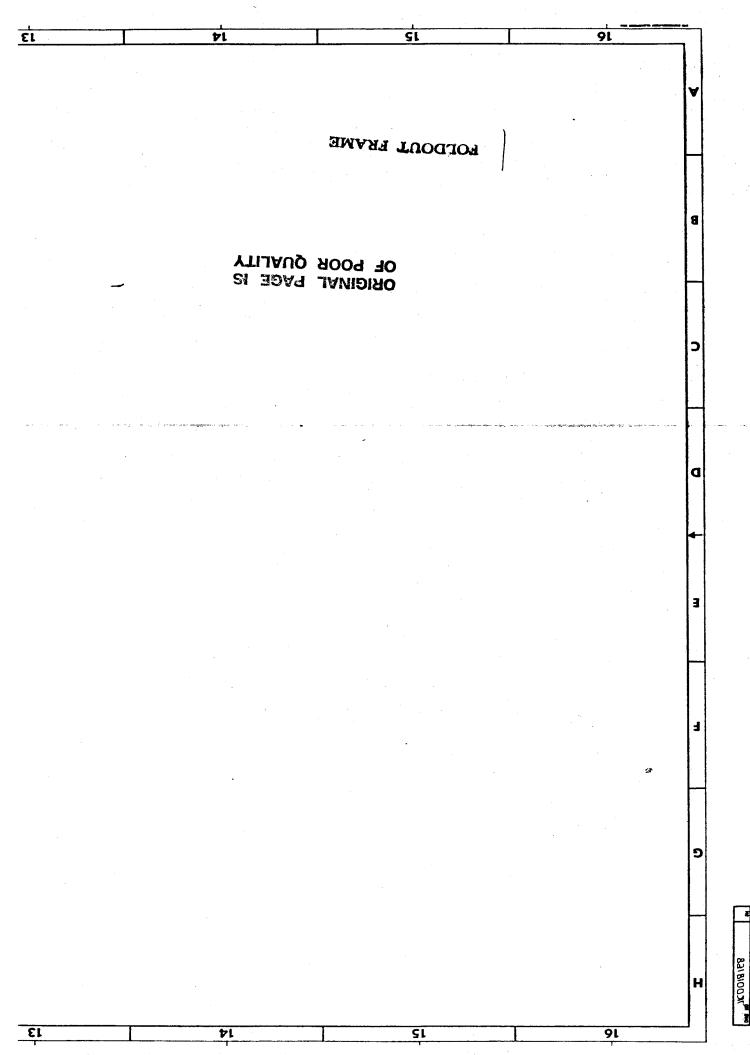


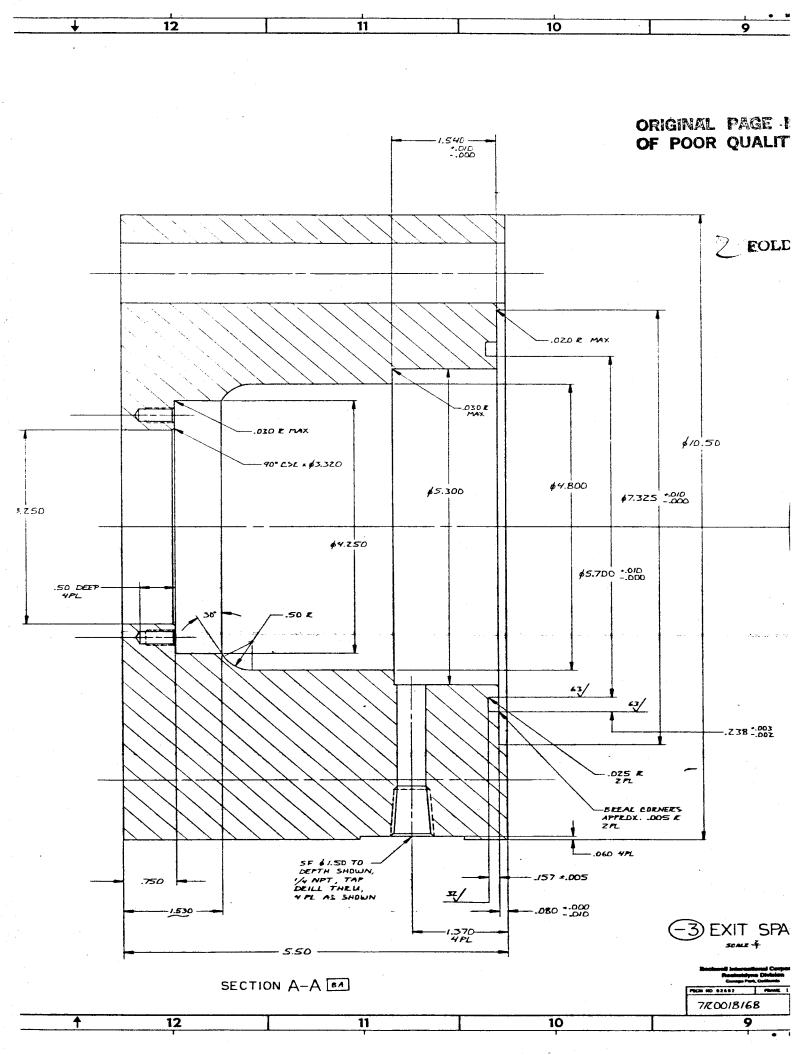


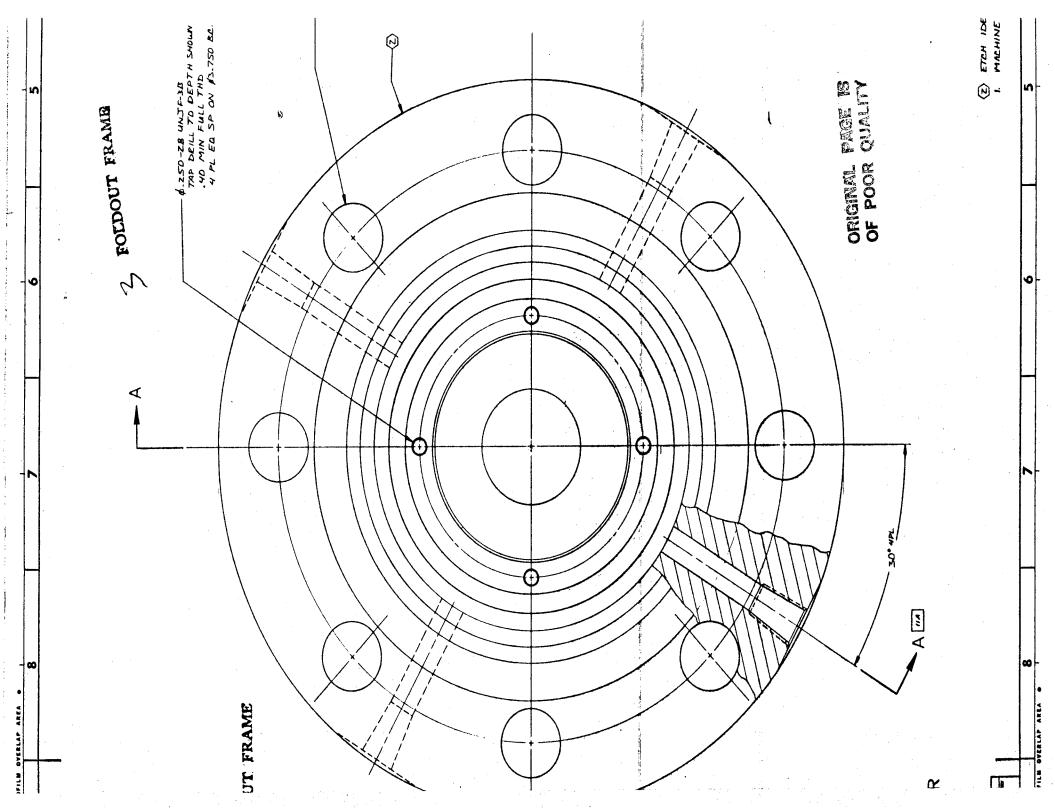


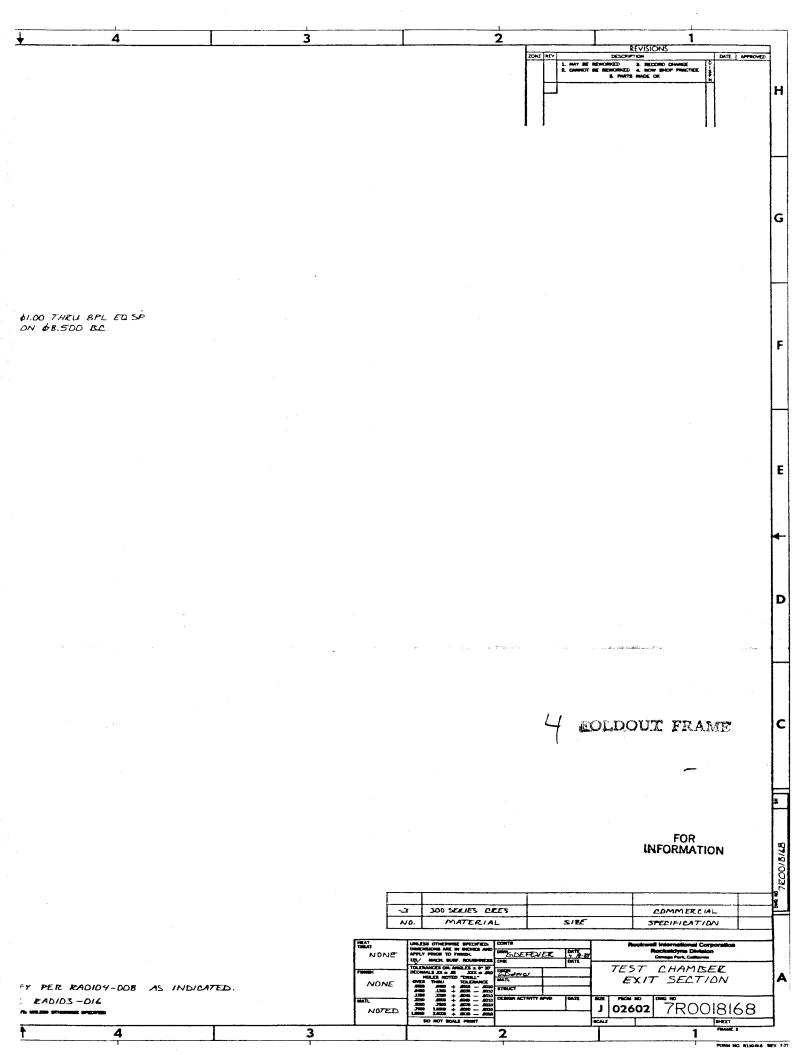
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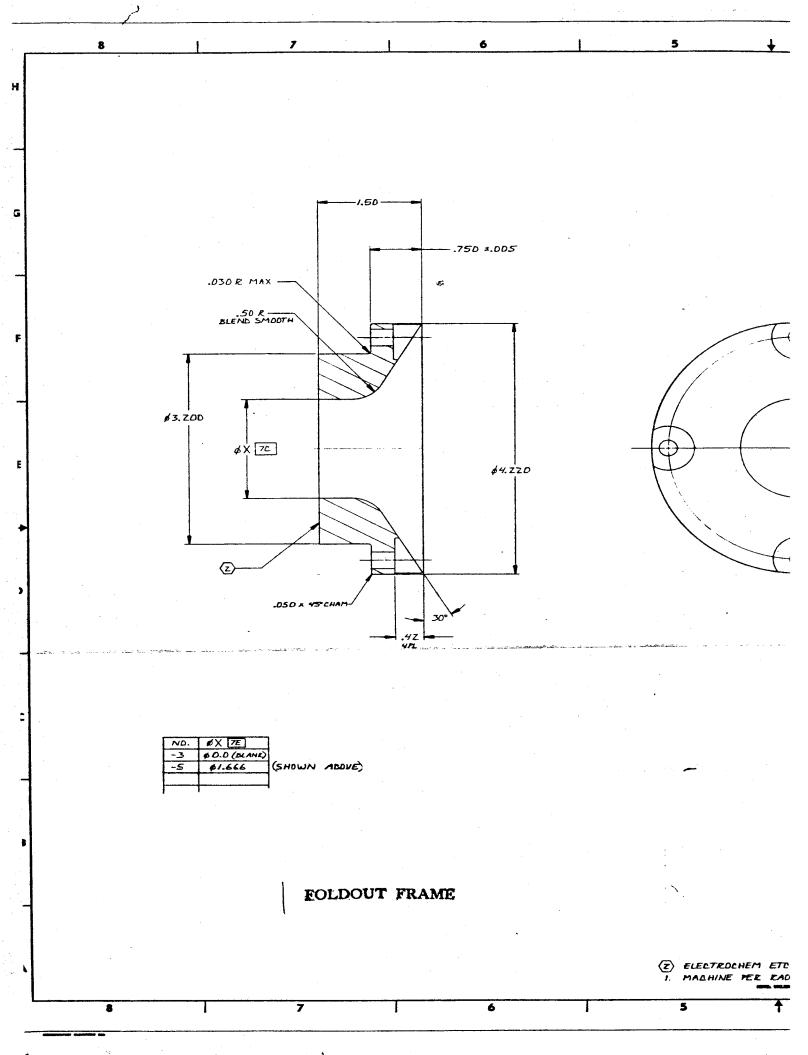
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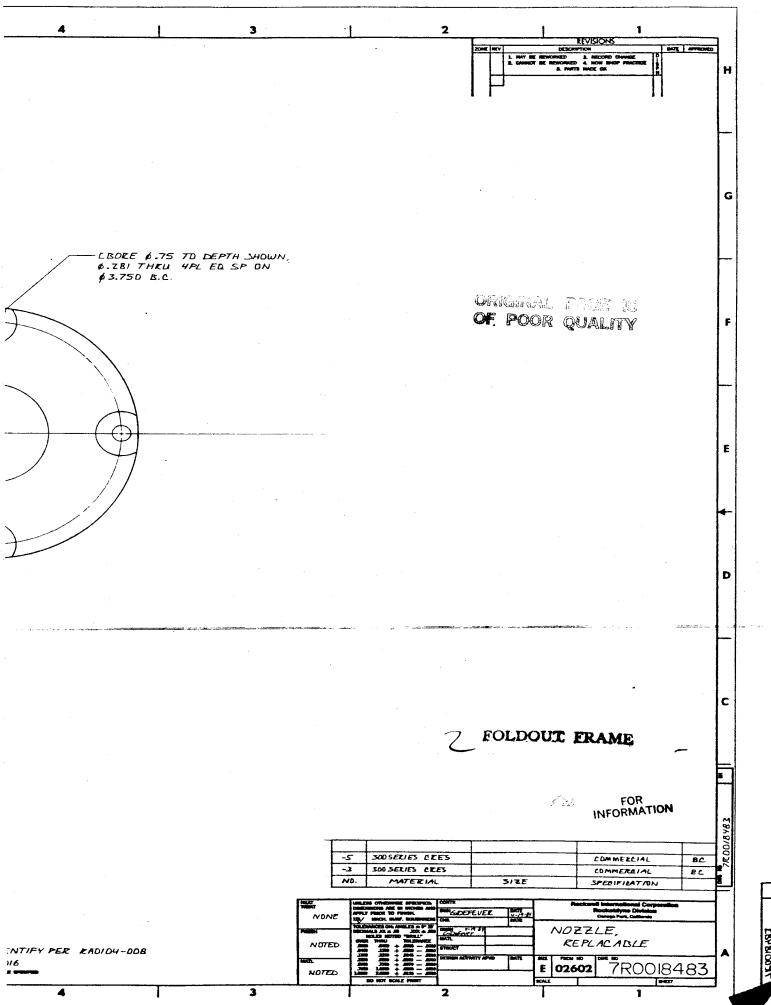


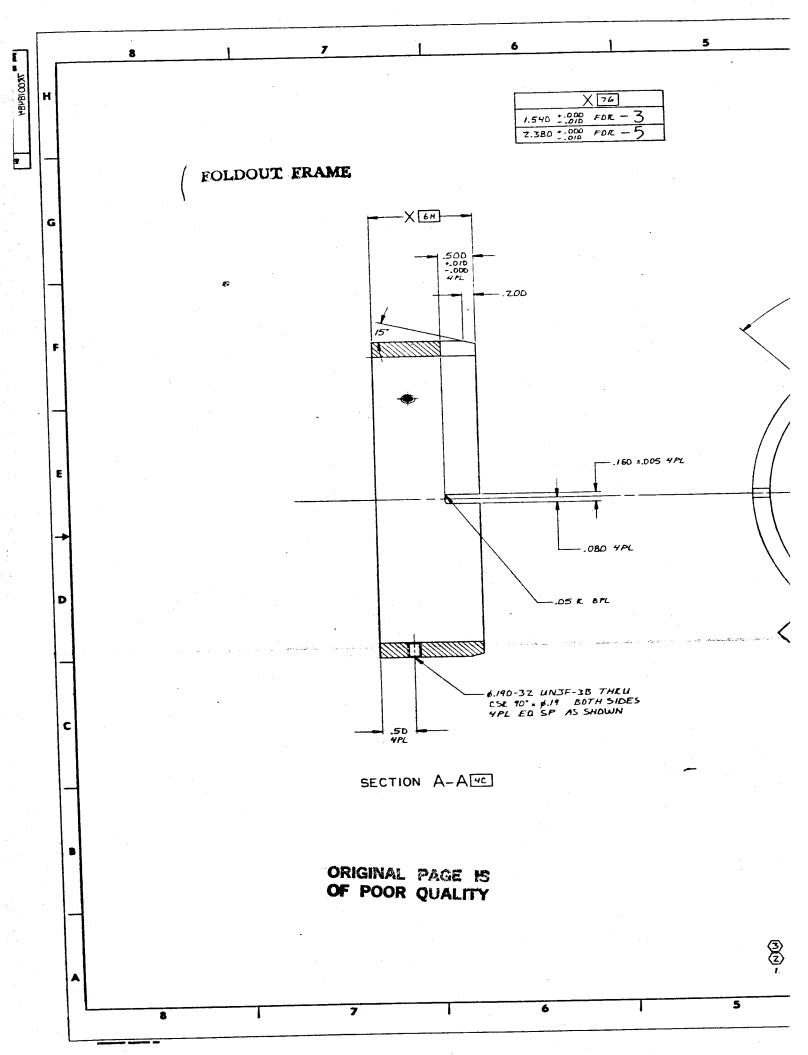


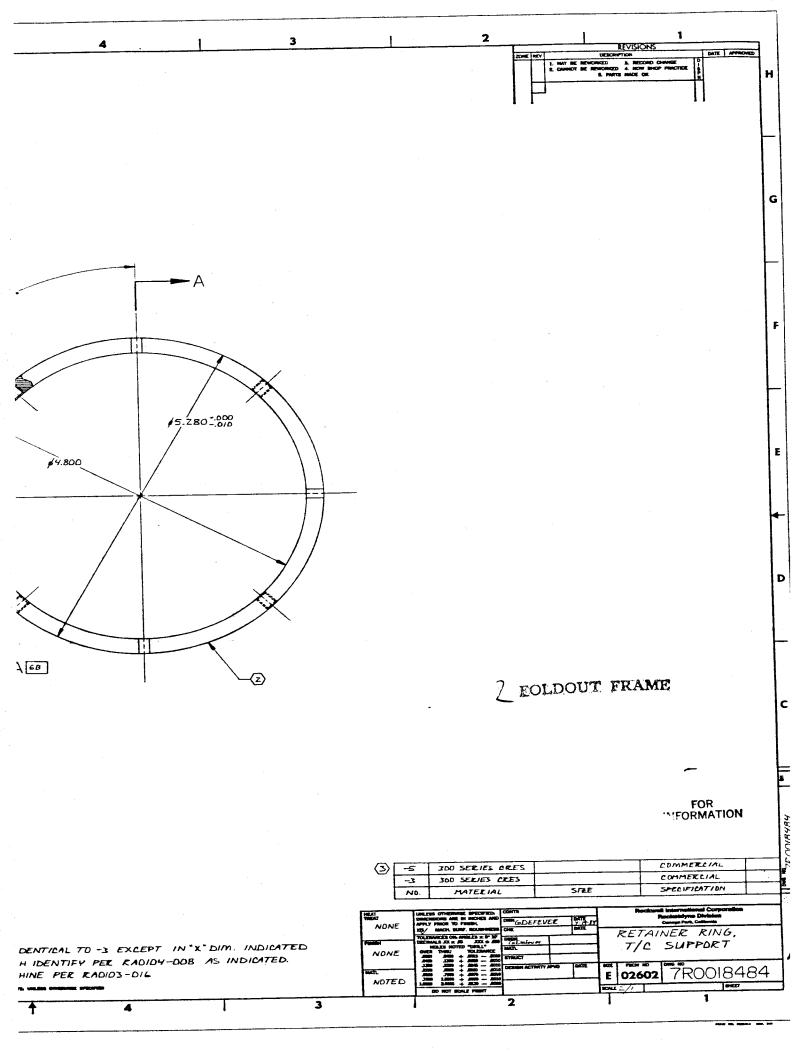


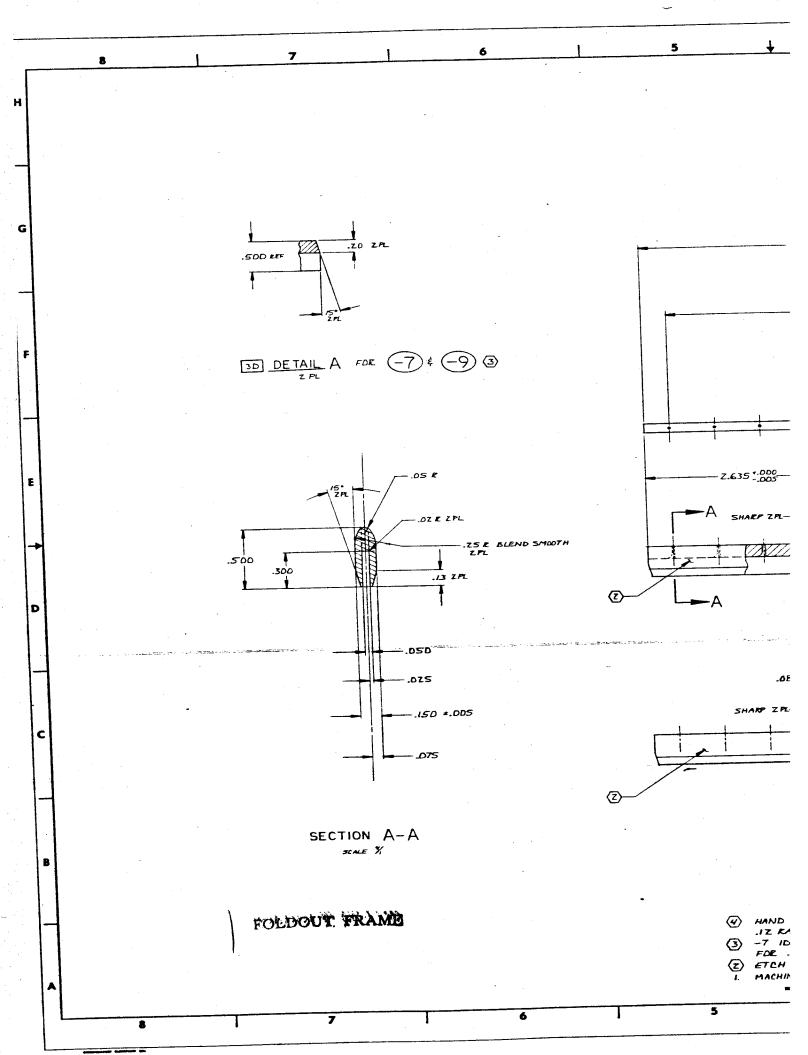


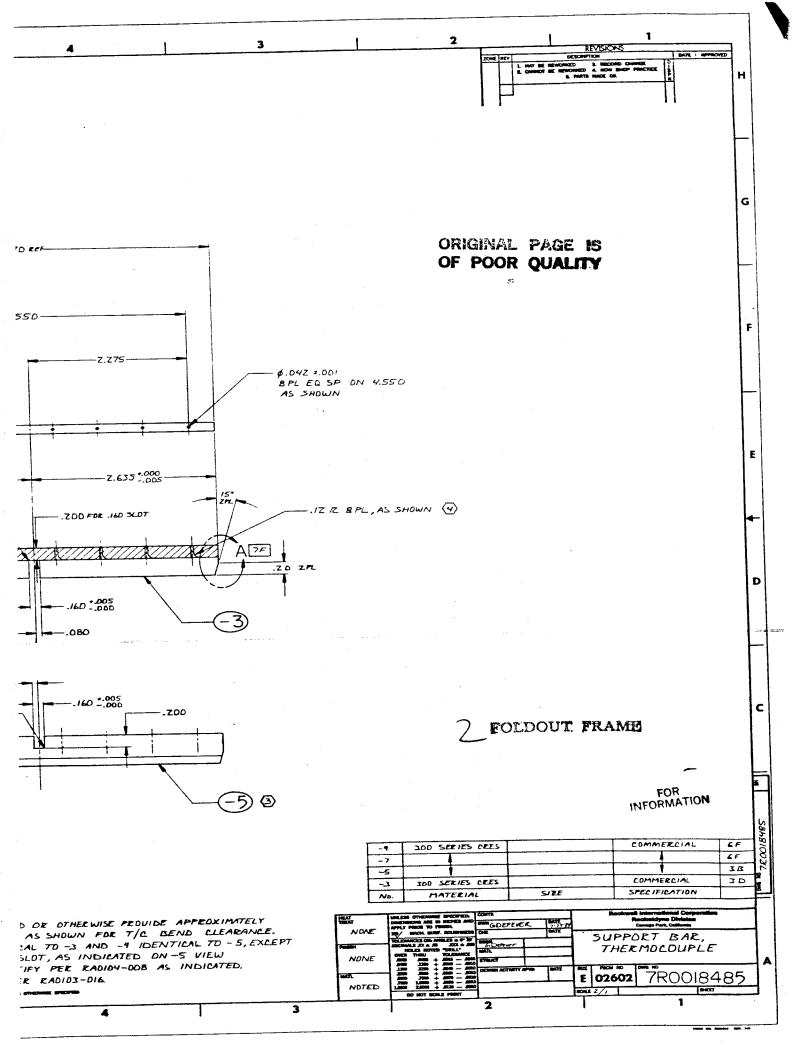


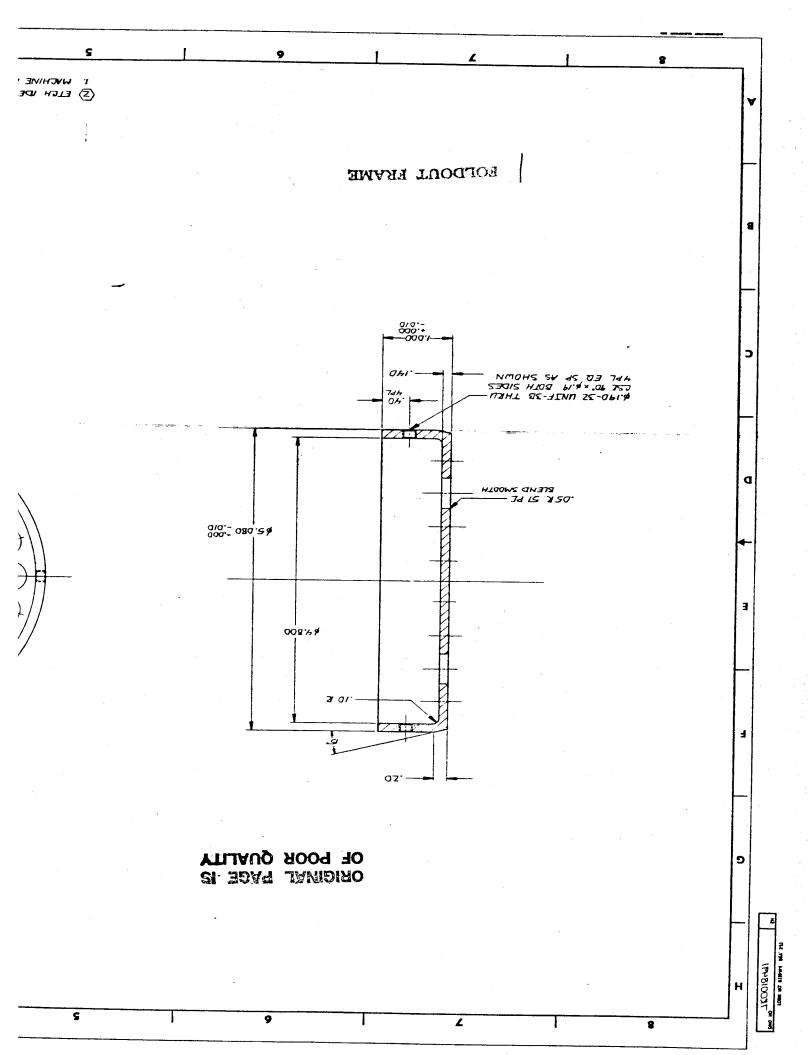


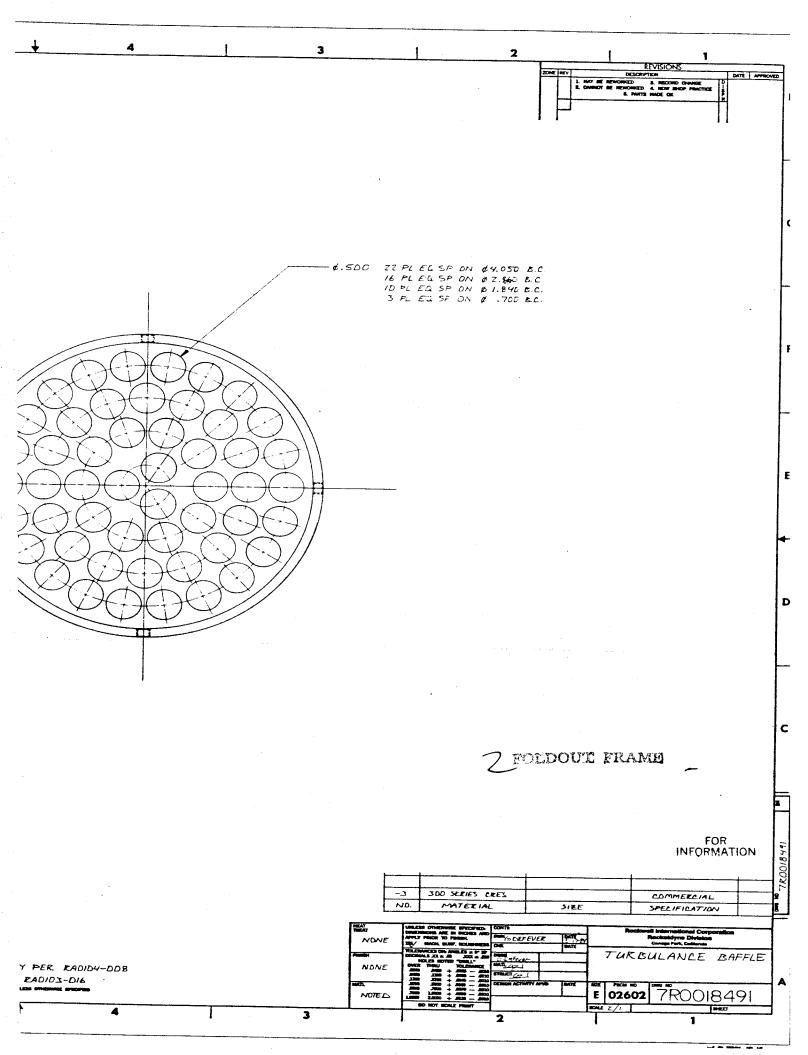












TEST PLAN FOR HOT AIR FLOW OF ADVANCED COMBUSTOR RIB GEOMETRIES

The following describes planned testing to be conducted at the Rockwell International NAAO Thermodynamics Laboratory. The testing will be done under Contract NAS3-23773, Enhanced Heat Transfer Combustor Technology with NASA Lewis Research Center.

SUMMARY

A 4.8 inch diameter calorimeter chamber will be built and supplied to the NAAO division for hot air flow testing. The chamber assembly will contain four 18-inch test panels, each assembled as a 90° segment of the cylindrical chamber (see assy dwg 7R0018169). Coolant (water) will be supplied to each panel and thermocouples used to monitor coolant temperature to derive heat transfer efficiency data on each test panel. A schematic of the test setup is shown in Figure 1. The apparatus will include a total of six test panels and one baseline reference panel.

TEST PLAN

Two separate test series are planned, since the segmented chamber will only accept three test panels at a time along with the one reference panel. These test series are outlined in Table 1. One test fixture tear-down and build-up will be required to change out the test panels between test series A and B. The testing will be accomplished per the schedule shown in Figure 2.

As shown in Figure 1, each of the four sectors of the calorimeter test chamber will have its own coolant water supply. The inlet and outlet temperatures and pressures will be recorded along with the water flowrates. Five wall temperature measurements will be made axially along the flow path on each of the test panels.

In addition to the water flow parameters, the chamber pressure and temperature profile will be recorded. A thermocouple rake at the injector end will give the actual hot air temperatures.

The targeted test conditions are given in Table 2.

The required instrumentation is listed in table 3. Parameters required to run the facility will be displayed on digital readout for monitoring purposes. Only those parameters required for data are shown in the table. Additional measurements will be required to monitor the test facility, and will be determined during facility set-up. Data will be collected using the Astrodata system at NAAO, where it is stored on magnetic type. Hard copy data will be obtained from the system.

G.J. Defever
Member of the Technical Staff
Advanced Combustion Devices

GJD:kw 2165/d

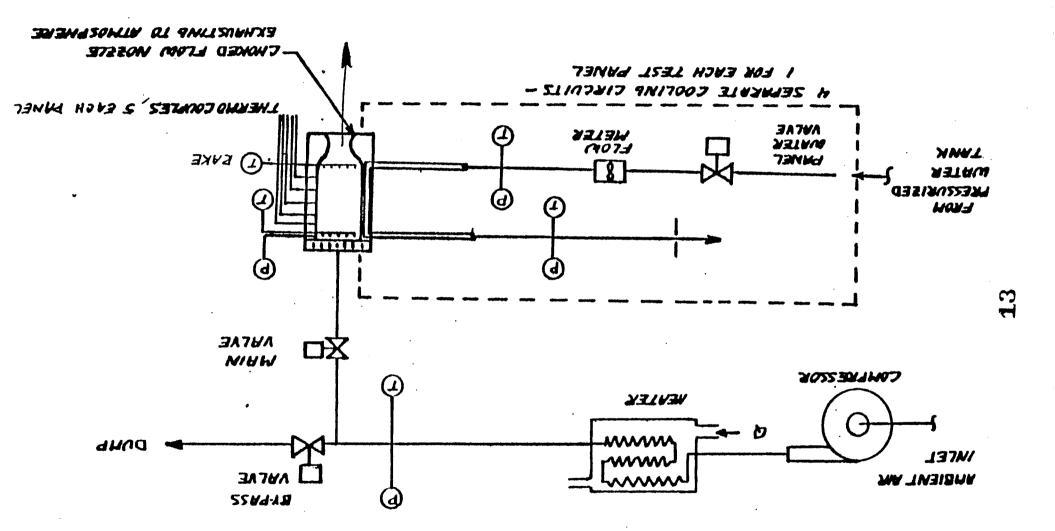


TABLE 1 TEST MATRIX

Series A	<u> Kardware</u>	<u>Description</u>
Test 1	Panels A,B,C and Baseline	Short Duration Facility/Data Acquisition Checkout
Test 2	. Panels A.B.C and Baseline	Long Duration to Steady State. Collect 20 Data Samples 900F
Test 3	Panels A.B.C and Baseline	Long Duration to Steady State. Collect 20 Data Samples 900F
Test 4	Panels A,B,C and Baseline	Long Duration to Steady State. Collect 20 Data Samples 700F
Test 5	Panels A.B.C and Baseline	Long Duration to Steady State. Collect 20 Data Samples 700F
Series B	•	
Test 1	Panels D.E.F and Baseline	Short Duration Facility/Data Acquisition Checkout
Test 2	Panels D.E.F and Baseline	Long Duration to Steady State. Collect 20 Data Samples at 900F
Test 3	Panels D.E.F and Baseline	Long Duration to Steady State. Collect 20 Data Samples at 900F
Test 4	Panels D.E.F and Baseline	Long Duration to Steady State. Collect 20 Data Samples at 700F
Test 5	Panels D.E.F and Baseline	Long Duration to Steady State. Collect 20 Data Samples at 700F

TABLE 2

HOT AIR TEST CONDITIONS

HOT AIR TEMPERATURE AT INLET 700° - 900°F

CHAMBER PRESSURE - 300 PSIA

HOT AIR FLOWRATE - 8.3 to 9 LB/SEC

WATER FLOW PER PANEL - .37 LB/SEC

TABLE B
INSTRUMENTATION LIST - HOT AIR TESTS

PARAMETER	NUMBER REQ'D	RANGE	TRANSDUCER	ASTRO - DATA	DIGITA DISPLA
BYPASS VALVE PRESS	1	0-500 PSIG	TABER	X	x
CHAMBER PRESS	1	0-500 PSIG	TABER	X	x
WATER TANK PRESS	1	0-500 PSIG	TABER	X	X
PANEL H20 PR IN	4	0-500 PS16	TABER	X	
PANEL H20 PR OUT	4	0-500 PSIG	TABER	X	
PANEL H20 FLOW	4	.5-2.5 GPM	TURBINE F/M	X	
BYPASS VALVE TEMP	1	0-1500°F	T/C	X	X
CHAMBER/C RAKE	32	0-1500°F	T/C	X (16)	
PANEL H ₂ O TEMP IN	4	0-200°F	T/C	X	
PANEL H20 TEMP OUT	4	0-200°F	T/C	x -	
PANEL H/G WALL TEMP	20	9 –1500 ⁰ F	T/C	X	

OTVW41Ø4 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .04

: 4-01-85

DATE

TIME **dTIME**

: 16:46

T AIR (F):

P AIR (psia):

418

163

W AIR (lb/sec): 6.256803

W H2O (lb/sec):

Ø (4-PANEL AVERAGE)

W AIR/W H2O :

ERROR (4-PANEL AVERAGE)

**********				,							
PANEL	T IN	1	2	IAL STATIO	ON4	5	T OUT	dТ	E.F.	W H2O (1b/sec)	W AIR/W H20
A	N/G	95.83	116.62	134.72	151.55	159.69	N/G	Ø	ERROR	N/G	ERROR
В	N/G	97.01	104.07	111.44	121	132.5	N/G	Ø	1	N/G	ERROR
С	N/G	99.37	130.16	125.86	132.07	146.61	N/G	Ø	ERROR	N/G	ERROR
D	N/G	107	119.83	127.17	136.11	148.62	N/G	ø	ERROR	N/G	ERROR

OTVW4105 4-30-85

dTIME

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .05

T AIR (F):

499

W AIR (lb/sec): 5.766370

DATE : 4-01-85 TIME

: 16:49

3

P AIR (psia):

157

W H2O (1b/sec):

Ø (4-PANEL AVERAGE)

W AIR/W H2O :

ERROR (4-PANEL AVERAGE)

			AX	والمراقب المحالة المحا	م مون د <u>ند. هی</u> وانند نموانند کود کاد این است	W H2O	ن جين خيف جيت انهان جينان جينان عمو طيف آلنان خيان ڪيان جينان جينان جينان خيان خيان خيان خيان خيان				
PANEL	T IN*	1	2	3	4	5	T OUT	dТ	E.F.	(lb/sec)	W AIR/W H2Ø
Α	N/G	98.47	127.34	140.58	159.16	166.75	N/G	Ø	ERROR	N/G	ERROR
В	N/G	95.54	103.65	116.82	126.76	134.2	N/G	Ø	1	N/G	ERROR
C	N/G	101.93	124.42	128.47	136.08	151.55	N/G	Ø	ERROR	N/G	ERROR
D	N/G	104.91	121.82	126.12	140.53	156.83	N/G	Ø	ERROR	N/G	ERROR

OTVW43Ø3 4-3Ø-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .03 T AIR (F) : 589 W AIR (lb/sec): 5.583693

W AIR/W H2O : 15.22479 (4-PANEL AVERAGE)

					W H2O						
PANEL	T IN*	1	2	3	ON4	5	T OUT	dТ	E.F.	(lb/sec)	W AIR/W H20
A	7ø	8Ø	90.2	98.94	103.82	108.58	106.3	36.3	1.532292	•351	15.90795668
В	7ø	79.45	80.94	93.98	89.85	96.29	93.69	23.69	1	•366	15.25599124
С	69.45	86.45	93.71	91.49	94.29	104.35	99.72	30.27	1.277754	.374	14.92965988
D	70.52	82.71	87.29	89.73	96.85	104.09	101.89	31.37	1.324187	•376	14.85024679

^{*} APPROX. VALUES, PANELS A, B.

OTVW43Ø4 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .Ø4 DATE

: 4-03-85

TIME : 14:17 dTIME

T AIR (F):

P AIR (psia):

694

199

W AIR (lb/sec): 6.662885

W H2O (lb/sec): .36675 (4-PANEL AVERAGE)

W AIR/W H2O : 18.16738 (4-PANEL AVERAGE)

هيم شهرستين مستوهات الجداعات الاستحدادة	روي المدين حديث حديث فيتحد خذين المنت المنتب الميان الميانات		AX	رهند وليوانده مدن وليد عباد عبدا عدد عدم الد		W H2O	ر. بندر بورو بورو مند نمد بندر بندر مدر شد بنرو شد بند است اندو بند است				
PANEL	T IN*	1	2	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H20
A	70	83.03	96.74	105.73	115.93	122.35	120.85	50.85	1.483805	•351	18.98257792
В	7ø	82.87	85.22	103.88	97.59	106.36	104.27	34.27	1	•366	18.20460342
С	69.22	91.86	102.63	99.66	103.63	117.47	112.06	42.84	1.250073	•374	17.81520014
D	70.33	86.63	93.27	97.22	106.78	117.04	114.65	44.32	1.293259	.376	17.72043843

^{*} APPROX. VALUES, PANELS A, B.

OTVW43Ø5 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .05

: 4-03-85

DATE TIME : 14:21

dTIME

T AIR (F):

P AIR (psia):

746

2Ø2

W AIR (lb/sec): 6.615914

W H2O (lb/sec): .366 (4-PANEL AVERAGE)

W AIR/W H2O : 18.07627 (4-PANEL AVERAGE)

			بلو بيونام مينه. هفيل خدات حفاق حفات خدات ويدي ناوات جدال خات خوش خوش ال	W H2O	ن ي						
PANEL	T IN*	1	2	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H2Ø
Α	7ø	84.06	98.93	108.35	120.34	127.71	126.03	56.03	1.479145	.351	18.84875784
В	70	84.15	86.71	107.19	100.22	109.9	107.88	37.88	1	•366	18.07626777
c	7Ø	93.91	106.39	102.62	107.17	122.37	116.7	46.7	1.232841	.371	17.83265230
D	70.36	87.67	95.62	100.09	110.64	121.96	119.72	49.36	1.303062	.376	17.59551596

^{*} APPROX. VALUES, PANELS A, B, C.

OTVW4306 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .06

: 4-03-85 DATE

: 14:24 : 3 TIME dTIME

T AIR (F):

786

W AIR (lb/sec): 8.023289

P AIR (psia):

249

W H2O (lb/sec):

.365 (4-PANEL AVERAGE)

W AIR/W H2O : 21.98162 (4-PANEL AVERAGE)

فيطف خشاق مبين خلط خسن موبن جين نيبن جينوجون			سري هندر هند خود سويه خود سويه خود الحود الحود الدو		W H2O	ر مربر مربر بینو مدر فیدر فیدر بندم چیدر شبه مدن سند مقد حدر فیدر سد					
PANEL	T IN*	1	2	3	4	5	T OUT	dТ	E.F.	(lb/sec)	W AIR/W H2Ø
Α	72	86.02	103.11	113.8	128.77	138.06	136.84	64.84	1.468297	•349	22.98936813
В	72	86.48	89.74	114.17	106.87	118.27	116.16	44.16	1	.364	22.04200406
С	71.51	97.43	112.16	108.02	113.32	131.25	127.48	55.97	1.267437	•373	21.51015946
D	72.41	90.43	100.05	105.73	117.94	131.38	131.21	58.8	1.331522	.374	21.45264567

^{*} APPROX. VALUES, PANELS A, B.

OTVW43Ø7 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .07

: 4-03-85

DATE

: 14:42 : 17 TIME dTIME

T AIR (F):

P AIR (psia):

792

242

W AIR (lb/sec): 7.779028

W H2O (lb/sec):

.365 (4-PANEL AVERAGE)

W AIR/W H2O : 21.31241 (4-PANEL AVERAGE)

		ر بيدم حديد خيد خيد كارث خيونونين	AX	W H2O							
PANEL	T IN*	1	2	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H2Ø
A .	72.5	87.72	105.98	117.21	133.34	143.9	141.83	69.33	1.476049	.349	22.28947865
В	72.5	88.72	91.65	116.96	109.38	120.97	119.47	46.97	1	.364	21.37095618
С	72.24	99.43	115.94	111.1	116.82	135.66	131.94	59.7	1.271024	.373	20.85530308
D	72.84	92.22	101.73	108.28	121.48	135.48	135.83	62.99	1.341069	.374	20.79954023

^{*} APPROX. VALUES, PANELS A, B.

OTVW4308 4-30-85

dTIME

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: >Ø8

:

T AIR (F) :

799

W AIR (lb/sec): 9.424246

DATE : 4-03-85 TIME

: 14:47

P AIR (psia):

294

W H2O (lb/sec):

.3645 (4-PANEL AVERAGE)

W AIR/W H2O : 25.85527 (4-PANEL AVERAGE)

مه بنو چیرجید میر جند سند سو سترمهن	مت خيدار سين نبيس خيدم خيدم جيمر خيمر خيدر کوبار مشم ه	ر عبد حدد حدر حدر حدوث خدد حدد م		W H2O							
PANEL	T IN*	1	2	3	4	5	T OUT	dТ	E.F.	(lb/sec)	W AIR/W H2Ø
A	73	87.42	105.86	117.63	135.11	144.8	145.36	72.36	1.457989	•349	27.00356941
В	73	88.81	92.24	119.84	111.38	124.36	122.63	49.63	1	•364	25.89078495
С	73	99.51	116.49	111.71	117.73	137.43	134.16	61.16	1.232319	.371	25.40227958
D	72.83	91.07	102.86	109.89	123.6	138.44	138.74	65.91	1.328027	.374	25.19851798

^{*} APPROX. VALUES, PANELS A, B, C.

OTVW4309 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .09 T AIR (F): 700 W AIR (lb/sec): 9.818168

DATE : 4-03-85
TIME : 15:04 P AIR (psia): 294 W H2O (1b/sec): .36725 (4-PANEL AVERAGE)

dTIME : 17

W AIR/W H2O : 26.73429 (4-PANEL AVERAGE)

PANEL	T IN*	1	AX	IAL STATI	ON4	5	T OUT	dT	E.F.	W H2O (1b/sec)	W AIR/W H2Ø
A	72	85.59	102.7	112.96	128.39	136.61	136.56	64.56	1.453727	.351	27.97198941
В	72	86.75	89.94	114.58	106.32	118.03	116.41	44.41	1	.367	26.75250213
С	7 1.93	96.67	113.38	107.76	113.2	130.56	126.24	54.31	1.222923	.374	26.25178685
D	71.06	88.64	99.55	105.43	118.15	130.89	129.98	58.92	1.326728	•377	26.04288669

^{*} APPROX. VALUES, PANELS A, B.

OTVW431Ø 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .10

: 4-03-85

DATE

TIME : 15:18 dTIME : 14 T AIR (F):

P AIR (psia):

7Ø5

294

W AIR (lb/sec): 9.797077

W H2O (1b/sec): .36525 (4-PANEL AVERAGE)

W AIR/W H20 : 26.82293 (4-PANEL AVERAGE)

			AX	W H2Ø							
PANEL	T IN*	1	2 	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H2Ø
A	72 (85.56	102.84	113	128.64	136.72	136.13	64.13	1.445346	.349	28.07185272
В	72	86.86	90	114.76	106.6	118.13	116.37	44.37	1	•366	26.76796885
С	72	96.21	113.14	107.6	113.14	130.51	126.6	54.6	1.230561	.37	26.47858540
D	71.67	88.46	99.55	105.43	118.13	131.44	130.4	58.73	1.323642	•376	26.05605478

^{*} APPROX. VALUES, PANELS A, B, C.

OTVW44Ø3 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .03

DATE : 4-04-85

TIME : 14:45

dTIME Ø T AIR (F): 598

W AIR (lb/sec): 10.21062

P AIR (psia): 292

W H2O (lb/sec): .373075 (4-PANEL AVERAGE)

W AIR/W H2O : 27.36882 (4-PANEL AVERAGE)

	AXIAL STATION								W H2O			
PANEL	T IN	1	2	3	4	5	T OUT	dТ	E.F.	(lb/sec)	W AIR/W H2Ø	
A	74.29	84.38	95.75	104.77	117.13	123.07	123.53	49.24	1.374267	•3755	27.19206640	
В	73.67	86.15	87.92	99.38	101.69	112.27	109.5	35.83	1	.3658	27.91312448	
c	71.99	59.Ø3 N/G	97.86	102.19	106.53	120.63	116.38	44.39	1.238906	•3755 ·	27.19206640	
D	72.92	86.73	95.51	99.72	109.84	120.68	119.2	46.28	1.291655	•3755	27.19206640	

OTVW44Ø4 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .Ø4

: 4-04-85

DATE TIME : 14:50

dTIME

T AIR (F):

594

W AIR (lb/sec): 10.22998

P AIR (psia):

292

W H2O (1b/sec): .372725 (4-PANEL AVERAGE)

W AIR/W H2O : 27.44645 (4-PANEL AVERAGE)

				· · · · · · · · · · · · · · · · · · ·							
PANEL	T IN	1	2	IAL STATIO	ON4	5	T OUT	dТ	E.F.	W H2O (1b/sec)	W AIR/W H2Ø
A	74.24	84.28	95.65	104.76	117.05	123.44	123.68	49.44	1.381006	.3741	27.34556958
В	73.64	86	87.81	99	101.37	112.03	109.44	35.8	1	.3658	27.96604040
c	72.03	60.58 N/G	98.18	102.02	106.4	120.41	116.56	44.53	1.243855	•3755	27.24361539
D	72.91	86.69	95.41	99.65	109.95	120.62	119.51	46.6	1.301676	•3755	27.24361539

OTVW4405 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .05

: 4-04-85 DATE

TIME : 14:55

dTIME 5 T AIR (F): 592 W AIR (lb/sec): 10.23970

P AIR (psia): 292 W H2O (lb/sec):

.3717 (4-PANEL AVERAGE)

W AIR/W H2O : 27.54828 (4-PANEL AVERAGE)

PANEL	T IN	1	2	IAL STATIO	ON4	5	T OUT	dТ	E.F.	W H2O (lb/sec)	W AIR/W H2Ø
A	74.16	84.28	95.74	104.99	117.3	123.41	123.92	49.76	1.381455	•3741	27.37155112
В	73.63	85.96	87.86	99.22	101.67	112.19	109.65	36.02	1	.3658	27.99261147
С	72.26	60.98 N/G	98.98	102.42	106.96	120.83	117.29	45.03	1.250139	.3728	27.46699913
D	73.24	86.8	95.88	100.1	110.64	121.11	120.33	47.09	1.307329	.3741	27.37155112

OTVW4406 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .06 T AIR (F): 608 W AIR (lb/sec): 10.16271

DATE : 4-04-85
TIME : 15:00 P AIR (psia): 292 W H2O (lb/sec): .372025 (4-PANEL AVERAGE)

dTIME : 5

W AIR/W H2O : 27.31727 (4-PANEL AVERAGE)

			·				~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~				
PANEL	T IN	1	2	IAL STATIO	ON	5	T OUT	dТ	E.F.	W H2O (lb/sec)	W AIR/W H2Ø
· A	73.85	84.24	96.09	105.49	118.37	124.81	125.31	51.46	1.400653	•3741	27.16574706
В	73.47	86.22	87.92	99.52	102.07	112.86	110.21	36.74	1	.3658	27.78213772
С	72.19	61.79 N/G	99.14	102.64	107.17	121.53	118.02	45.83	1.247414	.3741	27.165747Ø6
D	73.19	86.86	95.97	100.16	110.82	121.63	121.07	47.88	1.303212	.3741	27.16574706

OTVW4407 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .07

DATE : 4-04-85

TIME : 15:05

dTIME

T AIR (F):

P AIR (psia):

627

292

W AIR (lb/sec): 10.07350

W H2O (lb/sec): .372375 (4-PANEL AVERAGE)

W AIR/W H2O : 27.05202 (4-PANEL AVERAGE)

			AX	IAL STATI	ON	منع جنب خبير جنان آجاد خادد خارد			W H2O			
PANEL	T IN	1	2	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H20	
A	73.5	84.32	96.55	106.25	119.54	126.17	126.75	53.25	1.396538	.3741	26.92728128	
В	73.09	86.23	88.22	100.12	102.63	113.88	111.22	38.13	1	. 3658	27.53826115	
С	71.27	62 . 1 N/G	100.02	103.31	108.01	123.09	118.79	47.52	1.246263	.3741	26.92728128	
D	72.29	86.91	96.64	101.04	112.03	123.27	122.29	5ø	1.311303	.3755	26.82688663	

OTVW44Ø8 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

P AIR (psia):

TEST NO.: .08

DATE : 4-04-85

TIME : 15:10

dTIME 5 T AIR (F): 621

289

W AIR (lb/sec): 9.997632

W H2O (1b/sec): .3717 (4-PANEL AVERAGE)

W AIR/W H2O : 26.89705 (4-PANEL AVERAGE)

						~~~~~~~~					
PANEL.	T IN	1	dT	W H2O E.F. (lb/sec) W AIR/W H2Ø							
Α	73.75	84.43	96.33	105.93	119.04	125.77	126.41	52.66	1.391281	•3741	26.72448984
В	73.34	86.35	88.19	100.09	102.91	113.88	111.19	37.85	1	•3658	27.33Ø86837
С	72.6	63 N/G	100.25	103.2	108.06	122.71	119.6	47	1.241744	.3728	26.81768146
D	73.37	86.84	96.2	100.65	111.56	122.87	122.76	49.39	1.304888	.3741	26.72448984

OTVW44Ø9 4-30-85

#### HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .09 DATE

: 4-04-85

: 15:15 TIME

dTIME

T AIR (F):

62Ø

W AIR (lb/sec): 10.10609

P AIR (psia): 292

W H2O (1b/sec): .368225 (4-PANEL AVERAGE)

W AIR/W H2O : 27.44542 (4-PANEL AVERAGE)

	<del></del>		AX			W H2O	ر عبين ميند جيد عبيد جيد فيد. خيد شده جان شند مناه الله الله الله الله الله الله الله ا				
PANEL	T IN	1	2	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H2Ø
A	74.08	84.95	96.91	106.56	119.66	126.46	126.68	52.6	1.389696	.3755	26.91368519
В	73.67	86.88	88.56	100.62	103.03	114.15	111.52	37.85	1	.3672	27.52202829
С	71.51	63.7 N/G	99.96	103.82	108.58	123.28	118.61	47.1	1.244386	.3547	28.49193344
D	72.3	87.5	96.85	101.37	112.33	123.47	121.96	49.66	1.312021	•3755	26.91368519

OTVW4410 4-30-85

**dTIME** 

#### HOT AIR RIBBED CALORIMETER TESTS

#### DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .10

T AIR (F):

W AIR (lb/sec): 9.937300

: 4-04-85 DATE TIME : 15:21

6

P AIR (psia):

W H2O (lb/sec): .3724 (4-PANEL AVERAGE)

W AIR/W H2O : 26.68448 (4-PANEL AVERAGE)

_							<del> </del>					
	PANEL	T IN	1	AX	IAL STATIO	ON4	5	T OUT	dТ	E.F.	W H2O (lb/sec)	W AIR/W H2Ø
	A	74.27	85.63	98.61	109.1	123.17	130.39	131.58	57.31	1.395083	.3755	26.46418107
	В	73.86	87.9	89.8	102.72	105.64	117.47	114.94	41.08	1	.3672	27.06236381
	С	72.81	64.54 N/G	102.07	106.26	111.4	127.35	123.79	50.98	1.240993	.3714	26.75632739
	D	73.48	88.37	98.49	103.83	115.42	127.64	127.45	53.97	1.313778	•3755	26.46418107

657

292

OTVW4411 4-30-85

## HOT AIR RIBBED CALORIMETER TESTS

#### DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .11

T AIR (F): 734 W AIR (lb/sec): 9.644453

DATE : 4-04-85 TIME : 15:29

P AIR (psia):

W H2O (lb/sec): .373075 (4-PANEL AVERAGE)

**dTIME** 

W AIR/W H2O : 25.85124 (4-PANEL AVERAGE)

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PANEL	T IN	1	2	IAL STATIO	ON4	5	T OUT	dТ	E.F.	W H2O (lb/sec)	W AIR/W H2Ø
A	73.83	86.08	100.29	111.74	127.15	135.19	136.32	62.49	1.408702	.3755	25.68429512
В	73.49	88.75	90.69	104.74	106.95	120.04	117.85	44.36	1	.3672	26.26484972
С	71.16	64.7 N/G	103.2	108.71	114.42	131.83	126.07	54.91	1.237827	.3741	25.78041384
D	71.37	89.29	100.3	106.14	119.06	132.35	130.33	58.96	1.329125	.3755	25.68429512

293

#### OTVW4412 4-30-85

#### HOT AIR RIBBED CALORIMETER TESTS

#### DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .12 T AIR (F): 768 W AIR (lb/sec): 9.510001

DATE : 4-04-85
TIME : 15:38 P AIR (psia): 293 W H2O (lb/sec): .373425 (4-PANEL AVERAGE)

dtime : 9
W AIR/W H2O : 25.46696 (4-PANEL AVERAGE)

				<del></del>	<del></del>						ر. در جرد مرد بود برد مرد اسم الله الله عبد البدائد الله الله الله
PANEL	T IN*	1	AX	IAL STATIO	ON4	5	T OUT	dТ	E.F.	W H2O (1b/sec)	W AIR/W H2Ø
A	73.82	86.57	101.42	113.28	129.44	138.04	139.47	65.65	1.417008	•3755	25.32623495
В	73.41	89.22	91.17	105.92	108.77	122.34	119.74	46.33	1	•3672	25.89869614
С	72	65.6 N/G	104.25	110.4	116.39	134.66	130.06	58.06	1.253184	. 3755	25.32623495
D .	72.22	89.81	101.24	107.34	120.54	134.56	133.55	61.33	1.323764	.3755	25.32623495

^{*} APPROX. VALUE, PANEL C.

OTVW4413 4-30-85

#### HOT AIR RIBBED CALORIMETER TESTS

## DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .13

DATE : 4-04-85

TIME : 15:41

dTIME: 3

T AIR (F): 775

P AIR (psia):

W AIR (lb/sec): 9.483012

11.1.1. (1D) DCC) 1 71.303012

W AIR/W H2O : 25.49025 (4-PANEL AVERAGE)

W H2O (lb/sec): .372025 (4-PANEL AVERAGE)

		~~~~~~~~.	AX	IAL STATI	ONMC				W H2O			
PANEL	T IN*	1	2	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H2Ø	
A	74.04	86.96	102.05	113.94	130.33	138.98	140.9	66.86	1.417126	.3741	25.34886796	
В	73.81	89.49	91.92	106.8	109.98	123.66	120.99	47.18	1	•3658	25.92403363	
С	74	66.21 N/G	105.14	110.79	116.97	135.32	131.6	57.6	1.220856	•3741	25.34886796	
D	73.28	90.08	101.67	107.93	121.7	135.96	135.8	62.52	1.325138	.3741	25.34886796	

293

^{*} APPROX. VALUE, PANEL C.

OFVW4414 4-30-85

DATE

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .14

: 4-04-85

: 15:48 TIME

dTIME

T AIR (F):

813

W AIR (lb/sec): 7.937748

P AIR (psia):

249

W H2O (lb/sec): .372725 (4-PANEL AVERAGE)

W AIR/W H2O : 21.29653 (4-PANEL AVERAGE)

		د سد سید جد. جارجید جه. صب جد									·
PANEL	T IN*		E.F.	W H2O (lb/sec)	W AIR/W H2Ø						
			2 	3	4 .	5 	T OUT	dT		(1D/SeC)	
A	73.94	87.45	103.33	114.98	131.4	140.06	141.94	68	1.451131	.3741	21.21825053
В	73.6	90.46	92.04	107.16	109.25	122.18	120.46	46.86	1	. 3658	21.69969252
С	74	66.17 N/G	106.64	112.78	118.86	137.13	133.38	59.38	1.267179	.3769	21.06061959
D	73.1	91.4	102.85	109.66	123.7	137.99	137.74	64.64	1.379428	.3741	21.21825Ø53

^{*} APPROX. VALUE, PANEL C.

OTW4415 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

T AIR (F) : TEST NO.: .15 DATE

: 4-04-85

TIME :15:53 P AIR (psia): 252 W H2O (1b/sec): .373775 (4-PANEL AVERAGE) 5 dTIME

843

W AIR (lb/sec): 7.940365

W AIR/W H2O : 21.24370 (4-PANEL AVERAGE)

	٠		AX]	•		W H2O					
PANEL	T IN*	1	2	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H2Ø
Α	74.01	87.6	103.9	116.23	133.16	142.26	144.27	70.26	1.453455	.3755	21.14611197
В	73.67	90.87	92.56	108.12	109.55	123.03	122.01	48.34	1	.3672	21.62408781
С	73	66.79 N/G	107.73	114.13	120.44	139.48	134.94	61.94	1.281341	.3769	21.06756446
D	72.23	91.88	103.88	111.09	125.69	140.79	139.48	67.25	1.391187	•3755	21.14611197

^{*} APPROX. VALUE, PANEL C.

OTVW4416 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .16 T AIR (F) : 863 W AIR (lb/sec): 7.848848 DATE : 4-04-85

TIME : 15:58 P AIR (psia): 251 W H2O (lb/sec): .373425 (4-PANEL AVERAGE)

dTIME: 5

W AIR/W H2O : 21.01854 (4-PANEL AVERAGE)

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PANEL	T IN*	1	2 	IAL STATIO	ON4	5	T OUT	dT	E.F.	W H2O (lb/sec)	W AIR/W H2Ø
A	73.62	88.04	104.76	117.23	134.65	143.73	145.79	72.17	1.452113	.3755	20.90239227
В	73.29	91.28	92.94	109	110.66	124.4	122.99	49.7	1	.3658	21.45666566
С	73	67.Ø4 N/G	108.72	115.14	121.64	141.12	135.47	62.47	1.256942	.3769	20.82475006
D	71.95	92.15	104.7	112.13	127.05	142.6	141.15	69.2	1.392354	•3755	20.90239227

^{*} APPROX. VALUE, PANEL C.

OTVW4417 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .17 T AIR (F) : 873 W AIR (lb/sec): 7.850505

DATE : 4-04-85
TIME : 16:01 P AIR (psia): 252 W H2O (lb/sec): .372375 (4-PANEL AVERAGE)

dTIME : 3

W AIR/W H2O : 21.08226 (4-PANEL AVERAGE)

				W H2O							
PANEL	T IN*	1	2	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H2Ø
Α	73.54	87.91	104.88	117.59	135.28	144.8	147.27	73.73	1.455676	.3741	20.98504446
В	73.2	91.14	92.92	109.31	111.53	125.42	123.85	50.65	1	.3658	21.46119501
С	73	67.85 N/G	109.6	115.31	122.06	141.76	138.14	65.14	1.286081	·3755	20.90680462
D	72.85	91.9	104.92	112.16	127.17	142.97	142.76	69.91	1.380257	.3741	20.98504446

^{*} APPROX. VALUE, PANEL C.

OTVW4418 4-30-85

: 4-04-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

T AIR (F): TEST NO.: .18 887 W AIR (lb/sec): 7.778611 DATE

TIME : 16:06 P AIR (psia): 251 W H2O (lb/sec): .372375 (4-PANEL AVERAGE)

dTIME

W AIR/W H2O : 20.88919 (4-PANEL AVERAGE)

				W H2O							
PANEL	T IN*	1	2	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H2Ø
Α	73.5	88.12	105.49	118.51	136.63	145.91	148.89	75.39	1.4585Ø3	.3741	20.79286583
В	73.13	91.29	93.24	109.55	112.42	126.52	124.82	51.69	1	.3658	21.26465584
С	73.5	68.61 N/G	109.1	116.06	122.79	142.9	140.07	66.57	1.287870	.3755	20.71534250
D	73.52	91.85	105.27	112.86	128.21	144.09	144.82	71.3	1.379377	.3741	20.79286583

^{*} APPROX. VALUE, PANEL C.

OTVW4419 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .19 T AIR (F): 893 W AIR (lb/sec): 7.792266

DATE : 4-04-85

TIME :16:08 P AIR (psia): 252 W H2O (lb/sec): .372025 (4-PANEL AVERAGE) dTIME : 2

W AIR/W H2O : 20.94554 (4-PANEL AVERAGE)

			AX	IAL STATIO	ON					W H2O	
PANEL	T IN*	1	2	3	4	5	T OUT	dТ	E.F.	(lb/sec)	W AIR/W H20
Ą	73.55	88.17	105.66	118.67	136.65	146.25	149.04	75.49	1.457055	.3741	20.82936691
В	73.2	91.74	93.39	110.3	112.33	126.52	125.01	51.81	1	.3658	21.30198513
С	73	68.64 N/G	109.53	116.48	123.14	143.52	139.55	66.55	1.284501	.3741	20.82936691
D	72.79	91.9	105.32	113.04	128.64	144.46	144.28	71.49	1.379849	.3741	20.82936691

^{*} APPROX. VALUE, PANEL C

OTVW442Ø 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .20.

: 4-04-85

DATE : 16:09

TIME **dTIME** T AIR (F):

893

W AIR (lb/sec): 7.792266

P AIR (psia):

252

W H2O (lb/sec): .372375 (4-PANEL AVERAGE)

W AIR/W H2O : 20.92586 (4-PANEL AVERAGE)

			AX	IAL STATIO	ON			خبارة فينته نشبك مدين أحاة البات الباد فيناد الباد الباد الباد الباد	حيد جين ين آبيد خشر جان يبن نبيد اين خود الدو جين الدول	W H2O	
PANEL	T IN*	1	2	3	4	5	T OUT	dT	E.F.	(lb/sec)	W AIR/W H2Ø
Α	73.6	88.27	105.69	118.8	136.73	146.41	149.37	75.77	1.459642	.3741	20.82936691
В	73.22	91.76	93.4	110.2	112.41	126.66	125.13	51.91	1	•3658	21.30198513
С	73	68.64 N/G	109.47	116.63	123.42	143.6	140.12	67.12	1.293007	•3755	20.75170748
D	72.98	92.09	105.61	113.37	129	145.21	144.92	71.94	1.385860	.3741	20.82936691

^{*} APPROX. VALUE, PANEL C.

OTVW4421 4-30-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .21. T AIR (F): 625 W AIR (lb/sec): 8.667044

DATE : 4-04-85

TIME : 16:15 P AIR (psia): 251 W H2O (lb/sec): .37205 (4-PANEL AVERAGE) dTIME : 7

W AIR/W H2O : 23.29537 (4-PANEL AVERAGE)

			yy	IAL STATIO	WI				ليو هيونون ۽ بيت مون هيو جيڪ پيونيون آگا آها آها هيو المان اليون	W H2O	پر چین نشن هدر نیچ شد. نیپی شده نشاه نیند شده شده شده شده شده شده شده
PANEL	T IN*	1	2	3	4	5	T OUT	dТ	E.F.	(lb/sec)	W AIR/W H2Ø
A	73.65	84.78	97.56	106.82	119.96	126.83	127.56	53.91	1.417565	.3728	23.24850788
В	73.36	87.54	88.46	100.46	102.77	113.74	111.39	38.03	1	.3658	23.69339458
С	73.5	73.9 N/G	101.04	104.88	109.68	124.19	121.81	48.31	1.270313	•3755	23.08134151
D	73.91	87.36	97.13	101.96	113.34	124.85	125.25	51.34	1.349987	.3741	23.16771916

^{*} APPROX. VALUE, PANEL C.

OTVW48Ø5 4-29-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .05

:4-08-85 DATE

TIME : 12:06

dTIME

T AIR (F): 9Ø3

P AIR (psia): 198 W AIR (lb/sec): 6.099994

W H2O (lb/sec):

.3679 (4-PANEL AVERAGE)

W AIR/W H2O : 16.58058 (4-PANEL AVERAGE)

			AX	TAI. STATI					يسم مهيد النهيد چين چين پويد منه منظ خمل سند جدې خود کمن اخت	خیب نیبن سبی میبوشند امام خیب کنار فلب د	عيدر چين بنت مدد هيي خود الله الله طيار الله الله الله الله الله الله الله ال
PANEL	T IN	1	2	3	4		T OUT	dT	E.F.	W H2O	W AIR/W H2Ø
Α	73.13	85.35	99.89	110.43	125.41	133.74	135.92	62.79	1.508650	.3686	16.54908807
В	72.86	87.46	89.02	102.46	104.7	116.87	114.48	41.62	1	•3672	16.61218373
С	72.35	86.98	106.45	109.01	114.86	133.23	128.08	55.73	1.339020	.3672	16.61218373
D	72.44	88.21	100.46	107.19	119.63	133.31	131.94	59.5	1.429601	.3686	16.54908807

OTVW48Ø6 4-29-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .06 T AIR (F): 912 W AIR (lb/sec): 5.097335

DATE : 4-08-85

TIME : 12:16 P AIR (psia): 166 W H2O (1b/sec): .3672 (4-PANEL AVERAGE)
dTIME : 10

W AIR/W H2O : 13.88163 (4-PANEL AVERAGE)

			AX	IAL STATI	ON						
 PANEL	T IN	1	2	3	4	5	T OUT	dT	E.F.	W H2O	W AIR/W H2Ø
A	73.26	84.41	97.49	107.03	120.34	127.21	129.53	56.27	1.544606	.3686	13.82890640
В	72.99	85.37	87.41	99.2	101.5	112.06	109.42	36.43	1	•3658	13.93475916
С	72.51	85.88	102.41	105.44	110.71	126.94	122.13	49.62	1.362064	.3658	13.93475916
D	73.15	86.51	97.79	103.66	114.91	127.03	126.05	52.9	1.452100	.3686	13.82890640

OTVW4807 4-29-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .07 T AIR (F): 913 W AIR (lb/sec): 5.064783

DATE : 4-08-85
TIME : 12:21 P AIR (psia): 165 W H2O (1b/sec): .3693 (4-PANEL AVERAGE)

dTIME: 5

W AIR/W H2O: 13.71455 (4-PANEL AVERAGE)

--AXIAL STATION-----2 T OUT dТ E.F. W H2O W AIR/W H2Ø 3 T IN 1 4 5 PANEL 107.02 120.39 129.51 56.27 1.544606 .37 13.68860171 97.45 127.46 73.24 84.39 Α 72.98 85.87 87.48 99.28 101.27 111.87 109.41 36.43 .3672 13.79298103 В 105.39 110.71 126.95 48.73 1.337634 .37 C 72.51 85.84 102.71 121.24 13.68860171 1.456217 .37 13.68860171 97.75 103.64 114.83 127.18 125.23 53.05 D 72.18 86.51

OTVW48Ø8 4-29-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .08 T AIR (F): 915 W AIR (lb/sec): 5.091771

DATE : 4-08-85

TIME : 12:31 P AIR (psia): 166 W H2O (1b/sec): .280275 (4-PANEL AVERAGE)

dTIME : 10 W AIR/W H2O : 18.16705 (4-PANEL AVERAGE)

			AX	IAL STATIO	ON							
PANEL	T IN	1	2	3	4	5	T OUT	dT	E.F.	W H2O	W AIR/W H2Ø	
A	73.06	89.33	117.27	133.06	135.49	146.4	145.34	72.28	1.539182	.2796	18.21091250	
В	73.08	91.05	102.01	110.97	110.9	125.29	120.04	46.96	1	. 281	18.12018198	
С	72.7	92	131.74	133.89	123.93	145.37	135.74	63.04	1.342419	.2782	18.30255620	
D	72.15	92.45	119.37	125.45	129.55	145.54	140.63	68.48	1.458262	.2823	18.03673799	

OTVW48Ø9 4-29-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .09 T AIR (F): 916 W AIR (lb/sec): 5.028596

DATE : 4-08-85
TIME : 12:36 P AIR (psia): 164 W H2O (lb/sec): .27785 (4-PANEL AVERAGE)

dTIME: 5

W AIR/W H2O: 18.09824 (4-PANEL AVERAGE)

		ه حباد هدی هفاد ختن هفتر سنتن سپن پیزید در حبادر جایی دلیان کندار کردی در باید پیری	AX	IAL STATIO	ON		فتقد الله في القبلية القديد القبلية المبادلة في المبادلة المبادلة المبادلة المبادلة المبادلة المبادلة المبادلة	را خوري الناف لِلقائل طلبي طويل فيهي طوري فيهل طويد ويوس			
PANEL	T IN	1	2	3	4	5	T OUT	dТ	E.F.	W H2O	W AIR/W H2Ø
A	73.04	88.82	116.55	133.68	134.64	146.06	144.84	71.8	1.536815	. 2768	18.16689396
В	73.1	91.15	101.73	110.96	110.91	125.28	119.82	46.72	1	•2782	18.07547177
С	72.66	91.57	132.79	133.84	123.24	144.83	136.35	63.69	1.363228	• 2754	18.25924563
D	73.18	92.8	119.61	126.71	129.05	145.13	141.18	.68	1.455479	.281	17.89536031

OTVW481Ø 4-29-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .10 T AIR (F) : 916 W AIR (lb/sec): 8.984016

DATE : 4-08-85
TIME : 12:39 P AIR (psia): 293 W H2O (1b/sec): .280275 (4-PANEL AVERAGE)

dTIME : 3

W AIR/W H2O : 32.05429 (4-PANEL AVERAGE)

					و جين فين خيال فين فيل فين خين هيال الماء الماء						
PANEL	T IN	1	AX	IAL STATI 3	ON	5	T OUT	dТ	E.F.	W H2O	W AIR/W H2Ø
* * * * * * * * * * * * * * * * * * * *			<u> </u>	~					LI 0 1 0		
A	72.8	93.92	128.2	139.35	158.06	173.65	174.57	101.77	1.450955	•2796	32.13167549
В	72.96	97.68	112.4	125.89	126.27	148.27	143.1	70.14	1	.281	31.97158885
С	72.5	96.28	145.94	144.44	140.36	169.38	160.9	88.4	1.260336	.2782	32.29337335
D	72.11	100.47	132	133.74	147.9	170.29	167.61	95.5	1.361563	.2823	31.82435872

OTVW4811 4-29-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .11 T AIR (F): 894 W AIR (lb/sec): 9.056709

DATE : 4-08-85
TIME : 12:43 P AIR (psia): 293 W H2O (lb/sec): .279575 (4-PANEL AVERAGE)

dTIME: 4

W AIR/W H2O : 32.39456 (4-PANEL AVERAGE)

			AX	IAL STATI	ON						
PANEL	T IN	1	2	3	4	5	T OUT	dТ	E.F.	W H2O	W AIR/W H2Ø
Α	72.79	93.51	127.65	138.82	156.26	171.74	172	99.21	1.441377	.2782	32.55467007
В	72.95	97.31	111.76	125.09	125.65	147.32	141.78	68.83	1	.2796	32.39166386
c	72.48	95.76	146.11	143.55	139.02	167.5	159.56	87.Ø8	1.265146	•2782	32.55467007
D	72.77	100.01	130.62	132.97	146.54	168.45	166.02	93.25	1.354787	.2823	32.08186048

OTVW4812 4-29-85

HOT AIR RIBBED CALORIMETER TESTS

DATA SUMMARY: BULK COOLANT T AND PANEL COOLANT TEMPERATURE PROFILE

TEST NO.: .12

DATE : 4-08-85

: t2:48 TIME

dTIME 5 T AIR (F):

P AIR (psia):

698

290

W AIR (lb/sec): 9.692947

W H2O (lb/sec): .27925 (4-PANEL AVERAGE)

W AIR/W H2O : 34.71064 (4-PANEL AVERAGE)

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PANEL	T IN	1	2	3	ON	5	T OUT	dТ	E.F.	W H2O	W AIR/W H2Ø
A	73.02	90.06	121.26	135.74	139.83	152.93	150.61	77.59	1.414327	.2782	34.84165117
В	73.13	93.3	105.58	116.13	115.73	134	127.99	54.86	1	•2796	34.66719369
С	72.82	91.79	136.43	136.78	126.32	149.44	140.57	67.75	1.234962	.2782	34.84165117
D	72.52	95.93	123.81	133.15	132.64	149.33	146.03	73.51	1.339956	.281	34.49447458

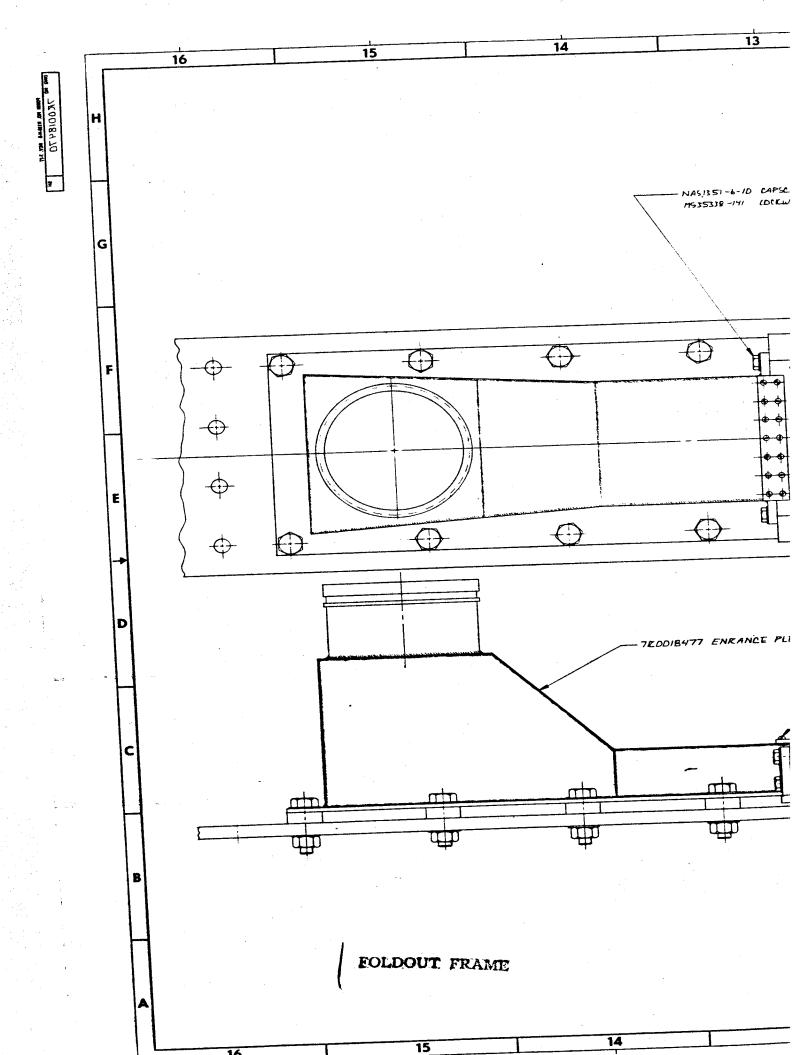
APPENDIX C RIB COLD FLOW TESTS

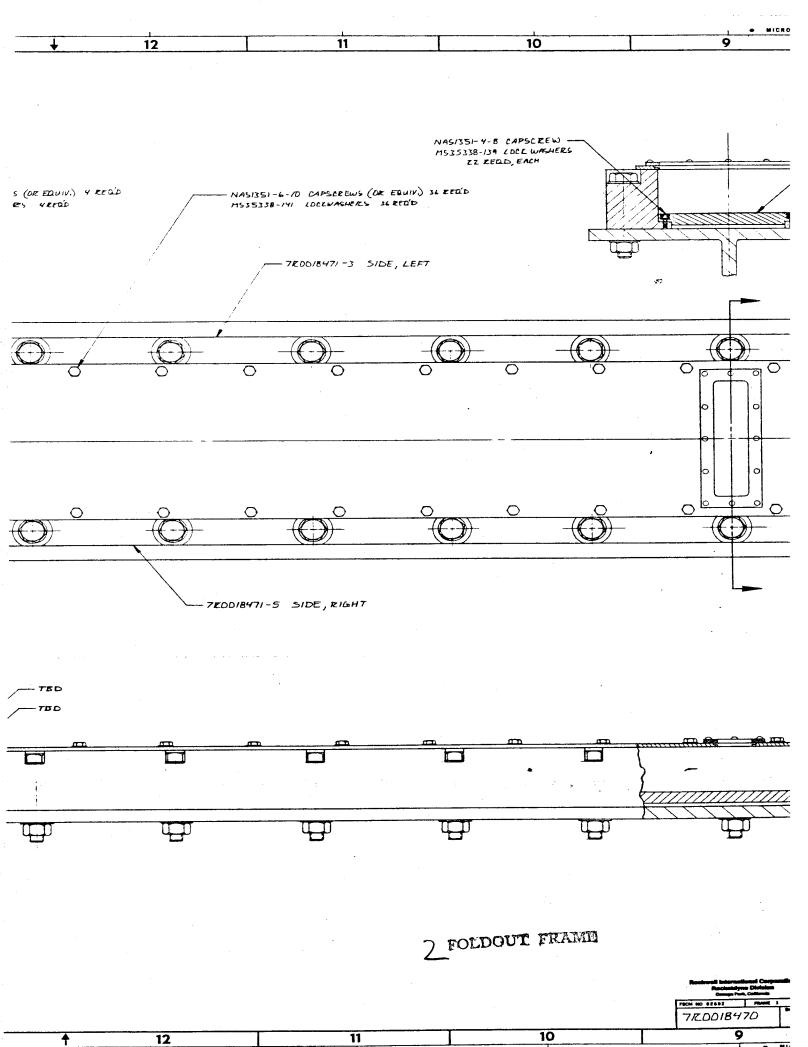
RIB COLD FLOW FIXTURE DRAWINGS

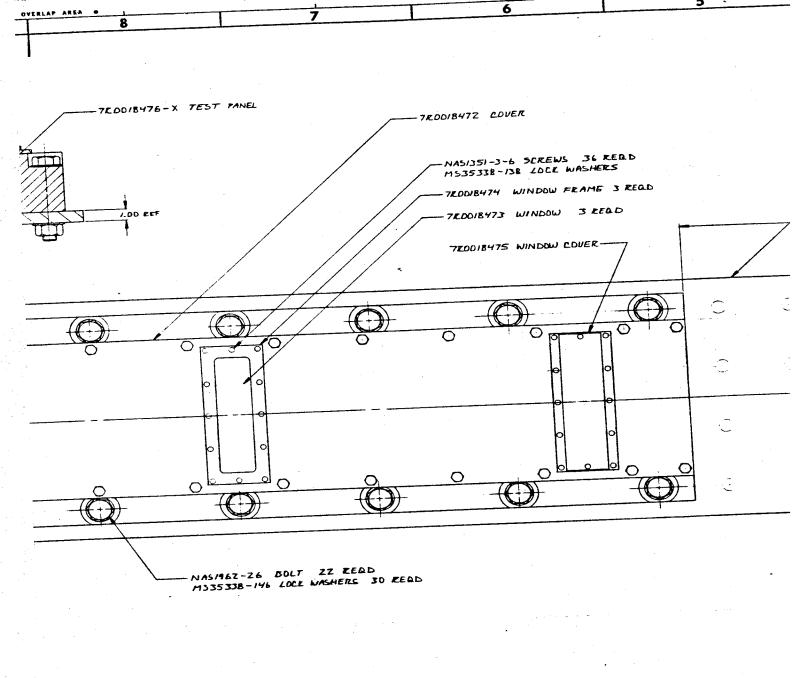
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7R0018475 7R0018476

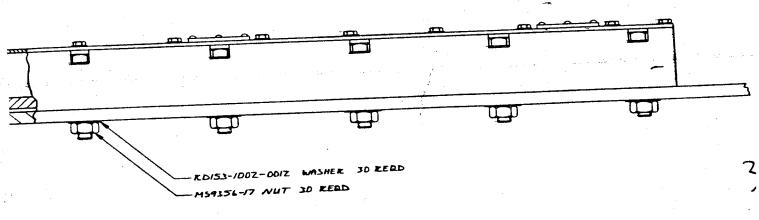
TEST PLAN
TEST DATA

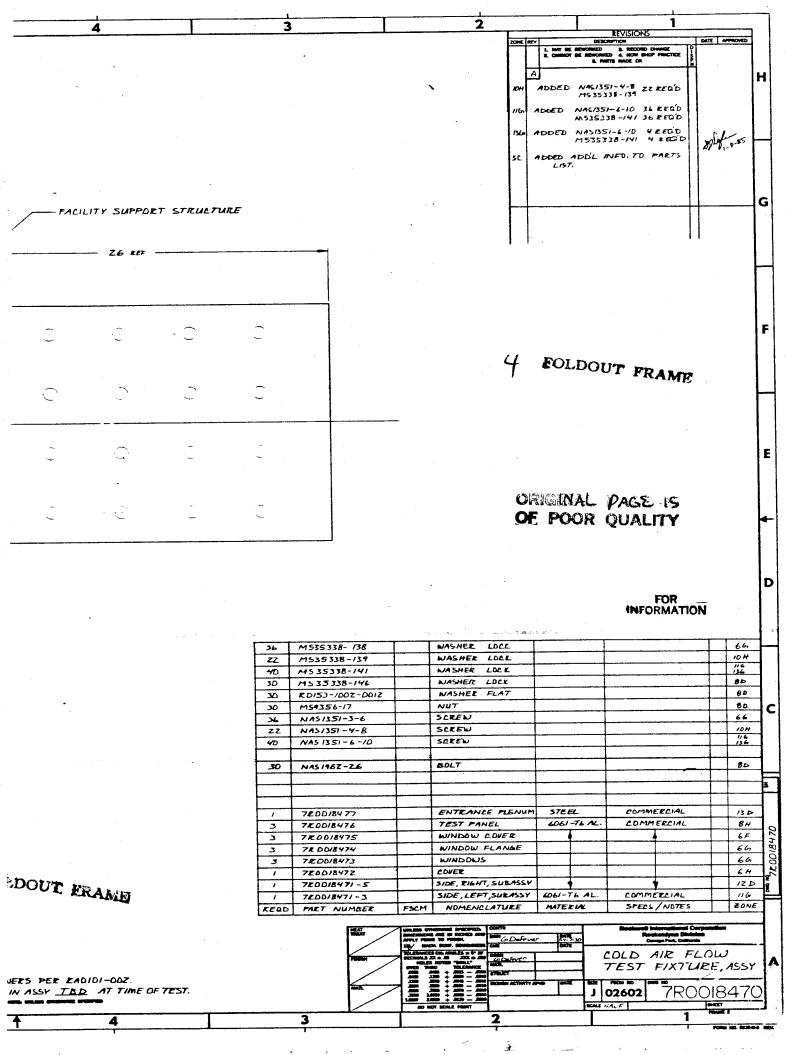
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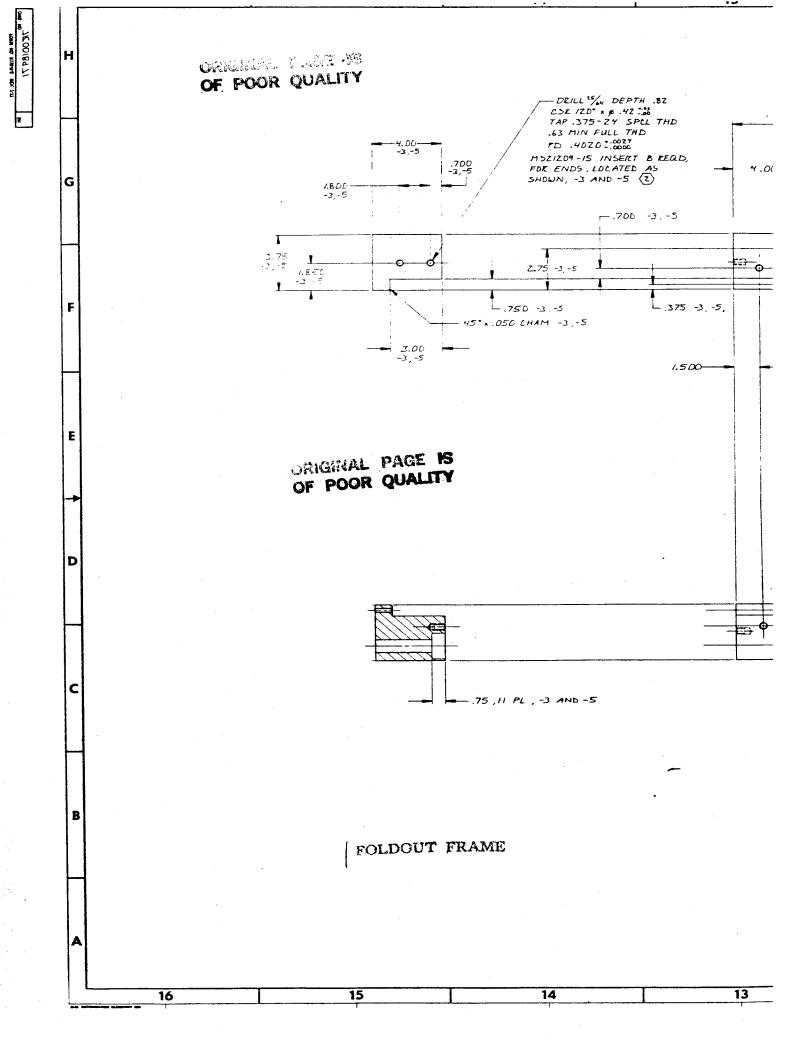


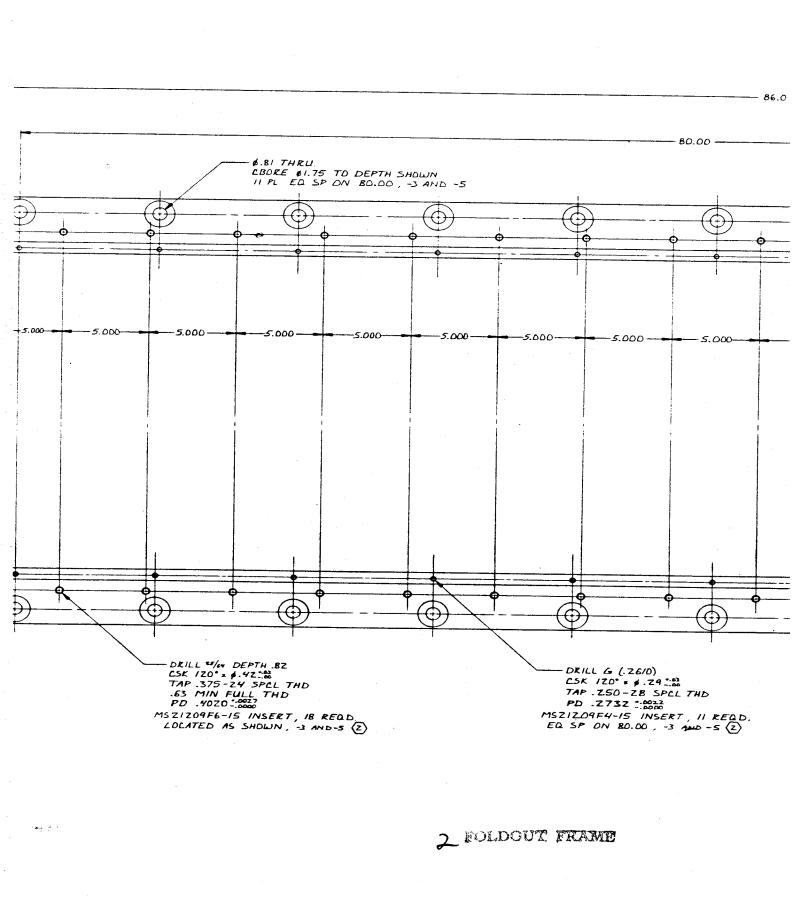






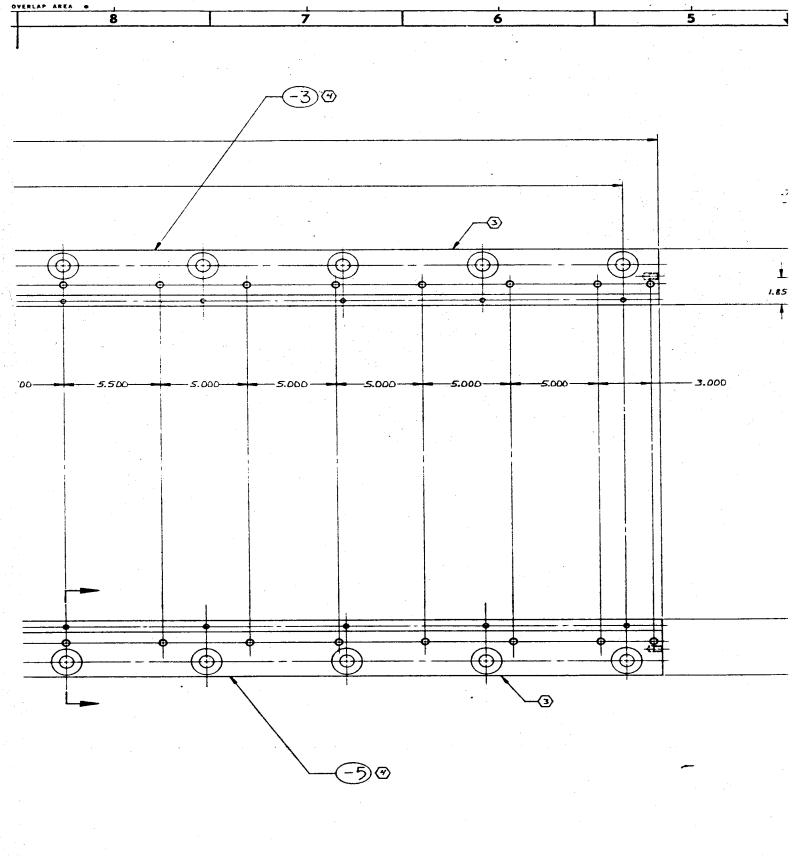






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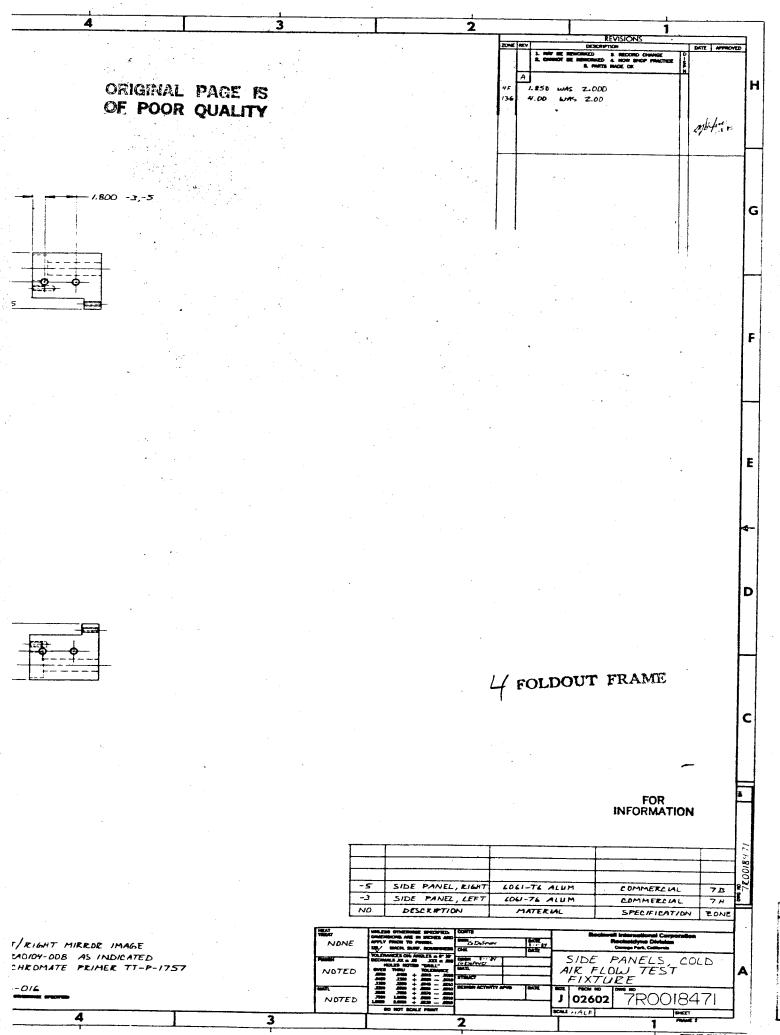
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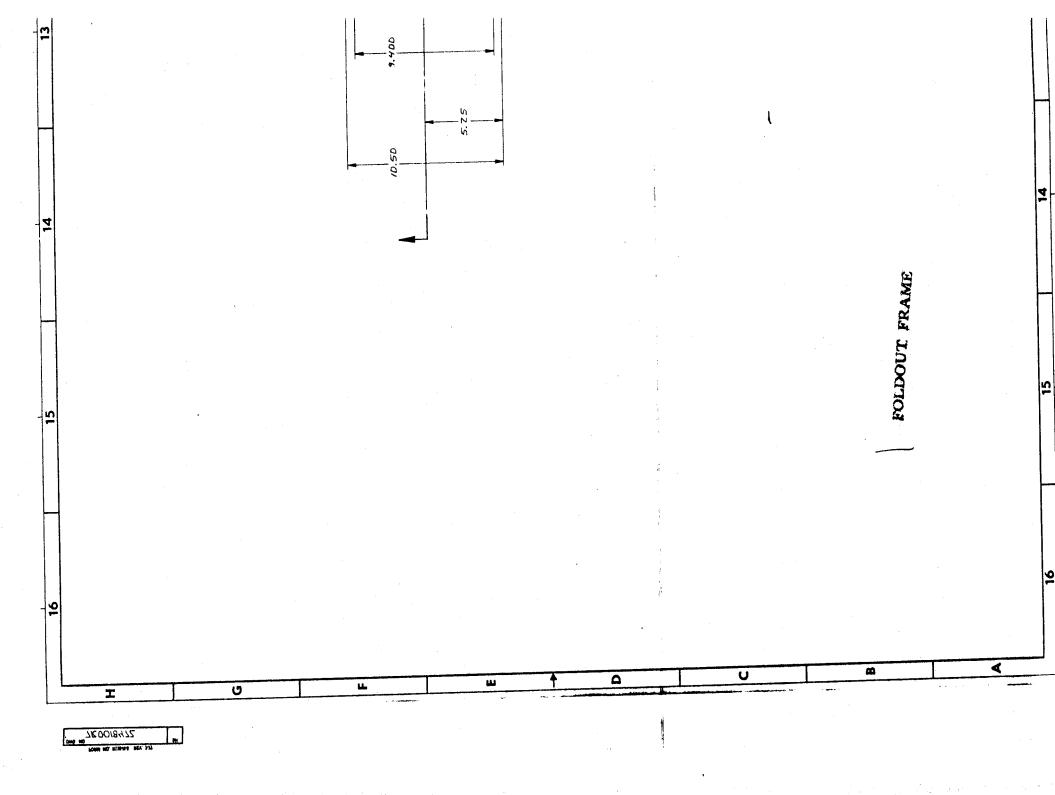


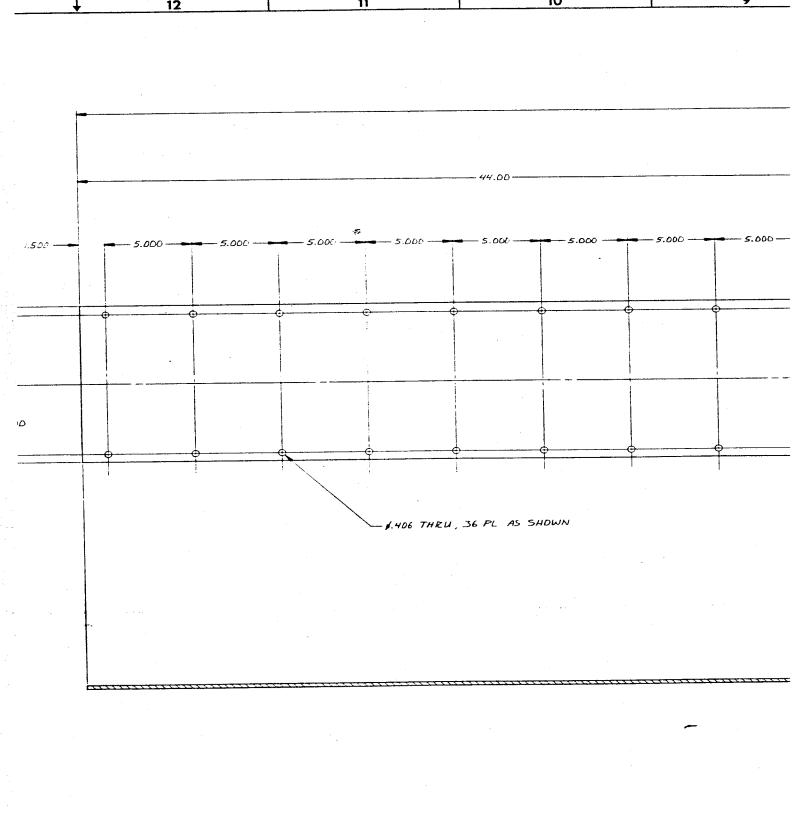
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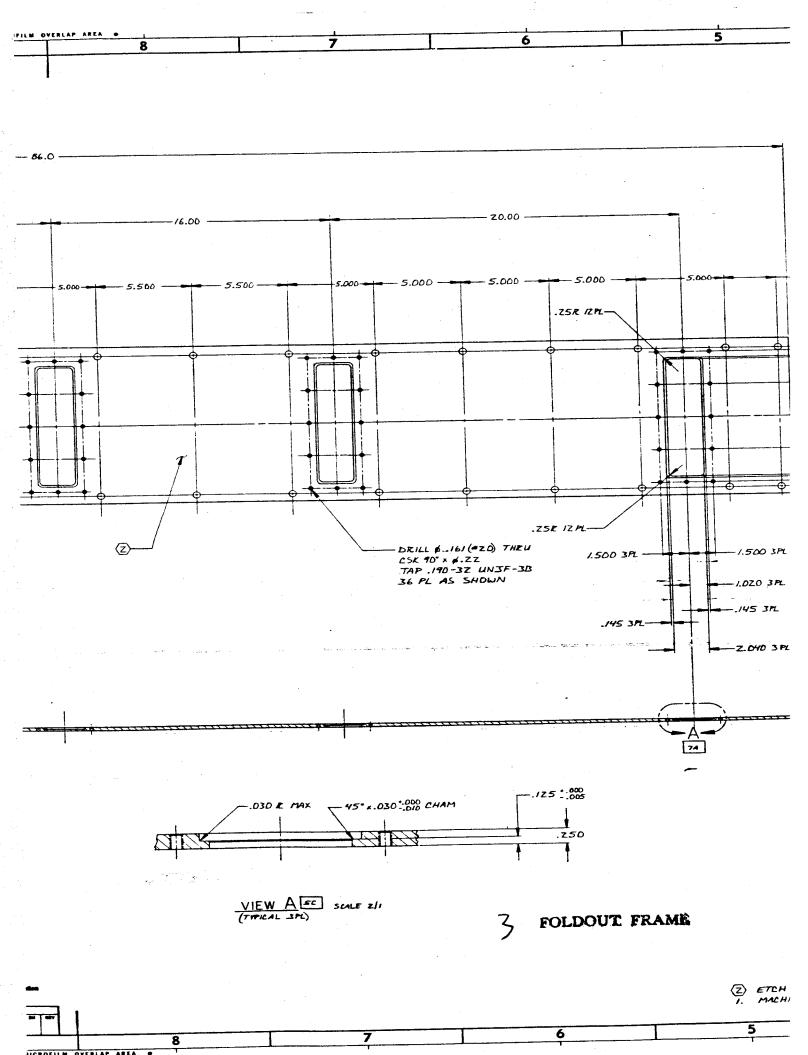
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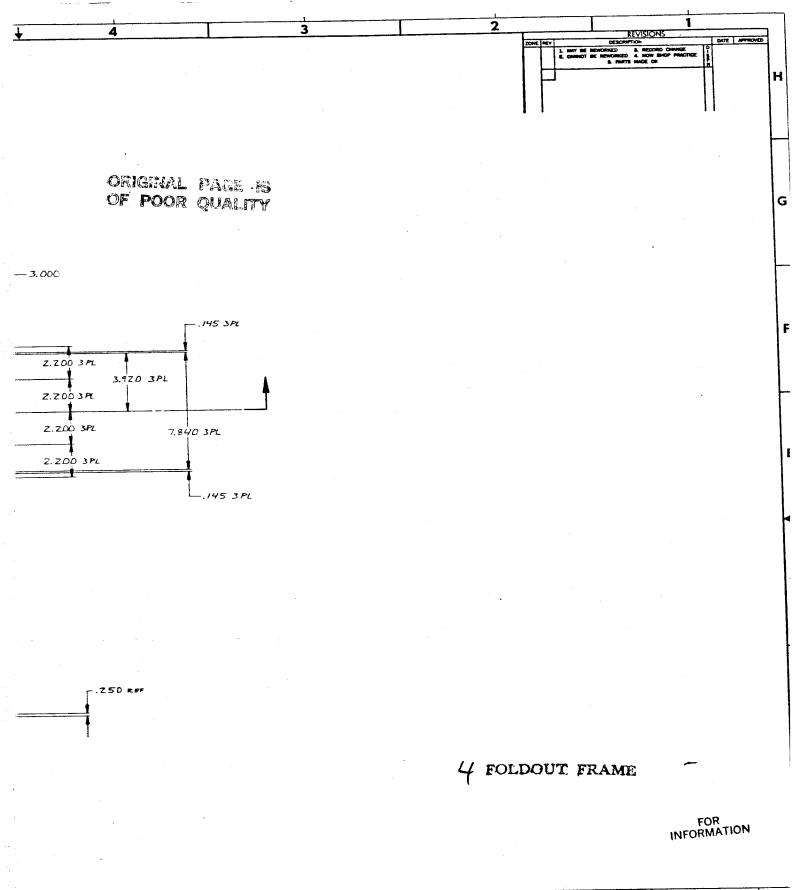
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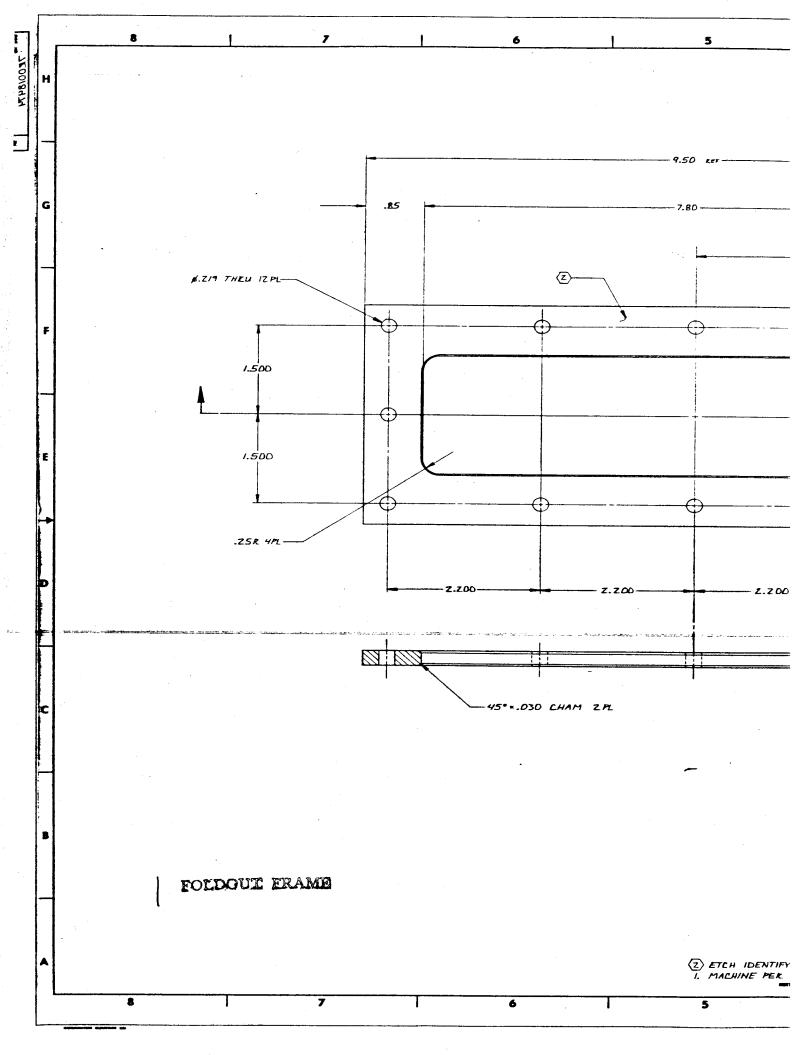


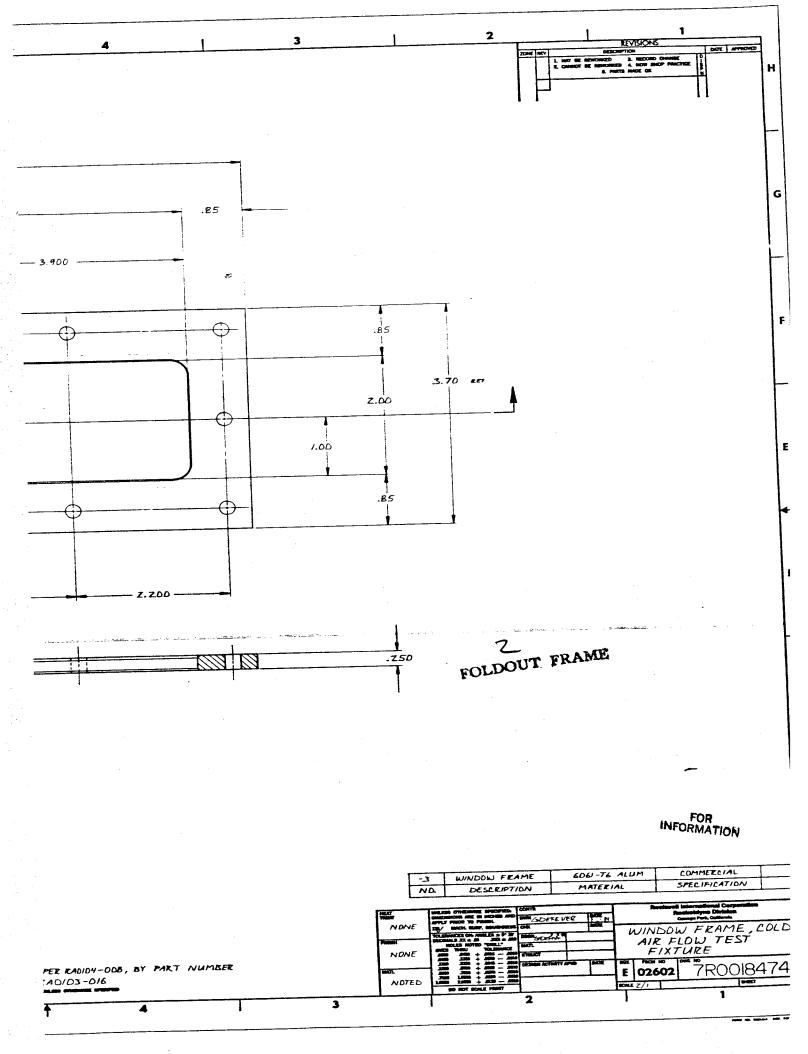


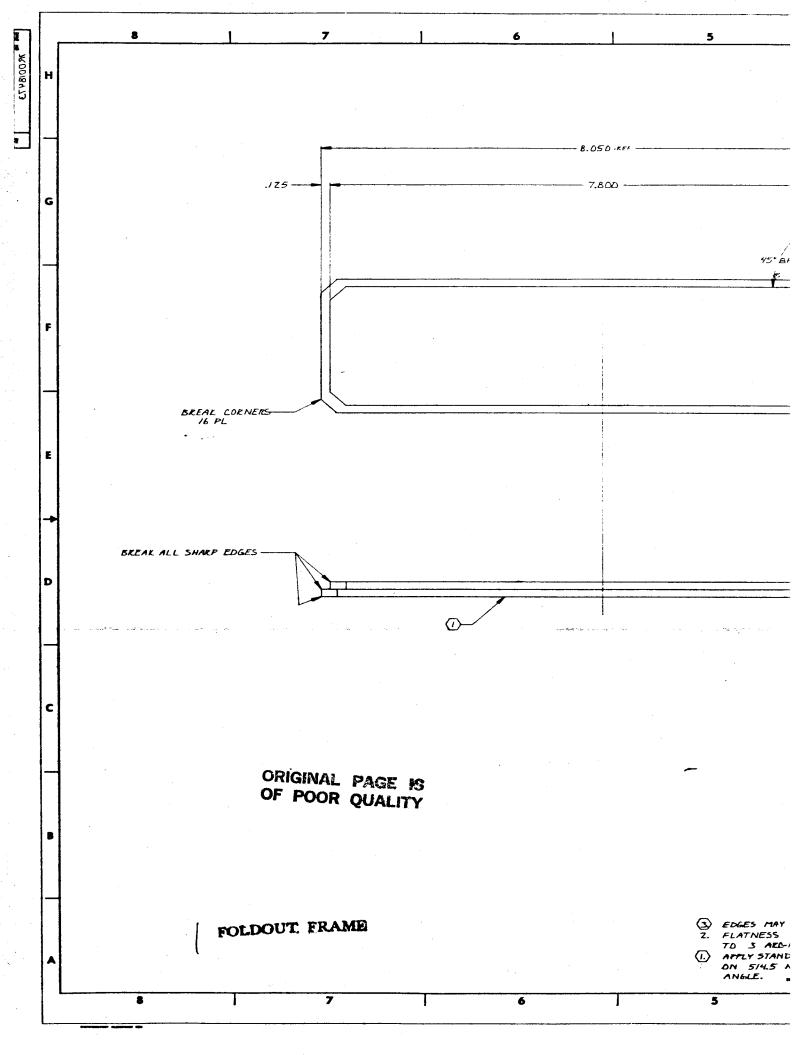
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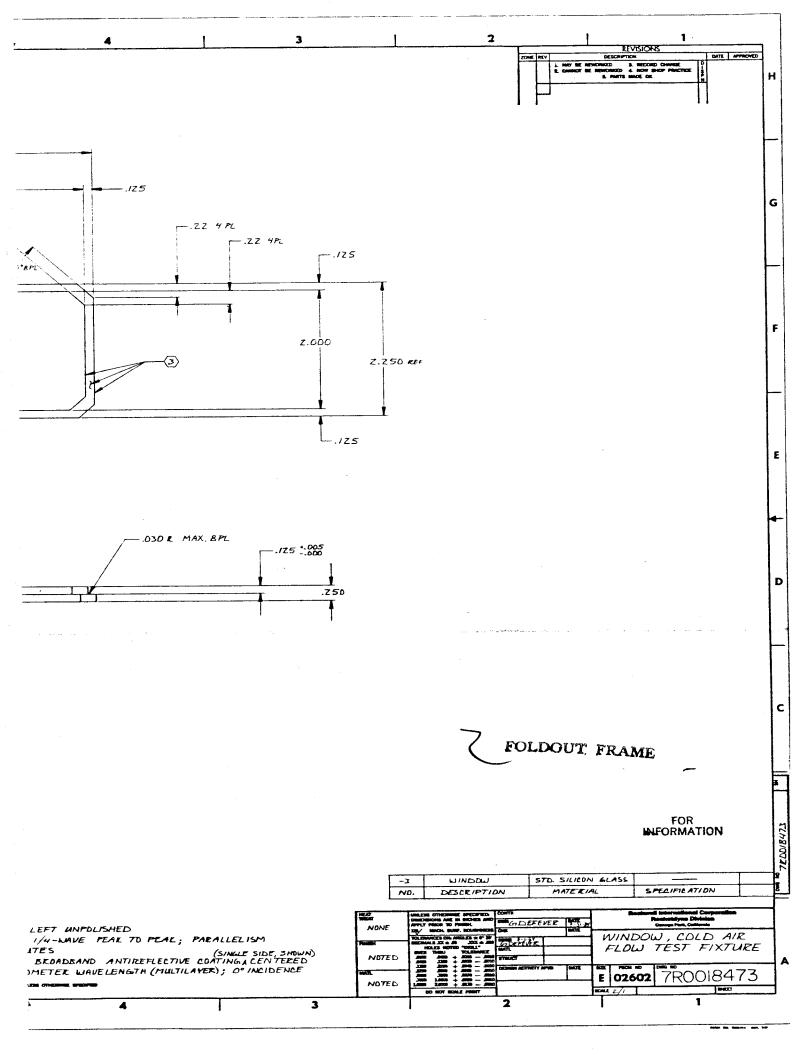
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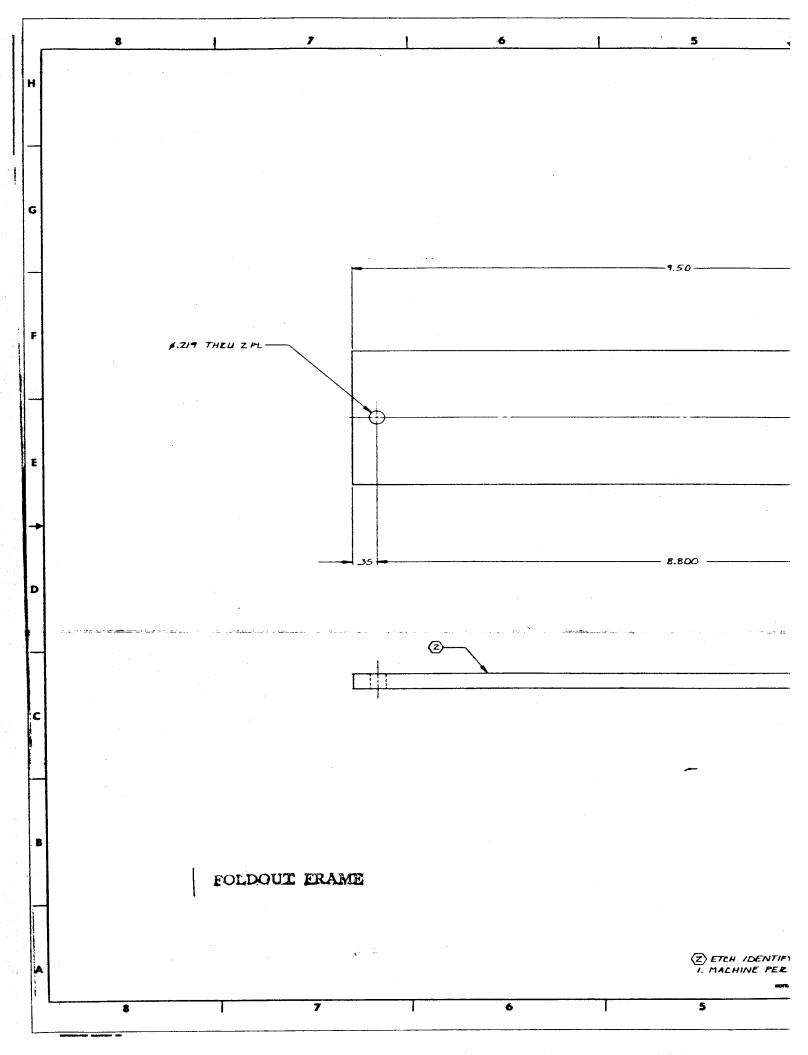
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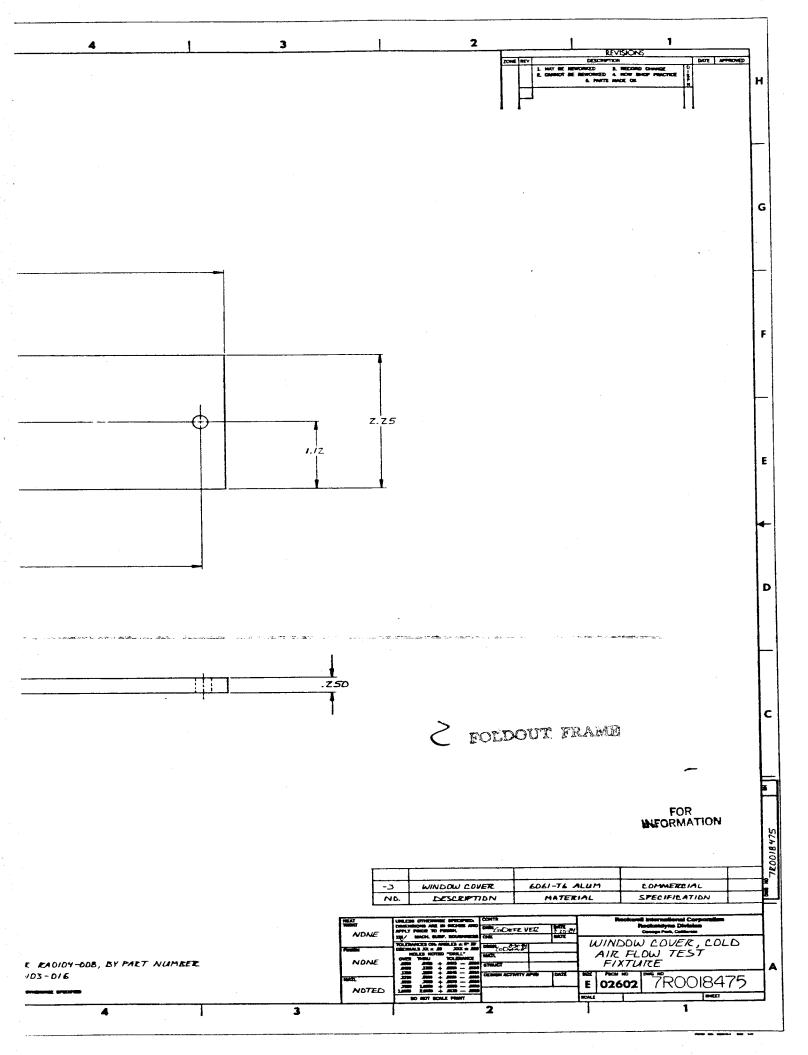


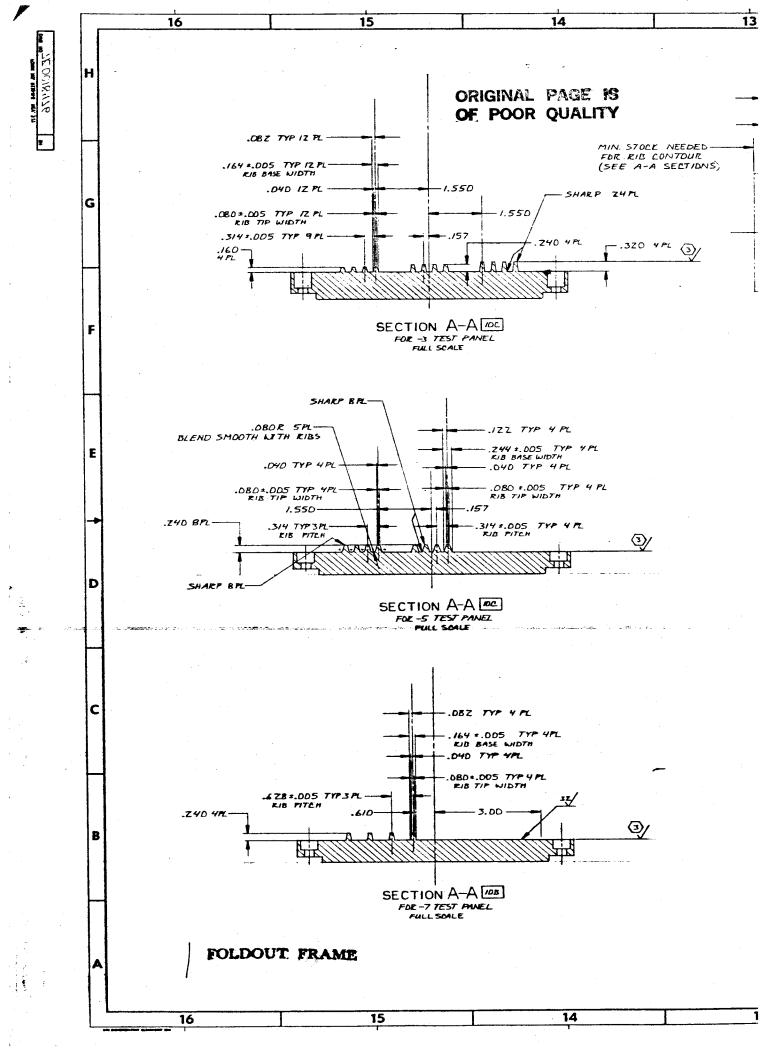


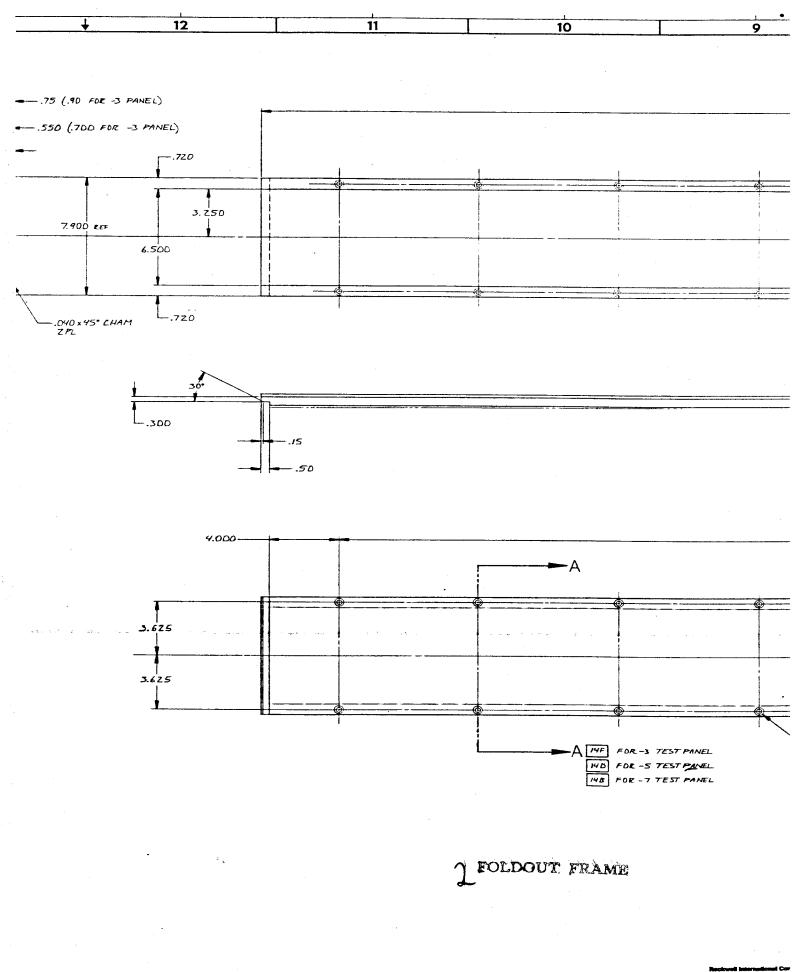




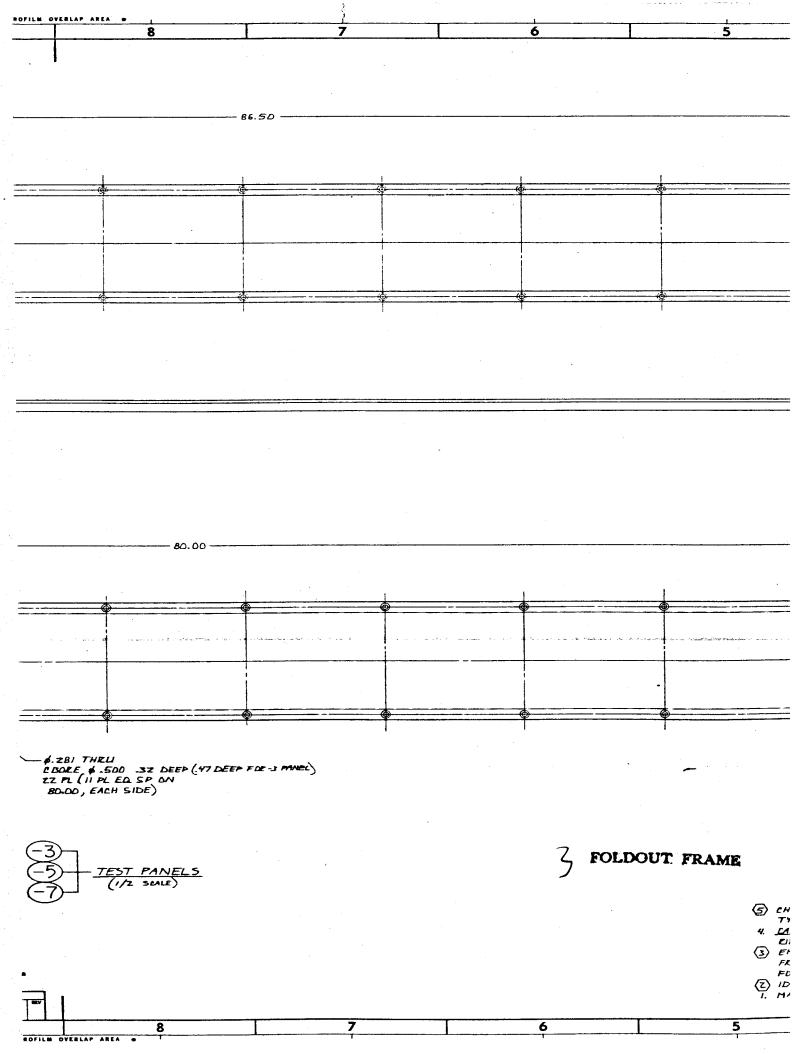


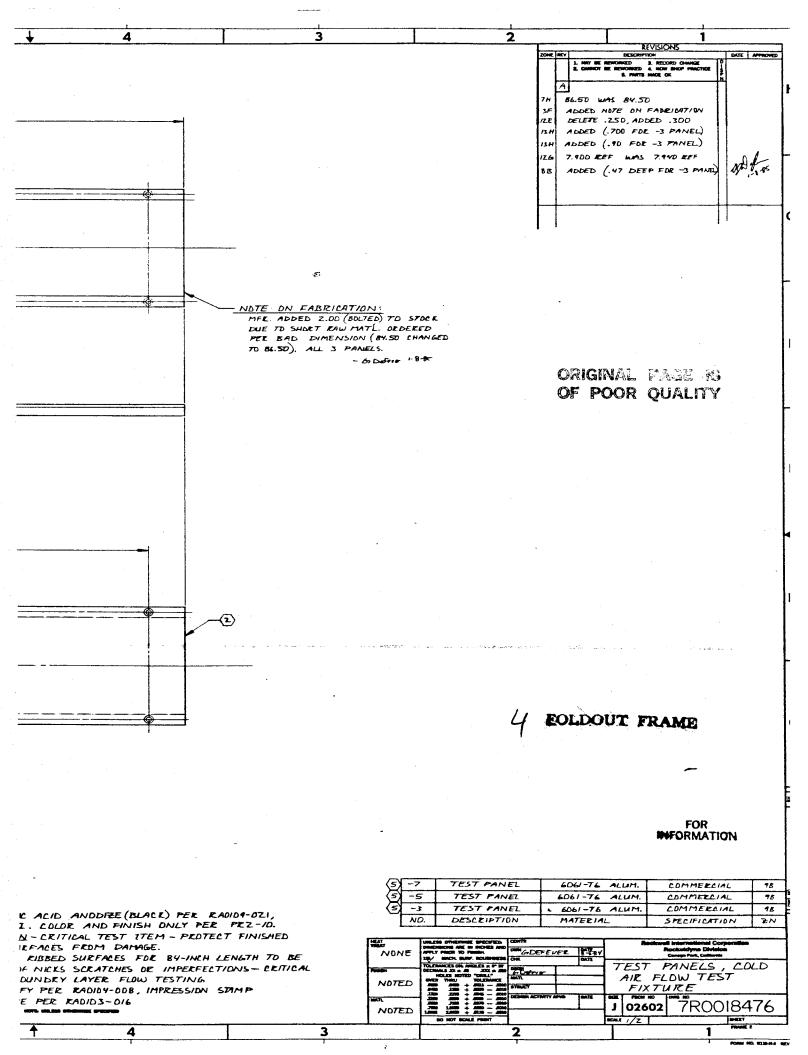


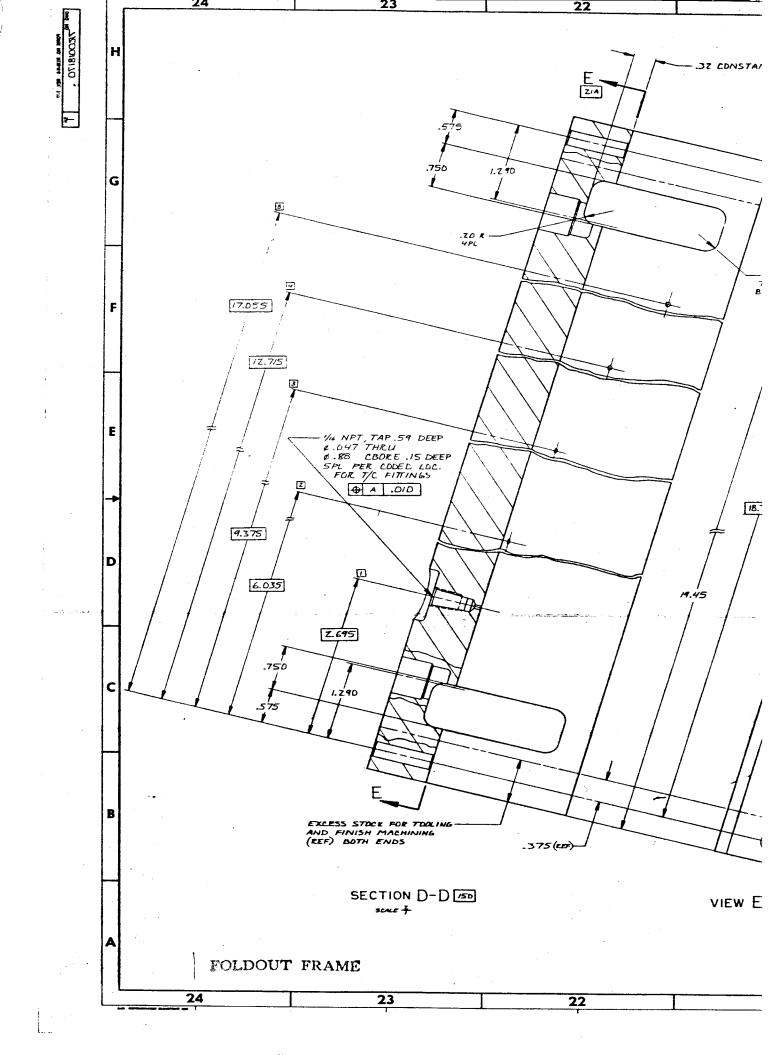


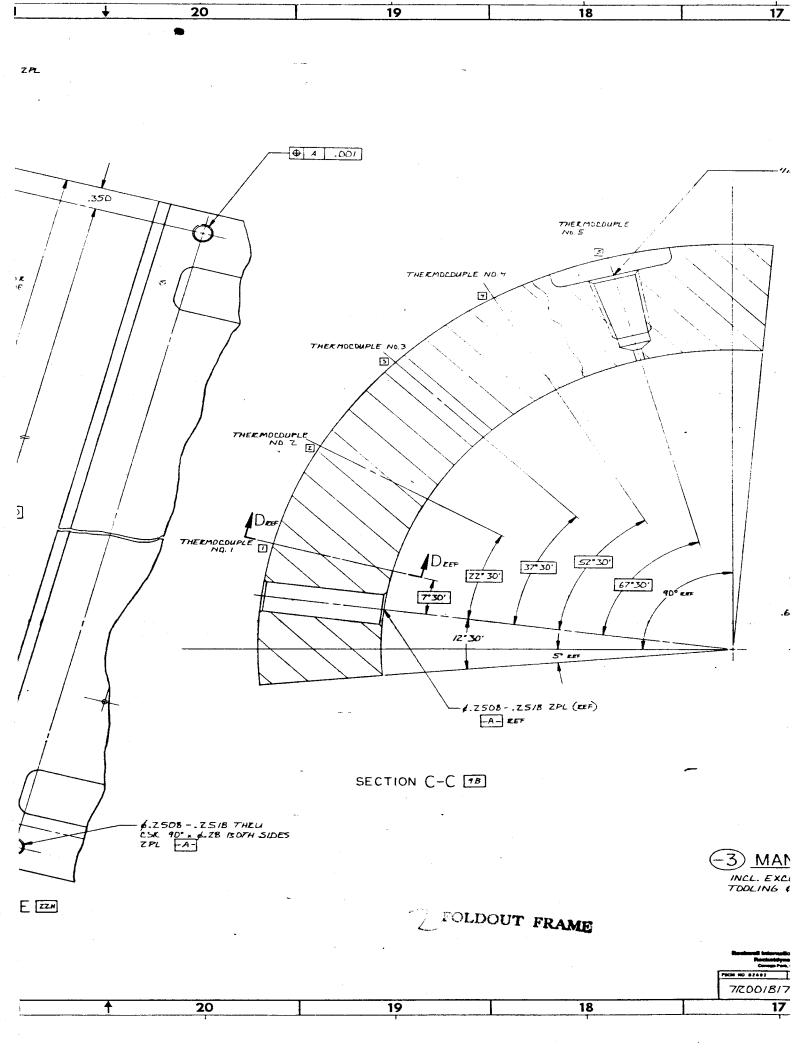


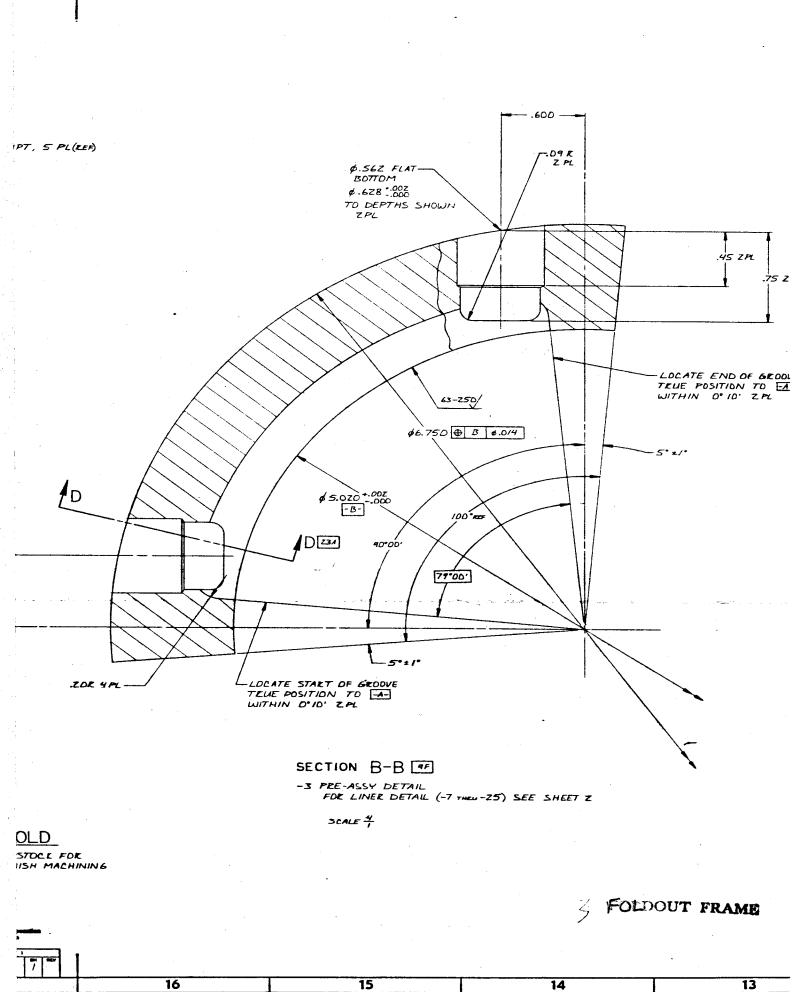
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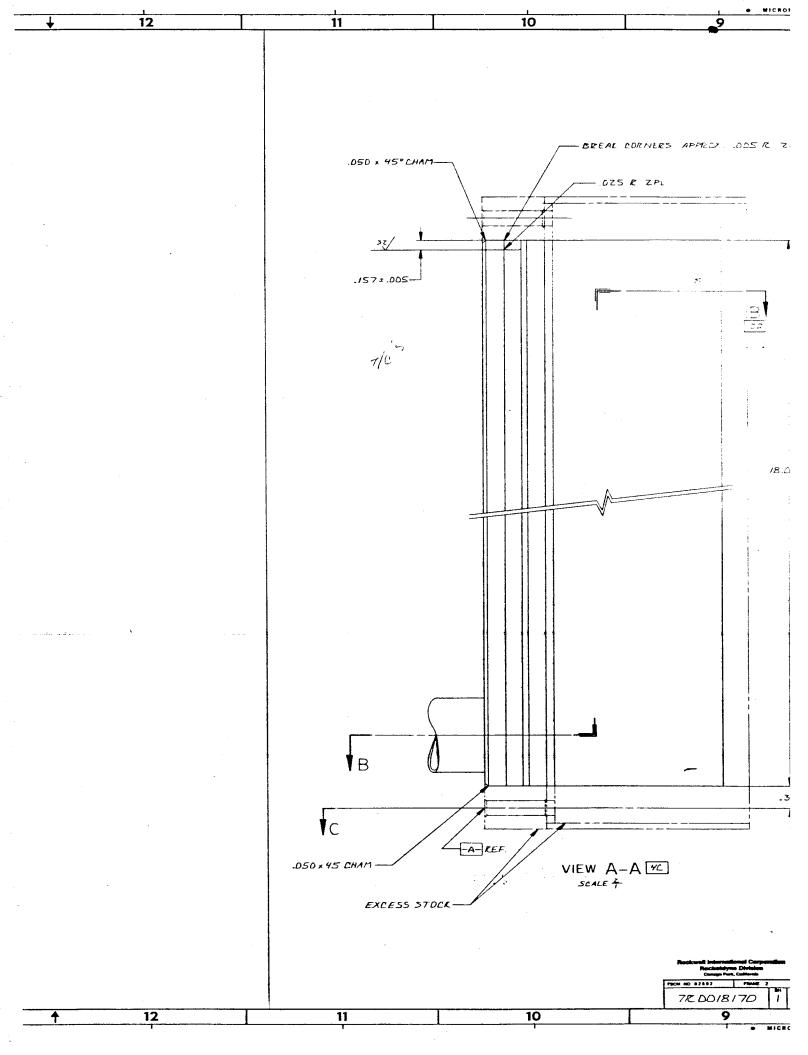


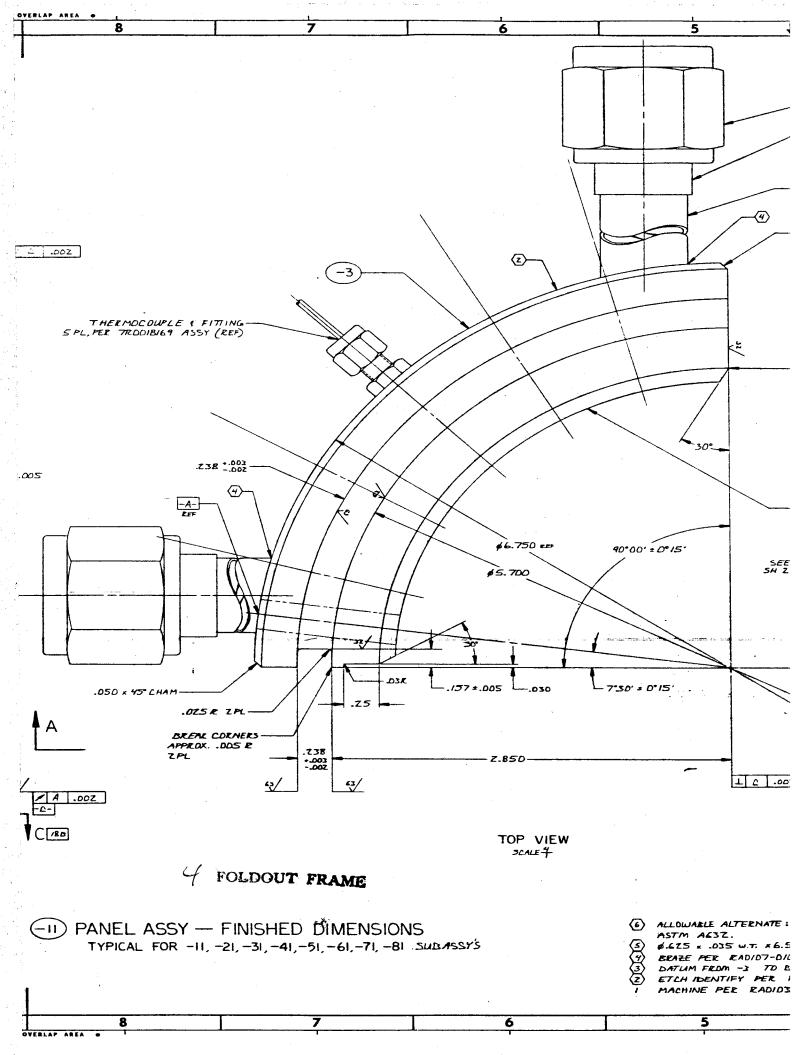


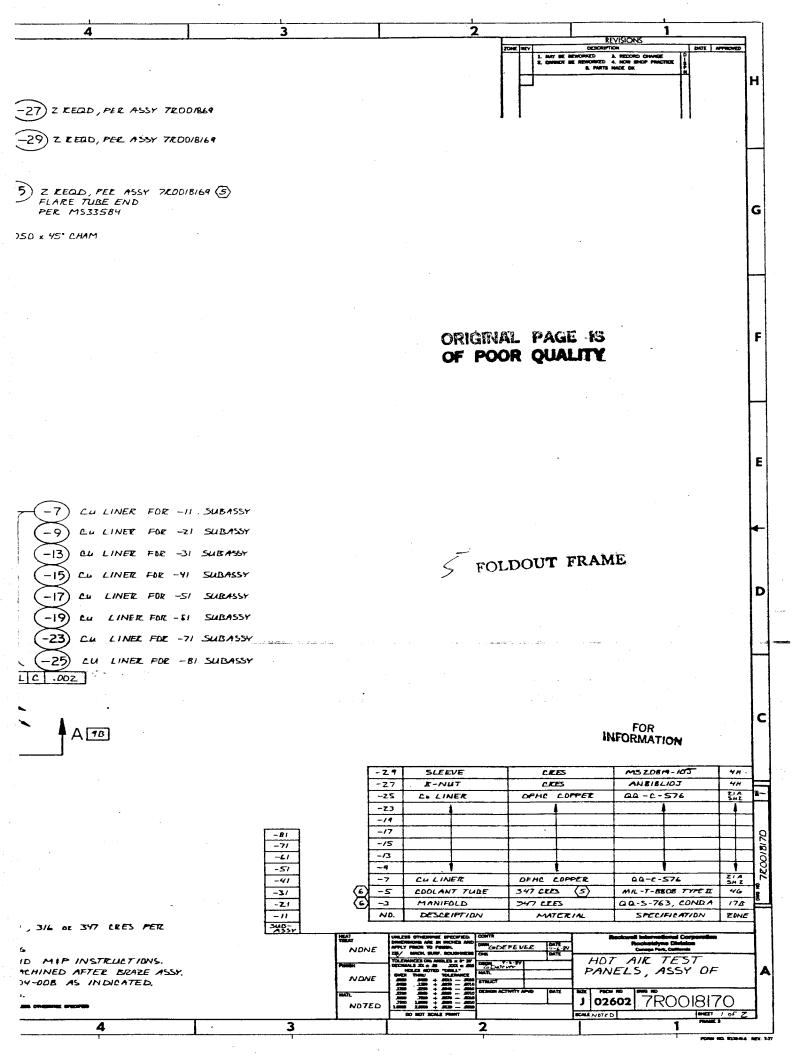




MICROFILM OVERLAP AREA







The following describes planned testing to be conducted in the Rocketdyne Experimental Development Laboratory (EDL). The testing is being conducted as part of Contract NAS3-23773 Enhanced Heat Transfer Combustor Technology, with NASA Lewis Research Center.

SUMMARY

An 80 inch long air-flow chamber will be fabricated and supplied to the EDL for testing. The chamber assembly will stand vertically, and be rigidly mounted to a structural beam to be supplied by the EDL. The chamber assembly will consist of 2 side pieces, a windowed cover plate, and 5 removable test panels (see drawing). Test data will be collected using Laser Velocimeter equipment, to be supplied by the Rocketdyne Turbomachinery Group. (ref. Tom Ferguson). Tests will be conducted in the "helium shack" area of the EDL, utilizing the large Spencer blower located there. Schematics of the test set-up are shown in Figure 1.

TEST PLAN

Two test series are planned in an effort to map the boundry layer flow field about 6 different rib shapes and 8 channel shapes, on five interchangable test panels. These test series are shown in Tables 1 and 2. Finalized testing matrix will be determined after flat plate calibration and analysis has been completed. Total number of test points and test velocity ranges will depend significantly on data aquisition rate and quality of data.

Test data aquisition will be accomplished utilizing the Laser Velocimeter. Facility preparation, calibration and testing will be conducted per the schedule presented in Figure 2. Instrumentation requirements are listed in Table 2. Some flow measurements may be acquired from instrumentation already a part of the Spencer blower assembly. This will be determined during facility preparation.

All test data in the test series will be acquired at steady-state flow conditions. Parameters required to monitor the facility test set-up during testing will be displayed on digital read-out and recorded periodically during data aquisition.

Actual testing will consist of relatively long steady state air flow runs for data collection. Length of individual test runs will depend on factors such as particle density and distribution within the boundary layer and will be better known after initial calibration tests.

Once the apparatus is assembled, calibrated and the running of matrix tests is initiated, the use of a lab technician full time may not be necessary. Start-up, shut-down, and test panel changes will be the only major lab tasks during the data collection phase.

-Pro-....<u>.</u>

TABLE 1 PRELIMINARY TEST MATRIX - COLD FLOW TESTS OF HOT GAS WALL RIBS

TEST SERIES 1:

	RIB PATTERN	WINDOW	VELOCITY	PRESSURE	TEMPERATURE	COMMENTS	
		POSITION (IN)	(1b/sec)	(psig)	(F)		
	Smooth	80	· 300.	Ambient	Ambient	Checkout & Baselin	e
		60	H		H	н	
		44	н	11	и	u	
	1	80	300	Ambient	Ambient	Velocity Profile	
Ď		60			on Pattern	•	
Ġ.			Ħ	H	W	H H	
	•	44	N	*	•	н	
	2	80	300	Ambient	Ambient on Pattern	Velocity Profile	
• • • •		60	44	H	H	n	
		44	11	N	н	#	
	3	80	300	Ambient	Ambient on Pattern	Velocity Profile	
		60	H	×	н	11	
		44	tt	H	H	и	
	4	80	300	Ambient	Ambient on Pattern	Velocity Profile	
		60	11	W	ĸ	Ħ	
		44	H			н	
	5	80	300	Ambient	Ambient on Pattern	Velocity Profile	
		60	H	u	H	Ħ	
		44	Ħ	*	u	н	
	6	80	300	Ambient	Ambient on Pattern	Velocity Profile	
		60	M	•	И	n	
		44	u			n	

1943/d

1943/d

A typical test day would consist of the following:

- Start-up of blower and velocimeter equipment.
- 2. Monitor flow conditions and manually adjust flow to set required flow velocity for test.
- 3. Record velocimeter data on boundary layer and flow conditions for as many points as time allows.
- 4. Shut-down of blower and velocimeter equipment.
- 5. Process data acquired-check content, quality; plan next tests.

Monitoring of test conditions and data collection will be accomplished by engineering personnel.

A drawing of the test fixture hardware assembly is included as figure 3. Assembly of the fixture will be directly to an upright beam secured firmly to the floor. Rigidity of the test assembly is important to the acquisition of accurate data with the velocimeter. Location of the test fixture with respect to the blower and test area will be such that in the event of a priority need for the blower facility during the course of these tests, the air flow piping can be readily moved. This would eliminate any need to disassemble or move the panel test fixture during the testing program, minimizing impact on test schedule should such a need arise.

G.J. Defever
Member of the Technical Staff
Advanced Combustion Devices

GJD:kw 2164/d

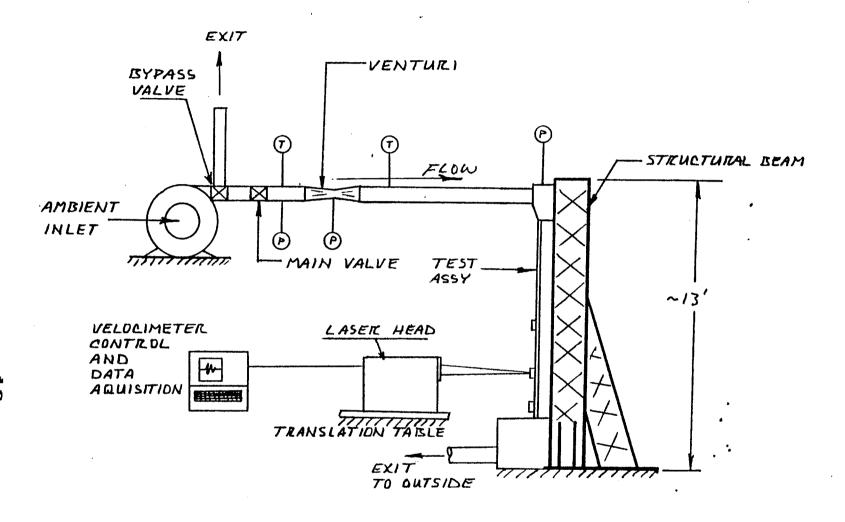


FIGURE 1. COLD FLOW TEST APPARATUS

		ت	ANUAR	4	FEBRUARY			•
	/	. 2	3	4	5	6	7	8
		∇				,		
FACILITY SET-UP		T	T					
CALIBRATION								
TESTING								

V HOWR RECEIVED FROM VENDOR

FIGURE Z.

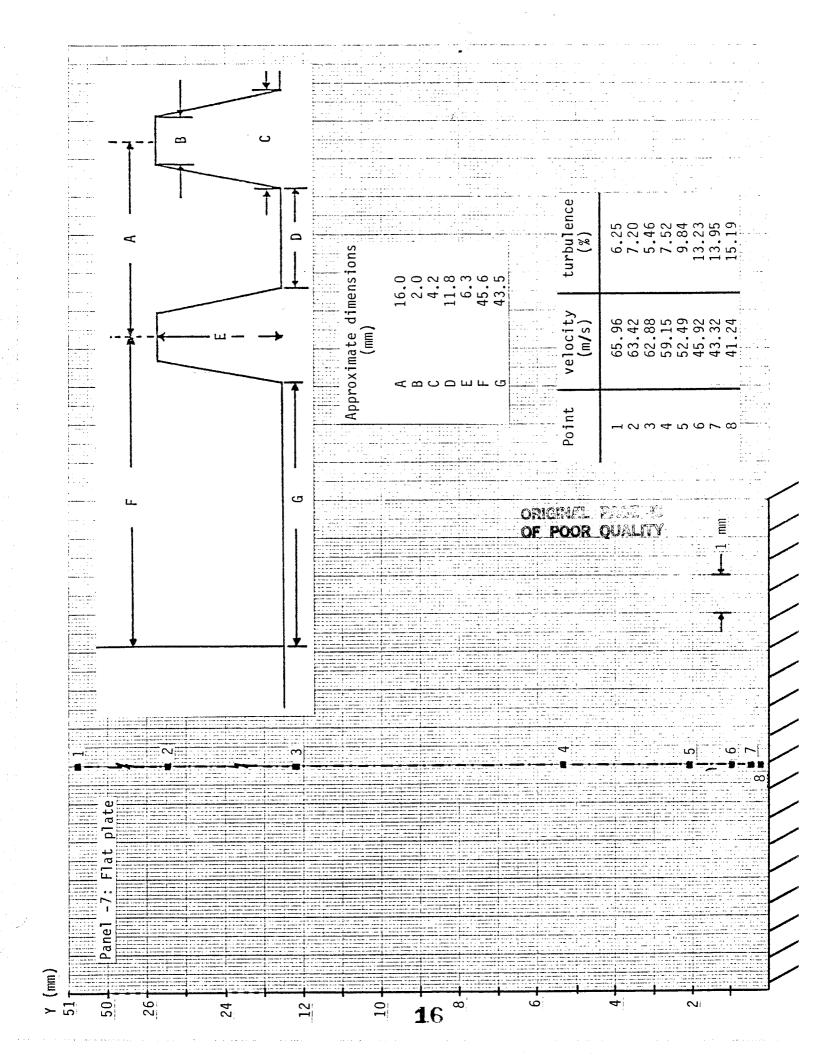
SCHEDULE, COLD AIR FLOW TESTING

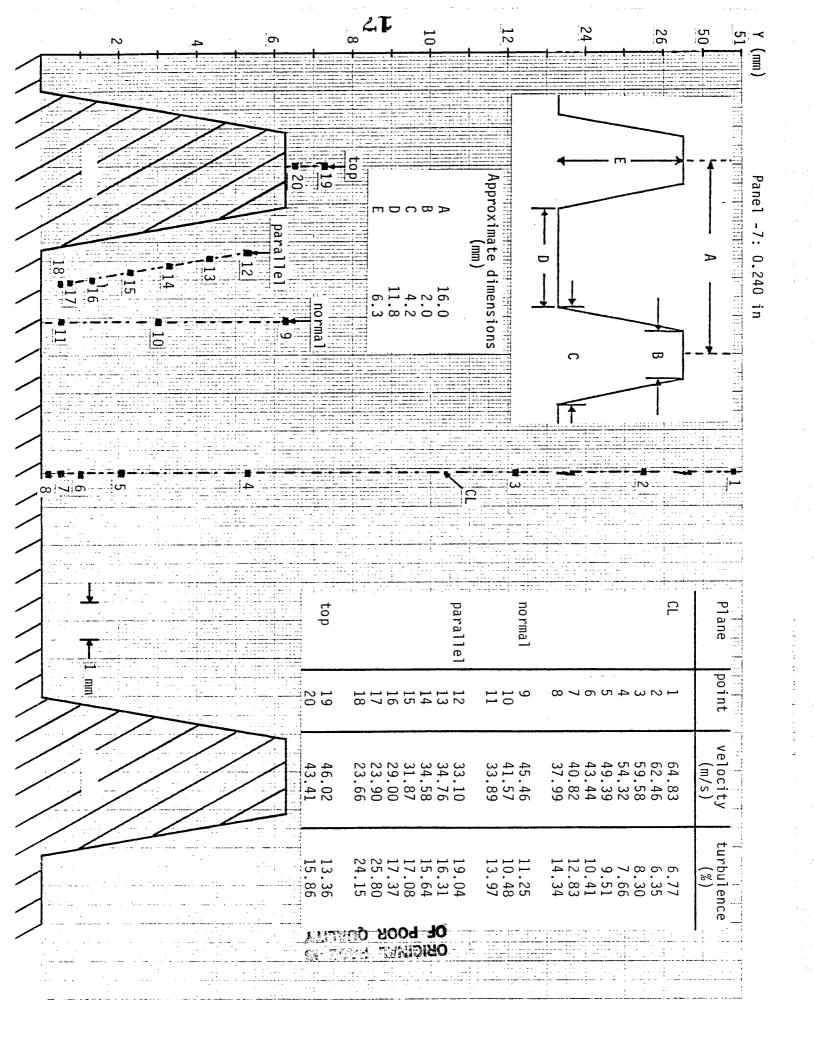
TABLE 3

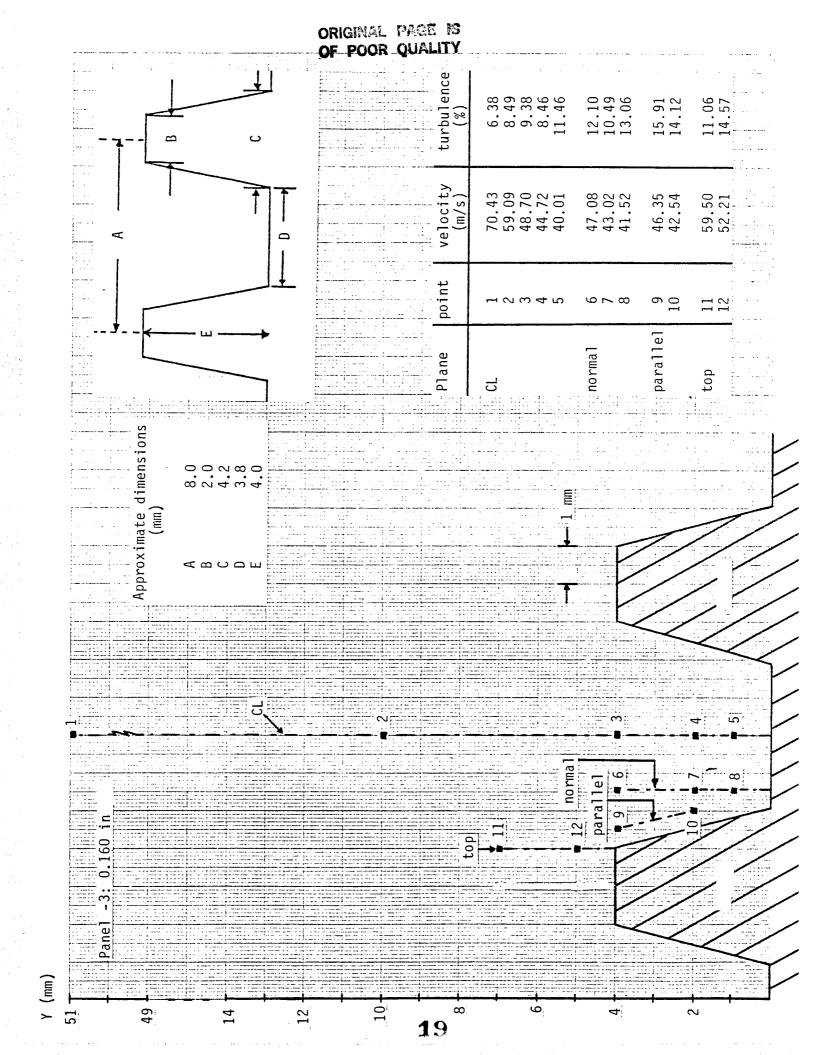
INSTRUMENTATION LIST - COLD FLOW TESTS

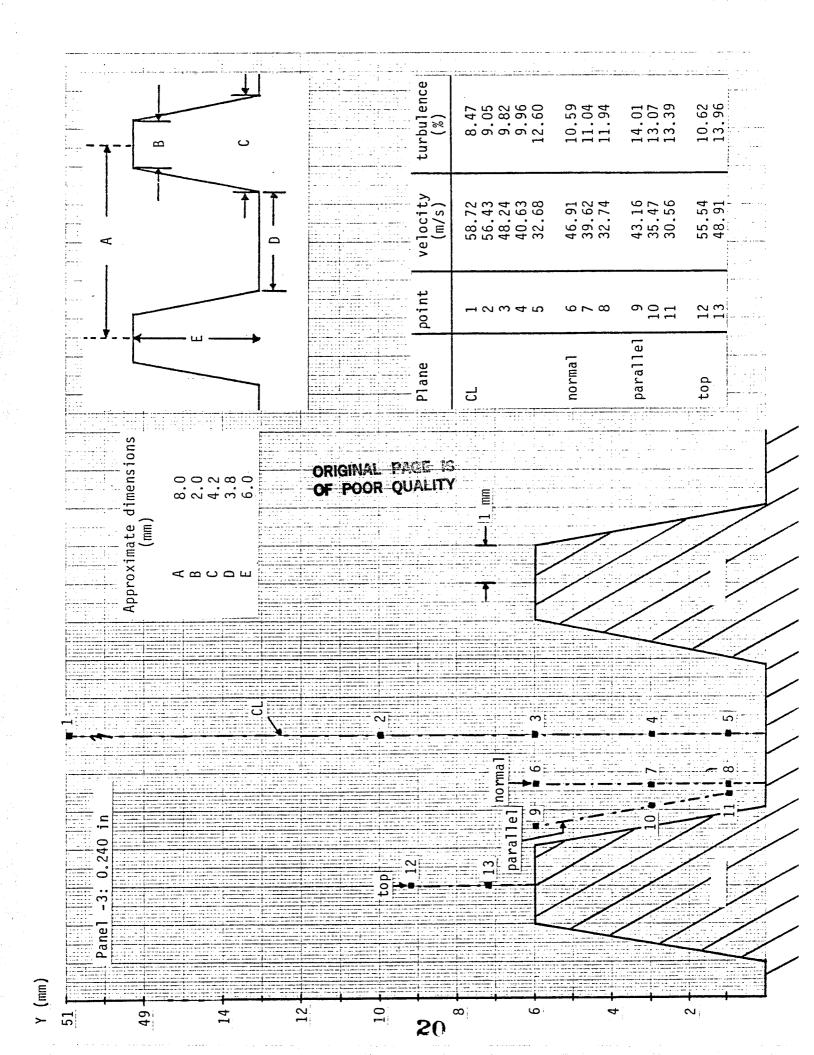
PANALLIEN	ABER Q'D	RANGE	··.		DIGITAL DISPLAY
VALVE DISCH PRESS	1	0-50 PS16	•	•	X
VENTURI THROAT PRESS	1	0-50 PSIG			X
MARIFOLD UPSTREAM PRESS	1	0-100 PSIG			X
MANIFOLD PRESS	1	0-100 PSIG			
VENTURI INLET TEMP	1	0-150 F	T/C		
MANIFOLD INLET TEMP	1	0-150 F	T/C		X

STANDARD INSTRUMENTATION FOR FACILITY OPERATION NOT LISTED.









APPENDIX D

RIB SCALED ANALYSIS

EXAMPLE CALCULATION FOR 0.040 RIB

STANTON NUMBER PROFILES

APPENDIX D. SAMPLE CALCULATION FOR THE 0.040 RIB

The method used to derive the thermal performance of a rib configuration from the measured velocity profiles was based upon the well established characteristics of a flat plate boundary layer. The local shear stress at any location on the rib wall was derived by fitting the measured local velocity profile to the established flat plate profile. The heat transfer Stanton number defined by St = h/(pUoCp) was found directly by assuming Reynold's analogy. Figure Dl. graphically illustrates these steps in the data reduction process. A numerical example of this method will be presented for the 0.040 rib configuration.

The measured velocity profile was fit to the established flat plate correlation by varying the friction velocity parameter defined as $V^* = Uo/(Cf/2)$. Figure D2. shows the measured velocity as a function of distance from the wall for the location midway between ribs. The solid line shown is the logrithmic overlap model corresponding to the best fit value of $V^* = 2.39$. It is evident that this coincides with the measured velocity profile near the wall.

The fit of the data was actually performed by inspection of the velocity profile expressed in terms of inner variables u+ = U/V* (dimensionless velocity) and y+ = yV*/v (dimensionless distance). A semilog plot shown in Figure D3. presents the logrithmic overlap correlation as a straight line. The measured velocity data is shown for the best choice of V*. Since the V* parameter by definition is in the denominator of u+ and in the numerator of y+, variation of V* results in a change of position of the measured data. Therefore, V* is chosen such that the data points, particularly those closest to the wall, fall on the correlation line.

Based upon a freestream velocity of Uo = 70.5 meters/sec, the best fit value for V* corresponds to a friction factor of,

$$Cf/2 = (V*/Uo)^2$$

= 0.00115

The Reynold's analogy with a Prandtl number correction (for air Pr = 0.69) provides the heat transfer Stanton number as,

$$-2/3$$

St = Pr Cf/2
= 0.00146

The Stanton number defines the heat transfer coefficient for a given set of flow conditions. This procedure was repeated for every location about the rib where velocity profiles were measured. Thus a Stanton number profile about the rib was calculated as shown

FIGURE DI. FLOWCHART OF THE DATA REDUCTION PROCEDURE FOR THE COLD FLOW TESTS.

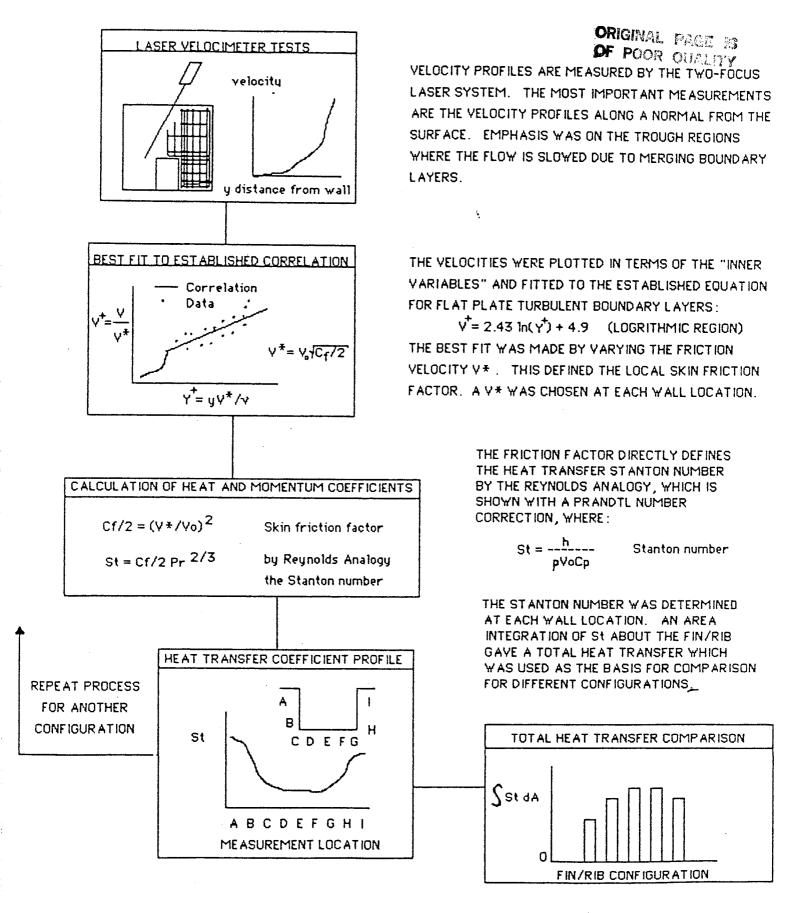


FIGURE D2
CENTERLINE VELOCITY PROFILE

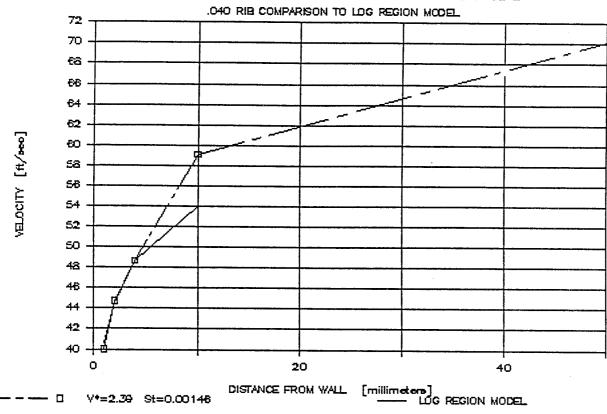
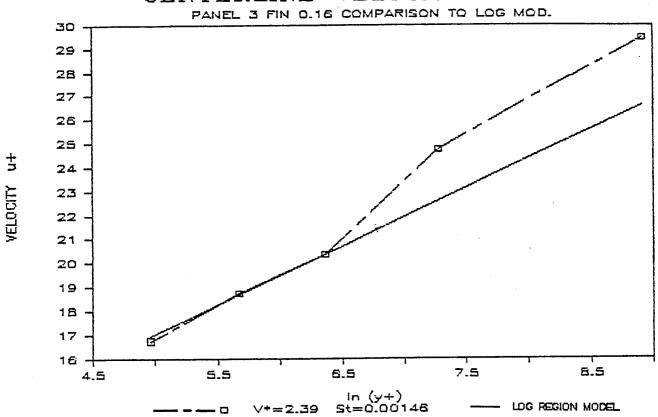


FIGURE D3

CENTERLINE VELOCITY PROFILE



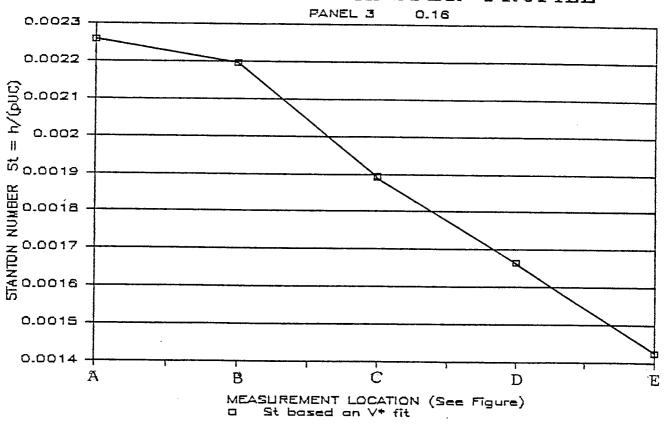
in Figure D4.

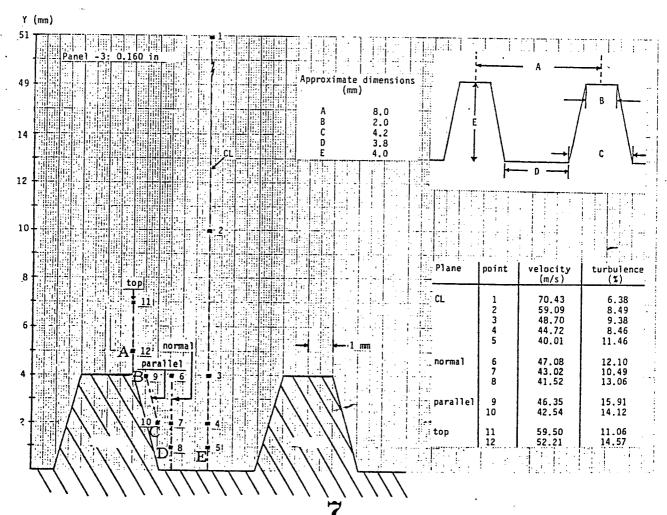
In order to compare the relative performances of different rib configurations, the Stanton number profiles were integrated with respect to surface area to provide a total heat transfer parameter. This parameter reflects the heat transferred per rib. Since the skipped rib configuration has a spacing twice that of the other configurations, one half of the calculated total heat transfer parameter was used for comparison.

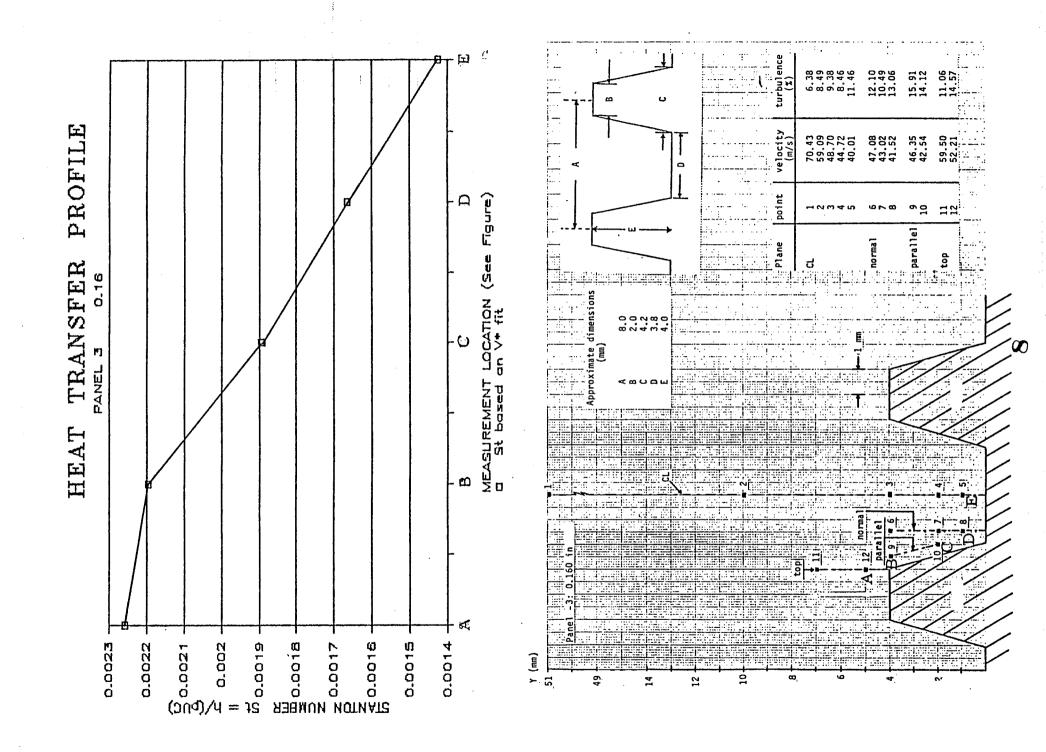
Scaling the Cold Flow results to hot-fire conditions required a scaling factor for the gas-side Stanton number. This scaling factor, denoted as Sg, was defined as the ratio of the Stanton number for a hot-fired smooth walled combustor to the Stanton number for a Cold Flow test on a flat plate. The boundary layer computer model predicted the hot-fire combustor Stanton number. The scaling factor was found to be Sg = 0.5. This was used as a Stanton number multiplier for all rib configurations.

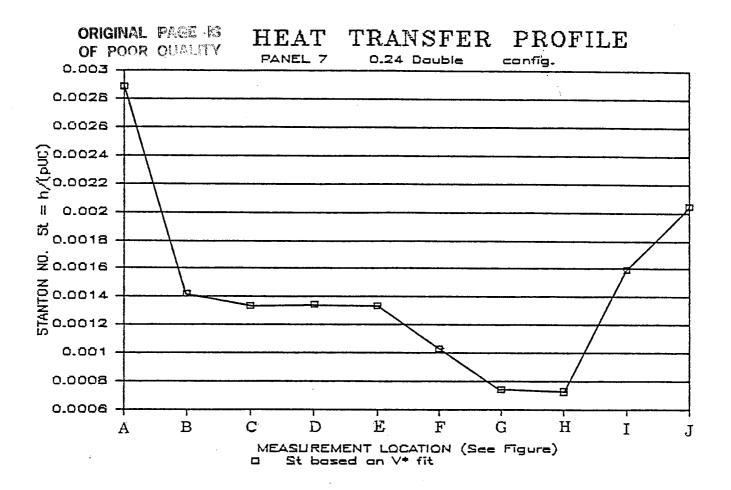
ORIGINAL PAGE IS OF POOR QUALITY FIGURE D4

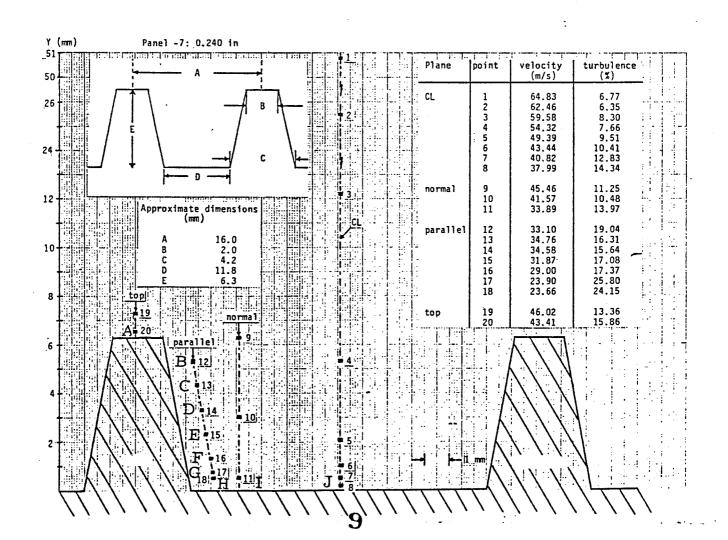
HEAT TRANSFER PROFILE



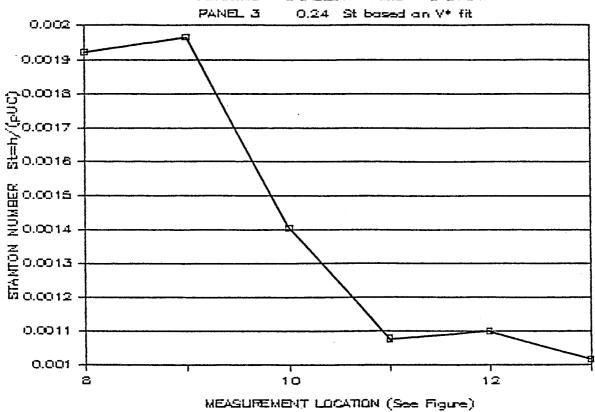








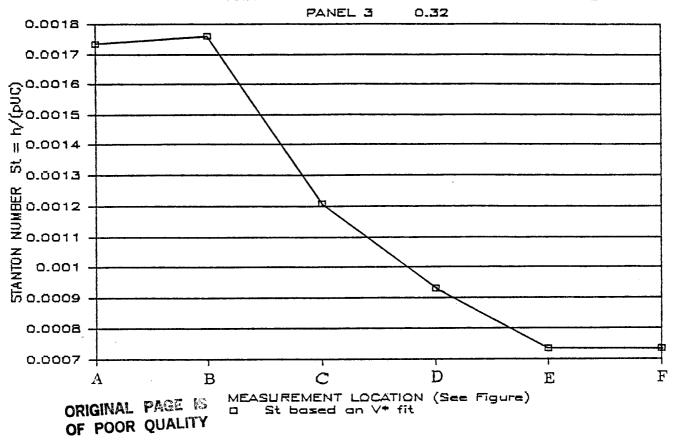
HEAT TRANSFER PROFILE

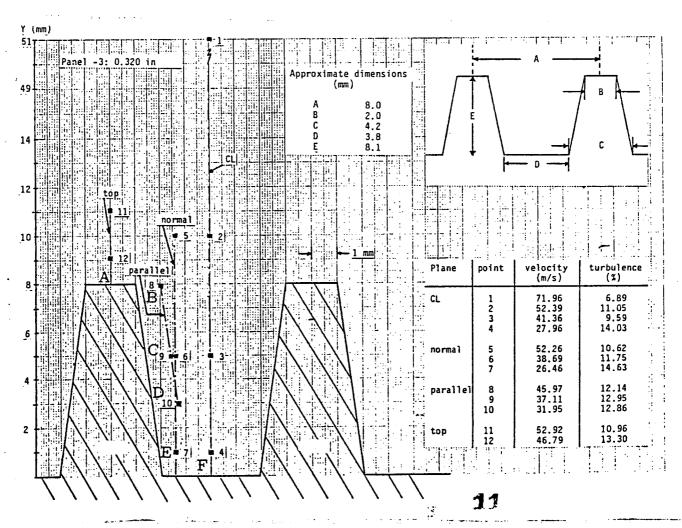


* (Specified Freestream los is 70.4 m/s)

Y (mm)		
Tanel -3: 0.240 in -7	- A	4
49 Approximate dimensions (mm)	- $$	В
A 8.0 /	['	'\
14 T T T T T T T T T T T T T T T T T T T		\
1	<u> </u>	c H
	— U ——¶	
Plane point	velocity t (m/s)	urbulence (%)
8 CL 1	58.72 56.43	8.47 9.05
A parallel normal	48.24 40.63	9.82 9.96
6 3 5	32.68	12.60
normal 6	46.91 39.62	10.59 11.04
	32.74	11.94
parallel 9 10	43.16 35.47	14.01 13.07 13.39
	30.56 55.54	10.62
	48.91	13.96
10		

HEAT TRANSFER PROFILE





				•	
<i>;</i>					
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	•				

APPENDIX E

CHANNEL ANALYSIS COMPUTER OUTPUTS
CHANNEL EVALUATION CRITERIA RATING SCALES

	R OF ITER		76 IN AND HE	ልኛ <i>ባ</i> መኛ ቋ።		ors
_			*** **** '16'		200300 FE	` . .
HEAT	INFLUX =	38.093	1586	- 1573	1568	
			1497	1480	1475	
			1364	1344	1337	
			1199		1172	
			and the same			
923	927	945	988	795	996	
863	885	893	905	912	914	
835	835	834-	831 -	833	834	
789	787	778	752	754	757	
			638	561	007	
		<u> </u>	560	583 -	- 59I ·-	
			500	521	528	
			455	473	479	
			- 420	- 436 -	- 441	. .
			395	408	413	
			376	389	394	
305-	310	325	360 -	— 379 —	385 -	-
338	339	-343	349	356	359	
344	344	346	349	352	354	
8 1 2 3	CHANNE MALL T	P #IDTH = IDTH = .: E #IDTH =	_02000 04084 04000 HI =02500	FACTUR	1_0000	

CATAGORY I .080x.040 channel.

TC = 252 DEG. F

	STATIO	N NO. 63	X = -10	3.400	K/RT = -1:	3 413	
	NUMBER	OF ITERAT	TIONS =	71		00667 PER	CENT
	HEAT II	NFLUX = 4	44.960	1640	1627	1622	
*********	***************************************	***************************************	••••••••••	1552	1535	1530	
				1419	1399	1392	#16
••••••	***************************************	***************************************	••••••	1252	1231	1225	
	1000	1004	1017	1041	1045	1046	
••••••	944	945	948	953	959	961	
	873	873	872	872	876	878	
•••••	808	804	797	784	795	799	
				677 ·	704	712	
••••••	***************************************	·····	••••	608	634	642	
				560	581	588	CAT. I., .080 × .02.0 CHANNEL
•••••	•••••	***************************************	***************************************	526	542	548	
				501	514	519	
••••••	•••••••		•••••	484	495	499	
				473	483	486	
•••••	447	448	454	465	477	481	
	465	465	465	468	469	470	
	467	467	467	467	468	468	
			BO. = THS WIDTH =				
*********	1.	LAND WID	TH = .03 WIDTH =	970	EACTOR -	. 1 00000	
	3.	WALL THI	CKNESS = DEPTH =	.02500	TACTOR -	1.00000	
••••••	5.	CLOSEOUT	THICKNES	S = .040	00	•••••••••	
		TAW = 62 $HG = .0$	159. DEG. 1034000	F			,
•	8,	TC = 41	6. DEG. F			•••••	
			E HC = . IR FOR UPP		1 0000		
			IR FOR LOW				
	12.	EXPONENT	= .550	۸			
	13-14.	K DF REG	ION 1 =	.004875 +	(1870	E-06) * T	
						E-06) * T	
						E-05) * T	
			NCE CRITE				





NUMBER OF ITERATIONS = 135

HEAT INFLUX = 38.907

11.

13-14.

15-18. 17-18. HC FACTOR LOWER WALL = 1.00000

 $K ext{ OF REGION 1} = .004875 + (-.1870E-06) * T$

K OF REGION 2 7 .004875 + (-.1870E-06) * T K OF REGION 3 2 .001340 + (-.1390E-05) * T

CONVERGENCE CRITERION = .0100 DEG. F

12. EXPONENT = ,55000

DIFFERENCE BETWEEN IN AND HEAT OUT = .01846 PERCENT

1490 1480 1474 1471



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								567 PE			•••••••••••••••••••••••	
	HEAT	INFLUX	·= 39	. 084		4400						#9
						1468	1458	1452	1450			
				•••••	•••••••	1377	1365	1357	1354		······································	•••••
						1241	1226	1216	1213			
********	***************************************	***************************************	······································	••••••	••••••	1072	1055	1046	1044			
	768	767	770	783	807	851	860	864	865			
********	722	723	725	735	748	764	776	782	784			
	-661	662	664	674	684	692	702	708	710			
	582	583	586	610	625	624	633	639	641			
	538	537	542			539	556	565	568			
•••••	513	511	505	••••••		480	495	504	507			
	491	489	480			436	449	456	459	CAT. II a	.024x.010	FIN
	473	470	461	••••••	***************************************	403	413	420	422			
	458	455	446			378	387	392	394			€
······································	447	444	436	••••••	••••••	360	367	372	373			•••••••••••••••••••••••••••••••••••••••
						347	354	359	360			
•••••	304	305	310	313	322	336	346	352	353			
	324	324	325	327	329	331	334	336	337			
	328	328	328	329	330	331	332	333	334			
	A .					FIN HE						
	В,	RIB	TOP W	IDTH :	020	000 F1	IN BASE	. ₽ .(1000	•••••		
	1. 2.					FIN TI						
	3.				= .040		PACIUS	. = 1.0	00000			
	4,				080							
	5.	CLO				.0400	00					***************************************
	8. 7		= 625 = .00		1. F							
	8.	TC	00 - 267	. DEG	3. F							
	9.	REF	ERENCE	HC =	.0702				***************************************		•••••••••••••••••••••••••••••••••••••••	••••••••••••••••••••••••••••••••••••
	10.					IALL =		0				
	11.					= 1.00	0000					
	12. 13-14.		DNENT F REGI			1875 +	(- 19	70F-09	i) * T			
	15-16.) * T			
	17-18.		F REGI	'								



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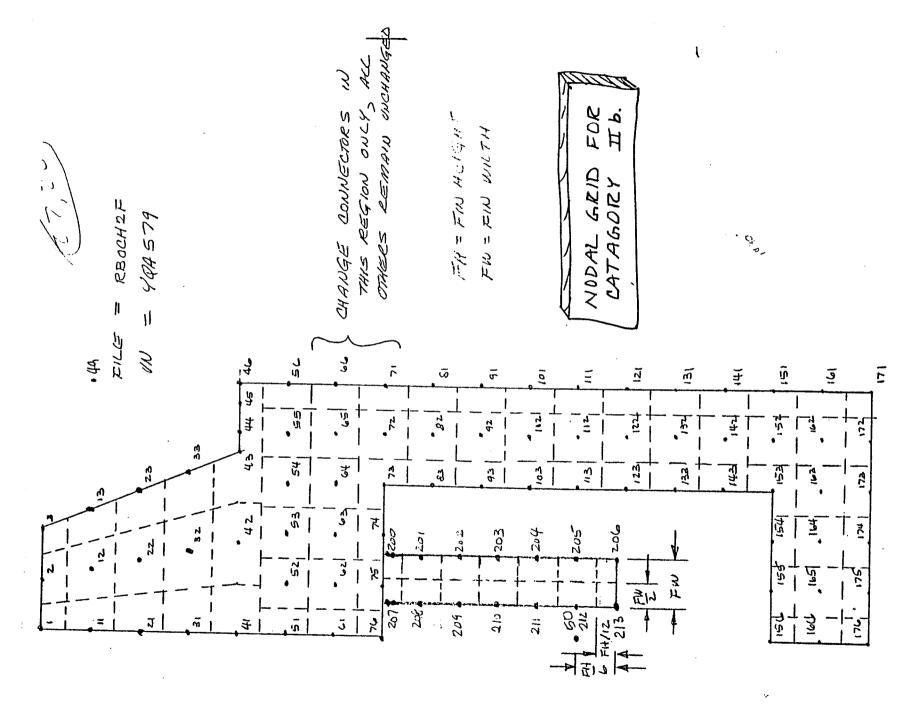
CONVERGENCE CRITERION = ,0100 DEG. F.







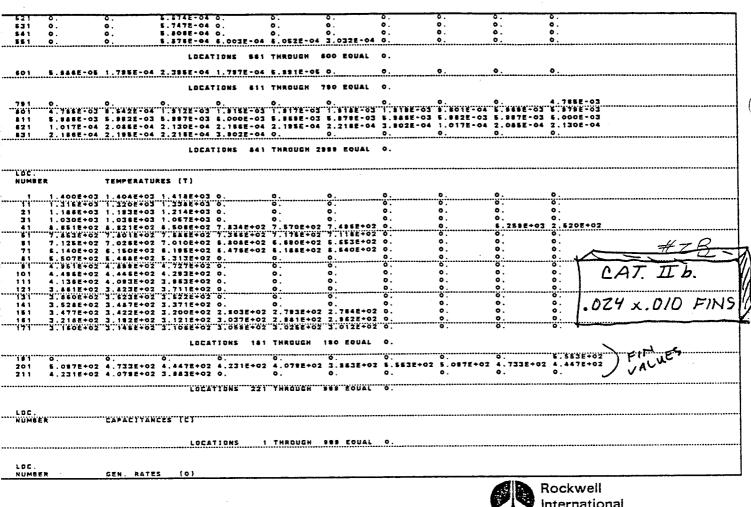
Rockwell International



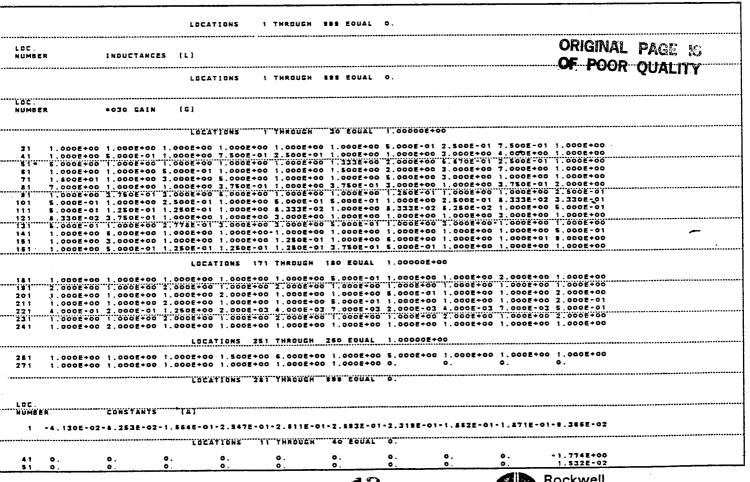
E04			F 6FFF 6:						·		
521 531	0. 0.	0. 0. ~	5.655E-04 5.730E-04		0. 0.	0. 0.	0. 0.	_		0.	
541	0. 0.	0.	5.791E-04		0. 0.	0.	0.	_		0.	
551	0. 0.	0.				3.030E-04		0.	0.	0.	
		. • • • • • • • • • • • • • • • • • • •	J.007L 07.			,	***************************************	ν.	U.	0.	•••••
			LOCAT	TIONS 561	THROUGH	BOO EQUAL	0.				
601	5.979E-05	1.793E-04	2.393E-04	1.796E-04	5,988E-05	0.	0.	0.	0,	0.	•••••
			LOCAT	TIONS 811	THROUGH	790 EQUAL	0.			9 9	
704	• 0	^						•	_	4.759E-03 PORIGINAL 9.543E-03 9.566E-03	<u> </u>
801	· 0,			0.	0.	0. 1.195E-03	0.	U.	0,	4.759E-03	j
811	4.755E~03	0.5500-04	1.192E-03	0 5665.03	1.1946-03	0 5425 02	1.190E-U3	5.98UE-U4	9.5346-03	9.543t-03 0 F	;
821	B.331E-03	1 2666-04	4 200E-04	4 204E-04	9.534E-U3	9.543E-03 1.313E-04	9.5516-03	9.55/6-03	9.562E-03	9.586E-03	•
	1,294E-04	1.2056-04	1.2006-04	2 2005 04	1.3052-04	1.3135-04	3.2995-04	0.2356-05	1.2056-04	1.280E-04	•
991	1,2345-04	1.3096-04	1,3135-04	3.2355-04	.y	v.	.y.,	v	ν	<u> </u>	<i>;</i> 5
			LOCAT	TIONS 841	THROUGH 2	999 EQUAL	0.			AL GE	1
										QUALITY	- 8
LOC.		TEMPERATUR	EC (T)		***************************************		•••••••••••	•	***************************************		g
NUMB										# 2 7	
1			1,438E+03		o,	o.	0.	0.	0,	0.	
11			1.358E+03		0.	0.			0.	0.	
21			1.235E+03		0.	0.				0.	
31			1.078E+03		0.	0.				0.	
41						7.668E+02		. .	6.259E+03	······································	
51						7.285E+02				0.	\sim
61						6.814E+02				CAT. II b	1
71	6.287E+02	6.300E+02	6.356E+02	B.686E+02	6.485E+02	6.796E+02	0.	0.		· ,	j
81			5,434E+02		0.	0.	0.	0.		0.	
91			4.823E+02		0.	0.				% / .015 x.010 FII	uc l
101			4.370E+02		0.	0.				· ,	43
111			4.026E+02		0.	0.	0.	0.	0.	0	
121			3.764E+02		0,	0.	0.	0.	0.	0.	
131		,	3.566E+02		0.	0.				0.	
141			3.409E+02		0.	0.				0.	
151						2.774E+02		0.	0.	0.	
161						2.981E+02		0.	0,	0.	
171						3.033E+02		0.	0.	0.	
			LOCAT	IONS 181	THROUGH	190 EQUAL	Ο.			FIN POINT	77
								<u></u>			
191	0.	O. 202	0. 203	0. 207	0. 205	0. = 06	0. 207	0. 208	0. TH	5.905E+02 (VALUES ((P)
201	5.638E+02	5.413E+02	5.226E+02	5.076E+02	4.961E+02	4.880E+02	5.905E+02	5.638E+02	5.413E+02	5.226E+ <u>0</u> 2	
211	5.076E+02		4.880E+02	0.	0.	0.	0.	0.	0.	0. zzo5.)	
	•••••	ZIZ	213						····		
	garger page of a fact that a substitution of the state		LOCAT	TIONS 221	THROUGH !	999 EQUAL	0.				
LOC.					•						
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			J							·	
				-	T1 10 01 10 1		_				•
			LOCAT	IONS 1	THROUGH !	999 EQUAL	0.				
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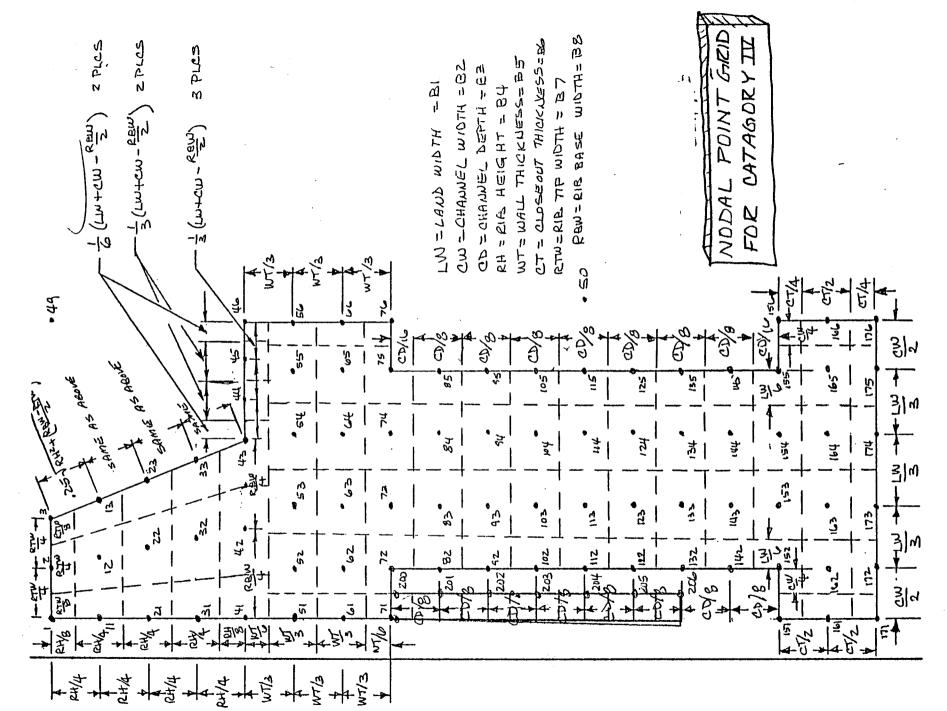
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UMBER	······································	ADMITTANCE	(V)	***************************************	••••••	***************************************	••••••		···•··································	
WIID E IV	•	ADMITTANGE	.5 (1)	•						
1	R 924F-03	1 102F-02	9 183F-03	7 890F-03	5 390F-03	1.972E-03	1 977F-03	9 909F-04	6 921F-03	1 102F=02
-						3.206E-03				* * * * * * = * =
************		• • • • • • • • • • • • • • • • • • • •			• • • • • • • • • • • • • • • • • • •	6.625E-04		• • • • • • • • • • • • • • • • • • • •	· ••····•· • · · · · · · · · · · · · ·	······································
						3.532E-03				
						3.517E-03				
						1.979E-03				
	· • • • • • • • • • • • • • • • • • • •				• • • • • • • • • • • • • • • • • • • •	1.077E-03				
						3.014E-03				
						3.276E-03				•
						6.492E-03				
01	6.541E-03	6.545E-03	6.548E-03	5.989E-04	6.097E-04	5.807E-03	7.758E-03	7.775E-03	6.492E-03	6.506E-03
11	8.518E-03	6.528E-03	6.536E-03	B.541E-03	6.545E-03	6.548E-03	5.985E-04	6.088E-04	9.530E-03	9.585E-03
21	9.602E-03	3.248E-03	3.256E-03	3.262E-03	3.266E-03	3.270E-03	3.272E-03	3.274E-03	3.276E-03	7.558E-04
31	7,562E-04	5.695E-03	5.703E-03	5.711E-03	2.775E-03	6,518E-03	5,644E-03	1.937E-03	3.986E-05	2.410E-03
41	2.409E-03	4.624E-04	4.541E-04	8.500E-06	1.700E-05	3.438E-05	5.176E-05	5.176E-05	5.176E-05	6.012E-05
51	8.848E-05	6.848E-05	3.424E-05	2.427E-04	7.371E-04	5.170E-04	5.354E-04	5.496E-04	5.610E-04	5.700E-04
						7.499E-04		5.370E-04	5.504E-04	5.613E-04
71	5,701E-04	5.771E-04	5.827E-04	8.832E-04	6.009E-04	1.937E-03	0,	0.	0,	0.
					TUDOUGU	400 501141	•			
•			LOCAT	TONS 181	THRUUGH	190 EQUAL	υ.			
~ 4	4.759E-03	0,	0,	0.	0,	0.	0.	0.		1.236E-01
91		4 00CE 04	1 236F-01	1 236F-01	1 238F-01	0	0.	0.	0.	6.221E-05
	1.236E-01	1.2306-01	I. ZOUL VI	I. AUGE OI	1.2306 0;	U .				
01	1.236E-01 1.245E-04	1.245E-04	1.245E-04	1.245E-04	1.245E-04	3.862E-04	Õ.	0.	Ο.	0.
191 201 211	1.236E-01 1.245E-04	1.245E-04	1.245E-04	1.245E-04	1.245E-04	3.862E-04 999 EQUAL		o. 	o.	O
201 211	1.245E-04	1.245E-04	1.245E-04 LOCAT	1.245E-04	1.245E-04	3.862E-04		o. 	0 .	0.
201 211	1.245E-04	1.245E-04	1.245E-04 LOCAT	1.245E-04	1.245E-04	3.862E-04		0.	0.	0.
O1 11 OC.	1.245E-04	1.245E-04	1.245E-04 LOCAT	1.245E-04 FIONS 221	1.245E-04	3.862E-04 999 EQUAL		0.	o. 	0.
O1 11 OC.	1.245E-04	1.245E-04 TEMPERATUR 1.387E+03	1.245E-04 LOCAT RES (T) 1.401E+03	1.245E-04 FIONS 221	1.245E-04 THROUGH 29	3.862E-04 999 EQUAL 0.	0,	•		· · · · · · · · · · · · · · · · · · ·
OI 11 OC. NUMBER	1.245E-04 1.382E+03 1.297E+03	1.245E-04 TEMPERATUR 1.387E+03 1.303E+03	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03	1.245E-04 FIONS 221 0. 0.	1.245E-04 THROUGH 29	3.862E-04 999 EQUAL 0.	0.	0.	0.	0.
01 11 0C. UMBER 1 11 21	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03	1.245E-04 TEMPERATUR 1.387E+03 1.303E+03 1.175E+03 1.018E+03	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03	1.245E-04 FIONS 221 0. 0. 0. 0.	1.245E-04 THROUGH 29	3.862E-04 999 EQUAL 0. 0.	0. 0. 0. 0.	0.	0. 0. 0.	0. 0. 0. 0.
01 11 0C. UMBER 1 11 21	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02	1.245E-04 TEMPERATUR 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02	1.245E-04 TIONS 221 0. 0. 0. 7.516E+02	1.245E-04 THROUGH 29 0. 0. 0. 0. 7.135E+02	3.862E-04 999 EQUAL 0. 0. 0. 0. 7.075E+02	0. 0. 0. 0.	o. o. o.	0. 0. 0. 0. 6.259E+03	0. 0. 0. 0. 0. 2.520E+02
OC. UMBER 1 11 21 31 41 51	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02	1.245E-04 TEMPERATUF 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02	1.245E-04 FIONS 221 0. 0. 0. 7.516E+02 6.984E+02	1.245E-04 THROUGH 29 0. 0. 0. 0. 7.135E+02 6.766E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02	0. 0. 0. 0. 0.	0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03	0. 0. 0. 0.
01 11 0C. UMBER 1 11 21 31 41 51 61	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02	TEMPERATUR 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.869E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02	1.245E-04 IIONS 221 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02	1.245E-04 THROUGH 29 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02	0. 0. 0. 0. 0. 0.	0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03	0. 0. 0. 0. 0. 2.520E+02
OC. UMBER 1 11 21 31 41 51 61	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02	TEMPERATUR 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.869E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02	1.245E-04 IIONS 221 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02	1.245E-04 THROUGH 29 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02	0. 0. 0. 0. 0. 0.	0. 0. 0. 0.	O. O. O. O. 6.259E+O3 O. O.	0. 0. 0. 0. 2.520E+02 0. 0.
OC. IUMBER 1 11 21 31 41 51 81	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02	TEMPERATUR 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.869E+02 6.196E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02 5.916E+02	1.245E-04 IIONS 221 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02 5.922E+02	1.245E-04 THROUGH 29 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02	3.862E-04 999 EQUAL 0. 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02 6.044E+02	0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0.	O. O. O. O. 6.259E+O3 O. O.	0. 0. 0. 0. 2.520E+02 0. 0.
OC. UMBER 11121 3141 5171 8191	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02 6.436E+02 0.	1.245E-04 TEMPERATUR 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.869E+02 6.196E+02 5.245E+02 4.638E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02 5.916E+02 5.929E+02 4.800E+02	0. 0. 0. 0. 0. 7.516E+02 6.462E+02 5.922E+02 5.307E+02 4.784E+02	1.245E-04 THROUGH 29 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02 5.863E+02 5.118E+02 4.587E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02 0. 0.	0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0.	O. O. O. O. 6.259E+O3 O. O.	0. 0. 0. 0. 2.520E+02 0. 0.
OC. UMBER 11121 3141 5171 8191	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02 6.436E+02 0.	TEMPERATUR 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.196E+02 5.245E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02 5.916E+02 5.929E+02 4.800E+02	0. 0. 0. 0. 0. 7.516E+02 6.462E+02 5.922E+02 5.307E+02 4.784E+02	1.245E-04 THROUGH 29 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02 5.863E+02 5.118E+02 4.587E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02 0. 0.	0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03 0. 0. 0.	0. 0. 0. 0. 2.520E+02 0. 0. 0.
OC. UMBER 111 21 31 41 51 61 71 81 91	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02 6.436E+02 0.	1.245E-04 TEMPERATUR 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.196E+02 5.245E+02 4.638E+02 4.207E+02 3.886E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02 5.916E+02 5.916E+02 4.800E+02 4.368E+02 4.029E+02	0. 0. 0. 0. 0. 5.516E+02 6.984E+02 6.462E+02 5.307E+02 4.784E+02 4.359E+02 4.025E+02	1.245E-04 THROUGH 29 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02 5.863E+02 5.118E+02 4.587E+02 4.185E+02 3.876E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 6.259E+03 0. 0. 0.	0. 0. 0. 0. 2.520E+02 0. 0. 0. 0.
OC. UMBER 1 11 21 31 41 51 71 81 91	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02 6.436E+02 0.	1.245E-04 TEMPERATUR 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.869E+02 5.245E+02 4.638E+02 4.638E+02 3.886E+02 3.644E+02	1.245E-04 LOCAT 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02 5.916E+02 5.329E+02 4.806E+02 4.806E+02 4.029E+02 3.770E+02	0. 0. 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02 5.307E+02 4.784E+02 4.359E+02 3.768E+02	1.245E-04 THROUGH 29 0. 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02 5.118E+02 4.587E+02 4.185E+02 3.876E+02 3.640E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0.	O. O. O. 6.259E+O3 O. O. O.	0. 0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
OC. IUMBER 1 11 21 31 41 51 61 71 81 91 101 111 121	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 1.012E+02 7.729E+02 7.729E+02 7.050E+02 0. 0. 0.	TEMPERATUF 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.196E+02 5.245E+02 4.638E+02 4.207E+02 3.886E+02 3.463E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 7.329E+02 6.640E+02 5.916E+02 5.916E+02 4.800E+02 4.368E+02 4.368E+02 3.770E+02 3.581E+02	0. 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02 5.922E+02 5.922E+02 4.359E+02 4.025E+02 3.768E+02 3.580E+02	1.245E-04 THROUGH 29 O. O	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02 0. 0. 0.	O. O	0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03 0. 0. 0.	0. 0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
OC. HUMBER 1 11 21 31 41 51 81 91 101 111 121 121	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02 0. 0. 0. 0.	TEMPERATUR 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.196E+02 5.245E+02 4.638E+02 4.207E+02 3.886E+02 3.644E+02 3.463E+02 3.320E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 7.329E+02 4.640E+02 5.916E+02 4.368E+02 4.368E+02 3.770E+02 3.581E+02 3.456E+02	1.245E-04 IIONS 221 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02 5.922E+02 4.784E+02 4.359E+02 4.359E+02 3.768E+02 3.768E+02 3.455E+02	1.245E-04 THROUGH 29 O. O	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02 0. 0. 0. 0.	O. O	0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03 0. 0. 0. 0.	0. 0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
OC. HUMBER 1 11 21 31 41 51 81 91 101 111 121 131	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.729E+02 0. 0. 0. 0. 0. 2.951E+02	1.245E-04 TEMPERATUF 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.869E+02 6.196E+02 5.245E+02 4.638E+02 4.207E+02 3.886E+02 3.644E+02 3.463E+02 3.320E+02 3.174E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02 5.916E+02 4.800E+02 4.800E+02 4.368E+02 4.029E+02 3.770E+02 3.7581E+02 3.456E+02 3.456E+02	1.245E-04 IIONS 221 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02 5.922E+02 4.784E+02 4.784E+02 4.359E+02 3.768E+02 3.455E+02 3.455E+02	1.245E-04 THROUGH 29 O. O	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02 0. 0. 0. 0. 0. 2.889E+02	O. O	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03 0. 0. 0. 0. 0.	0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
CO1 211 211 211 21 31 41 51 81 81 91 101 111 121 131 141	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02 6.436E+02 0. 0. 0. 0. 2.951E+02 3.016E+02	1.245E-04 TEMPERATUF 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.869E+02 6.196E+02 5.245E+02 4.638E+02 3.886E+02 3.886E+02 3.463E+02 3.463E+02 3.174E+02 3.141E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02 5.916E+02 4.800E+02 4.800E+02 4.029E+02 3.770E+02 3.581E+02 3.466E+02 3.404E+02 3.216E+02	1.245E-04 IIONS 221 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02 5.922E+02 4.784E+02 4.784E+02 4.359E+02 3.580E+02 3.455E+02 3.455E+02 3.225E+02	1.245E-04 THROUGH 29 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02 5.863E+02 5.118E+02 4.587E+02 4.185E+02 3.876E+02 3.640E+02 3.461E+02 3.319E+02 3.172E+02 3.168E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.733E+02 0. 0. 0. 0. 0. 0. 0. 2.889E+02 3.087E+02	O. O	0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03 0. 0. 0. 0. 0.	0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
OC. NUMBER 1 11 21 31 41 51 81 81 91 101 111 121 131 141	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02 6.436E+02 0. 0. 0. 0. 2.951E+02 3.016E+02	1.245E-04 TEMPERATUF 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.869E+02 6.196E+02 5.245E+02 4.638E+02 3.886E+02 3.886E+02 3.463E+02 3.463E+02 3.174E+02 3.141E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02 5.916E+02 4.800E+02 4.800E+02 4.029E+02 3.770E+02 3.581E+02 3.466E+02 3.404E+02 3.216E+02	1.245E-04 IIONS 221 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02 5.922E+02 4.784E+02 4.784E+02 4.359E+02 3.580E+02 3.455E+02 3.455E+02 3.225E+02	1.245E-04 THROUGH 29 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02 5.863E+02 5.118E+02 4.587E+02 4.185E+02 3.876E+02 3.640E+02 3.461E+02 3.319E+02 3.172E+02 3.168E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02 0. 0. 0. 0. 0. 2.889E+02	O. O	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03 0. 0. 0. 0. 0.	0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
OC. HUMBER 1 11 21 31 41 51 81 91 01 11 121 121 131 141	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02 6.436E+02 0. 0. 0. 0. 2.951E+02 3.016E+02	1.245E-04 TEMPERATUF 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.869E+02 6.196E+02 5.245E+02 4.638E+02 3.886E+02 3.886E+02 3.463E+02 3.463E+02 3.174E+02 3.141E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02 5.916E+02 5.916E+02 4.800E+02 4.800E+02 4.029E+02 3.770E+02 3.456E+02 3.456E+02 3.404E+02 3.216E+02 3.176E+02	1.245E-04 IIONS 221 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02 5.922E+02 4.784E+02 4.359E+02 3.768E+02 3.768E+02 3.404E+02 3.404E+02 3.225E+02 3.187E+02	1.245E-04 THROUGH 29 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02 5.863E+02 5.118E+02 4.587E+02 4.587E+02 3.876E+02 3.640E+02 3.319E+02 3.172E+02 3.168E+02 3.165E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.733E+02 0. 0. 0. 0. 0. 0. 2.889E+02 3.087E+02	O. O	0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03 0. 0. 0. 0. 0.	0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
.0C. .UMBER 1 11 21 31 41 51 81 91 101 111 121 131 141	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.050E+02 6.436E+02 0. 0. 0. 0. 2.951E+02 3.016E+02	1.245E-04 TEMPERATUF 1.387E+03 1.303E+03 1.175E+03 1.018E+03 8.440E+02 7.576E+02 6.869E+02 6.196E+02 5.245E+02 4.638E+02 3.886E+02 3.886E+02 3.463E+02 3.463E+02 3.174E+02 3.141E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 7.329E+02 6.640E+02 5.916E+02 5.916E+02 4.800E+02 4.800E+02 4.029E+02 3.770E+02 3.456E+02 3.456E+02 3.404E+02 3.216E+02 3.176E+02	1.245E-04 IIONS 221 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02 5.922E+02 4.784E+02 4.359E+02 3.768E+02 3.768E+02 3.404E+02 3.404E+02 3.225E+02 3.187E+02	1.245E-04 THROUGH 29 0. 0. 0. 7.135E+02 6.766E+02 6.337E+02 5.863E+02 5.118E+02 4.587E+02 4.587E+02 3.876E+02 3.640E+02 3.319E+02 3.172E+02 3.168E+02 3.165E+02	3.862E-04 999 EQUAL 0. 0. 0. 7.075E+02 6.733E+02 6.733E+02 0. 0. 0. 0. 0. 0. 0. 2.889E+02 3.087E+02	O. O	0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03 0. 0. 0. 0. 0.	0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
OC. HUMBER 11121 3141 5181 8191 101 111	1.245E-04 1.382E+03 1.297E+03 1.168E+03 1.012E+03 8.487E+02 7.729E+02 7.729E+02 0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0	1.245E-04 TEMPERATUF 1.387E+03 1.303E+03 1.175E+03 1.018E+02 7.576E+02 6.196E+02 5.245E+02 4.638E+02 4.207E+02 3.886E+02 3.644E+02 3.463E+02 3.174E+02 3.174E+02 3.127E+02	1.245E-04 LOCAT RES (T) 1.401E+03 1.320E+03 1.196E+03 1.038E+03 8.277E+02 6.640E+02 5.916E+02 5.916E+02 4.368E+02 4.368E+02 3.770E+02 3.770E+02 3.770E+02 3.404E+02 3.216E+02 3.178E+02	1.245E-04 IIONS 221 0. 0. 0. 7.516E+02 6.984E+02 6.462E+02 5.922E+02 4.784E+02 4.359E+02 3.768E+02 3.768E+02 3.464E+02 3.455E+02 3.404E+02 3.225E+02 3.187E+02	1.245E-04 THROUGH 29 O. O	3.862E-04 999 EQUAL 0. 0. 0. 0. 7.075E+02 6.733E+02 6.381E+02 6.044E+02 0. 0. 0. 2.889E+02 3.087E+02 3.126E+02	O. O	0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 6.259E+03 0. 0. 0. 0. 0.	0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.



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1 6.9	928E-03 1.103E-	02 9.188E-03	7.894E-03	5.393E-03	1.973E-03	1.978E-03	9.917E-04	6.925E-03	1.102E-02
11 9.	183E-03 7.890E-	·03 5.395E-03	2.900E-03	2.908E-03	3 208E-03	3.509E-03	3 517E-03	3 523F-03	3 527F-03
21 3.	531E-03 3.533E-	·03 3 535E-03	9 759F-04	1 323F-03	B 642F-04	9 785F-04	2 903F-03	2 910F-03	3 209F-03
31 3.	509E-03 3.518E-	·03 3 522E-03	3 526F-03	3 530F-03	3 532F-03	3 534F-03	9 587F-04	1 315F-03	8 813F-04
41 9.4	808E-04 2.907E-	·03 2 912F-03	3 209F-03	3 510F-03	3 517F-03	3 5235-03	3 527F-02	2 E21E-02	2 5225-02
	535E-03 9.761E-								
	589E-04 4.603E-								
	704E-03 1.743E-								
	262E-03 3.266E-								
	285E-03 1,499E-	**************							**** ** ** ***************************
1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	542E-03 B.546E-								
1 111 211	520E-03 8.529E-								
	B05E-03 3.248E-								
	582E-04 5.697E-								
	409E-03 4.832E-								
	848E-05 8.848E-								
	780E-04 5.838E-								5.628E-04
171 5.	713E-04 5.781E-	-04 5.838E-04	B.843E-04	6,014E-04	1.938E-03	0.	0.	0.	0.
1		LOCAT	TIONS 181	THROUGH	190 EQUAL	0.			
1									
191 4.	768E-03 O.	0,	0.	0.	Ο.	0.	0.	0,	1.158E-01
	158E-01 1.158E-			1.158E-01	0.	0.	0.	0.	1.021E-04
211 2.0	044E-04 2.045E-	·04 2.045E-04	2.045E-04	2.045E-04	5.870E-04	0.	0.	0.	0.
		LOCAT	IONS 221	THROUGH 2	999 EQUAL	0.			
LOC.	•								
NUMBER	TEMPER/	TURES (T)							
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,	369E+03 1.374E4	.03 1.388E+03	0.	0.	0.	0.	0.	0.	0.
11 1.3	AA48.AA 4 AAA81								
		03 1.307E+03		0.	0.	ŏ.	0.	0.	0.
21 1.	155E+03 1.162E			0. 0.	o.	0. 0.	0. 0.	0. 0.	0. 0.
31 9.	155E+03 1.162E+ 983E+02 1.004E+	03 1,183E+03 03 1.024E+03	0.	0. 0.	0.	0. 0.	0. 0.	0.	0. 0. 0.
31 9.1 41 8.3	155E+03 1.162E+ 983E+02 1.004E+ 339E+02 8.299E+	03 1,183E+03 03 1.024E+03 02 8.148E+02	0. 0. 7.416E+02	0. 0. 0. 7.050E+02	0. 0. 6.998E+02	0. 0. 0.	0. 0. 0.	0. 0. 6.259E+03	0. 0. 0. 2.520E+02
31 9.1 41 8.3 51 7.1	155E+03 1.162E+ 983E+02 1.004E+	03 1,183E+03 03 1.024E+03 02 8.148E+02	0. 0. 7.416E+02	0. 0. 0. 7.050E+02	0. 0. 6.998E+02	0. 0. 0.	0. 0. 0. 0.	0. 0. 6.259E+03 0.	0. 0. 0. 2.520E+02 0.
31 9.1 41 8.5 51 7.1 61 6,1	155E+03 1.162E 983E+02 1.004E+ 339E+02 8.299E+ 563E+02 7.446E+ 848E+02 6.743E+	1.183E+03 1.024E+03 1.024E+03 1.02 8.148E+02 1.02 7.222E+02 1.02 6.539E+02	O. 7.416E+02 6.892E+02 6.376E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02	0. 0. 6.998E+02 6.657E+02 6.308E+02	0. 0. 0. 0. 0.	0. 0. 0. 0. 0.	0. 0. 6.259E+03 0.	0. 0. 0. 2.520E+02 0. 0.
31 9.1 41 8.5 51 7.1 61 6,1	155E+03 1.162E 983E+02 1.004E+ 339E+02 8.299E+ 563E+02 7.446E+ 848E+02 6.743E+ 173E+02 6.082E+	03 1.183E+03 03 1.024E+03 02 8.148E+02 02 7.222E+02 02 6.539E+02 02 5.827E+02	0. 7.416E+02 6.892E+02 6.376E+02 5.844E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02 5.792E+02	0. 0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02	0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0.	0. 0. 6.259E+03 0. 0.	0. 0. 0. 2.520E+02 0. 0.
31 9.1 41 8.5 51 7.1 61 6,	155E+03 1.162E 983E+02 1.004E+ 339E+02 8.299E+ 563E+02 7.446E+ 848E+02 6.743E+ 173E+02 6.082E+	1.183E+03 1.024E+03 1.024E+03 1.02 8.148E+02 1.02 7.222E+02 1.02 6.539E+02	0. 7.416E+02 6.892E+02 6.376E+02 5.844E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02 5.792E+02	0. 0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02	0. 0. 0. 0. 0.	0. 0. 0. 0. 0.	0. 0. 6.259E+03 0. 0.	0. 0. 2.520E+02 0. 0. 0. 0.
31 9.4 41 8.5 51 7.5 61 6.7 71 6.8 81 0.91 0.	155E+03 1.162E+ 983E+02 1.004E+ 339E+02 8.299E+ 563E+02 7.446E+ 848E+02 8.743E+ 173E+02 6.082E+ 5.166E4 4.580E+	03 1.183E+03 03 1.024E+03 02 8.148E+02 02 7.222E+02 02 6.539E+02 02 5.827E+02	O. 7.416E+02 6.892E+02 8.376E+02 5.844E+02 5.240E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02 5.792E+02 5.058E+02	0. 0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02	0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0.	0. 0. 6.259E+03 0. 0. 0.	0. 0. 2.520E+02 0. 0. 0. 0.
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31 9.4 41 8.5 51 7.5 61 6.7 71 6.8 81 0.91 0.	155E+03 1.162E 983E+02 1.004E+ 339E+02 8.299E+ 563E+02 7.446E+ 848E+02 6.743E+ 173E+02 6.082E+ 5.166E+ 4.580E+ 4.161E+	03 1,183E+03 03 1.024E+03 02 8.148E+02 02 7.222E+02 02 6.539E+02 02 5.827E+02 02 5.255E+02 02 4.740E+02	O. 7.416E+02 6.892E+02 6.376E+02 5.844E+02 5.240E+02 4.728E+02 4.313E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02 5.792E+02 5.058E+02 4.536E+02 4.143E+02	0. 0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02 0. 0.	0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0.	0. 0. 6.259E+03 0. 0. 0.	0. 0. 0. 2.520E+02 0. 0. 0. 0.
31 9.4 41 8.5 51 7.4 61 6.7 71 6.8 81 0.91 0.101 0.101	155E+03 1.162E+ 983E+02 1.004E+ 339E+02 8.299E+ 563E+02 7.446E+ 848E+02 8.743E+ 173E+02 6.082E+ 5.166E+ 4.580E+ 4.161E+ 3.849E+	03 1.183E+03 03 1.024E+03 02 8.148E+02 02 7.222E+02 02 6.539E+02 02 5.827E+02 02 5.255E+02 02 4.740E+02 02 4.320E+02	O. 7.416E+02 6.892E+02 8.376E+02 5.844E+02 5.240E+02 4.728E+02 4.313E+02 3.986E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02 5.792E+02 5.058E+02 4.536E+02 4.143E+02 3.841E+02	0. 0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02 0. 0.	0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 6.259E+03 0. 0. 0. 0.	0. 0. 0. 2.520E+02 0. 0. 0. 0. 0.
31 9.4 41 8.5 51 7.5 61 6.7 71 6.8 81 0.91 0.101 0.111 0.111	155E+03 1.162E+ 983E+02 1.004E+ 339E+02 8.299E+ 563E+02 7.446E+ 848E+02 6.743E+ 173E+02 6.082E+ 5.166E+ 4.580E+ 4.161E+ 3.849E+ 3.614E+	03 1.183E+03 03 1.024E+03 02 8.148E+02 02 7.222E+02 02 8.539E+02 02 5.827E+02 02 5.255E+02 02 4.740E+02 02 4.320E+02	O. 7.416E+02 6.892E+02 6.376E+02 5.844E+02 5.240E+02 4.728E+02 4.313E+02 3.986E+02 3.735E+02	0. 0. 7.050E+02 6.684E+02 8.260E+02 5.792E+02 5.058E+02 4.536E+02 4.143E+02 3.841E+02 3.610E+02	0. 0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 6.259E+03 0. 0. 0. 0. 0.	0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
31 9.4 41 8.5 51 7.4 61 6.7 71 8.8 81 0.91 0.101 0.101 0.111	155E+03 1.162E 983E+02 1.004E 339E+02 8.299E 563E+02 7.446E 848E+02 6.743E 173E+02 6.082E 5.166E 4.580E 4.161E 3.849E 3.614E 3.438E	03 1.183E+03 03 1.024E+03 02 8.148E+02 02 7.222E+02 02 6.539E+02 02 5.827E+02 02 5.255E+02 02 4.740E+02 02 4.320E+02 02 3.989E+02 02 3.737E+02 02 3.553E+02	O. 7.416E+02 6.892E+02 6.376E+02 5.844E+02 5.240E+02 4.728E+02 4.313E+02 3.986E+02 3.735E+02 3.552E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02 5.792E+02 5.058E+02 4.536E+02 4.143E+02 3.841E+02 3.610E+02 3.436E+02	0. 0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 6.259E+03 0. 0. 0. 0. 0.	0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
31 9.4 41 8.5 51 7.1 61 6.1 71 6. 81 0. 91 0. 101 0. 111 0. 121 0. 131 0.	155E+03 1.162E+ 983E+02 1.004E+ 339E+02 8.299E+ 563E+02 7.446E+ 848E+02 6.743E+ 173E+02 6.082E+ 5.166E+ 4.580E+ 4.161E+ 3.849E+ 3.614E+	03 1.183E+03 03 1.024E+03 02 8.148E+02 02 7.222E+02 02 6.539E+02 02 5.827E+02 02 5.255E+02 02 4.740E+02 02 4.320E+02 02 3.989E+02 02 3.737E+02 02 3.553E+02 02 3.431E+02	O. 7.416E+02 6.892E+02 6.376E+02 5.844E+02 5.240E+02 4.728E+02 4.313E+02 3.986E+02 3.735E+02 3.552E+02 3.430E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02 5.792E+02 5.058E+02 4.536E+02 4.143E+02 3.841E+02 3.610E+02 3.436E+02 3.297E+02	0. 0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 6.259E+03 0. 0. 0. 0. 0.	0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
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31 9.4 41 8.5 51 7.1 61 6.1 71 6. 81 0. 91 0. 101 0. 111 0. 121 0. 131 0. 141 0.	155E+03 1.162E 983E+02 1.004E 339E+02 8.299E 563E+02 7.446E 848E+02 8.743E 173E+02 6.082E 5.166E 4.580E 4.161E 3.849E 3.614E 3.438E 3.299E 940E+02 3.158E	03 1.183E+03 03 1.024E+03 02 8.148E+02 02 7.222E+02 02 6.539E+02 02 5.255E+02 02 4.740E+02 02 4.320E+02 02 3.989E+02 02 3.737E+02 02 3.431E+02 02 3.381E+02 02 3.198E+02	O. 7.416E+02 6.892E+02 6.376E+02 5.844E+02 5.240E+02 4.728E+02 4.313E+02 3.986E+02 3.735E+02 3.552E+02 3.430E+02 3.381E+02 3.206E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02 5.792E+02 5.058E+02 4.536E+02 4.143E+02 3.841E+02 3.610E+02 3.436E+02 3.297E+02 3.154E+02 3.151E+02	0. 0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02 0. 0. 0. 0. 0. 0. 0. 2.879E+02 3.072E+02	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	O. O. 6.259E+O3 O.	0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
31 9.4 41 8.5 51 7.1 61 6.1 71 6. 81 0. 91 0. 101 0. 111 0. 121 0. 131 0. 141 0. 151 2. 161 3.6	155E+03 1.162E: 983E+02 1.004E: 339E+02 8.299E: 563E+02 7.446E: 848E+02 8.743E: 173E+02 6.082E: 5.166E: 4.580E: 4.161E: 3.849E: 3.614E: 3.438E: 3.299E: 940E+02 3.158E: 003E+02 3.124E:	03 1.183E+03 03 1.024E+03 02 8.148E+02 02 7.222E+02 02 6.539E+02 02 5.827E+02 02 5.255E+02 02 4.740E+02 02 4.320E+02 02 3.989E+02 02 3.737E+02 02 3.431E+02 02 3.198E+02 02 3.158E+02	O. 7.416E+02 6.892E+02 8.376E+02 5.844E+02 5.240E+02 4.728E+02 4.313E+02 3.986E+02 3.735E+02 3.552E+02 3.430E+02 3.381E+02 3.206E+02 3.170E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02 5.792E+02 5.058E+02 4.536E+02 4.143E+02 3.610E+02 3.436E+02 3.297E+02 3.154E+02 3.151E+02 3.148E+02	0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02 0. 0. 0. 0. 0. 2.879E+02 3.072E+02 3.110E+02	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	O. O	0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
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31 9.4 41 8.5 51 7.1 61 6, 71 8. 81 0. 91 0. 101 0. 121 0. 131 0. 141 0. 151 2. 161 3.	155E+03 1.162E+ 983E+02 1.004E+ 339E+02 8.299E+ 563E+02 6.743E+ 173E+02 6.082E+ 4.580E+ 4.161E+ 3.849E+ 3.614E+ 3.438E+ 3.299E+ 940E+02 3.158E+ 003E+02 3.111E+	03 1.183E+03 03 1.024E+03 02 8.148E+02 02 8.539E+02 02 6.539E+02 02 5.827E+02 02 5.255E+02 02 4.740E+02 02 4.320E+02 02 3.989E+02 02 3.737E+02 02 3.431E+02 02 3.158E+02 02 3.158E+02	O. 7.416E+02 6.892E+02 8.376E+02 5.844E+02 5.240E+02 4.728E+02 4.313E+02 3.986E+02 3.735E+02 3.552E+02 3.430E+02 3.381E+02 3.206E+02 3.170E+02	0. 0. 7.050E+02 6.684E+02 6.260E+02 5.792E+02 5.058E+02 4.536E+02 4.143E+02 3.841E+02 3.610E+02 3.436E+02 3.297E+02 3.154E+02 3.154E+02 THROUGH	0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02 0. 0. 0. 0. 0. 0. 2.879E+02 3.072E+02 3.110E+02	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	O. O	0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
31 9.4 41 8.5 51 7.1 61 6, 71 6. 81 0. 91 0. 101 0. 121 0. 131 0. 141 0. 151 2.1 161 3. 171 3.	155E+03 1.162E+ 983E+02 1.004E+ 339E+02 8.299E+ 563E+02 6.743E+ 173E+02 6.082E+ 4.580E+ 4.161E+ 3.849E+ 3.614E+ 3.438E+ 3.299E+ 940E+02 3.158E+ 003E+02 3.111E+	03 1.183E+03 03 1.024E+03 02 8.148E+02 02 8.539E+02 02 6.539E+02 02 5.827E+02 02 5.255E+02 02 4.740E+02 02 4.320E+02 02 3.989E+02 02 3.737E+02 02 3.431E+02 02 3.198E+02 02 3.158E+02 02 3.158E+02	O. 7.416E+02 6.892E+02 6.376E+02 5.844E+02 5.240E+02 4.728E+02 4.313E+02 3.986E+02 3.735E+02 3.552E+02 3.430E+02 3.381E+02 3.206E+02 3.170E+02	0. 0. 7.050E+02 6.684E+02 8.260E+02 5.792E+02 5.058E+02 4.536E+02 4.143E+02 3.841E+02 3.610E+02 3.436E+02 3.297E+02 3.154E+02 3.151E+02 3.148E+02 THROUGH	0. 0. 6.998E+02 6.657E+02 6.308E+02 5.975E+02 0. 0. 0. 0. 0. 0. 2.879E+02 3.072E+02 3.110E+02 190 EQUAL 0.	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	O. O	0. 0. 0. 2.520E+02 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.



Rockwell International

CHANNEL EVALUATION CRITERIA RATING SCALES

DURABILITY (STRUCTURE/LIFE)

Based primarily on increased material durability resulting from a decrease in maximum material temperature (NARloy -Z) from enhanced coolant channel design, as compared with baseline channel.

RATING	DESCRIPTION
10	Major temperature reduction yeilding a large life enhancement. (greater than 150°F reduction).
8	Significant temperature reduction providing durability that exceeds design requirements. (100°F to 150°F reduction).
5	Durability improved, but occasional material roughening at rib tips (1400°F +) remains. (50°F to 100°F reduction)
2	Material temperature improved but still too high to provide reasonable life at normal operating conditions. (0°F to 50°F reduction).
0	Material temperature remains the same or increases, yielding no improvement or a decrease in material durability.

Durability Rating

COOLANT PRESSURE DROP

Ratings based on increase/decrease in coolant pressure drop (ΔP) through chamber, as compared with baseline .040 x .080 channel.

RATING	DESCRIPTION
10	Significant decrease in ΔP
9	No significant change in ΔP (\pm 10% from baseline)
8	10 - 25% ΔP increase
7	25 - 50% ΔP increase
6	50 - 75% ΔP increase
5	75 - 100% ΔP increase
. 3	Large increase in ΔP (>100%), but remains within the bounds of consideration.
0	ΔP increase too high to justify further consideration.

Pressure ΔP Rating

BOUNDARY LAYER GROWTH

Based on estimated boundary layer (b.1.) growth over channel length.

RATING	DESCRIPTION
10	Optimal b.l. growth within channel/fin contour. No significant degradation in material cooling enhancement over length of channel due to b.l. effects.
8	Well defined b.l. through channel. Some degradation in channel cooling enhancement.
6	Boundary layer blends to fill narrow or finned contours prior to end of channel.
3	Boundary layer blends to fill narrow or finned contour over most of channel length. Channel cooling enhancement severly reduced.
0	Contour fills quickly - negligible cooling improvement derived from enhanced channel geometry.

Boundary Layer Risk Rating

PRODUCIBILITY RISK

Based on scale, aspect ratio and contour complexity.

RATING	DESCRIPTION
10	Simple in shape; moderate feature size (approximately .040)
8	Basic shape; higher aspect ratio (i.e. deeper cut).
6	Additional contour complexity: single fin.
4	Smaller feature size; double fin.
2	Combinations of fins and high aspect ratio channels.
0	Size and complexity requirements make fabrication prohibitively difficult and expensive.

Producibility Rating

HEAT TRANSFER ENHANCEMENT

Based on increase in total Q avilable from combustor (.060 Ribbed) as compared to baseline .040 \times .080 channel.

RATING	DESCRIPTION
10	Reflects a great improvement in total energy extracted (20% increase).
8	Significant increase (10-20%).
6	Modest increase (5-10%).
3	Small increase (0-5%).
0	Negligible increase, or decrease, in total energy available.

Heat Transfer Rating

.

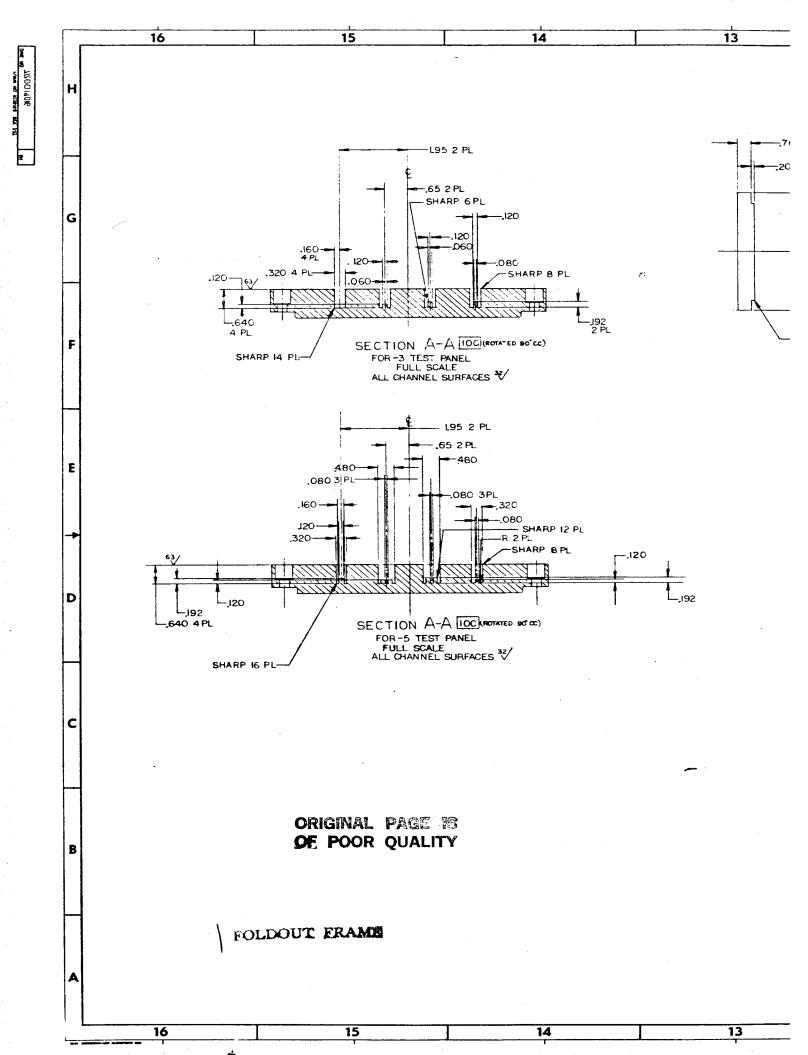
APPENDIX F CHANNEL COLD FLOW TESTS

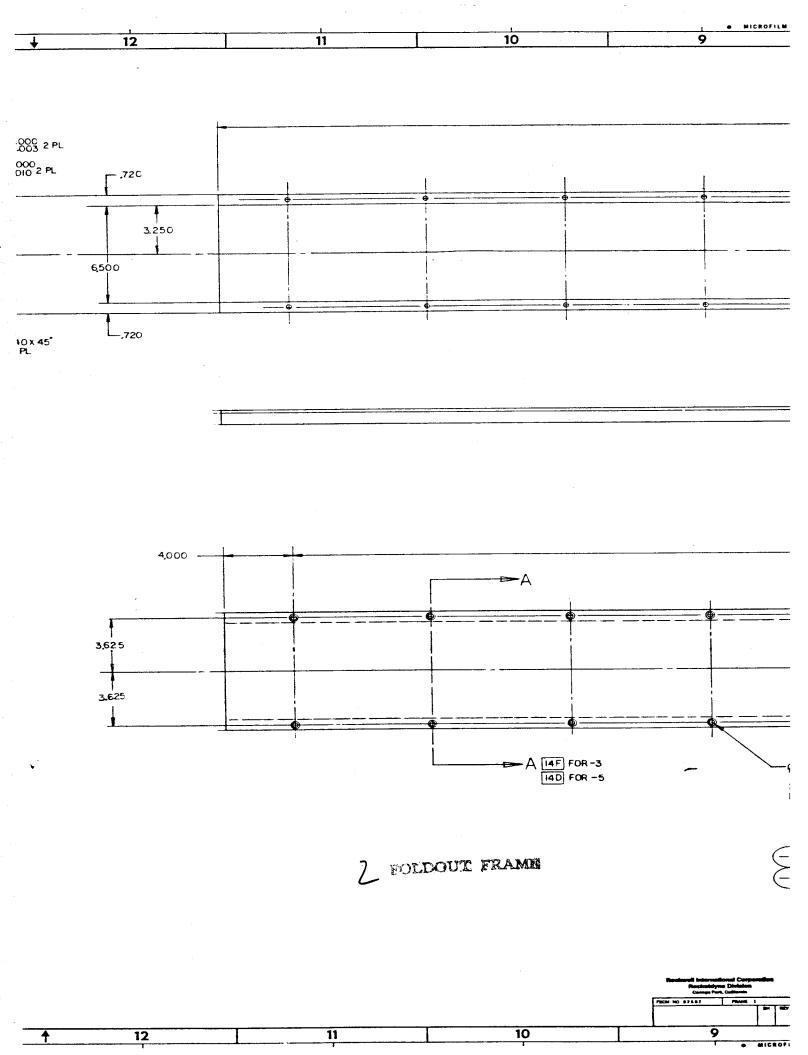
CHANNEL COLD FLOW FIXTURE DRAWINGS

TITLE	DWG #
TEST PANELS SPACERS	7R0019016
	7R0019008

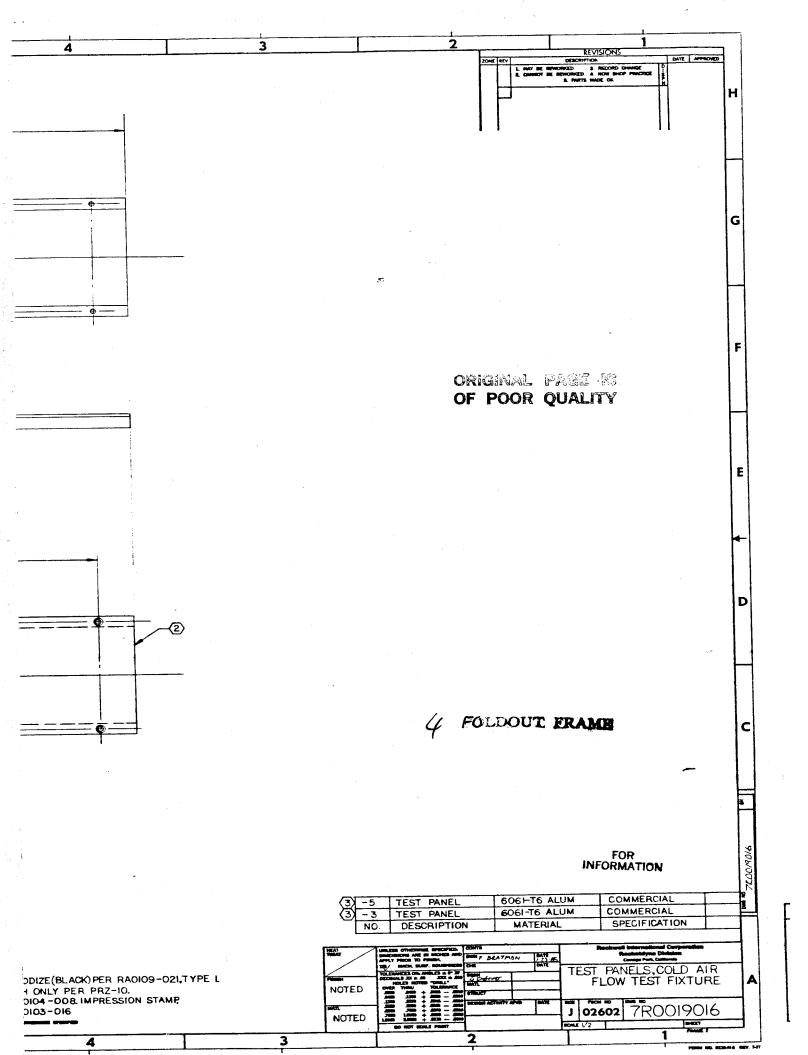
TEST DATA

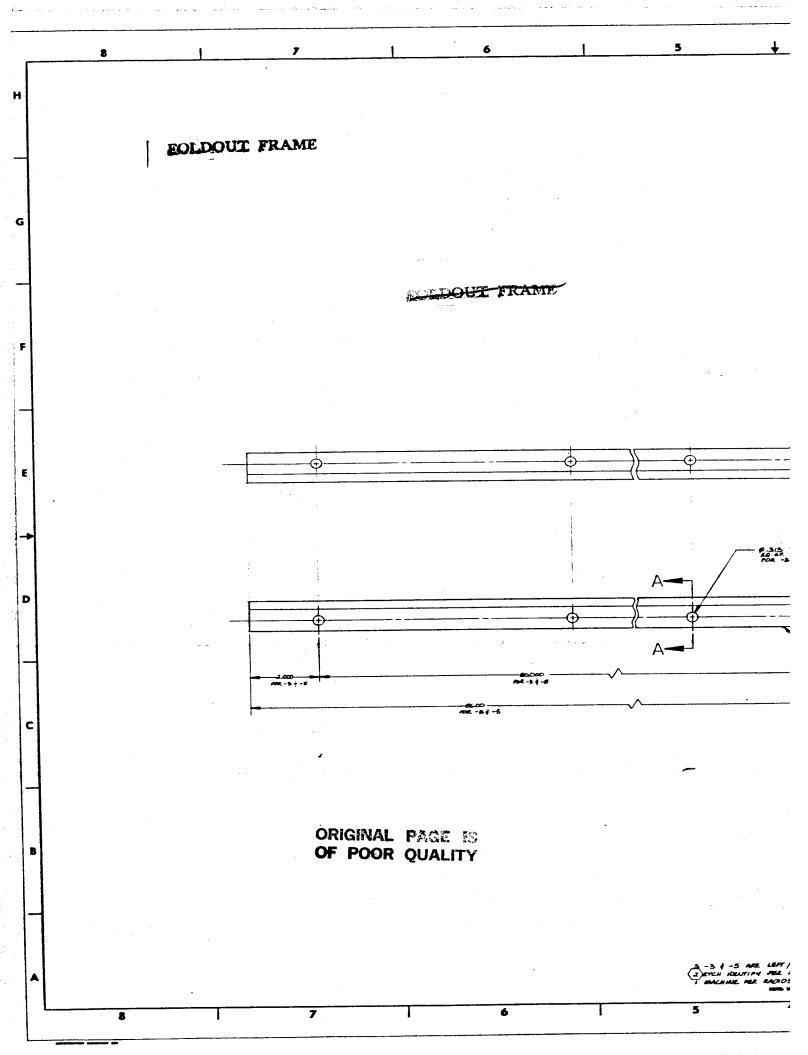
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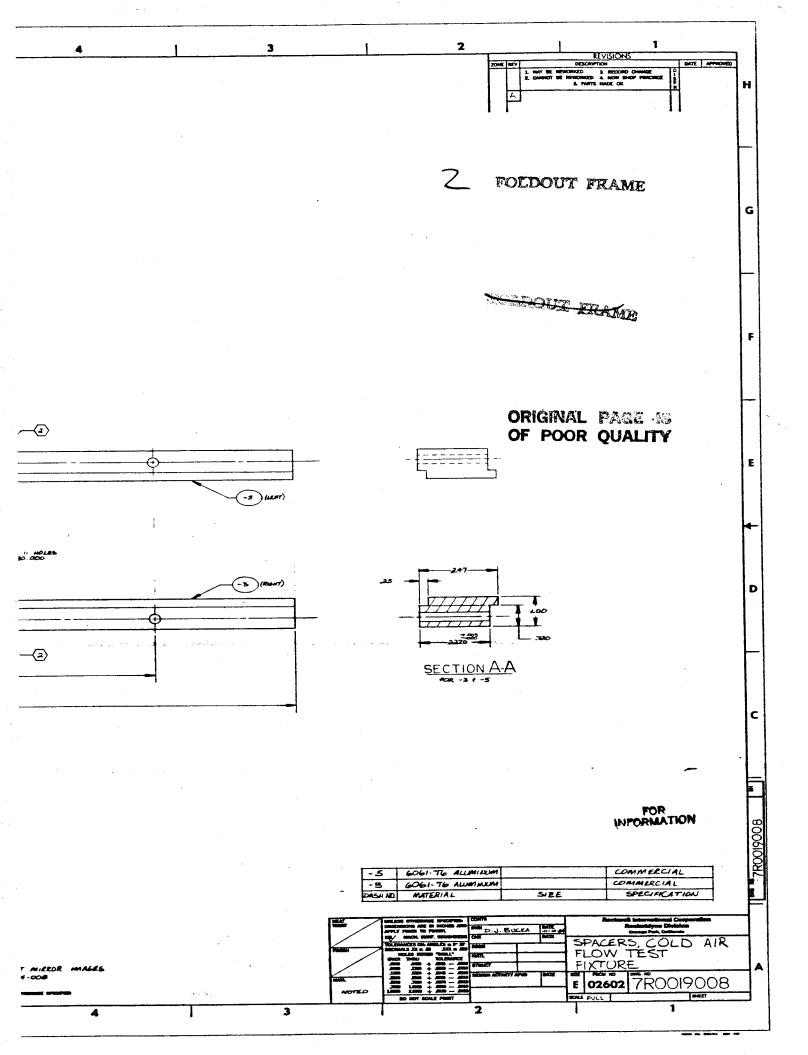






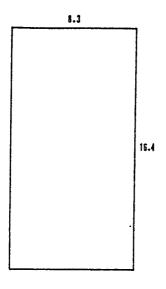






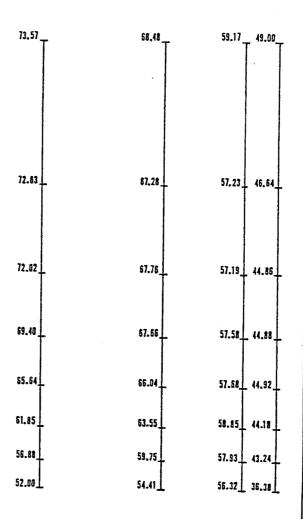
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				_	
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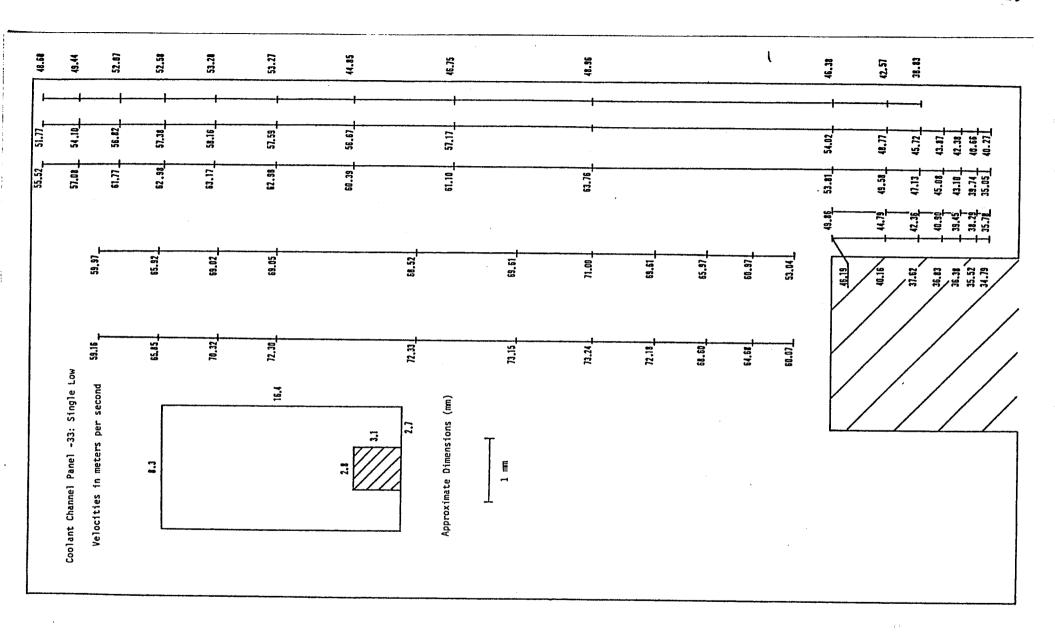
Coolant Channel Panel -34: Empty Baseline
Velocities in meters per second

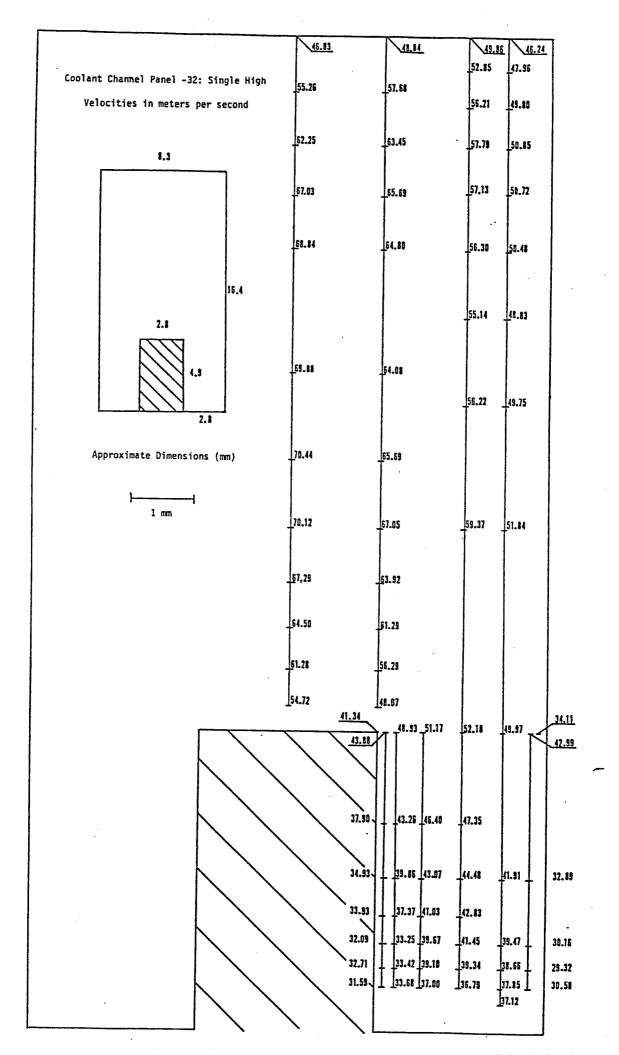


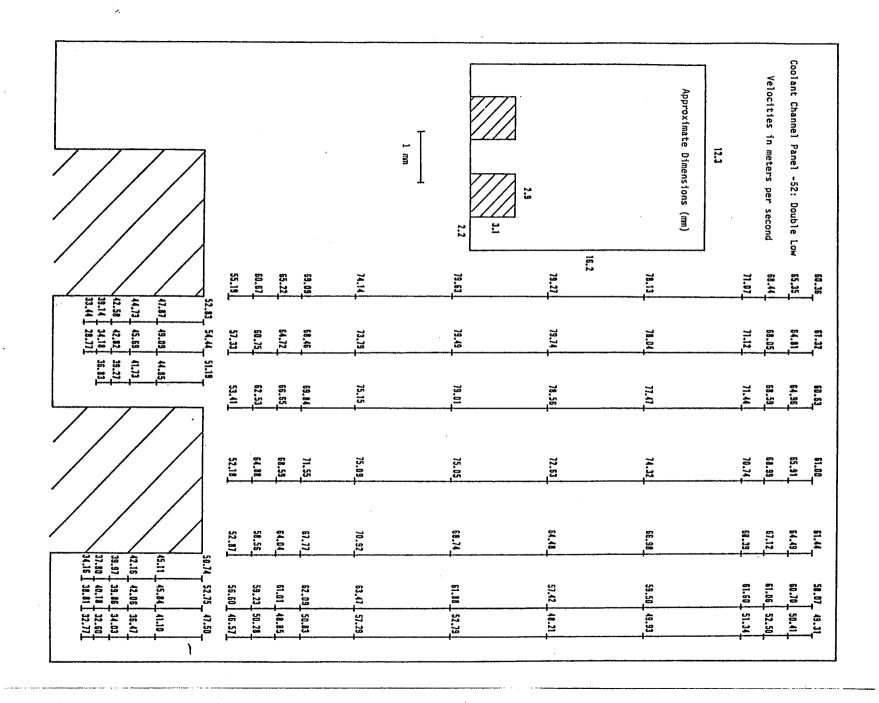
Approximate Dimensions (mm)



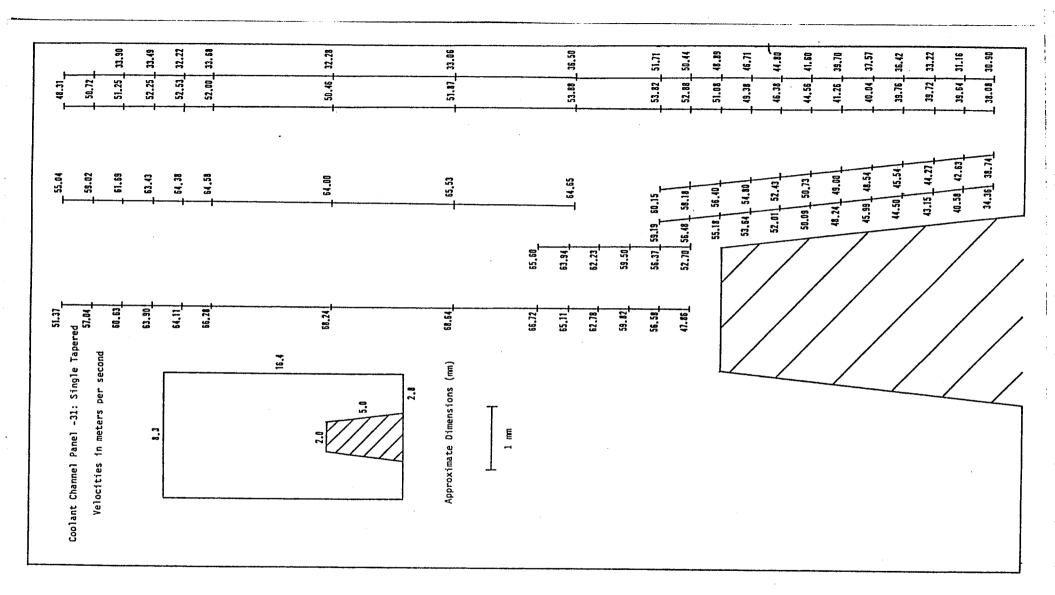








r								
55.70 48.59	58.35 50.05	56.48 48.00	56.70 46.84	59.48 49.70	51.79	59.30 51.02		12 53.61 46.32 18 46.38 38.89 19 39.47 33.25 2 38.06 28.85 2 36.21 5 36.24 24.20 5 35.06
59.87	65. 33 56. 78	66.24	65.91	68.43	71.26	65 te	55.44	33.02
64.81	68.32 70.64	73.36	74.35	75.69	75.83	72.16	65.84	
50.85	67.76	74.70	77.53	71.31	76.17	65.92 66.39	58.04	23.04 21.53 21.53 21.53 18.39
	64.83	74.44	77.99	78.46	74.92	67.58	56. 58	54.93 54.26 4 45.68 46.22 3 41.20 41.48 2 36.36 39.10 2 35.77 35.32 1 31.69 30.57
	67.35	74.26	78.10	18.73	75.84	58.20	55.97	
Coolant Channel Panel -53: Double High	Velocities in meters per second	12.4 Approximate Dimensions (mm)		pr	177	T E		



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APPENDIX G

CHANNEL SCALED ANALYSIS

EXAMPLE CALCULATION FOR SINGLE HIGH FIN CONFIGURATION
STANTON NUMBER PROFILES

APPENDIX G. SAMPLE CALCULATION FOR A SINGLE HIGH FINNED CHANNEL

The basic method of analysis for the finned channel was the same as that employed for the rib flow tests. This similarity was afforded by the results of past studies on internal (pipe) and external (flat plate) flows which demonstrated that the velocity profiles very close to the wall were described by a single relationship for both configurations, namely the logrithmic overlap correlation. One difference was that the freestream velocity Uo used in the rib tests was defined as the channel centerline velocity.

The method used to derive the thermal performance of a finned channel configuration from the measured velocity profiles was based upon the well established characteristics of internal flow as in a pipe. The local shear stress at any location on the rib wall was derived by fitting the measured local velocity profile to the established pipe flow profile. The heat transfer Stanton number defined by St = h/(pUoCp) was found directly by assuming Reynold's analogy. Figure Dl. graphically illustrates these steps in the data reduction process. A numerical example of this method will be presented for the trough region of the single high fin configuration.

The measured velocity profile was fit to the established pipe flow correlation by varying the friction velocity parameter defined as $V^* = Uo/(Cf/2)$. The fit of the data was performed by inspection of the velocity profile expressed in terms of inner variables $u^+ = U/V^*$ (dimensionless velocity) and $y^+ = yV^*/v$ (dimensionless distance). Since the V^* parameter by definition is in the denominator of u^+ and in the numerator of y^+ , variation of V^* results in a change of position of the measured data. Therefore, V^* is chosen such that the data points, particularly those closest to the wall, fall on the correlation line.

The best fit friction velocity for the location in the trough region midway between the fin and the channel wall was V*=2.3. Based upon a centerline velocity of Uo=70.16 meters/sec, the best fit value for V* correspondes to a friction factor of,

$$Cf/2 = (V*/Uo)^2$$

= 0.00107

The Reynold's analogy with a Prandtl number correction (for air Pr = 0.69) provides the heat transfer Stanton number as,

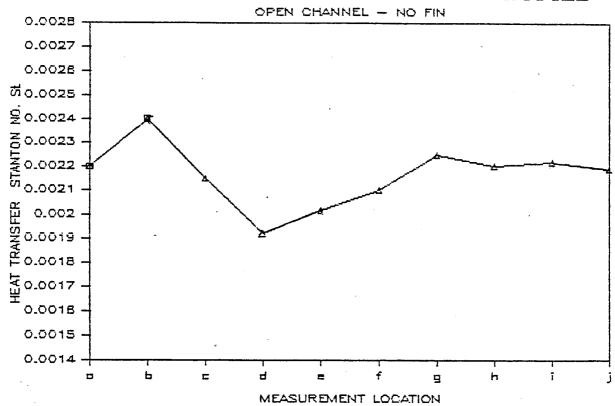
$$-2/3$$
St = Pr Cf/2
= 0.00136

The Stanton number defines the heat transfer coefficient for a given set of flow conditions. This procedure was repeated for every location about the fin where velocity profiles were measured.

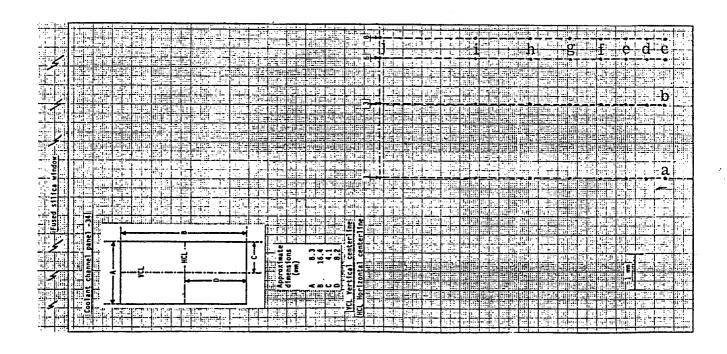
Thus a Stanton number profile about the fin was calculated as shown in Figure Gl.

In order to compare the relative performances of different rib configurations, the Stanton number profiles were integrated with respect to surface area to provide a total heat transfer per channel parameter. This parameter was adjusted for the wider double finned channels on an equivalent flow area basis.

Scaling the Cold Flow results to hot-fire conditions required a scaling factor for the gas-side Stanton number. This scaling factor, denoted as Sl, was defined as the ratio of the Stanton number for a open channel under hot-fire conditions to the Stanton number for a Cold Flow test on an open channel. The REGEN thermal program predicted the hot-fire channel Stanton number. The scaling factor was found to be Sl=1.2. This was used as a Stanton number multiplier for all fin configurations.

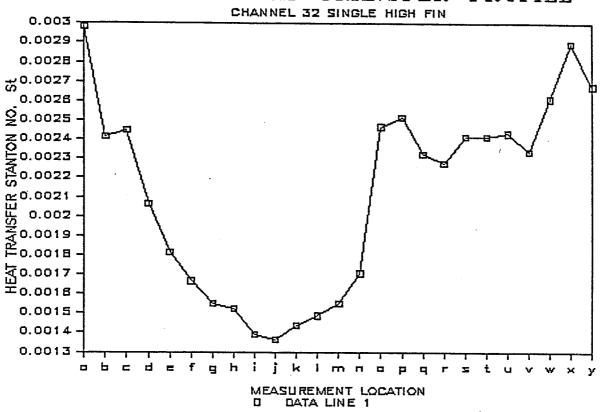


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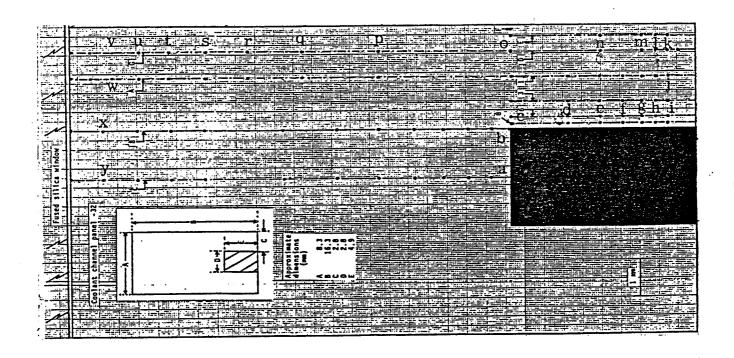


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OPEN CHANNEL SCALED (1/2 CHANNEL)							
NODE		Area, in	h*Area				
93 103 113	0.06549 0.06183 0.05790 0.06155 0.06127 0.06043	0.006666 0.006666 0.003333 0.010000 0.010000 0.010000	4.33E-04 4.37E-04 2.06E-04 5.79E-04 6.16E-04 6.13E-04 6.04E-04				
123 133 143 153 154 155 156	0.06155 0.05790 0.06015 0.06492 0.06549	0.010000 0.008333	6.16E-04 5.79E-04 5.01E-04 4.33E-04 4.37E-04				
		cotal =	0.007371				
FULL	CHANNEL SO	CALED =	0.014743	ΙN			

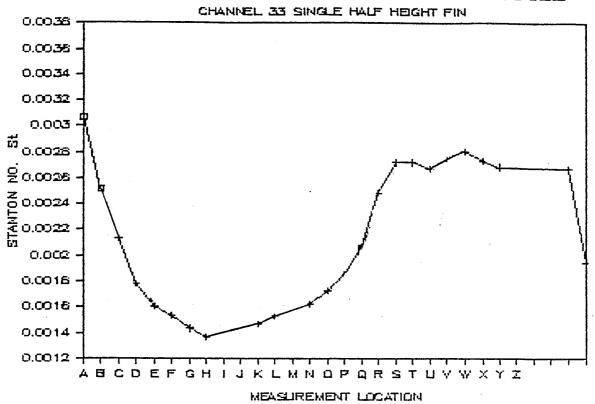


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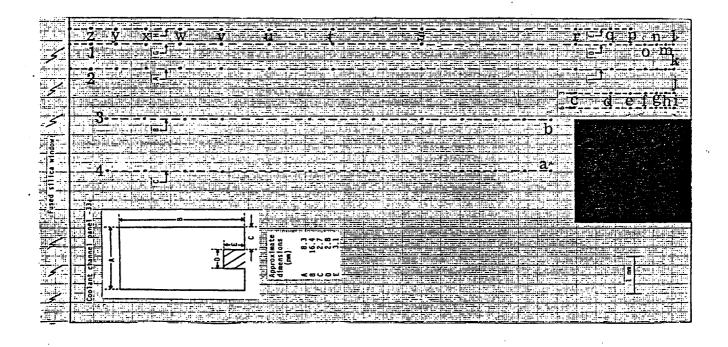


SINGLE HIGH FIN SCALED (1/2 CHANNEL)

	(1/2 CH	HANNEL))		
NODE	h	Area,	in	h*Area	
73	0.04550	0.0083	333	3.79E-04	
74	0.04297	0.0066	666	2.86E-04	
75	0.04408	0.0025	500	1.10E-04	
83	0.05150	0.0100	000	5.15E-04	
93	0.06951	0.0100	000	6.95E-04	
103	0.07836	0.0100	000	7.84E-04	
113	0.07931	0.0100	000	7.93E-04	
123	0.07330	0:0100	000	7.33E-04	
133	0.07349	0.0100	000	7.35E-04	
143	0.07630	0.0100	000	7.63E-04	
153	0.07362	0.0083	333	6.13E-04	
154	0.08215	0.0066	566	5.48E-04	
155	0.09163	0.0066	666	6.11E-04	
156	0.08531	0.0033	533	2.84E-04	
200	0.04487	0.0020	000	8.97E-05	
201	0.04724	0.0040	001	1.89E-04	
202	0.05027	0.0040	001	2.01E-04	
203	0.05627	0.0040	001	2.25E-04	
204	0.06392	0.0040	001	2.56E-04	
205	0.07062	0.0040	100	2.83E-04	
206	0.08247	0.0095	500	7.83E-04	
	(h*Area)t	cotal	==	0.009876	IN
F*** 11 1	CHARBET CO	NI EED	==	0.019752	IN
r (.) L.	CHANNEL SCA	ィーにひ		0.017/02	T. 1.A
IORMAL I	ZED(hAsf/h6	lopen)	=	1.339821	IN



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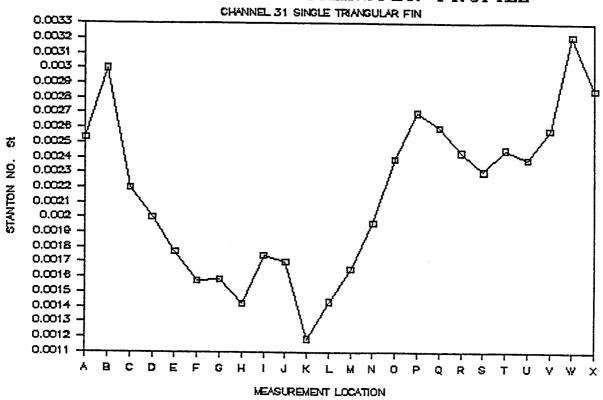
SINGLE LOW FIN SCALED (1/2 CHANNEL)

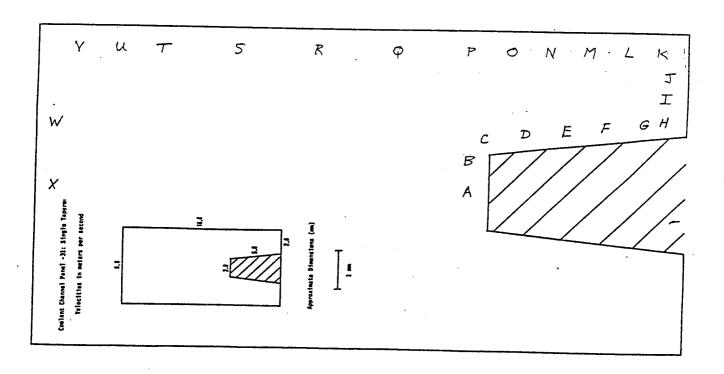
NODE	h	Area, in	h*Area
NODE 73 74 75 83 93 103 123 133 143 155 156 200 201 202 204 205	h 0.04648 0.04467 0.04225 0.06238 0.07641 0.08076 0.08269 0.08269 0.08330 0.08299 0.08058 0.08058 0.08058 0.08058 0.08058 0.04213 0.04213 0.04213 0.04506 0.04814 0.05339 0.05897	Area, in 0.008333 0.004646 0.002500 0.010000 0.002501 0.002501 0.002501	h*Area 3.87E-04 2.98E-04 1.06E-04 6.24E-04 7.64E-04 8.08E-04 8.10E-04 8.30E-04 6.71E-04 5.37E-04 5.37E-04 1.97E-04 1.13E-04 1.13E-04 1.13E-04 1.47E-04
206	0.07777	0.008750	6.80E-04

(h*Area)total = 0.009580 IN

FULL CHANNEL SCALED = 0.019161 IN

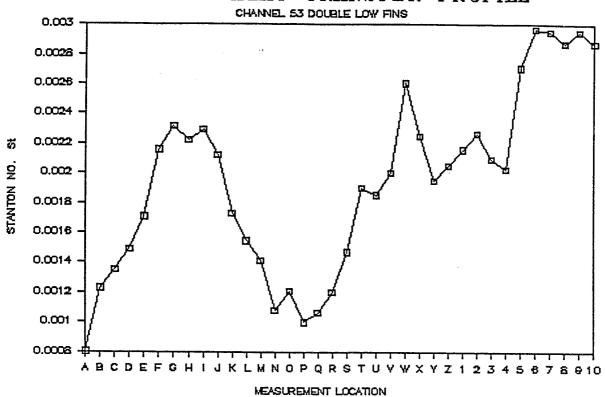
NORMALIZED(hAsf/hAopen) = 1.299728 IN

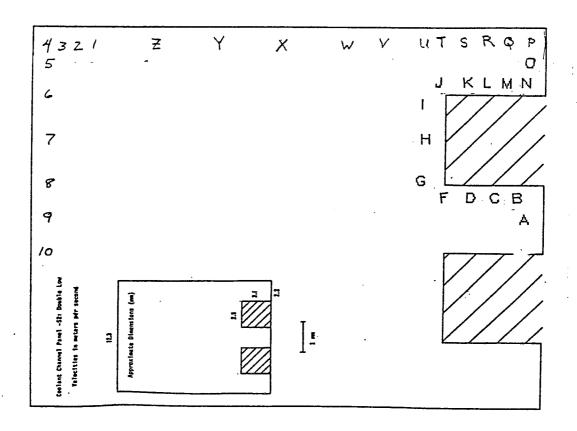




SIN	NGLE TRIANG		SCALED	
ЙОРЕ		CHANNEL) Area, in	h*Area	
73	0.03668	ò.008333	3.06E-04	
74	0.06221	0.006667	4.15E-04	
75	0.02928	0.002500	7.32E-05	
83	0.04875	0.010000	4.88E-04	
93	0.06983	0.010000	6.98E-04	
103	0.08416	0.010000	8.42E-04	
113	0.04593	0.010000	4.59E-04	
123	0.04058	0.010000	4.06E-04	
133	0.04104	0.010000	4.10E-04	
143	0.04188	0.010000	4.19E-04	
153	0.04671	0.008333	3.89E-04	
154	0.08453	0.006666	5.63E-04	
155	0.09815	0.006666	6.54E-04	
156	0.08840	0.003333	2.95E-04	
200	0.04095	0.002095	8.58E-05	
201	0.04729	0.004191	1.98E-04	
202	0.05079	0.004191	2.13E-04	
203	0.05054	0.004191	2.12E-04	
204	0.05686	0.004191	2.38E-04	
205	0.06255	0.004191	2.62E-04	
206	0.07973	0.007095	5.66E-04	
	(h*Area)t	otal =	0.008191	IN
FULL C	CHANNEL SCA	ALED =	0.016383	IN
NORMALIZ	(ED(hAtf/h6	Aopen) =	1.111268	IN

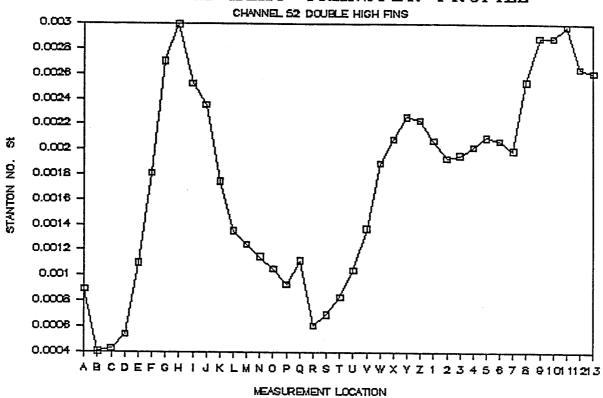
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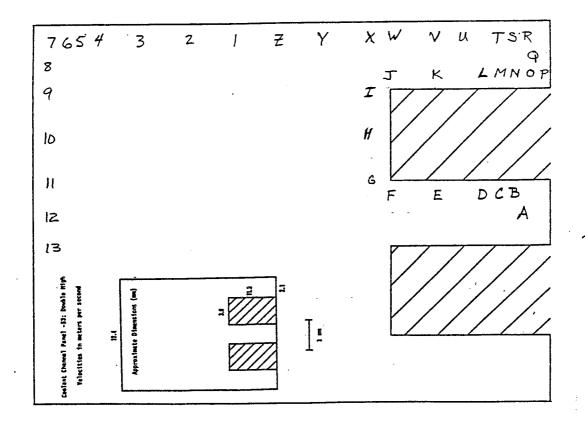




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DOUBLE LOW FIN SCALED (1/2 CHANNEL)							
NODE	h	Area, in	h*Area				
73 74 76 83 93	0.02888 0.02022 0.03441 0.05092	0.010000 0.010000 0.005000 0.010000 0.010000	2.89E-04 1.01E-04 3.44E-04 5.09E-04				
103 113 123 133 143	0.05726 0.04948 0.05180 0.05448	0.010000 0.010000 0.010000 0.010000	5.73E-04 4.95E-04 5.18E-04 5.45E-04				
153 154 155 156 200	0.07013 0.07475 0.07452 0.01540	0.010000 0.010000 0.010000 0.005000	7.01E-04 7.48E-04 3.73E-04 1.93E-05				
201 202 203 204 205	0.03380 0.03840 0.04248 0.04807	0.002500 0.002500 0.002500 0.002500	8.45E-05 9.60E-05 1.06E-04 1.20E-04				
206 207 208 209 210	0.02252 0.02658 0.03201 0.03709	0.006250 0.001250 0.002500 0.002500 0.002500	8.00E-05 9.27E-05				
211 212 213	0.04819 0.05859	0.002500 0.002500 0.006250 total =	1.20E-04 3.66E-04				
FULL	CHANNEL SO	CALED =	0.013156	IN			
NORMALI	ZED(hAdf/h	Appen) =	0.892395	IN			





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DOUBLE HIGH FIN SCALED (1/2 CHANNEL)						
NODE	h	Area, in	h*Area			
73	0.01057	0.010000	1.06E-04			
74	0.02177	0.010000	2.18E-04			
76	0.02340	0.005000	1.17E-04			
83	0.02743	0.010000	2.74E-04			
93		0.010000				
103	0.05538	0.010000				
113	0.05893		5.89E-04			
123		0.010000				
133		0.010000	5.08E-04			
143	0.05315		5.32E-04			
153		0.010000	5.25E-04			
154		0.010000	7.48E-04			
155		0.010000	7.68E-04			
156	0.07021		3.51E-04			
200	0.02064		4.13E-05			
201	0.02827		1.13E-04			
202	0.03366		1.34E-04			
203		0.003980	1.55E-04			
204		0.003980	1.78E-04			
205		0.003980	2.10E-04			
206	0.06653		4.66E-04			
207		0.001999	4.98E-06			
208	0.00810		3.22E-05			
209		0.003980	5.75E-05			
210	0.02056		8.18E-05			
211		0.003980	1.10E-04			
212		0.003980				
213	0.07119	0.006999	4.98E-04			
	(h*Area)	total =	0.006695	IN		
FULL	CHANNEL S	SCALED =	0.013390	IN		
NORMAL I ZI	ED(hAdf/h	Aopen) =	0.908238	IN		

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